

**EPA's APTI**  
**Course #450/#468**  
*Monitoring Compliance  
Test And  
Source Test Observation*



*Student Workbook*



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## Notice

This is not an official policy and standards document. The opinions and selections are those of the author and not necessarily those of the Environmental Protection Agency. Every attempt has been made to represent the present state of the art as well as subject areas still under evaluation. Any mention of products or organizations does not constitute endorsement by the United States Environmental Protection Agency (USEPA).

## Usage of This Manual

The Central States Air Resource Agencies Association (CenSARA) is one of several multi- jurisdictional organizations (MJOs) operating for the U.S. Environmental Protection Agency (USEPA), through the Air Pollution Training Institute (APTI), to update more of the frequently used APTI courses. The primary objectives of the MJOs are to:

- Promote the exchange of information between the States;
- Serve as a forum to discuss regional air quality issues of common concern;
- Share resources for the common benefit of the member states; and
- Provide training services to their member air pollution control agencies.

APTI provides courses on air pollution control technology, ambient air and source monitoring, and air quality management. Historically, APTI designed courses that meet the job training needs of governmental agency personnel and others in the field of air pollution. This requires a thorough examination of both the materials for instruction and the characteristics of the student audience. Based on studies conducted by APTI of those who have participated in the various training courses, courses were developed and revised to provide training that enables every student to achieve specific course objectives. A basic goal of APTI was to provide training that will enable a student to do specific jobs in his or her home environmental agency. However, recently APTI has taken a new direction and has given money to the various MJOs, of which CenSARA is one, to update needed training course for their member states.

CenSARA meets these training needs of its member states by identifying, designing, developing and delivering needed, cost-effective, responsive, and focused educational opportunities for state and local air agency staff. Agenda and course materials are obtained from a variety of sources including EPA, colleges and universities, regional training consortia, and individual instructors. Yet, due to changes in environmental regulations, the implementation of new policies, and the advancement of technologies, agendas and course materials become out-of-date. When this happens, staffs' ability to enhance skills, knowledge and abilities are constrained, limiting their ability to excel in the dynamic field of air pollution control. So by providing up-to-date, high quality educational opportunities for staff, their chances to greatly enhance their skills, knowledge and abilities is significantly improved.

Consequently, CenSARA announced a Request for Proposals (RFP) to the environmental training community to solicit technical proposals and cost bids to review current compliance test and observation programs within the USEPA and to **update** as necessary the content title, agenda topics, course length, instructor and student manuals, lectures involving presentation slides, classroom and homework exercises, and other handouts and materials for EPA's APTI Course #450/#468 entitled: *"Monitoring Compliance Test and Source Test Observation."* In response to CenSARA's RFP, EnviroTech Solutions, William T. "Jerry" Winberry, 1502 Laughridge Drive, Cary, North Carolina 27511, [jwinberry@mindspring.com](mailto:jwinberry@mindspring.com), 919-467-2785, was awarded the contract to update EPA's APTI Course #450/#468. Mr. Winberry is the author of this Student Workbook (SW) and every attempt has been made to represent the most recent advances in sampling and analytical methodology

## Disclaimer

This material has been developed and assembled to provide training associated with EPA's APTI Course #450/#468 entitled: *"Monitoring Compliance Test and Source Test Observation."* It is not intended to be used for regulatory purposes, or to be a substitute for, nor interpreted as official Agency policy. Every attempt was made to reflect the technical state of art and regulatory information as of the date of this publication. This is not an official policy and standards document. The opinions and selections are those of the author and not necessarily those of the EPA. Any mention of products or organizations does not constitute endorsement by the EPA.

# **U.S. Environmental Protection Agency Air Pollution Training Institute Course #450/#468 Monitoring Compliance Test and Source Test Observation Student Workbook (SW)**

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educational opportunities for staff, their chances to greatly enhance their skills, knowledge and abilities is significantly improved. Consequently, CenSARA has taken the initiative to update EPA's APT! Course #450/#468.

The updated Course #450/#468 is targeted primarily at agency personnel who have the responsibility to monitor compliance test and source test observation of various FRMs and SW- 846 methodologies. The revised course materials provide the best available and most current information as well as relevant example exercises to improve the knowledge and expertise of agency observer personnel. The desired outcome of this effort is that agency staff be able to properly observe compliance test and perform source test observations to protect public health and the environment by developing an understanding of EPA's stack testing programs and strategy, various stack test methodologies for quantifying HAPs from industrial processes, and associated quality assurance/quality control activities and requirements.

The specific objectives of updating APTI Course #450/#468 materials include:

- Explain why sampling of source emissions for PM and HAPs is important in air pollution control agency programs;
- Define symbols and common terms used in the application of FRMs 1-5 and SW-846 source sampling;
- Recognize, interpret and apply sections of the Code of Federal Regulations, Appendix A, pertinent to source sampling for particulate pollutants;
- Understand the construction, operation and calibration of the component parts of the FRM 5 particulate matter sampling train;
- Define "Isokinetic sampling" and illustrate why it is important in sampling for PM;
- Understanding the "working" isokinetic rate equation and its derivation
- Learn how to use specific software for determining isokinetic sampling rates;
- Apply FRMs 1 through 4 in preparation for applying FRM 5 at a source to characterize PM emissions;
- Understand how the "S-type" pitot tube is constructed and standardized and how it is applied in source sampling;
- Understand the difference between systematic error and precision as applied to source test measurements;
- Properly assemble and leak check a FRM 5 sampling train;
- Describe the operation of the VOST, Semi-VOST, Acid Gas and FRM 201/201A sampling trains;
- Describe what are "condensable" and how the FRM 202 sampling train operates to measure condensable; and
- Calculate the "% Isokinetic" value for a source test, and interpret the effect of over or under- isokinetic values on the source test results.

One of the products of the #450/#468 update is the Student Workbook (SW). The SW provides copies of visuals presented in each technical lecture. Contained in this SW are the visuals for each of the Sessions and lessons presented in APT! Course #450/#468.

## **I. Background**

Over the last several years, public awareness of air pollution and its sources has increased steadily. Specifically, since the passage of the Clean Air Act Amendments (the Act) of 1990 and the implementation of EPA's maximum achievable control technology (MACT) program, more emphasis has been placed on local, State, and Federal agencies to keep the public informed on health effects of various air pollutants and their levels of exposure. This awareness has required industry to become accountable for air pollution emissions as part of their source's compliance strategy and regulatory agencies to become knowledgeable of the methodology used to quantify reported emissions.

Traditionally, air pollution control agencies require all sources to quantitate their emissions in order to demonstrate compliance. To insure that the source test methods utilized to demonstrate compliance are performed according to EPA guidelines, regulatory agencies observe stack test to document compliance with the methodology. This has meant that sources must know how to properly sample and report emissions using EPA reference methods and that regulatory agencies must know how to properly observe these test to insure that reliable and accurate data is gathered and reported.

In addition, with the passage of the Act and Title IV, Acid Rain, those fossil-fueled-fired-steam generators (FFFSG) covered must report emissions in units of pollutant mass rate (pmr) as part of EPA's emission trading program. This required the installation and certification of velocity monitors if the continuous emission monitoring system (CEMS) data was to be used as part of EPA's market base-trading program. These new regulatory requirements have now required Agency personnel to know how to observe and verify the proper use and implementation of Federal Reference Methods 2F, 2G, and 2H in certification of the velocity CEMS as part of a source's market base-trading emission program.

Consequently, the Act has required regional, state, and local air pollution control agencies to better understand the stack test methodologies that are used to quantitate air pollution emissions from industrial sources. Agencies see a need to provide training to its personnel on how to properly observe stack test used to meet regulatory compliance for criteria and hazardous air pollutants (HAPs).

## **II. Course Objective**

The objective of EPA's APTI Course #450/#468 is to provide Agency personnel the needed background information, checklist, and guidance associated with EPA methodologies involving stack test for characterizing and quantifying criteria and HAPs from industrial sources. This course will address Federal Reference Methods (FRMs) 1-5 (isokinetic stack testing and stack test basics), FRMs 2F, 2G, and 2H (velocity), stack testing for volatile organic compounds (FRMs 18, 25, 25A/B), SO<sub>2</sub> (FRMs 6, 6A, and 8), NO<sub>x</sub> (FRMs 7, 7C), dioxin/furans and PCBs (FRM 23), heavy metals (FRM 29), and instrumental (FRMs 3A, 6C, and 7E).

The course will present standardized stack test methodology for sampling and analysis of air pollutants as identified in the Code of Federal Regulations (CFR), Part 60, Appendix A. In addition, information will be presented on EPA's stack test monitoring programs associated with PM-10 (Methods 201 A/B) and condensable particulate (Method 202) monitoring from CFR 51 Subpart M. Specific source test checklists will be demonstrated during the presentation for each test methodology as part of the course. Participants will learn how to use the checklist in performing source test observations, how to observe mandated QA/QC requirements associated with each methodology, and how to use source test databases available to the air pollution scientist.

At the end of this course, the agency personnel will gain an understanding of the unique source test methods used to accurately characterize air pollutant emissions from industrial sources. The agency personnel will learn about EPA's programs that require characterization of air pollutants from industrial sources utilizing FRMs.

### III. Course Manuals

Course presentations and videos will be supported by four manuals. They are:

- **#468 Student Workbook (Hard Copy):** The updated Student Workbook (SW) contains copies of selected slides from each of the lecture presentations, and **Agency Inspector Checklist**.
- **#468 Stack Test Manual (Flash Drive):** The Stack Test Manual contains full copies of selected stack test sampling and analytical methods found in the CFR, Part 60, Appendix A, and SW-846, Standard Methods.
- **Apex Instruments Federal Reference Method 5 Operational Manual:** The Federal Reference Method 5 Operation Manual is a document describing specifically the construction and operation of Federal Reference Method 5 stack testing sampling train. <http://www.apexinst.com/cms/wp-content/uploads/2015/03/Model-500-Series-Manual-Method-5.pdf>.



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<b>EPA APTI Course #450/468</b> <b>Monitoring Compliance Testing and Source Test Observation</b>
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**COURSE LOCATION**

Internet Presentation

**INSTRUCTORS**

 William Franek, Ph.D., P.E., DEE  
 Kevin Mattison, B.S.

DAY/TIME	SUBJECT	LESSON
<i>(Monday, Day 1)</i>		
8:30 AM	<b>Welcome</b>	
8:45	Introduction to/Sources of Methods	1
<b>Topics Dealing with Source Testing Guidance</b>		
9:15	EPA's National Stack Test Guidance and Compliance Monitoring Strategy	2
10:00	Introduction to Stack Testing and Gas Physics <ul style="list-style-type: none"> <li>• Gas Physics</li> <li>• Boyle/Charles Laws</li> <li>• Correction to Standard Temperature and Pressure</li> </ul>	3
10:45	<b>BREAK</b>	
11:00	Overview of Federal Reference Methods 1-5 (Video)	
11:30	Stack Testing Basics: Overview of Federal Reference Methods Federal Reference Methods 1-2 <ul style="list-style-type: none"> <li>• Sampling Point Locations (IsoCalc Spreadsheet)</li> <li>• Stack Gas Velocity (IsoCalc Spreadsheet)</li> <li>• Cyclonic and Non-Parallel Flows &amp; Port Locations</li> </ul>	4
12:30 PM	Adjourn/Homework Problems Assignment	
<b>Topics Dealing with FRM's 1 Through 5</b>		
<i>(Tuesday, Day 2)</i>		
8:30AM	Homework Review	
8:45	-Agency Observer Checklists	
9:15	Stack Testing Basics (Cont'd) <ul style="list-style-type: none"> <li>• <b>Federal Reference Methods 3-4</b></li> <li>• Stack Gas Molecular Weight (<b>IsoCalc Spreadsheet</b>)</li> <li>• Stack Gas Moisture (<b>IsoCalc Spreadsheet</b>)</li> <li>• Sampling Train Configuration</li> </ul>	5
10:30	<b>BREAK</b>	
10:45	Federal Reference Method 5 Operation/Associated Equations/Setting % Isokinetic Sampling Rate <b>Agency Observer Checklist</b>	6

DAY/TIME	SUBJECT	LESSON
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*(Tuesday, Day 2)*

11:45	<b>The Source Test</b>	7
12:15	Role of the Agency Inspector	8
12:30	Homework/Adjourn	

*(Wednesday, Day 3)*

8:30	Homework Review	
8:15	F-Factors	10
8:45	FRM 201/201A for PM-10, PM-2.5	9
9:15	FRM 202 Condensable PM	11
10:30	<b>BREAK</b>	
10:45	FRM 29/SW-846, Method 0060, Multi-Metals Sampling, FRM 12 for Inorganic Lead and FRM 306 for Chromium	12
11:15	Federal Reference Method 26/26A/SW-846 Methods 0050/0051 (HCl/Cl <sub>2</sub> )	13
12:30	Adjourn/Homework	

DAY/TIME	SUBJECT	LESSON
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*( Day 4) Topics Dealing With VOC Stack Testing*

8:30	Homework Review	
8:45	Introduction to VOCs/Selecting VOC Sampling and Analytical Methods ( <b>State of Pennsylvania Selection Process</b> ) Reporting VOC Emissions (in ppms? In #/Hr.? etc.) and Calculations (i.e., “As Carbon?”; “As VOCs?”; “As Organics?”; “As Propane?”)	14
9:45	Overview of Stack Testing for VOCs Utilizing FRMs 18, 25, 25A, CTS 035 and SW-846 Methods	15
10:45	<b>BREAK</b> <b>Topics Dealing With VOC Stack Testing (cont.)</b>	
11:00	Municipal Solid Waste Landfill Emissions and Sampling of VOC and HAP's	16
11:30	Federal Reference Method 18, 25, & 25A Weaknesses/Strengths of FRMs 18, 25, 25A	17
12:30	Adjourn/Homework	

## Friday Day 5

8:30	FRM Method 204 PTE/TTE Enclosures, Capture Efficiency/Calculations	18
9:30	Stack Testing Special Topics	19
	<ul style="list-style-type: none"><li>• High Moisture Stacks</li><li>• High Pressure Stacks</li><li>• High VOC Concentration Stacks/Molecular Weight Determination</li></ul>	

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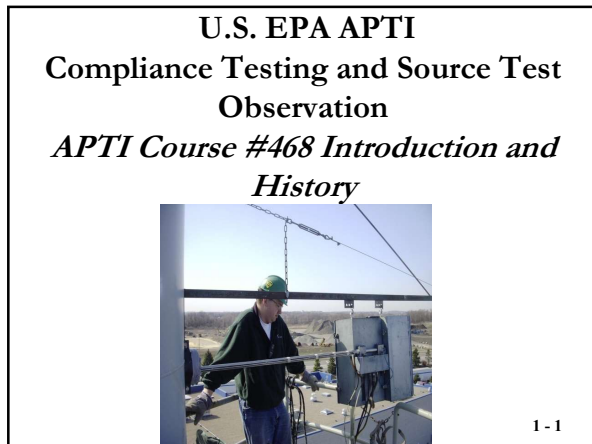
### Topics Dealing With Stack Testing Gas Turbines, Acid Gas Monitoring and Other Topics

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#### Day 5

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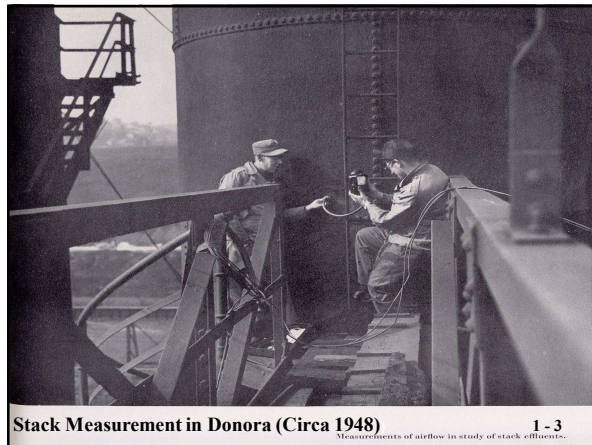
10:00	Reciprocating Internal Combustion Engine (RICE) Sampling and Overview of CEMS for Engines and Gas Turbine Testing	20
	<ul style="list-style-type: none"><li>• Federal Reference Method 6C/7E/3A and 20</li><li>• Fourier Transform Infrared (FTIR) Spectroscopy Technology</li><li>• ASTM D6522-00 (Portable Analyzer Technology)</li></ul>	
10:30	<b>BREAK</b>	
10:45	RATA and CGAs	21
11:15	FRM 205 (Gas Dilution System)	22
12:15	FRM 320/ASTM D6348-03	23
	Safety on the Stack Test	24
	Final Exam Instructions	
	Course Adjourn	



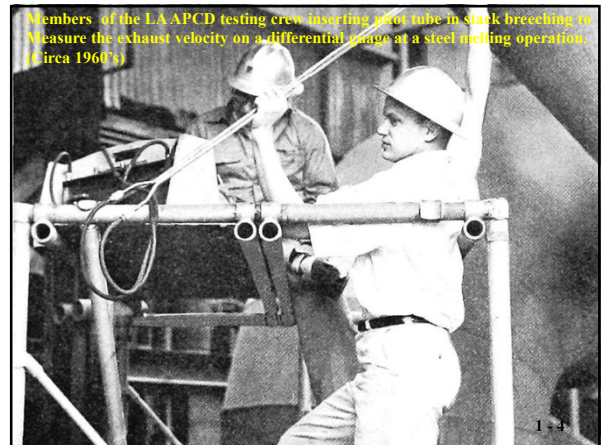
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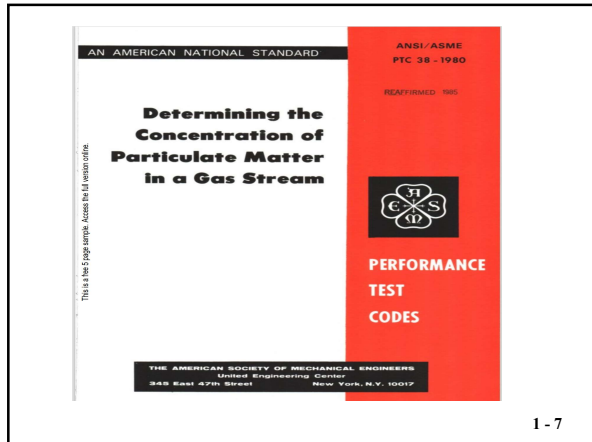
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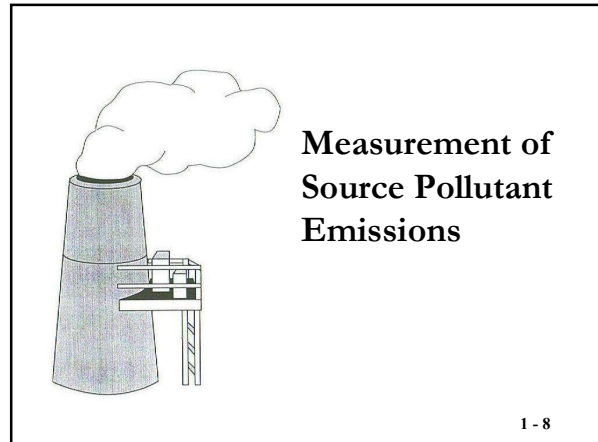
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7



8

### Measurement Methods of Source Pollutant Emissions

1. Stack testing
  - Manual methods
  - Instrumental methods
2. Continuous Emission monitoring
  - Instrumental methods
3. Remote Sensing

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### Manual Sampling

The diagram shows a smokestack with a sampling train connected to it. The sampling train leads to a box labeled "Off-site lab analysis". To the right of the diagram, the text reads: "Extract samples from various points in stack. Analyze samples in lab. Procedures described by federal reference methods (FRMs)".

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### Manual vs. Instrumental

<p><b>Manual</b></p> <p>Anything related to PM and some gases</p> <ul style="list-style-type: none"> <li>• PM</li> <li>• PM<sub>10</sub></li> <li>• Metals</li> <li>• Semi-volatile</li> <li>• Organisms</li> <li>• HCL &amp; H2SO4</li> </ul>	<p><b>Instrumental</b></p> <p>Anything related to gases</p> <ul style="list-style-type: none"> <li>• NO<sub>x</sub></li> <li>• SO<sub>2</sub></li> <li>• CO</li> <li>• Opacity</li> <li>• Volatile Organics</li> <li>• O<sub>2</sub></li> <li>• CO<sub>2</sub></li> <li>• H<sub>2</sub>S</li> </ul>
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### Remote Sensing: Another Type of Source Emission Measurement

The diagram shows a 3D perspective of a source area. A "Scan plane" is shown as a grid of red lines extending from a "DIAL" (Differential Absorption Lidar) system. "Emissions" are shown as a plume of smoke. A "Wind" arrow points to the left. A color scale for "Concentration (mg/m<sup>3</sup>)" is shown. The axes are labeled "Height (m)" and "Range (m)".

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### Differential Absorption Light Detection and Ranging (DIAL)

Species Measured by DIAL	Sensitivity (1)	Maximum Range (2)
Benzene	10 ppb	800 m
Sulfur Dioxide	10 ppb	3 km
Toluene	10 ppb	800 m
Ethane	20 ppb	800 m
Ethylene	10 ppb	800 m
Methane	50 ppb	1 km
General Hydrocarbons	40 ppb	800 m
Hydrogen Chloride	20 ppb	1 km
Methanol	200 ppb	500 m

**DIAL Strengths**

- Provides spatially resolved pollutant concentration in two dimensions
- Measurements are provided in a relatively short period of time
- Deployable in many different applications and configurations, moveable
- Can measure long path lengths (1 to 3 km)

**DIAL Limitations**

- Due to limited availability, DIAL systems used in North America are typically imported, which increases the expense
- Chemical species that can be characterized are limited to those compounds with the unique chemical properties required to be detected
- Only a few wavelengths are measured (spectral artifacts cannot be fixed or investigated)

(1) Concentration sensitivities from NPL for measurements of a 50 meter wide plume at a range of 200 meters, under typical meteorological conditions.  
(2) The range value represents the typical working maximum range for the NPL DIAL system.

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### DIAL Applications

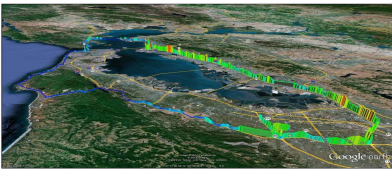
- **Tonawanda Coke: Coke oven site, July 2009 Test Order for Benzene Emissions, May 2010**
- **BP Texas City: Voluntary Study with TCEQ and EPA funding, Benzene and VOC emissions, July to August, 2007**
- **Shell Deer Park: Voluntary Study with EPA, Environment Canada and City of Houston funding, Benzene and VOC emissions, January to March, 2010**

DIAL Vendors	
Spectrasyne	<a href="http://www.spectrasyne.ltd.uk/">http://www.spectrasyne.ltd.uk/</a>
LASEN	<a href="http://www.lasen.com/">http://www.lasen.com/</a>
National Physical Laboratory	<a href="http://www.npl.co.uk/">http://www.npl.co.uk/</a>
ITT	<a href="http://www.itt.com/">http://www.itt.com/</a>

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### EPA Handbook: Optical and Remote Sensing for Measurement and Monitoring of Emissions Flux of Gases and Particulate Matter



**Informational Document**

This informational document describes the emerging technologies that can measure and/or identify pollutants using state of the science techniques

**EPA 454/B-18-008 August 2018**

1 - 15

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### EPA Manual Federal Reference Methods (FRMs)

Used for source compliance testing  
Describe actual testing procedure  
Found in Code of Federal Regulations

1 - 16

16

### Agency's Purpose for Stack Testing

- Compliance Evaluation
- Regulatory Support
- Emission Inventory
- Method Development
- Certify CEM's

1 - 17

17

### Industry's Purpose for Stack Testing

- Determine Control Device Efficiency
- Evaluate process operation
- Design new process and equipment
- Demonstrate compliance

1-18

18

### Types of Emission Points Tested

- Stacks
- Process vents
- Building exhausts
- Tank emissions
- Fugitive emissions

1 - 19

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### Typical Sampling Point Provisions

**SAMPLING PORTS**  
 A. 2 PORTS, 90° W DIAMETER LESS THAN 3M \* PORT LENGTH  
 B. PORTS 90° APART, W DIAMETER OVER 3M \* PORT LENGTH

**PORT DIMENSION REQUIREMENTS**  
 (OUTSIDE) 0.5M MIN  
 2.4M MAX UNLESS GATE VALVE INSTALLED  
 0.5M TO END INDUSTRIAL FLANGE CAPPED  
 WHEN NOT IN USE  
 INSTALL GATE VALVE IF STACK CONTAINS  
 DANGEROUS GASES OR GRADES OVER 200' UNDER POSITIVE PRESSURE

**STRENGTH REQUIREMENTS**  
 225 Kg SIDE LOAD  
 225 Kg RADIAL PERSON LOAD  
 31 Kg VERTICAL SHEAR LOAD  
 100 Kg M MOMENT

**AT LEAST TWO STACK DIAMETERS BELOW STACK BAY**

**GUARD RAIL**

**AT LEAST ONE STACK DIAMETER PLUS 0.5M FROM STACK CIRCUMFERENCE**

**CLEARANCE ZONE** 0.5M

**WORK AREA CLEARANCE**  
 AT LEAST EIGHT STACK DIAMETERS ABOVE LAST OBSTRUCTION

**WORK PLATFORM**  
 A. AT LEAST 1M WIDE (1.2M WIDE FOR STACKS WITH 3M OR GREATER ID) AND CAPABLE OF SUPPORTING 2 PEOPLE AND 91 Kg OF TEST EQUIPMENT  
 B. SAFE GUARDRAIL ON PLATFORM WITH ACCESS BY SAFE LADDER OR OTHER SUITABLE MEANS. IF LADDER IS USED LADDERS WILL MUST BE LOCATED AT LEAST 1M FROM PORTS  
 C. NO OBSTRUCTIONS TO BE WITHIN 1M HORIZONTAL RADIUS ON PLATFORM BENEATH PORTS

**POWER SOURCE**  
 220V 1FA SINGLE PHASE 50 HZ AC LOCATED ON PLATFORM

1 - 20

20

### Four H's of Source Testing

- High** -- up to 300 feet
- Hot** -- stacks up to 2000
- Heavy** -- sampling equipment
- Hazardous** -- noxious gases

1 - 21

21



22



23



24



### Types of Emissions Tested

- Particulate matter (Total PM;  $PM_{10}$ ;  $PM_{2.5}$ )
- Inorganic gases
- Organic gases and vapors
- Combinations of solids and gases

1 - 25

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### Where Methods are Found

- U.S. EPA test methods (CFR)
- State Implementation Plans (SIPs) and regulations
- Industrial and trade associations, Publications

<http://www.epa.gov/ttn/emc/>

1 - 26

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### Part 60 Promulgated Methods in 1971

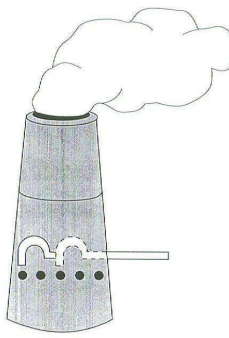
- FRM 1 Sample and Velocity Traverses for Stationary Sources
- FRM 2 Determination of Stack Gas Velocity and Volumetric Flow Rate (Type S Pitot Tube)
- FRM 3 Gas Analysis For The Determination Of Dry Molecular Weight
- FRM 4 Determination Of Moisture Content In Stack Gases
- FRM 5 Determination Of Particulate Matter Emissions From Stationary Source
- FRM 6 Determination Of Sulfur Dioxide Emissions From Stationary Sources
- FRM 7 Determination Of Nitrogen Oxide Emissions From Stationary Sources
- FRM 8 Determination Of Sulfuric Acid And Sulfur Dioxide Emissions From Stationary Sources
- FRM 9 Visual Determination Of The Opacity Of Emissions From Stationary Sources

1 - 27

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### Method 1

#### Selection of sampling traverse points

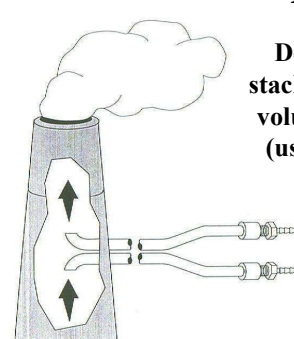


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### Method 2

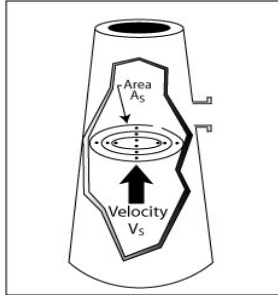
#### Determination of stack gas velocity and volumetric flow rate (using Type S pitot tube)



1 - 29

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### Distributed Sampling Points

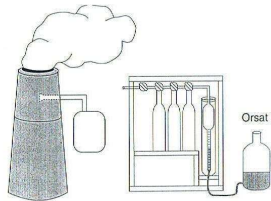


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**Method 3**

Determination of the dry molecular weight of flue gas (using Orsat apparatus measuring %O<sub>2</sub>, %CO<sub>2</sub>, and %CO)

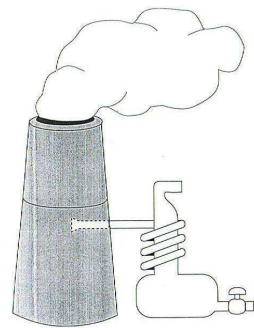


1 - 31

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**Method 4**

Determination of moisture content of stack gas (by condensation method)

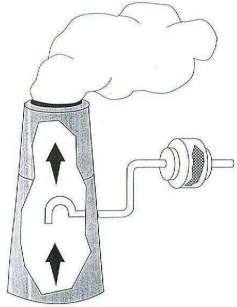


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**Method 5**

Sampling method for particulate matter (isokinetic collection of particles on a filter)

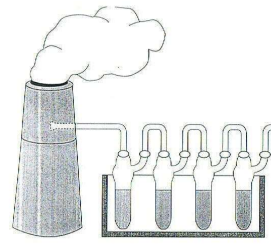


1 - 33

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**Method 6**

Sampling and analytic method for determining SO<sub>2</sub> emissions (barium-thorin titration)

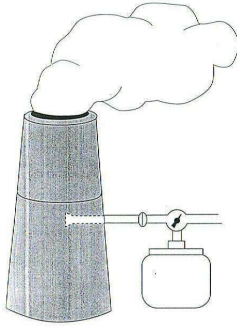


1 - 34

34

**Method 7**

Determination of NO<sub>x</sub> emissions (colorimetric phenoldisulfonic acid method)

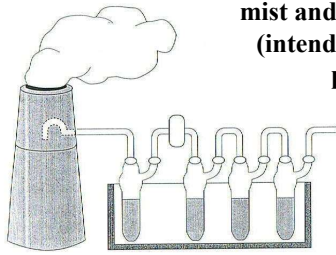


1 - 35

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**Method 8**

Determination of H<sub>2</sub>SO<sub>4</sub> mist and SO<sub>2</sub> emissions (intended for H<sub>2</sub>SO<sub>4</sub> plants)

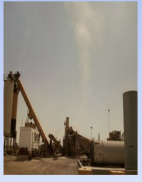


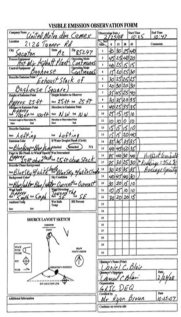
1 - 36


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### Method 9

U.S. EPA Method 9  
Visible Emissions  
Observations







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### Part 60 Methods Promulgated in the 1970's

FRM 10	Determination of CO
FRM 11	Determination of fluorides
FRM 12	Determination of inorganic lead emissions
FRM 13, 14	Determination of H <sub>2</sub> S
FRM 15	Determination of H <sub>2</sub> O, COS, CS <sub>2</sub>
FRM 16	Determination of total reduced sulfur
FRM 17	Determination of particulates (in-stack filtration method)

1 - 38

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### Part 60 Methods Promulgated in the 1980's

FRM 26	Determination of HCl/Cl <sub>2</sub>
FRM 29	Determination of multi-metals
FRM 201/201A	Determination of PM-10
FRM 316	Determination of formaldehyde
FRM 202	Determination of condensables
SW-846 Methods	Determination of volatiles, semi-volatiles etc.

[Chronology OF EPA EMISSION TEST METHODS](#) 1 - 39

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### Objectives

**Gain knowledge on a vast number of methods found in EPA's Federal Register methods (FRMs) and SW-846 test methodology.**

**Learn the proper observation and measurement techniques for quantifying particulate and gaseous stack emissions.**

1 - 40

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### Objectives

**Focus on groups of compounds**

- Volatile Organic Compounds (VOCs)
- Hydrogen Halides and Halogens
- Particulate Matter (Total and Speciated) and Condensables
- Inorganic-base Compounds (Lead and Metals)

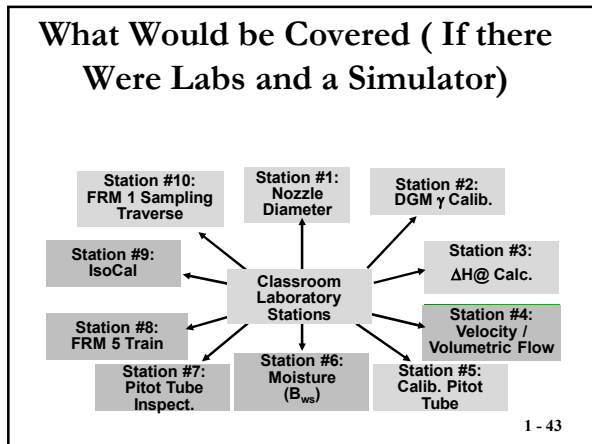
**Update changes associated with FRMs 1-5**

1 - 41

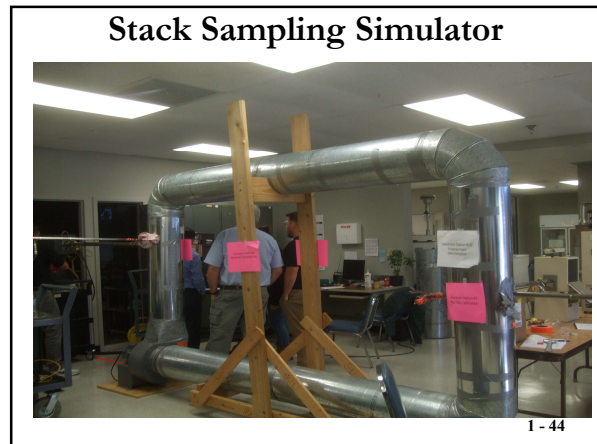
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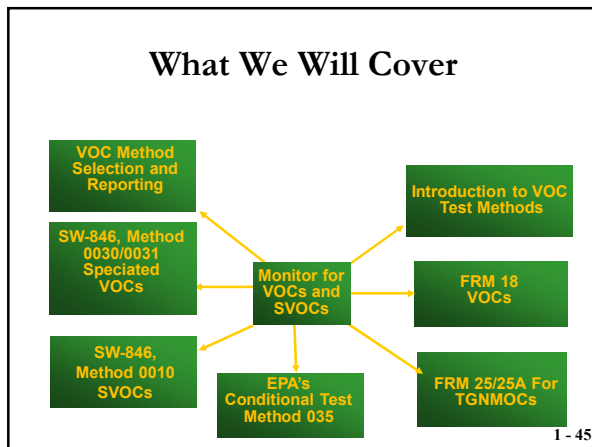
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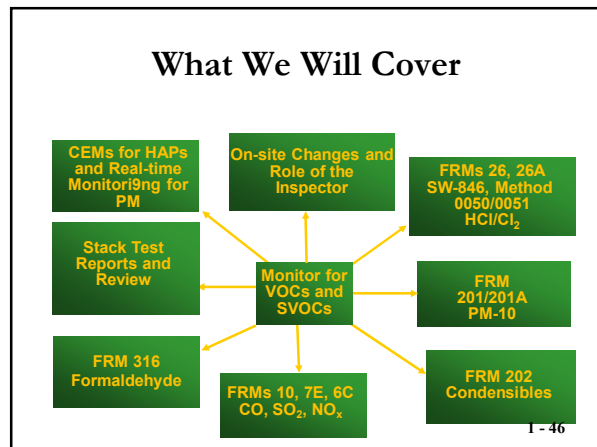
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### Course Materials

**Student Workbook**  
Contains the course agenda and copies of selected slides presented in each of the topic areas

**Student Manual**  
APTI Course #450 Manual and Checklist

1 - 47

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### Course Materials

**Federal Reference Method 5 Manual Operating Manual**  
Agency observation checklist, and various reference materials  
Federal Register containing FRM 1-5

1 - 48

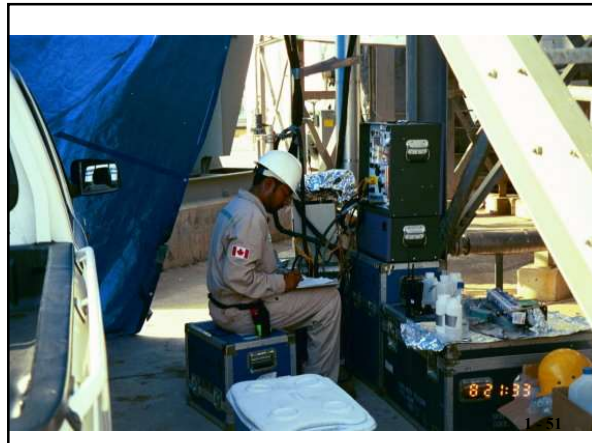
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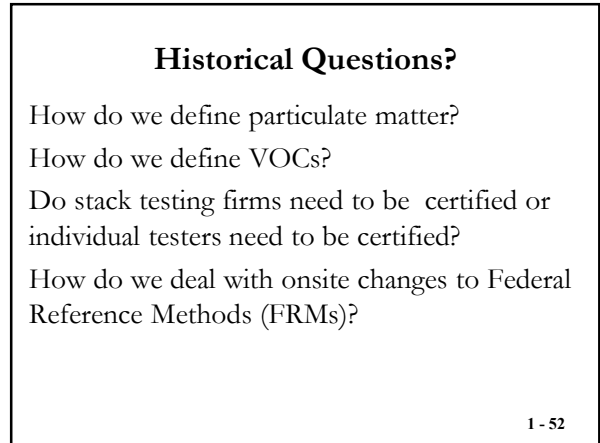
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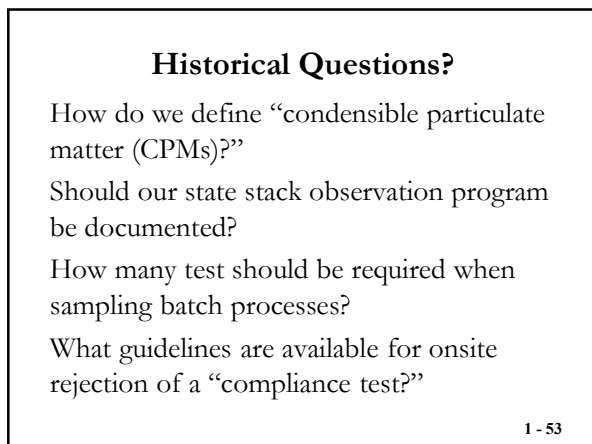
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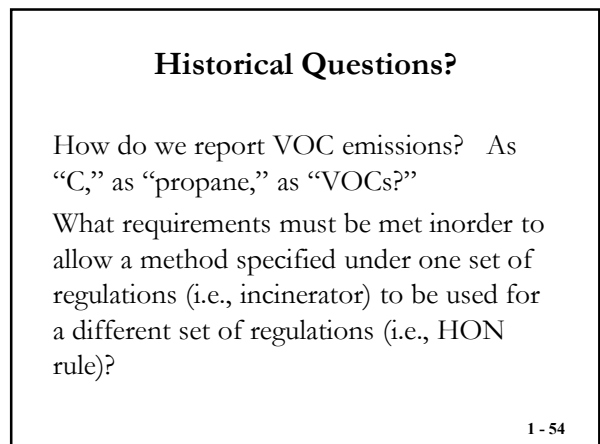
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### Historical Questions?

During compliance testing, what guidelines are available for allowing a “procedure-based method” to become a “performance-based method?”

Are there guidelines available to determine if a source test observation has been performed correctly?

1 - 55

55

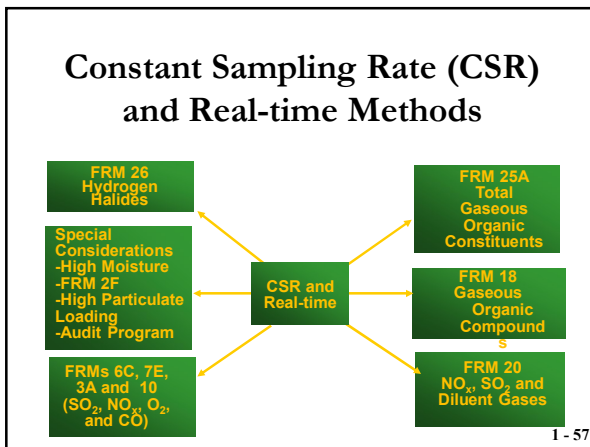
### Historical Questions?

As an Agency inspector, what guidelines are available to help me make correct decisions between “Regulatory Science” and “Measurement Science?”

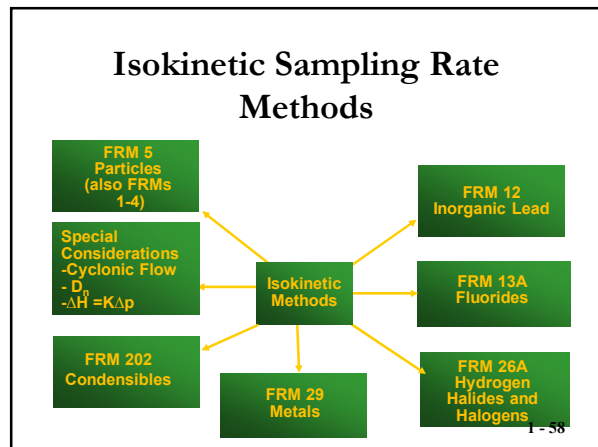
How do we implement good non-EPA programs that haven't been certified by the Agency into a State Agency program that can't be any more strict than the EPA program?

1 - 56

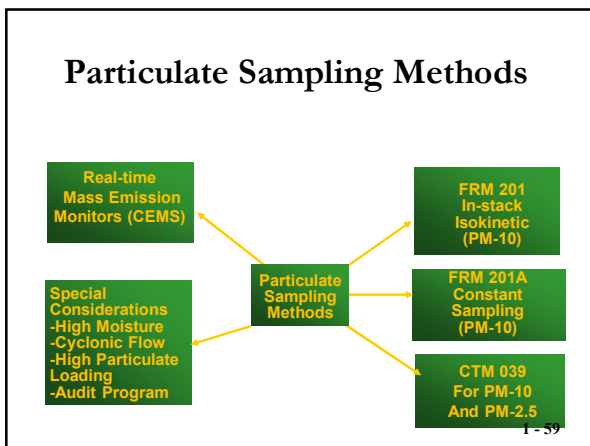
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### Stack Test Methods

Why Develop Stack Test Methods and What is the Driving Force In The United States?

1 - 60

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### Objective of Stack Testing

The objective of performing a stack test is to determine the pollutant mass rate (pmr) or emission rate (E) of pollutant being emitted to determine whether compliance limits are being met

1 - 61

61

### Measurement Units

Concentration	c (ppm, gr/dscf)
Stack gas flow rate	Q (dscm)
Pollutant mass rate	pmr (lb/hr)
Mass emission rate	E (lb/10 <sup>6</sup> Btu)
Process weight rate	E (lb/lbs product produced)

1 - 62

62

### POLLUTANT MASS RATE

$$PMR_s = \bar{c}_s Q_s$$

(  $\bar{v}_s = \bar{v}_n$  )  
for  
Isokinetic Conditions

$\bar{Q}_s = A_s \bar{v}_s$   
 $v_s = K_p c_p \sqrt{\frac{T_s \Delta P}{M_s P_s}}$   
 obtain  $c_p, T_s, \Delta P$   
 $M_s, P_s$

obtain  $\Delta H @, D_n$   
 $B_{ws}, B_{wm},$   
 $P_m, T_m$

1 - 63

63

### What is the Driving Force?

- New Source Performance Standards (NSPS-1970)
- National Emission Standards for Hazardous Air Pollutants (NESHAP-1977)
- Prevention of Significant Deterioration (PSD-1977)

1 - 64

64

### What is the Driving Force?

- Resource Conservation and Recovery Act (RCRA-1978)
- Boiler and Industrial Furnace (BIF-1990)
- Clean Air Act Amendments (CAAA-1990)
  - Maximum Achievable Control Technology (MACT)
  - Title III Hazardous Air Pollutants (HAPs) list of 188

1 - 65

65

### Why Have Title III Hazardous Air Pollutants?

Section 112 of CAA established standards for only seven hazardous air pollutants to date

- Asbestos, mercury, beryllium, vinyl chloride, benzene, radionuclides, arsenic

1 - 66

66

**Why Have Title III  
Hazardous Air Pollutants?**

Additional controls needed for large number of toxic substances not covered in Section 112

1 - 67

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**Title III  
Hazardous Air Pollutants**

**Title III**  
Establishes a list of 188 designated substances to be regulated  
Requires sources to apply maximum achievable control technology (MACT)

1 - 68

68

**Title III  
Hazardous Air Pollutants**

Provides that EPA may require additional controls after MACT to  $10^{-6}$  residual risk levels at the property line (Driving detection limits lower)  
Establishes a program associated with accidental releases

1 - 69

69

**Title III  
Hazardous Air Pollutants**

Requires MACT for all major sources > 10 tons/year or 25 tons/year for combination of toxics  
Requires emission reductions of 75 to 90% below current levels through MACT controls

1 - 70

70

**Title III  
Hazardous Air Pollutants**

Impact on Industry  
Application of maximum achievable control technology (MACT)  
Standards are technology-based  
May have to control after MACT to  $10^{-6}$  risk level at property line

1 - 71

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**Example of  
MACT Standards**

Subpart FFFF (Misc. Organic Chemical Production and Processes [MON])  
Subpart DDDDD (Industrial, Commercial and Institutional Boilers and Process Heaters)  
Hazardous Organic NESHAP (HON) Rule: Regulates SOCOMI  
370 Facilities  
111 of the 188 Title III HAPs

1 - 72

72



### Where Do We Find the Test Methods?

Federal Test Methods- Methods are those (Federal Reference Methods and others) specified in the applicable standards as the test methods used to demonstrate compliance with emission limits or quantitate emissions in meeting regulatory initiatives

1 - 73

73

### Where Do We Find the Test Methods?

[www.epa.gov/ttn/emc/tmethods.html](http://www.epa.gov/ttn/emc/tmethods.html)

1 - 74

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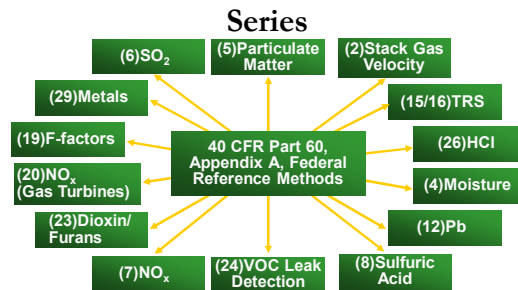
### Regulations

40 CFR Part 60, Appendix A Standards of Performance for New Stationary Sources (i.e., NSPS), Federal Reference Methods (00 Series)

1 - 75

75

### New Source Performance Standard (NSPS) Reference Methods-00 Series



1 - 76

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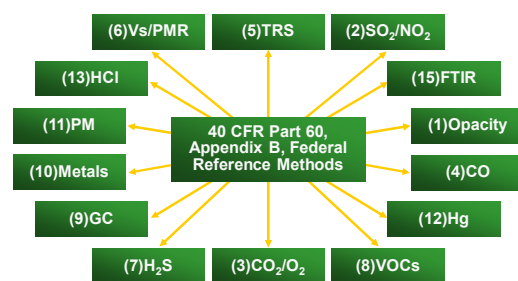
### Regulations

40 CFR Part 60, Appendix B Performance Specification Test (PST) Methods (00 Series)  
40 CFR Part 51, Appendix M State Implementation Plan (SIP) Methods (200 Series)

1 - 77

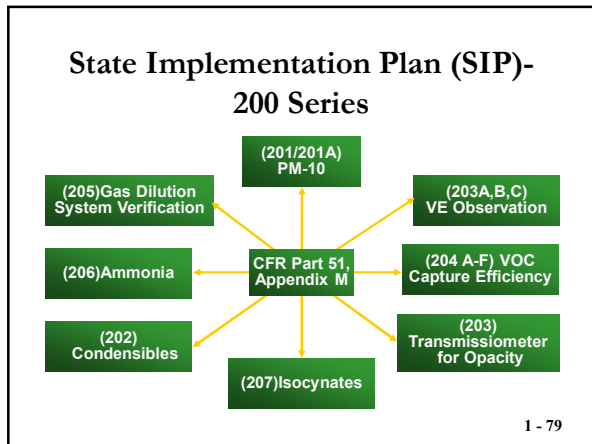
77

### Performance Specification Test (PSTs)-00 Series



1 - 78

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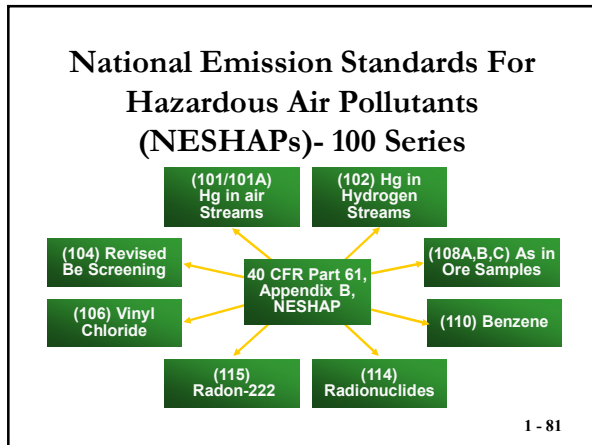
### Clean Air Act and It's Amendments

40 CFR Part 61  
National Emission Standards for Hazardous Air Pollutants (NESHAP)(100 Series, Appendix B)

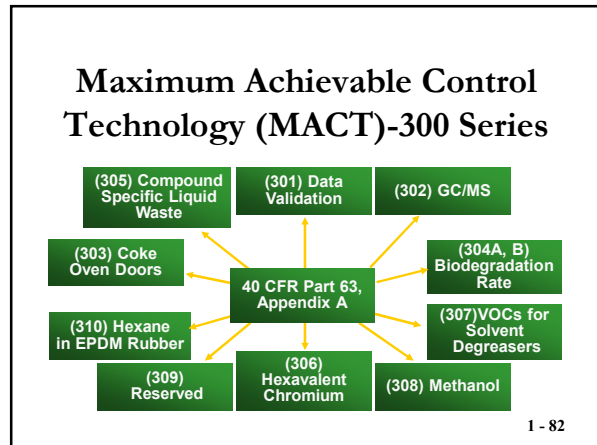
40 CFR Part 63  
Maximum Achievable Control Technology (MACT) Methods (300 Series, Appendix A)

1 - 80

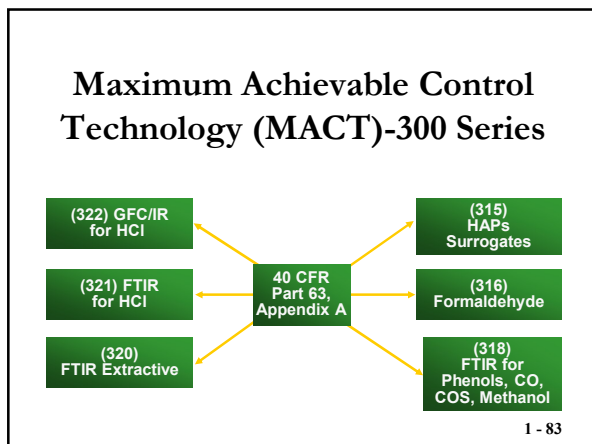
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### Categories of Stack Test Methods by EPA

Category A: Methods proposed or promulgated in Federal Register  
Compliance Methods for 40 CFR Parts 60, 61, and 63

Category B: Source category approved “Approved Alternative”  
Compliance Methods for specific applications with approval from EPA

1 - 84

84

### Categories

Category C:  
“Conditional Methods” evaluated  
by EPA; methods may be used by state/local  
in conjunction with federal enforcement;  
must be “Alternative Method” to be used as  
meeting 40 CFR Parts 60, 61, and 63

1 - 85

85

### Categories

Category D: Methods which may be useful  
in limited applications until more  
supporting information is provided; “gap  
filling” methods (Preliminary Methods)

1 - 86

86

### Categories

Category E: “Idea Box” contain method  
concepts intended to promote information  
exchange

These methods generally have  
had no EPA review or analysis

1 - 87

87

### Example Category Stack Test Methods

Category A (FRMs):  
FRMs 1-29, FRM 100s,  
200s, and 300s

Category B (Approved Alternatives): ALT-  
007 (use of dilution probe in Methods 6C,  
7B, 3A, 10 and 20)

1 - 88

88

### Example Category Stack Test Methods

Category C (Conditional): Particulate (PM  
Screening) Method; conditional test method  
for Acrylonitrile; halogenated organic  
method; Method for isocyanates

1 - 89

89

### Example Category Stack Test Methods

Category D (Preliminary Methods): PRE 5-  
Determination of oxides of nitrogen from  
stationary sources (UV Instrumental  
Analyzer)

1 - 90

90

### Example Category Stack Test Methods

Category E (Idea Box):  
 Sampling and analysis for phosgene emissions from stationary sources  
 All categories of methods found on [www.epa.gov/ttn/emc/tmethods.html](http://www.epa.gov/ttn/emc/tmethods.html)

1 - 91

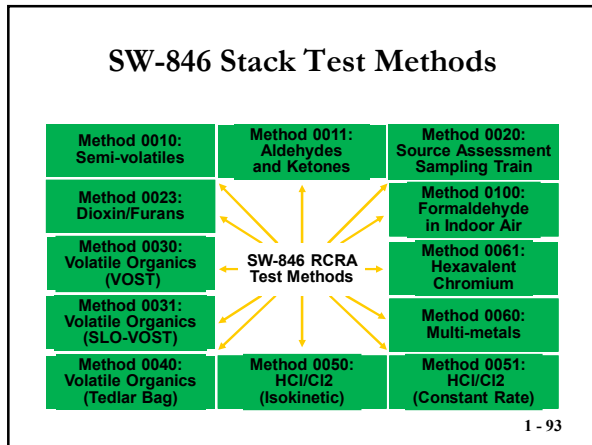
91

### Resource Conservation And Recovery Act (RCRA)

SW-846 is the compendium of analytical and test methods used in determining regulatory compliance under RCRA  
<http://www.epa.gov/sw-846>

1 - 92

92



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### How Do We Define HAPs

CAAA of 1990, Title III now contains a list of 188 HAPs containing both organic and inorganic analytes  
 Defining the 188 HAPs according to  
 Vapor Pressure (in mm Hg at 25°C)  
 Boiling Point Temperature (°C)

1 - 94

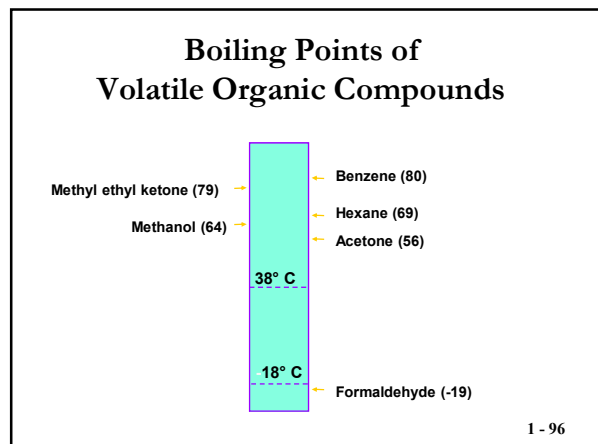
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### General Classification of VOCs

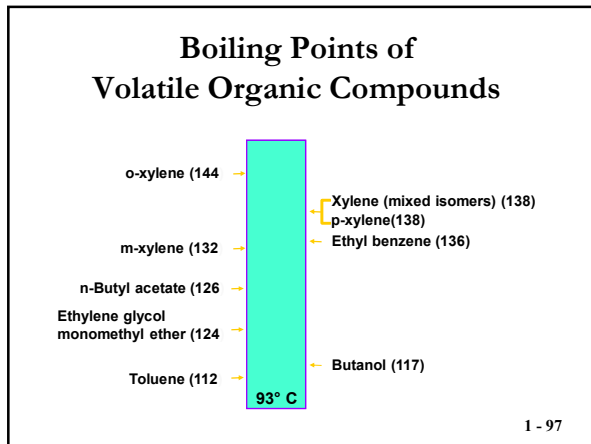
Classification	Vapor Pressure mm Hg	Boiling Point °C
Volatiles (VV/V)	> 10 <sup>-1</sup>	< 200°C
Semi-volatiles (SV)	10 <sup>-1</sup> to 10 <sup>-7</sup>	200 - 500°C
Particles (NV)	< 10 <sup>-7</sup>	> 500°C

1 - 95

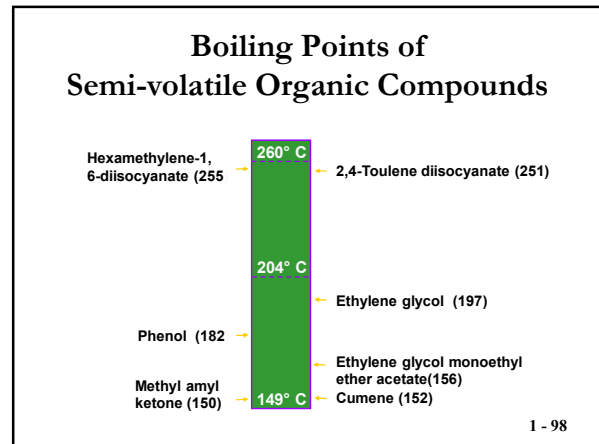
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### General Classification of HAPs

Volatility Class	Number of HAPs in Class
Volatiles (VV/V)	106
Semi-volatiles (SV)	65
Non-Volatile (NV) Particles	17
<b>Total HAPs</b>	<b>188</b>

1 - 99

99

### Example of HAPs in Each Volatility Class

**VP (0.1- 380 mm Hg)  
BP (< 200°C)**

**VOLATILE**

Benzene	76 mm Hg	80.1°C
Xylene, ortho	5 mm Hg	144.4°C
Hydrazine	16 mm Hg	113°C
Hydrochloric acid	23 mm Hg	110°C

1 - 100

100

### Example of HAPs in Each Volatility Class

**VP ( $10^{-7}$  to  $10^{-1}$  mm Hg)  
BP (200 to 500°C)**

**SEMI-VOLATILE (65 HAPs)**

Benzidine	$10^{-5}$ mm Hg	402°C
Captan	$10^{-6}$ mm Hg	479°C
Phosphorus	$10^{-2}$ mm Hg	280°C
Mercury Compounds	$10^{-3}$ mm Hg	356°C

1 - 101

101

### Example of HAPs in Each Volatility Class

**VP (<  $10^{-7}$  mm Hg)  
BP (>500°C)**

**NON-VOLATILE [Particles] (17 HAPs)**

3,3'-Dimethoxybenzidine	$10^{-13}$ mm Hg	458°C
Antimony	Very Low	656°C
Coronene	$10^{-13}$ mm Hg	525°C

1 - 102

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## General Classification of VOCs

Classification	Vapor Pressure mm Hg	Boiling Point °C
Volatiles (VV/V)	$> 10^{-1}$	$< 200^{\circ}\text{C}$
Semi-volatiles (SV)	$10^{-1}$ to $10^{-7}$	200 - $500^{\circ}\text{C}$
Particles (NV)	$< 10^{-7}$	$> 500^{\circ}\text{C}$

1 - 103

**Compliance Test and Source Test Observation**  
**EPA's National Stack Testing Guidance**



2 - 1

1

UNITED STATES ENVIRONMENTAL PROTECTION AGENCY  
WASHINGTON, D.C. 20460

APR 27 2009

OFFICE OF  
ENFORCEMENT AND  
COMPLIANCE ASSISTANCE

**MEMORANDUM**

**SUBJECT:** Issuance of the Clean Air Act National Stack Testing Guidance

**FROM:** Lisa C. Lund, Director  
*Lisa C. Lund*  
Office of Compliance

**TO:** Regional Compliance/Enforcement Division Directors

Attached is a copy of the revised Clean Air Act National Stack Testing Guidance. Final guidance was initially issued on September 30, 2005. At the time of issuance, the Agency indicated that notice and comment rulemaking would be conducted regarding the appropriate circumstances in which an extension of performance test deadlines may be allowed by regulation. This document incorporates the ensuing regulatory revisions which allow source owners or operators to petition for an extension to the test deadlines as a result of a force majeure event. It also includes other minor clarifications and revisions based on feedback we have received since issuance of the 2005 guidance. This revised guidance supersedes the 2005 guidance.

We appreciate the feedback that we have received from each of your offices as well as from state/local agencies. If you or your staff has any questions concerning the guidance, please contact Marilee Miller at (202) 431-7011, or Robert Lischinsky at (202) 564-2628.

Attachment

cc: Regional Air Compliance/Enforcement Branch Chiefs  
 Pamela Mazakas, Acting Director, Air Enforcement Division,  
 Office of Civil Enforcement  
 Peter Tsatsoglis, Director, Sector Policies and Programs Division,  
 Office of Air Quality Planning and Standards (OAQPS)  
 Richard Wayland, Director, Air Quality Assessment Division, OAQPS  
 Compliance and Enforcement Committee Co-Chairs,  
 The National Association of Clean Air Agencies (NACAA)

2 - 2

2

**Purpose/Goals**

- Recognize importance of stack testing as a primary method for determining whether facility has ability to comply with CAA and continues to be in compliance with emission limits
- Expand upon CMS and HPV policy
- Improve uniformity in how tests are conducted, evaluated, and reported
- Improve coordination with states/locals
- Enhance oversight

2 - 3

3

**Background of National Testing Guidance**

- Interim Guidance: February 2, 2004
- Final Guidance: September 30, 2005
- Subsequent rulemaking to allow for extensions in testing deadlines in Force Majeure events effective August 9, 2006
  - Parts 60, 61, 63 of General Provisions amended May 16, 2007
  - Consolidated Federal Air Rule (GP Part 65) amended August 27, 2007
- Guidance issuance: April 27, 2009

2 - 4

4

**Definition**

- Definition and "Scope of Guidance" sections clarify guidance applies only to tests conducted for compliance purposes under NSPS, NESHAP, and MACT programs:  
*Any Performance Testing Conducted for the Purposes of Determining and Demonstrating Compliance with the Applicable Standards of 40 CFR Parts 60, 61, and 63 Using Promulgated Test Methods, Other Test Methods or Procedures Cited in the Applicable Subpart(s), or Alternative Test Methods Approved by the Administrator Under §§60.8, 61.13, or 63.7. It Does Not Include Visible Emission Observation Testing.*

2 - 5

5

**Compliance Monitoring Strategy (CMS)**

- Provides national consistency in developing stationary source CAA compliance monitoring programs while allowing states/locals flexibility to address local air pollution/compliance problems
- States/locals submit CMS plans biennially to Regions
- Enter compliance evaluation results in AFS
- Sources covered are Title V majors and synthetic minors that emit or have potential to emit emissions at or above 80 percent of Title V major source threshold (SM80s)

2 - 6

6

### CMS

- Agency should conduct, or require facility to conduct, a stack test:
  - Whenever the Agency deems appropriate
  - Where there is no other means for determining compliance with emission limits
- Report date and results of all stack tests in AFS, and adjust HPV status, if necessary

2 - 7

7

### Time Frame

- Current regulations do not provide for extensions of test deadlines, except in the event of a force majeure
  - Violation of requirement to stack test
  - Violation of requirement to demonstrate compliance with underlying standard
- Failure to conduct test established in permit or enforcement document
  - Violation of permit or enforcement document
  - May be a violation of underlying requirement
- Concern that only way to grant additional time to test is through formal enforcement action regardless of circumstances

2 - 8

8

### Time Frame (Cont.)

- Guidance takes into account inability to meet regulatory testing deadlines due to circumstances beyond facilities' control
- Currently, four scenarios for how delegated agencies should respond to facilities not testing by deadline
  - Scenarios range from "Force Majeure events" beyond control of facility to those instances where the facility knowingly and willfully violates test requirement
  - Prior to Force Majeure rule, delegated agency was to use enforcement discretion by issuing letter (versus a formal AO) acknowledging circumstances and establishing new test date

2 - 9

9

### Waivers For Identical Units

- Text includes pertinent regulatory references
- Criteria for determining when stack tests for identical units may be waived
- Concept that margin of compliance may not have to be significant where the emissions variability of identical units is low

2 - 10

10

### Notification

- Sufficiency of both the timing and content of the notification is discussed
- Text clarifies that notification is not necessary if test is outside scope of guidance, unless potential for applicable limits to be exceeded
- Clarifying language on submitting site-specific test plans and the contents of such plans

2 - 11

11

### Observation

- No requirement that agency be present for tests. However, whenever possible, delegated agencies should observe
- If agency unable to observe test, review of test protocol even more important
- If timely notification and opportunity to observe not provided, results may be rejected

2 - 12

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### Representative Testing Conditions

- Guidance reinforces Agency position that the CAA requires continuous compliance with emissions limits except where explicitly excused
- Tests should be performed under those representative conditions that:
  - Represent the range of combined process and control measure conditions under which the facility expects to operate (regardless of the frequency of the conditions)
  - Are likely to most challenge the emissions control measures of the facility with regard to meeting the applicable emission standards, but without creating an unsafe condition

2 - 13

13

### Stoppages/Postponements

- No regulatory provision allows stoppage, except for force majeure event
- Depending on circumstances, facility may be in violation of requirement to conduct test, underlying requirement, or both
  - If in jeopardy of failing test, violation of both
  - Currently, Guidance states that if facility is forced to stop due to a force majeure event, agency should evaluate circumstances to determine appropriate enforcement response, if needed
- Guidance is being updated consistent with rulemaking
- Postponements should be treated similar to stoppages
  - If fail to complete test within required time, violation of requirement to test

2 - 14

14

### Test Reports

- Information necessary to adequately document results:
- At a minimum, test submittal:
  - NSPS: Within 180 days after initial startup date or within 60 days after reaching maximum production rate.
  - NESHAP: Within 31 days after test completed.
  - MACT: Within 60 days after test completed.

2 - 15

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### Data Reporting

- Minimum Data Requirements (MDRs) for reporting air compliance monitoring and enforcement activity
- Stack test data reported into national air data system (CEDRA)
- Test date reported with compliance determination from results
  - Compliance status updated, as appropriate
  - High Priority Violator (HPV): failing test for pollutant for which facility is major
  - Test date is to be reported within 60 days of event
- Test results reported as pass, fail, or pending
  - Tests may be reported as pending for up to 120 days from test date
- Reporting of stack test pollutant
  - Mandatory for federal reporters
  - Optional for state reporters

2 - 16

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### Alternative Test Methods

- Requests for alternative test methods (including major, intermediate, and minor changes) involve changes to a test method or testing procedures designated in a NSPS, NESHAP, section 111(d), or section 129 rule as the primary means for determining compliance with an emission standard.
- EPA regulations define "test method" as "the validated procedure for sampling, preparing, and analyzing for an air pollutant specified in a relevant standard as the performance test procedure." 40 CFR § 63.2. Test methods are designated in each NSPS, NESHAP, section 111(d), or section 129 rule as the primary means for determining compliance with an emission standard. An initial or periodic performance test that directly measures emissions is the most common form of test.

2 - 17

17

### Major, Intermediate, and Minor Changes to Test Methods

Major*	Intermediate*	Major* Intermediate* Minor (& reduced sampling times/volumes)
Any of the following: <ul style="list-style-type: none"> <li>• Uses unproven technology or procedures or</li> <li>• Entirely new method or</li> <li>• Broadly applicable (not site-specific)</li> </ul> • Must be validated using EPA Method 301	All of the following: <ul style="list-style-type: none"> <li>• Uses proven technology</li> <li>• Within an existing method</li> <li>• Site-specific Plus, any of the following:                             <ul style="list-style-type: none"> <li>• Potential to set national precedent or</li> <li>• Potential to decrease stringency of standard</li> </ul> </li> </ul>	All of the following: <ul style="list-style-type: none"> <li>• Uses proven technology</li> <li>• Within an existing method</li> <li>• Site-specific, accommodating site-specific constraints</li> <li>• No national significance or precedent</li> <li>• No potential to decrease stringency of standard</li> </ul>

2 - 18

18

### Examples Of Major Changes To Test Methods

- Examples of major changes to a test method include, but are not limited to:
  - Use of an unproven analytical finish;
  - Use of a method developed to fill a test method gap;
  - Use of a new test method such as one developed to apply to a control technology not contemplated in the applicable regulation; and
  - Combining two or more sampling/analytical methods (at least one unproven) into one for application to processes emitting multiple pollutants.

2 - 19

19

### Examples of intermediate changes to a test methods

- Modifications to a test method's sampling procedure including substitution of sampling equipment that has been demonstrated for a particular sample matrix, and use of a different impinger absorbing solution;
- Changes in sample recovery procedures and analytical techniques, such as changes to sample holding times and use of a different analytical finish with proven capability for the analyte of interest; and
- "Combining" a federally required method with another proven method for application to processes emitting multiple pollutants

2 - 20

20

### Examples of minor changes to a test methods

- Field adjustments in a test method's sampling procedure, such as a modified sampling traverse or location to avoid interference from an obstruction in the stack, increasing the sampling time or volume, use of additional impingers for a high moisture situation, accepting particulate emission results for a test run that was conducted with a lower than specified temperature, substitution of a material in the sampling train that has been demonstrated to be more inert for the sample matrix; and
- Changes in recovery and analytical techniques such as a change in quality control/quality assurance requirements needed to adjust for analysis of a certain sample matrix.

2 - 21

21

**Certain Clean Air Act Stationary Source Programs:**  
 New Source Performance Standards (NSPS) under CAA section 111(b) and 40 CFR part 60  
 National Emission Standards for Hazardous Air Pollutants (NESHAP) under CAA section 112 and 40 CFR parts 61 and 63  
 Emission Guidelines for Federal Plans and State Plans under CAA section 111(d) and 40 CFR parts 60 and 62  
 Solid Waste Incinerator Rules under CAA section 129 and 40 CFR parts 60 and 62

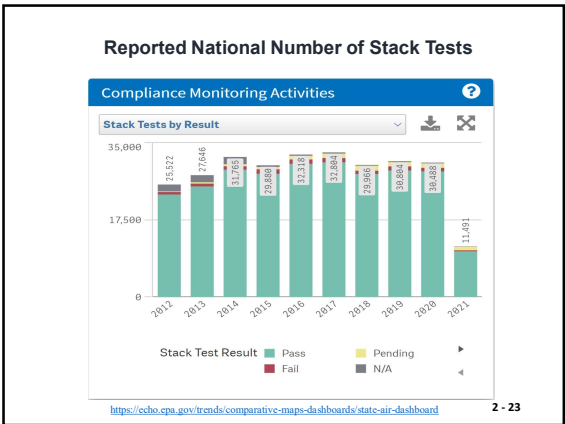
July 2020

Office of Air Quality Planning and Standards  
Office of Air and Radiation  
U.S. Environmental Protection Agency

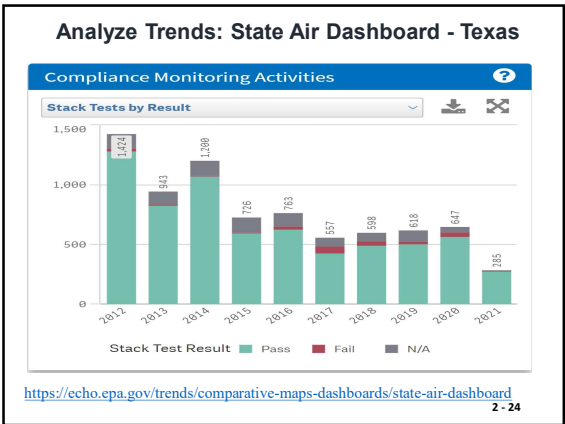
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2 - 22

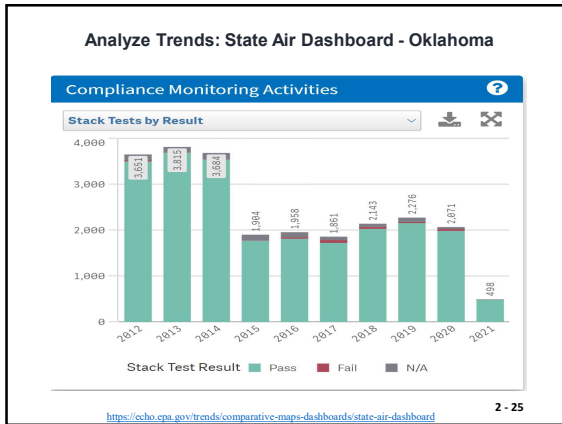
22



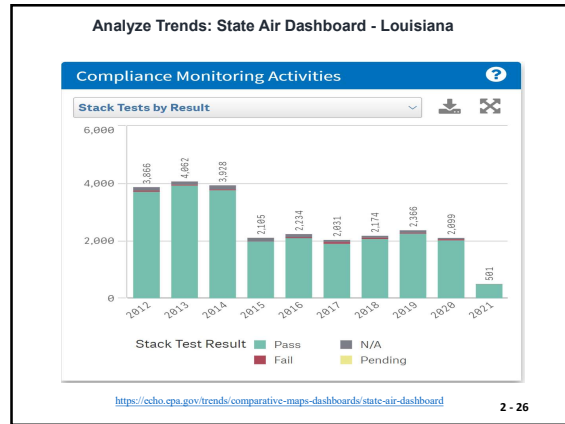
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24



25



26

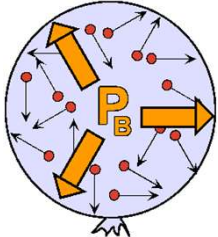
### Additional Information

- Robert Lischinsky  
[lischinsky.robert@epa.gov](mailto:lischinsky.robert@epa.gov)  
202-564-2628
- Internet Address:  
<https://echo.epa.gov/trends/comparative-maps-dashboards/state-air-dashboard?state=IL&view=activity>

2 - 27

27

Compliance Test and Source Test  
Observation  
Properties of Gases



3 - 1

1

Properties of Gases

- Temperature
- Pressure
- Atomic Weight
- Molecular Weight and Moles
- Avogadro's Number
- Ideal Gas Law
- Moving Gases

3 - 2

2

Temperature

- Degrees Fahrenheit: °F
- Degrees Centigrade: °C
- °C =  $5/9 (\text{°F} - 32)$
- °F =  $9/5 (\text{°C}) + 32$

3 - 3

3

Absolute Temperature


- Degrees Rankine: R
- Degrees Kelvin: K
- R = °F + 459.49
- K = °C + 273.16

3 - 4

4

Absolute Pressure, P

- P = P<sub>b</sub> + p<sub>g</sub>
- P<sub>b</sub> = Barometric pressure
- P<sub>g</sub> = Gauge pressure



3 - 5

5

Units of Pressure

- in. Hg            atmospheres
- mmHg            torr
- in. H<sub>2</sub>O            pascals

3 - 6

6

1 Atmosphere =

- 29.92 in. Hg
- 39.90 ft H<sub>2</sub>O
- 14.70 lbs/in.<sup>2</sup>
- 760 mmHg
- 1 torr

3 - 7

7

EPA Standard Pressure  
and Temperature

- P<sub>std</sub> = 29.92 in. Hg
- T<sub>std</sub> = 20° C or 68° F

**for source testing**

3 - 8

8

Atomic Weight

A number that indicates how heavy  
(on the average) an atom is compared  
to an atom of another element

(Assign **carbon** atomic wt = 12)

3 - 9

9

Molecular Weight, M

The sum of the atomic weights of all the  
atoms in a molecule

MW of CO

$$12 + 16 = 28$$

3 - 10

10

n = number of moles  
1 mole =

The molecular weight of a compound  
expressed in lbs (lb-mole )

or

in grams (g-mole )

1 mole of CO = 28 grams

3 - 11

11

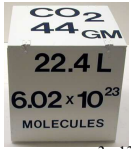
1 gram-mole =

$6.023 \times 10^{23}$  molecules  
(Avogadro's Number)

3 - 12

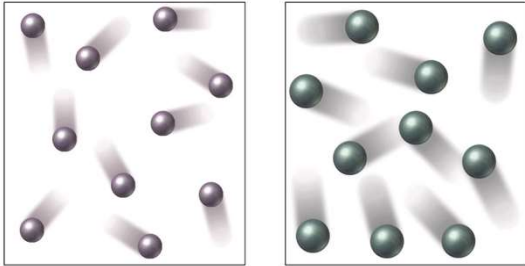
12

1 mole = Avogadro's Number  
worth of molecules  
( $6.023 \times 10^{23}$ )  
Occupies  
22.4 L  
At 0° C and 1 atmosphere



3 - 13

13



1 mol helium at STP  
Volume = 22.4 L  
Mass = 4.00 g

1 mol xenon at STP  
Volume = 22.4 L  
Mass = 131.3 g

3 - 14

14

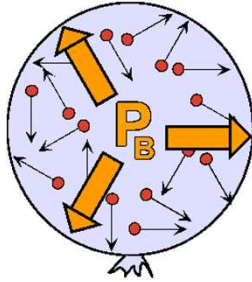
Given a mass, m, of a  
compound, the number of  
moles is calculated by:

$$n = \frac{m}{M}$$

3 - 15

15

The Ideal Gas Law



3 - 16

16

The Ideal Gas Law

$$PV = nRT$$

Absolute Pressure → P  
Volume → V  
# moles → n  
Absolute Temperature → T  
Ideal Gas Law constant → R

3 - 17

17

R

The gas law constant is dependent on  
units used for EPA reference methods in  
English units:

$$R = 21.83 \frac{(in.Hg)(ft^3)}{(lb-mole)(^{\circ}R)}$$

3 - 18

18

Correcting Volume to Standard  
Conditions

$$V_{s \text{ stack}} = nR \frac{T_s}{P_s}$$

$$V_{s \text{ std}} = nR \frac{T_{std}}{P_{std}}$$

3 - 19

19

Dividing top by bottom gives

$$V_{std} = V_s \frac{T_{std} P_s}{P_{std} T_s}$$

3 - 20

20

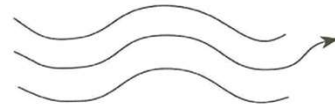
Properties of Moving Gases

- Velocity
- Volumetric flow rate
- Isokinetic sampling
- Pollutant mass rate

3 - 21

21

Velocity



$$V_s = \text{ft/sec or ft/hr}$$

3 - 22

22

Velocity,  $V_s$ ,  $\frac{\text{ft}}{\text{sec}}$ ,  $\frac{\text{ft}}{\text{hr}}$

Determined by Method 2 using the  
Type S pitot tube

3 - 23

23

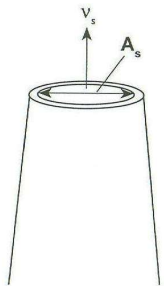
The Pitot Tube Equation

$$v_s = K_p C_p (\sqrt{\Delta p})_{avg} \sqrt{\frac{T_{s(avg)}}{P_s M_s}}$$

3 - 24

24

### Volumetric Flow Rate



$$Q_s = V_s A_s$$

$$\frac{ft^3}{sec} = \frac{ft}{sec} \times ft^2$$

or

$$\frac{ft^3}{hr} = \frac{ft}{hr} \times ft^2$$

3 - 25

25

### Isokinetic Sampling

$$\% \text{ Isokinetic} = \frac{V_n}{V_s} \times 100$$

3 - 26

26

### FRM 5 Isokinetic Rate Equation

$$\%I_{int} = 100 \frac{T_s V_{m(std)} P_{std}}{T_{std} V_s \theta A_n P_s 60 (1 - B_{ws(est)})}$$

$$\%I_{final} = \frac{100 T_{s(avg)} K_3 V_{ic} + \frac{V_{m(avg)}}{T_{m(avg)}} P_{bar} + \frac{\Delta H}{13.6}}{60 \theta V_{s(avg)} P_s A_n}$$

3 - 27

27

### FRM 5 Isokinetic Rate Equation (Simplified)

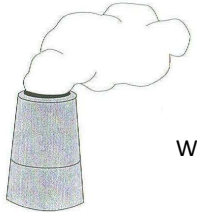
$$D_{n(est)} = \frac{0.0358 Q_m P_m}{T_m C_p (1 - B_{ws(est)})} \frac{T_s M_s}{P_s \Delta p_{est}}$$

$$\Delta H = 846.72 D_n^4 \Delta H_{@ C_p^2} (1 - B_{ws})^2 \frac{M_d T_m P_s}{M_s T_s P_m} \Delta P$$

3 - 28

28

### Pollutant Mass Rate (pmr)



$$pmr = c_s Q_s$$

Where:  $c_s$  = the pollutant concentration

3 - 29

29

### Concentration, $c_s$

$$c_s = \frac{m}{V} = \frac{\text{Quantity of pollutant (mass)}}{\text{Quantity of effluent gas (vol)}}$$

Units: g/m<sup>3</sup>, lbs/ft<sup>3</sup>, gr/ft<sup>3</sup>, ppm

Note: 7000 grains (gr) = 1 lb

3 - 30

30



$$pmrS = c_s Q_s$$

$$\frac{\text{lbs}}{\text{hr}} = \frac{\text{lbs}}{\cancel{\text{ft}^3}} \times \frac{\cancel{\text{ft}^3}}{\text{hr}}$$

3 - 31

31

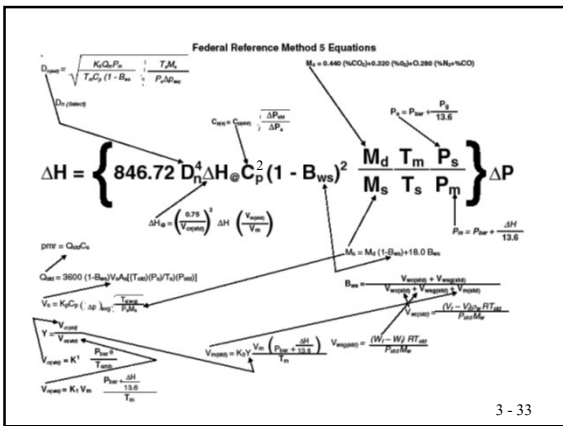
Emission Rate  
(Combustion Sources)

$$E = \frac{pmr_s}{Q_H} \left( \frac{\text{lbs}}{10^6 \text{ Btu}} \right)$$

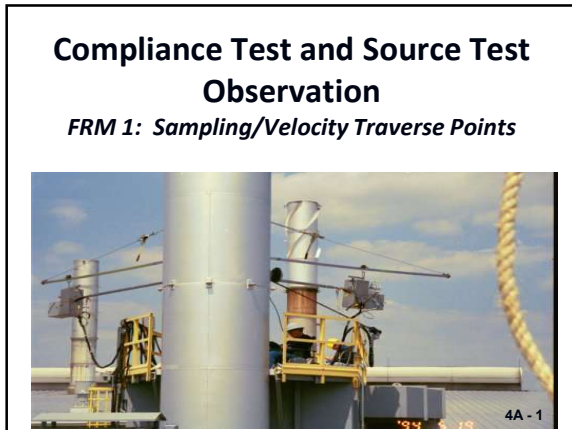
Where:  $Q_H$  = heat input rate in units of Btu/hr

3 - 32

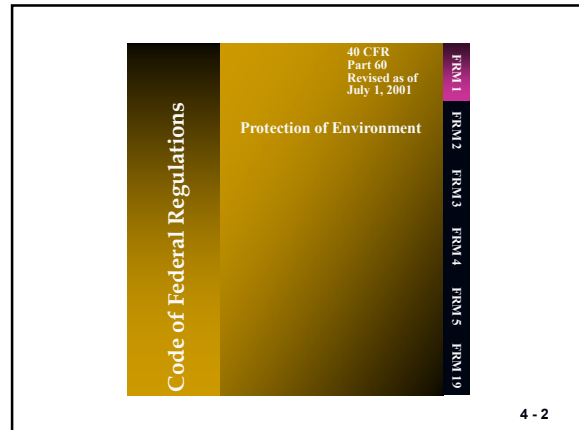
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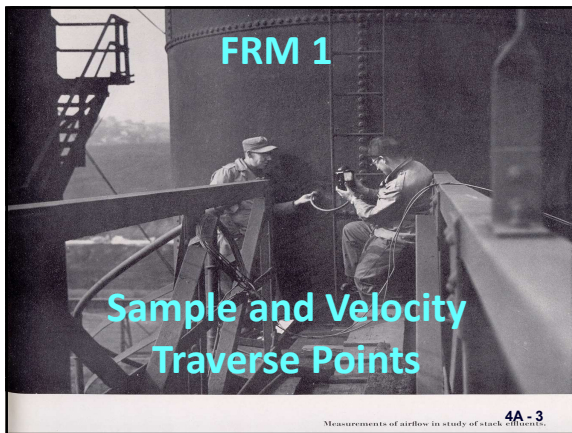
33



1



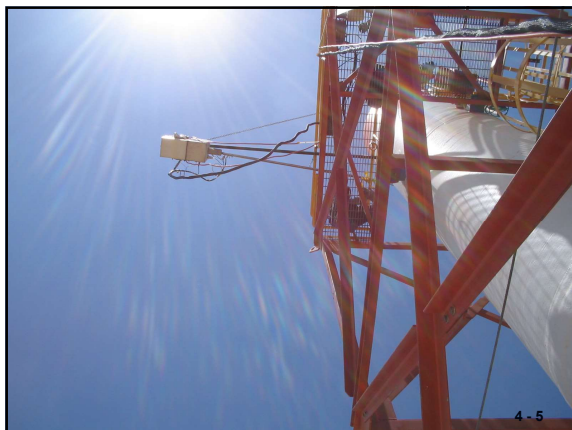
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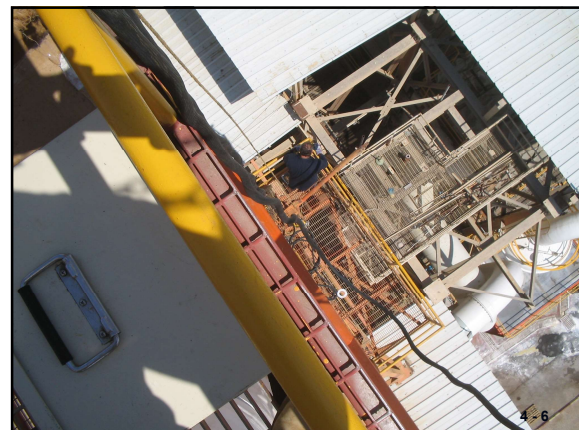
3



4



5



6

### FRM 1 History

- 1970 Promulgated
- 1983 Reduced Number of Traverse Points
- 1986 Alternative Procedure for Site Selection
- 1989 Method 1A, Traverse Points in Small Ducts

4A - 7

7

### FRM 1

- Method 1 specifies both the sampling site location and the location of the sampling points to which the source tester will measure a representative sample
  - Pollutant emissions
  - Total volumetric flow rate

4A - 8

8

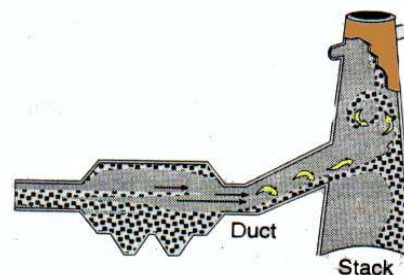
### FRM 1 Basic Principle

- "...the more convoluted the ductwork, the more points will need to be tested."
- Representative measurement
- Modifications to FRM 1
  - Rectangular stacks
  - Only measuring velocity
  - Stacks smaller than 12 inches

4A - 9

9

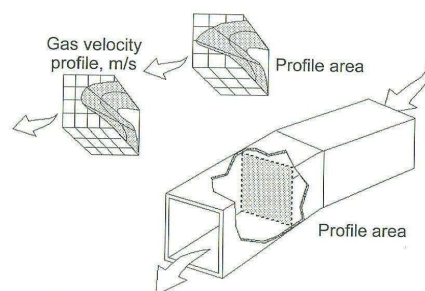
### FRM 1 Sampling Site Locations



4A - 10

10

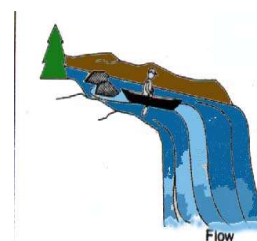
### Particle mass concentration profile, mg/m<sup>3</sup>



4A - 11

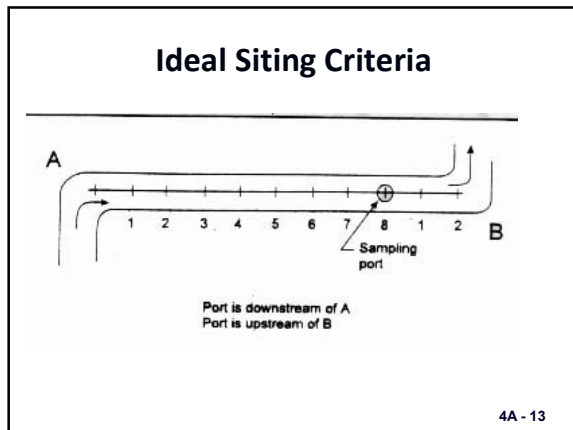
11

### FRM 1 Siting Criteria



2 - 12

12



13

### FRM 1 Applicability

- > 12" diameter duct, stack
- Not for use in cyclonic, swirling
- Not for sample locations
  - < 2 Diameter downstream from flow disturbance
  - < 0.5 Diameter upstream from flow disturbance
- Check "as built" drawings for external and internal interferences above and below sampling port locations

4A - 14

14

### Exceptions to FRM 1 (Can't use FRM 1)

- #1: Cyclonic or swirling gas flow (>20 degrees)
- #2: Stack smaller than 0.30 m (12") in diameter or cross-section area is less than 0.71 m<sup>2</sup> (113 in<sup>2</sup>), Use Method 1A

4A - 15

15

### Exceptions to FRM 1 (Can't use FRM 1)

- #3: Measurement site is less than 2 duct diameters downstream or less than 0.5 diameters upstream from a flow disturbance  
(Use Alternative Procedure, Section 11.1.2)

4A - 16

16

### FRM 1 Flow Disturbance

- Bend in duct
- Expansion or contraction in the duct
- Visible flame

4A - 17

17

### Stack Extensions Required

- When stack is too short for proper port location
- Straightening vanes are needed to remove cyclonic or swirling flow
- Possible down draft from wind blowing across stack

4A - 18

18

### Sampling Location

- Determine the upstream and downstream disturbances
- Measure the distance the sampling port is from those disturbances
- Divide the distance by the diameter of the stack
- Ideal location is 8 downstream and 2 upstream

4A - 19

19



20



21



22

### FRM 1 Siting Criteria

- At 8 duct diameters downstream and 2 duct diameters upstream of a flow disturbance, the siting criteria states
  - Velocity head profile is assumed to resemble laminar flow

4A - 23

23

### FRM 1 Siting Criteria

- The minimum number of sampling points can be used
  - 8 or 9 for 12-24 in. stacks
  - 12 for > 24 in. stacks

4A - 24

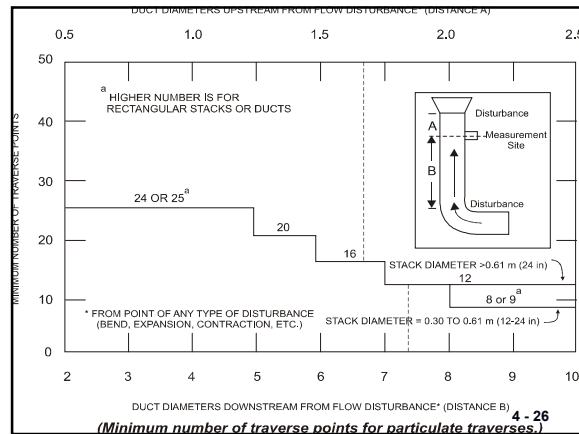
24

### FRM 1 Siting Guidance

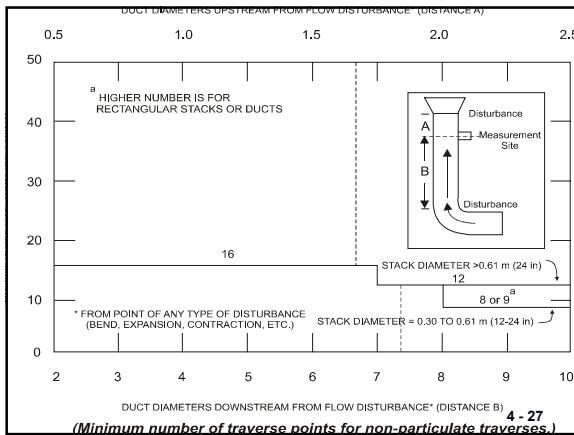
- Federal Register provides illustrations for minimum number of traverse points for particulate traverses and velocity traverses (Figure 1-1 in Federal Register)
- Federal Register provides location of traverse points (Figure 1-2 in Federal Register)

4A - 25

25



26



27

### FRM 1 Equal Areas

- The circular duct is divided up into four equal quadrants, each of which is divided into equal areas
- Traverse points are then located at the centroid of these areas
  - Two perpendicular diameters
  - One diameter must be in the "plain of the bend."

4A - 28

28

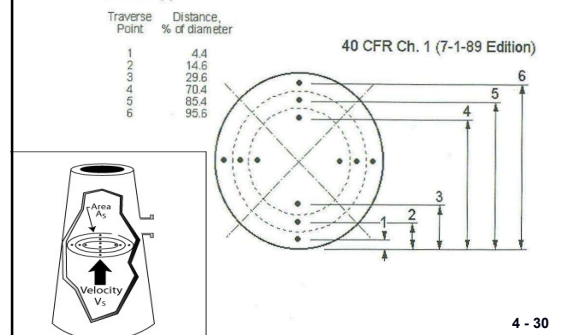
Table 1-2 Location of Traverse Points in Circular Stacks  
(Percent of stack diameter from inside wall to traverse point)

Traverse point on a diameter	Number of traverse points on a diameter																								
	2	4	6	8	10	12	14	16	18	20	22	24	2	4	6	8	10	12	14	16	18	20	22	24	
1	14.6	8.7	4.4	3.2	2.6	2.1	1.8	1.6	1.4	1.3	1.1	1.1	85.4	25.0	14.6	10.5	8.2	6.7	5.7	4.9	4.4	3.9	3.5	3.2	
2		75.0	29.6	19.4	14.6	11.8	9.9	8.5	7.5	6.7	6.0	5.5		93.3	70.4	32.3	22.6	17.7	14.6	12.5	10.9	9.7	8.7	7.9	
3			85.4	67.7	34.2	25.0	20.1	16.9	14.6	12.9	11.6	10.5			95.6	80.6	55.8	35.6	26.9	22.0	18.8	16.5	14.6	13.2	
4				95.6	89.5	77.4	64.4	36.6	28.3	23.6	20.4	18.0	16.1			96.8	85.4	75.0	63.4	37.5	29.6	25.0	21.8	19.4	
5					91.8	82.3	73.1	62.5	38.2	30.6	26.2	23.0				91.8	82.3	73.1	62.5	38.2	30.6	26.2	23.0		
6						97.4	88.2	79.9	71.7	61.8	38.8	31.5	27.2				93.3	85.4	76.0	70.4	61.2	39.3	32.3		
7							97.9	90.1	83.1	76.4	69.4	60.7	39.8					94.3	87.5	81.2	75.0	68.5	60.2		
8								98.2	91.5	85.4	79.6	73.8	67.7					98.2	91.5	85.4	79.6	73.8	67.7		
9									95.1	89.1	83.5	78.2	72.8						95.1	89.1	83.5	78.2	72.8		
10									98.4	92.5	87.1	82.0	77.0						98.4	92.5	87.1	82.0	77.0		
11										95.6	90.3	85.4	80.6							95.6	90.3	85.4	80.6		
12										96.8	93.3	88.4	83.9							96.8	93.3	88.4	83.9		
13										96.1	91.3	86.8									96.1	91.3	86.8		
14										98.7	94.0	89.5									98.7	94.0	89.5		
15											96.5	92.1										96.5	92.1		
16												98.9	94.5										98.9	94.5	
17													96.8										96.8		
18														98.9									98.9		
19															96.1								96.1		
20																98.7							98.7		
21																	96.5						96.5		
22																		98.9					98.9		
23																			96.8				96.8		
24																				98.9			98.9		

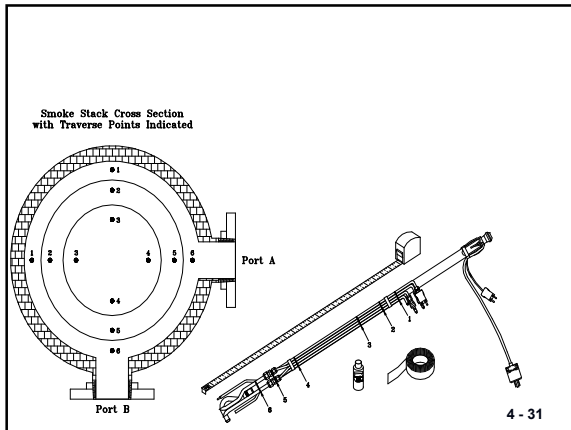
4 - 29

29

Pt. 60, App. Meth. 1



30



31



32

### FRM 1 Location of Traverse Points

- Percent distance of traverse point from inside wall of duct determined from Table 1-2 in Method 1
  - >24" stacks, no traverse point within 1 inch
  - <24" stacks, no traverse point within 0.5 inches

4A - 33

33



34

### FRM 1 Rectangular Ducts

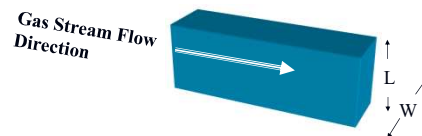
- In the case of rectangular ducts, an "equivalent diameter",  $D_e$ , is used in the siting and traverse point consideration
  - $D_e = 2LW / (L + W)$
  - Must use balance matrix

4A - 35

35

### FRM 1 Diameter Equivalent Formula for Rectangular Ducts

$$D_e = \frac{2LW}{(L + W)}$$



2 - 36

36

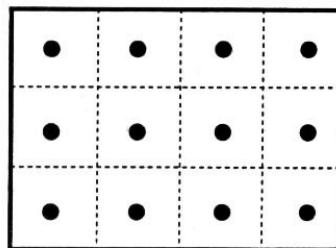
**Table 1-1 Cross-section Layout For Rectangular Stacks 40CFR Part 60 Appendix A**

Number of transverse points layout	Matrix
9 .....	3 x 3
12 .....	4 x 3
16 .....	4 x 4
20 .....	5 x 4
25 .....	5 x 5
30 .....	6 x 5
36 .....	6 x 6
42 .....	7 x 6
49 .....	7 x 7

4A - 37

37

**Rectangular Duct  
(3 X 4)**



4 - 38

38

**FRM 1 Verification or Absence of Cyclonic Flow**

- Cyclonic flow may exist (Section 1.1)
  - After such devices as cyclones and inertial demisters following venturi scrubbers
  - In stacks having tangential inlets or other duct configurations which tend to induce swirling

4A - 39

39

**Cyclonic Flow Determination  
(Ducts >4in.)**

- Equipment
  - Manometer
  - Type S pitot tube/level indicator
- Procedure
  - "Null" reading; O.K.
  - Determine delta p if not "null"
  - Acceptance avg.  $\Delta p < 20$  degrees

4A - 40

40

**FRM 1 Alternative Measurement Site Selection Procedure**

- Applies at sites  $< 2/0.5$  siting
  - Must use "directional probe" to measure "yaw" and "pitch" angles at more than 40 traverse points
  - Calculate Resultant Angle (Ri)
    - $Ri = \text{Arccos}[(\cos Y_i)(\cos P_i)]$
    - If  $Ri < 20$  degrees, then can use sample location

4A - 41

41

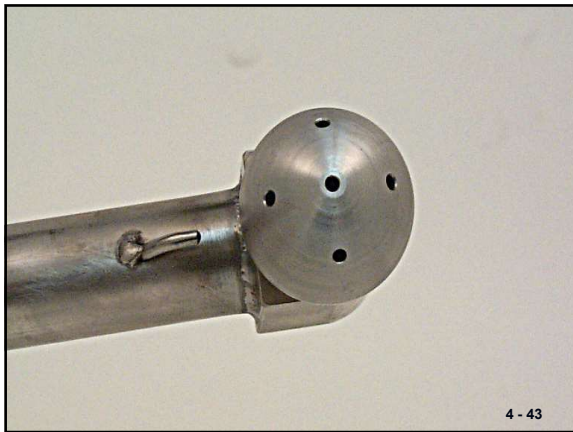
**Method 2F Equipment**

- 3D Probes
  - Spherical
    - Easy Leak Check
    - More Sensitive
    - Less Costly
  - Prism (DAT)

4A - 42

42





43

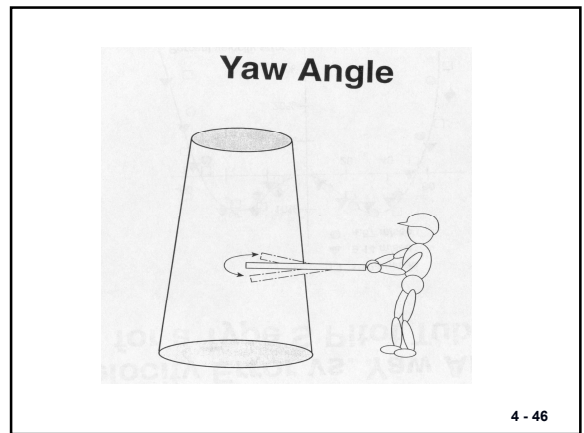


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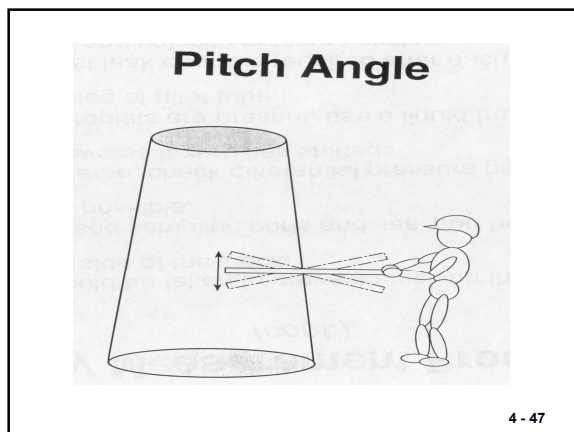
### 3-D Probe Measurements

- P1: Impact Pressure
- P2-P3: Yaw Angle
- P4-P5: Pitch Angle
- P1-P2: Total Velocity

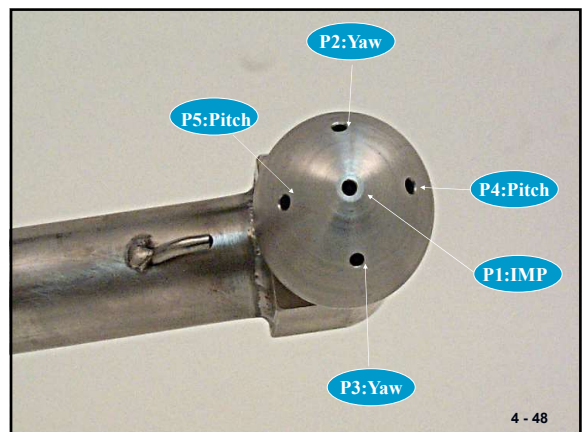
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46



47



48

### 3-D Probe Measurement

- Position probe at traverse point and verify position of “scribe line.”
- Pre leak check
- Record yaw and pitch angles at each traverse point
- Calculate resultant angle
- Post leak check

4A - 49

49

### 3-D Probe Measurement

- Yaw to “null”; Record gauge reading yaw angle (Yi) at traverse point.
- Record gauge reading pitch angle and determine pitch angle (Pi) from calibration curve.
- Complete for each traverse point.
- Calculate Resultant Angle (Ri)
  - $R_i = \text{Arccos}[(\cos Y_i)(\cos P_i)]$

4A - 50

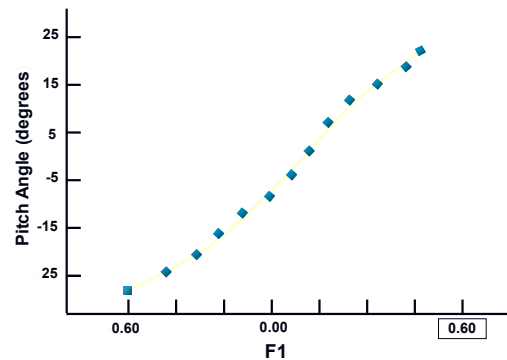
50

### Pitch Angle Curve (F1 Calibration Curve)

- $F1 = (P4 - P5) / (P1 - P2)$
- Manufacturer plots F1 vs. Pitch Angle at Qualified Wind Tunnel at Two Flow Rates (60 and 90 ft/sec)

4A - 51

51



4 - 52

52

### 3-D Probe Measurement For Acceptance Criteria

- Calculate Resultant Angle (Ri)
  - $R_i = \text{Arccos}[(\cos Y_i)(\cos P_i)]$
- Measurement location is acceptable if
  - $R_{i\text{ avg}} \leq 20$  degrees
  - $S_d = 10$  degrees

4A - 53

53

$$R_{\text{avg}} = \sum R_i / n \quad \text{Eq. 1-3}$$

$$S_d = \sqrt{\frac{\sum_{i=1}^n (R_i - R_{\text{avg}})^2}{(n-1)}} \quad \text{Eq. 1-4}$$

12.3.4 Acceptability Criteria. The measurement location is acceptable if  $R_{\text{avg}} \leq 20^\circ$  and  $S_d \leq 10^\circ$ .

4A - 54

54

**Traverse Points.** Use a minimum of 40 traverse points for circular ducts and 42 points for rectangular ducts for the gas flow angle determinations. Follow the procedure outlined in Section 11.3 and Table 1-1 or 1-2 for the location and layout of the traverse points. If the measurement location is determined to be acceptable according to the criteria in this alternative procedure, use the same traverse point number and locations for sampling and velocity measurements.

4A - 55

55

### Role of the Inspector FRM 1 Activities

- Verify duct > 12 in. diameter for proper equipment selection
- Verify duct dimensions
- Verify upstream/downstream distances
- Check for blockage (Feel, look into duct for blockage)

4A - 56

56

### Role of the Inspector FRM 1 Activities

- Verify required number of points
- Adjust the required number of points if required (0.5 in. < 12 in.; 1 in. > 12 in. to stack wall)
- Check for cyclonic flow (average of < 20 degrees for all sampling point)
- Observe "Alternative Site Selection" verification

4A - 57

57

### Major Points in FRM 1

- Limitation of method (Sec. 1.2)
- For rectangular stacks, equivalent diameter (Sec. 2.1)
- Minimum number of traverse points (Sec. 11.2.1.1)
- For particle sampling, one diameter in plain of bend (Sec. 11.3.1.2)

4A - 58

58

### Major Points in FRM 1

- Relocation of traverse points (Sec. 2.3.1.1)
- Definition of cyclonic flow (Sec. 2.4)
- Verification of absence of cyclonic flow (Sec. 2.4)

4A - 59

59

### Major Points in FRM 1

- Alternative Measurement Site Location (Sec. 2.5)
  - Directional flow sensor and resultant angle (Sec. 2.5.1.1)
  - Post leak check required at 3 in. water (Sec. 2.5.3.3)

4A - 60

60

### Major Points in FRM 1

- Alternative Measurement Site Location (Sec. 2.5) Continued
  - Calculate resultant angle at each traverse point (Sec. 2.5.4.1)
  - Calibration of directional flow sensor (Sec. 2.5.6)

4A - 61

61

### FRM 1 Inspector Tools

- Tape measure
- Field Observation Agency Checklist
- Type S pitot tube (cyclonic flow check) and level indicator
- 3-D pitot tube (alt. meas. site) and level indicator

4A - 62

62

### FRM 1 Tips

- Measure the stack diameter from each sampling port and average values
- Find in-stack restrictions by using gloved hand and visual inspection of internal area
- Don't forget to take into consideration the nipple of the stack or inner lining in calculations

4A - 63

63

### FRM 1 Tips

- If measurement site location is after venturi scrubber or stack has tangential inlets, verify absence of cyclonic flow
- If stack is < 12 in., do not use this method (Use FRM 1A)
- If measurement site location < 2 D/0.5 D, don't use method

4A - 64

64

### FRM 1 Tips

- Add first and last traverse points together to get internal stack diameter and compare to calculated value
- Don't forget to add pipe coupling (nipple) diameter to calculated traverse points
- "White-out" is an excellent tool for marking probe

4A - 65

65

### METHOD 1A—SAMPLE AND VELOCITY TRAVERSES FOR STATIONARY SOURCES WITH SMALL STACKS OR DUCTS

4A - 66

66

**METHOD 1A**

- The applicability and principle of this method are identical to Method 1, except its applicability is limited to stacks or ducts.
- This method is applicable to flowing gas streams in ducts, stacks, and flues of less than about 0.30 meter (12 in.) in diameter, or 0.071 m<sup>2</sup> (113 in.<sup>2</sup>) in cross-sectional area, but equal to or greater than about 0.10 meter (4 in.) in diameter, or 0.0081 m<sup>2</sup> (12.57 in.<sup>2</sup>) in cross-sectional area.
- This method cannot be used when the flow is cyclonic or swirling.

4A - 67

67

**METHOD 1A**

- The method is designed to aid in the representative measurement of pollutant emissions and/or total volumetric flow rate from a stationary source.
- A measurement site or a pair of measurement sites where the effluent stream is flowing in a known direction is (are) selected.
- The cross-section of the stack is divided into a number of equal areas with the traverse points located within each of these equal areas.

4A - 68

68

**METHOD 1A**

- In these small diameter stacks or ducts, the conventional Method 5 stack assembly (consisting of a Type S pitot tube attached to a sampling probe, equipped with a nozzle and thermocouple) blocks a significant portion of the cross-section of the duct and causes inaccurate measurements.
- Particulate matter (PM) sampling in small stacks or ducts, the gas velocity is measured using a standard pitot tube downstream of the actual emission sampling site.
- The straight run of duct between the PM sampling and velocity measurement sites allows the flow profile, temporarily disturbed by the presence of the sampling probe, to redevelop and stabilize.

4A - 69

69

**METHOD 1A**

- Particulate Measurements—Steady or Unsteady Flow. Select a particulate measurement site located preferably at least eight equivalent stack or duct diameters downstream and 10 equivalent diameters upstream from any flow disturbances such as bends, expansions, or contractions in the stack, or from a visible flame.

4A - 70

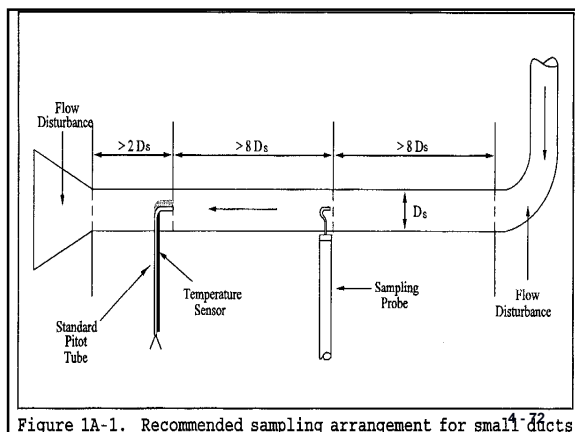
70

**METHOD 1A**

- Next, locate the velocity measurement site eight equivalent diameters downstream of the particulate measurement site (see Figure 1A-1).

4A - 71

71



72

### Method 1A

- If such locations are not available, select an alternative particulate measurement location at least two equivalent stack or duct diameters downstream and two and one-half diameters upstream from any flow disturbance.
- Locate the velocity measurement site two equivalent diameters downstream from the particulate measurement site. (See Section 12.2 of Method 1 for calculating equivalent diameters for a rectangular cross-section.)4A - 73

73

### Method 1A

- PM Sampling (Steady Flow) or Velocity (Steady or Unsteady Flow) Measurements.
- For PM sampling when the volumetric flow rate in a duct is constant with respect to time
- Section 11.1.1 of Method 1 may be followed, with the PM sampling and velocity measurement performed at one location.

4A - 74

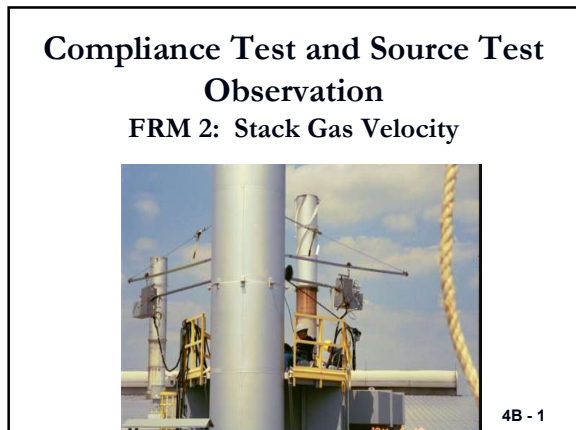
74

### Method 1A

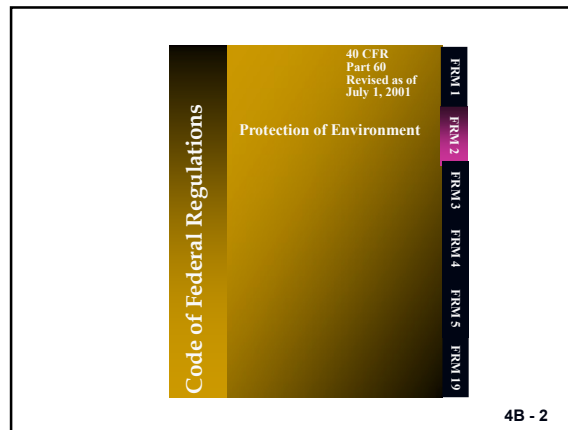
- To demonstrate that the flow rate is constant (within 10 percent) when PM measurements are made, perform complete velocity traverses before and after the PM sampling run.
- Calculate the deviation of the flow rate derived after the PM sampling run from the one derived before the PM sampling run.
- The PM sampling run is acceptable if the deviation does not exceed 10 percent.

4A - 75

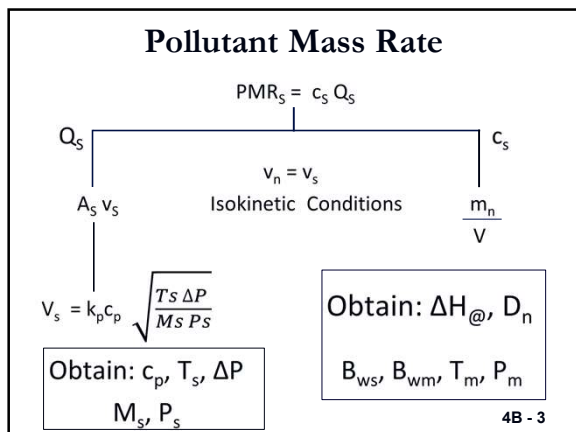
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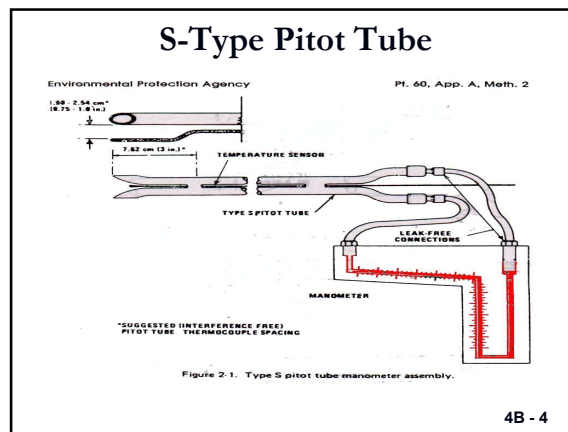
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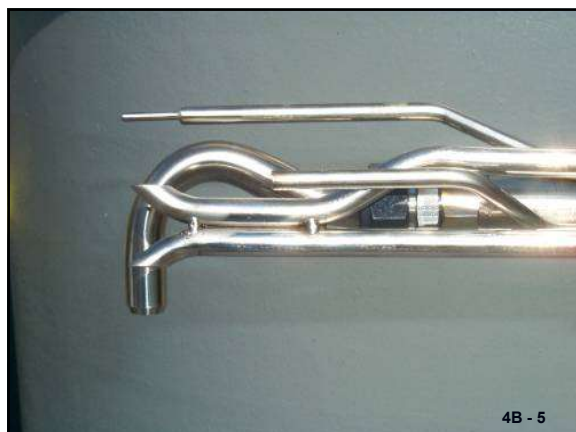
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3



4



5

**FRM 2**

- This method is applicable for measurement of the average velocity of a gas stream
- The average gas velocity in a stack is determined from the gas density and from measurement of the average velocity head with a Type S (Stausscheibe or reverse type) pitot tube

4B - 6

6

### FRM 2 History

- 1970 Promulgation of FRM 2
- 1983 FRM 2A in Small Ducts
- 1983 FRM 2B Stoichiometry Flow
- 1989 FRM 2C Std Pitot Small Ducts
- 1989 FRM 2D Rate Meter
- 1996 FRM 2E Landfills
- 1999 FRM 2F 3-D Yaw/Pitch Angle
- 1999 FRM 2G Type S/3-D
- 1999 FRM 2H Wall Effects

4B - 7

7

### When FRM 2 Cannot be Used

- Failed siting criteria (Minimum of 2/0.5 diameters)
- Duct/stack < 12"
- Cyclonic flow exist at location
  - Install straightening vanes
  - Calculate total volume flow stoichiometry
  - Go to another sampling location

4B - 8

8

### FRM 2 Pitot Tubes

- Each type pitot tube measures an impact and stagnation pressure and combines the measurements to obtain a velocity pressure
- Size of manometer requires:
  - $\Delta p > 0.05$  " water, then 0-10 " manometer adequate
  - $\Delta p < 0.05$  " water, then use manometer with 0.005 /division (i.e., micro-manometer)
  - $\Delta p < 0.01$  "water, then use high sensitivity transducer such as Hasting Thermo Probe

4B - 9

9

### Interference-Free Component Arrangement

- Pitot tube distance to nozzle: >3/4 inches for 1/2 nozzles
- Center of nozzle and pitot tube opening aligned
- Thermocouple location to pitot tube > 3/4 inch for 3 inches
- Back-recess thermo. > 2 inches
- Gas sampling assembly > 3 inches from pitot tube

4B - 10

10

### Type S Pitot Tube

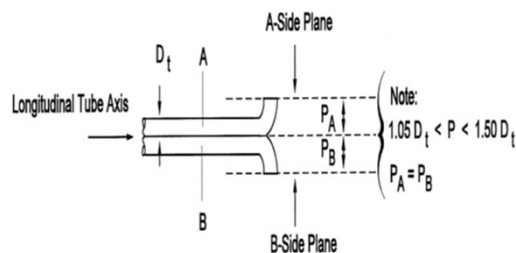
Design criteria for assigning

$$C_p = 0.84$$

4B - 11

11

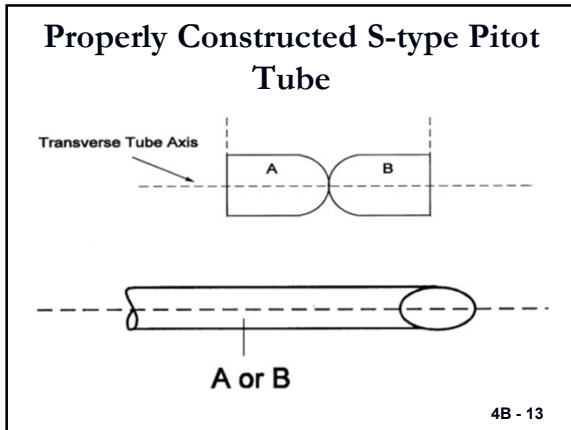
### Properly Constructed S-type Pitot Tube



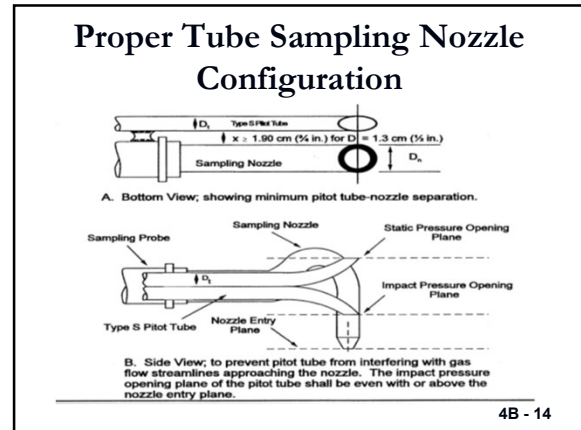
4B - 12

12

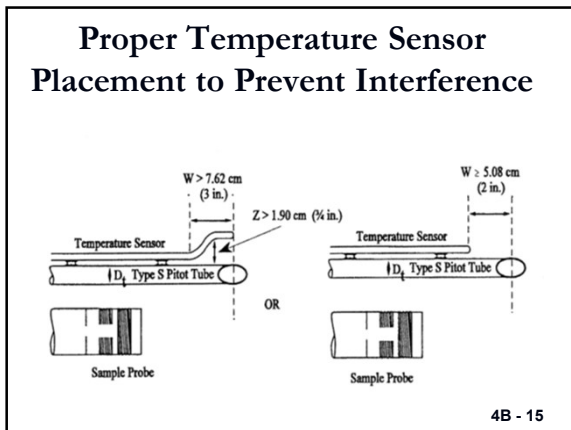




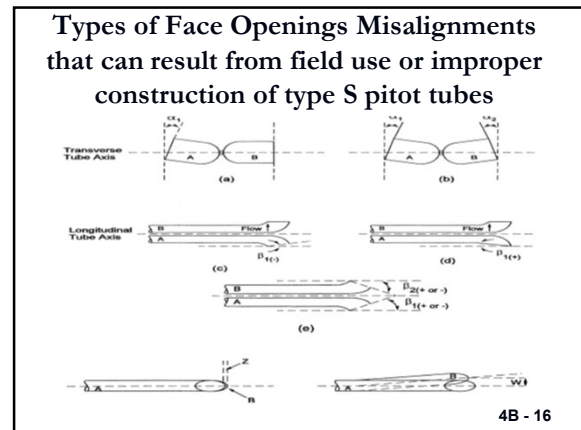
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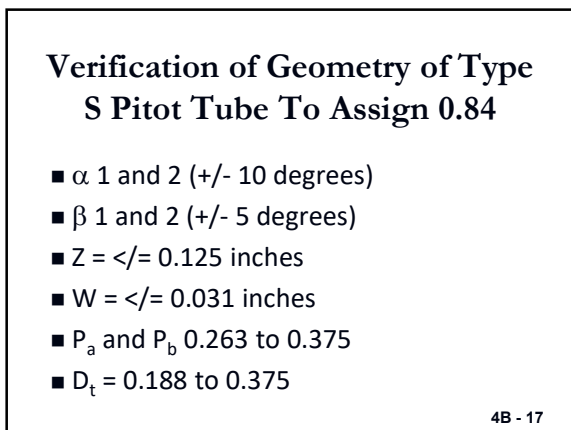
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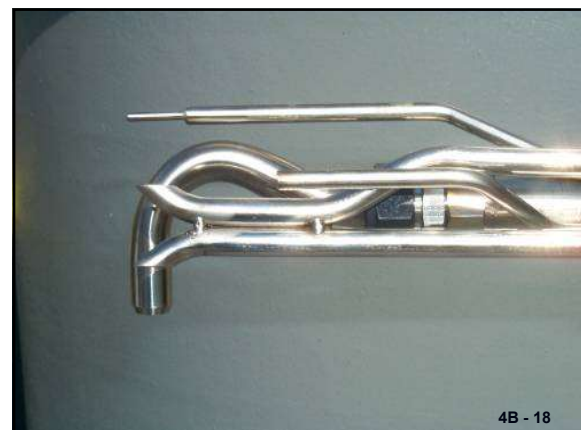
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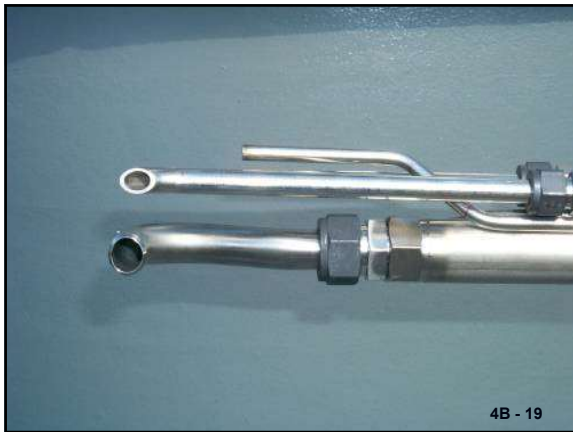
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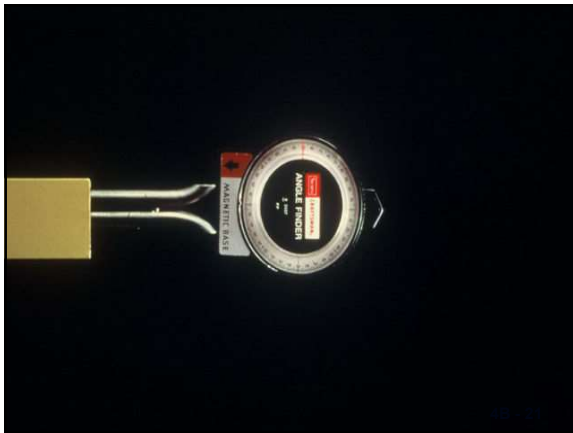
4B - 19

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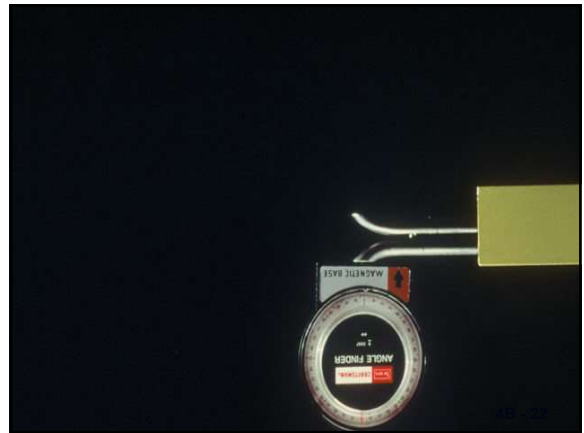


4B - 20

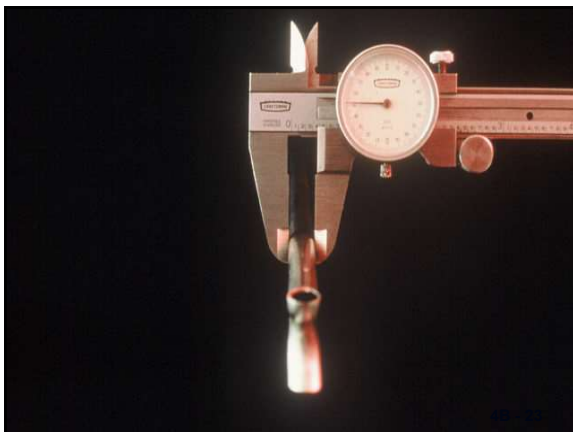
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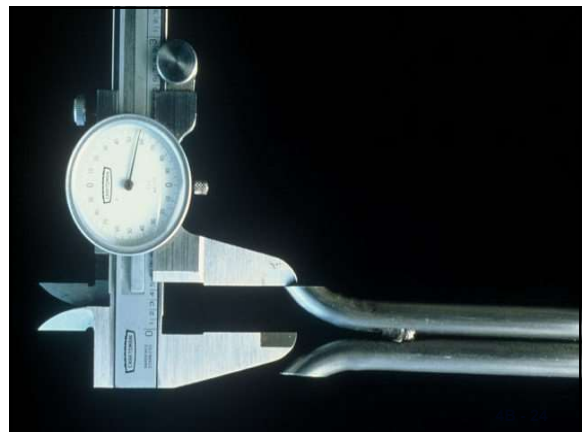
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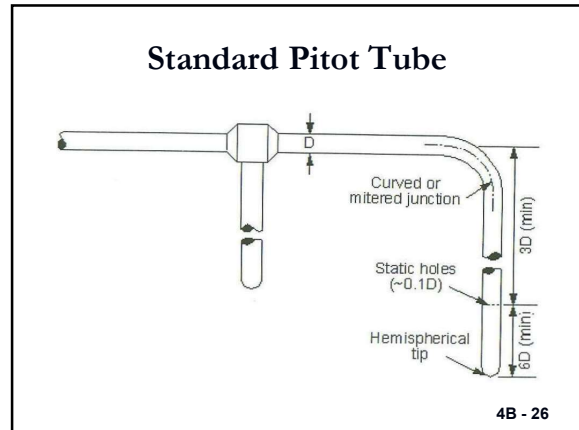


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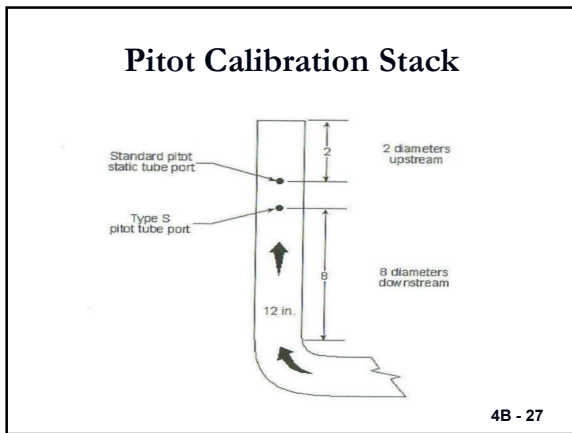
### Type S Pitot Tube Calibrate Using a Standard Pitot Tube and Wind Tunnel

4B - 25

25



26



27

### Pitot Tube Calibration Equation

$$C_{p(s)} = \left[ \frac{\Delta P_{std}}{\Delta P_s} \right]^{1/2} C_{p(std)}$$

3 - 28

28

### Pitot Tube Calibration Data Sheet

PITOT TUBE IDENTIFICATION NUMBER: \_\_\_\_\_ DATE: \_\_\_\_\_  
 CALIBRATED BY: \_\_\_\_\_

\*A\* SIDE CALIBRATION—Continued

Run No.	$\Delta P_{std}$ cm H <sub>2</sub> O (in H <sub>2</sub> O)	$\Delta P_s$ cm H <sub>2</sub> O (in H <sub>2</sub> O)	$C_{p(Std)}$	Deviation $C_{p(s)} - C_{p(A)}$
			$C_{p,avg}$ (SIDE A)	

\*B\* SIDE CALIBRATION

Run No.	$\Delta P_{std}$ cm H <sub>2</sub> O (in H <sub>2</sub> O)	$\Delta P_s$ cm H <sub>2</sub> O (in H <sub>2</sub> O)	$C_{p(Std)}$	Deviation $C_{p(s)} - C_{p(B)}$
1				
2				
3				
			$C_{p,avg}$ (SIDE B)	

$\sigma_{A \text{ or } B} = \frac{\sum_{i=1}^3 |C_{p(i)} - \bar{C}_{p(A \text{ or } B)}|}{3}$  Eq. 2-5

(C<sub>p, avg</sub> (side A)) - (C<sub>p, avg</sub> (side B))  
 \*Must be less than or equal to 0.01

Figure 2-9. Pitot Tube Calibration Data

4B - 29

29

- ### Velocity Measurement Procedures
1. Leak-check pitot tube and differential pressure gauge.
  2. For circular stacks less than 10 ft in diameter, two ports are sufficient. Use four ports when stack diameter is greater than 10 ft.
  3. Pitot tubes longer than 10 ft should be structurally reinforced to prevent bending of tube and misalignment errors.
  4. Identify each sample port and traverse point with a letter or number.
  5. Read velocity head and temperature at least twice at each point and record the average.
- 4B - 30

30

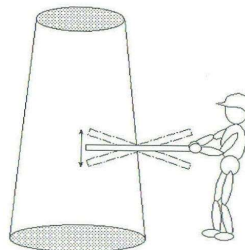
**Velocity Measurement Procedures**(cont.)

6. Care should be taken to prevent touching the pitot tube tip to the side of the stack.
7. Plug unused sampling ports and seal port being used as tightly as possible.
8. After traverse, check differential pressure gauge; repeat traverse if zero has shifted.
9. If liquid droplets are present, use a liquid trap in positive pressure leg of pitot tube.
10. A post-test leak check is required after each run of the pitot tube and velocity pressure system.

4B - 31

31

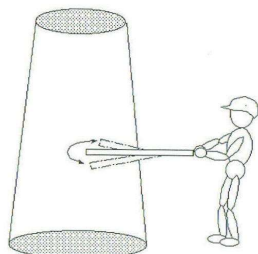
**Pitch Angle**



4B - 32

32

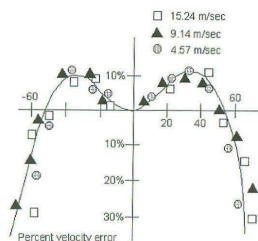
**Yaw Angle**



4B - 33

33

**Velocity Error vs. Yaw Angle  
For a Type S Pitot Tube**



4B - 34

34

**Federal Reference Method 2  
Average Velocity Over Cross-Section  
Area of Stack**

$$\bar{v}_s = K_p C_p (\sqrt{\Delta p})_{avg} \sqrt{\frac{T_{s(avg)}}{M_s P_s}}$$

4B - 35

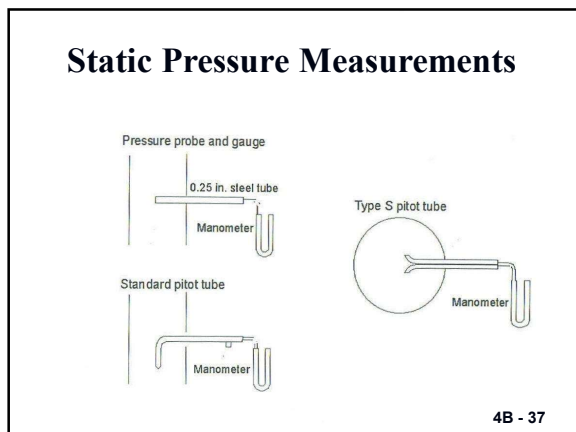
35

**Average Stack Gas Dry  
Volumetric Flow Rate**

$$Q_{std} = 3600 (1 - B_{ws(avg)}) v_{s(avg)} A \frac{T_{std}}{T_{s(avg)}} \frac{P_s}{P_{std}}$$

4B - 36

36



37

### Stack Pressure ( $P_s$ )

$$P_s = P_b + \frac{P_g}{13.6}$$

4B - 38

38

- ### Barometric Pressure
- Barometric pressure during testing is obtained by:
- Instrument:
- Mercury, aneroid or other barometer (with required sensitivity)
  - Other
  - Obtain barometric pressure from nearby National Weather Service station (station pressure) and adjust for elevation differences between sampling site and weather station.
- 4B - 39

39

- ### Pressure Probe and Gauge
- Static pressure measurement must be accurate to within 1 in. Hg (13.6 in. H<sub>2</sub>O).
- Pressure sensors typically used to measure static pressure during testing include:
- A piezometer tube and mercury or water-filled U-tube manometer
  - The static tap of a pitot tube
  - One leg of the Type S pitot tube
- 4B - 40

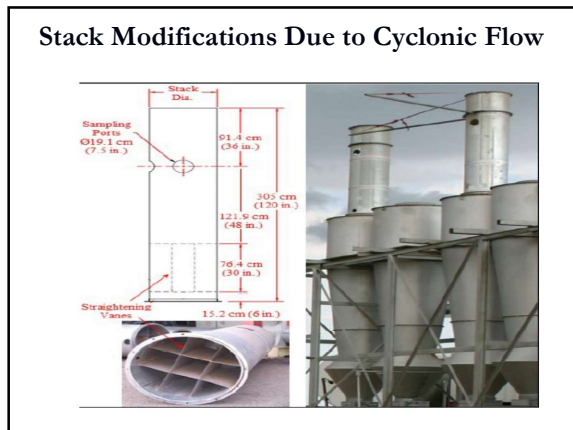
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- ### Applicability
- Method 2 is applicable only at sites that:
- Meet the criteria of Method 1
  - Do not contain cyclonic or non-parallel flow
- 4B - 41

41

- ### Alternatives When Unacceptable Conditions Exist
- (Subject to approval of the Administrator)
- Install straightening vanes.
  - Calculate total volumetric flow rate stoichiometrically.
  - Move to a measurement site at which flow is acceptable.
  - Use procedures as described in Method 2 for cyclonic flow.
- 4B - 42

42



43

**Type S Pitot Tube Inspection Data Sheet**

- With the S-Type pitot tube, determine whether it meets the design specifications to be able to assign a  $C_p$  of 0.84
- $C_p$  may be determined in conjunction with standard pitot tube
- Identification number scribed on pitot tube

4B - 44

44

**FRM 2 Velocity Equation**

$$v_s = K_p C_p \left( \sqrt{\Delta p} \right)_{avg} \sqrt{\frac{T_{s(avg)}}{P_s M_s}}$$

4B - 45

45

**FRM 2 Inspector Tools For Testing Observation**

- Level indicator
- Modular pitot tube
- Hand-held manometer
- Pocket barometer
- Hand-held digital thermometer and thermocouples

4B - 46

46

**FRM 2 Inspector Tools For Testing Observation**

- Bull's eye level
- Field observation agency checklist
- Stack sampling nomographs for field estimations
- 3-D pitot tube

4B - 47

47

**Major Points in FRM 2**

- 0-10 in. manometer for  $> 0.05 \Delta p$
- $< 0.05 \Delta p$ , use 0.005 in. divisions
- Thermocouple and magnehelic calibration required
- Type S pitot tube: configuration, calibration, and leak check

4B - 48

48

### Major Points in FRM 2

- FRM 2 not applicable at sites not meeting FRM 1 (Sec. 1.2)
- FRM 2 cannot be used in cyclonic or swirling flow (Sec. 1.2)
- Alternative guidance
  - install straightening vanes
  - calculate flow stoichiometrically
  - select another location (Sec. 11.5)

4B - 49

49

### Major Points in FRM 2

- Type S pitot tube should have a known coefficient (Sec. 2.1)
- Ident. # on pitot tube (Sec. 2.1)
- Acceptable design specifications allow  $C_p$  of 0.84 (Sec. 2.1)
- Standard pitot may be used, but must demonstrate not plugged during use (Sec. 2.1)

4B - 50

50

### Major Points in FRM 2

- Design specification of Type S pitot tube (Fig. 2-3)
- Manometer specifications of 0-10 in. for  $>0.05 \Delta p$  (Sec. 2.2)
- Provides guidance on use of more sensitive gauge (Sec. 2.2)
- Provides calibration of magnehelic gauge (Sec. 2.2)

4B - 51

51

### Major Points in FRM 2

- FRM 2 provides guidance on adjustment of barometric pressure with altitude (Sec. 2.5)
- Need to take static pressure measurement only once during the test (Sec. 3.4)
- Must verify the face opening alignment, measure and record (Sec. 4.1)

4B - 52

52

### Major Points in FRM 2

- Guidance with Type S pitot tube in association to probe/nozzle/thermocouple placement (Sec. 4.1)
- Calibrate against standard pitot tube at 3,000 ft/min (Sec. 4.1.2.3)

4B - 53

53

### Major Points in FRM 2

- Must leak check all pitot lines (Sec. 4.1.3.1)
- May calibrate Type S pitot tube at source (Sec. 4.1.5.1.1)

4B - 54

54

### Major Points in FRM 2

- Must verify that probe sheath interference is < 2% of area of stack (Sec. 4.1.5.1.3)
- May use of  $C_p$  for Side A or B or may average (Sec. 4.1.6.1.1)

4B - 55

55

### Dismiss Stack Test FRM 2

- Pitot tube leak check at 3 " water failed
- Pitot tube geometry not to specifications
- Pitot tube orientation during test not proper

4B - 56

56

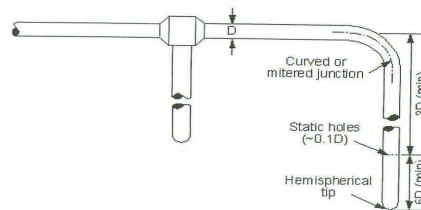
### Use of Standard Type Pitot Tube

- Alternatively, a standard pitot tube designed according to the criteria given in Sections 6.7.1 through 6.7.5 below and illustrated in Figure 2–5. Pitot tubes designed according to these specifications will have baseline coefficients of  $0.99 \pm 0.01$ .

4B - 57

57

### Standard Type Pitot Tube



4B - 58

58

### Use of Standard Type Pitot Tube

#### Standard Pitot Design:

**Hemispherical (shown in previous figure, ellipsoidal, or conical tip.**

**A minimum of six diameters straight run (based upon D, the external diameter of the tube) between the tip and the static pressure holes.**

4B - 59

59

### Use of Standard Type Pitot Tube

- **Field Use.**
- **When a Type S pitot tube (isolated or in an assembly) is used in the field, the appropriate coefficient value (whether assigned or obtained by calibration) shall be used to perform velocity calculations. For calibrated Type S pitot tubes, the A side coefficient shall be used when the A side of the tube faces the flow, and the B side coefficient shall be used when the B side faces the flow. Alternatively, the arithmetic average of the A and B side coefficient values may be used,irrespective of which side faces the flow.**

4B - 60

60



### Use of Standard Type Pitot Tube

Standard Pitot Tube (if applicable). If a standard pitot tube is used for the velocity traverse, the tube shall be constructed according to the criteria of Section 6.7 and shall be assigned a baseline coefficient value of 0.99. If the standard pitot tube is used as part of an assembly, the tube shall be in an interference-free arrangement (subject to the approval of the Administrator).

4B - 61

61

### Data Analysis and Calculations:

Carry out calculations, retaining at least one extra significant figure beyond that of the acquired data. Round off figures after final calculation.

4B - 62

62

12.2 Calculate T as follows:

$$T = \frac{\sum_{i=1}^n \sqrt{\Delta p_i + K}}{\sum_{i=1}^n \sqrt{\Delta p_i}} \quad \text{Eq. 2-1}$$

4B - 63

63

### METHOD 2A—DIRECT MEASUREMENT OF GAS VOLUME THROUGH PIPES AND SMALL DUCTS

4B - 64

64

### METHOD 2A

- This method is applicable for the determination of gas flow rates in pipes and small ducts, either in-line or at exhaust positions, within the temperature range of 0 to 50 °C (32 to 122 °F).
- A gas volume meter is used to measure gas volume directly. Temperature and pressure measurements are made to allow correction of the volume to standard conditions.

4B - 65

65

### METHOD 2A

- Gas Volume Meter. A positive displacement meter, turbine meter, or other direct measuring device capable of measuring volume to within 2 percent.
- The meter shall be equipped with a temperature sensor (accurate to within ±2 percent of the minimum absolute temperature) and a pressure gauge (accurate to within ±2.5 mm Hg).
- The manufacturer's recommended capacity of the meter shall be sufficient for the expected maximum and minimum flow rates for the sampling conditions. Temperature, pressure, corrosive characteristics, and pipe size are factors necessary to consider in selecting a suitable gas meter.

4B - 66

66

**METHOD 2A**

- The volume meter is calibrated against a standard reference meter prior to its initial use in the field. The reference meter is a spirometer or liquid displacement meter with a capacity consistent with that of the test meter.
- Alternatively, a calibrated, standard pitot may be used as the reference meter in conjunction with a wind tunnel assembly. Attach the test meter to the wind tunnel so that the total flow passes through the test meter.

4B - 67

67

**Method 2A**



4B - 68

68

**Method 2A Test Meter Calibration Coefficient.**

$$Y_m = \frac{(V_{r_f} - V_{r_i}) P_b T_{r(abs)}}{(V_{m_f} - V_{m_i}) (P_b + P_g) T_{m(abs)}} \quad \text{Eq. 2A-1}$$

4B - 69

69

$$Y_{m_s} = Y_m \left[ \frac{(P_{bar} + P_g)(V_{m_f} - V_{m_i})(293 \text{ }^\circ\text{K})}{(T_m)(760 \text{ mmHg})} \right] \quad \text{Eq. 2-2}$$

4B - 70

70

**Method 2A Gas Flow Rate Equation**

$$Q_s = \frac{V_{m_s}}{\theta} \quad \text{Eq. 2A-3}$$

4B - 71

71

**METHOD 2B—DETERMINATION OF  
EXHAUST GAS  
VOLUME FLOW RATE FROM  
GASOLINE VAPOR  
INCINERATORS**

4B - 72

72

**METHOD 2B**

- This method is applicable for the determination of exhaust volume flow rate from incinerators that process gasoline vapors consisting primarily of alkanes, alkenes, and/or arenes (aromatic hydrocarbons). It is assumed that the amount of auxiliary fuel is negligible.

4B - 73

73

**Method 2B**

**Summary of Method**

- Organic carbon concentration and volume flow rate are measured at the incinerator inlet using either Method 25A or Method 25B and Method 2A, respectively.
- Organic carbon, carbon dioxide (CO<sub>2</sub>), and carbon monoxide (CO) concentrations are measured at the outlet using either Method 25A or Method 25B and Method 10, respectively.
- The ratio of total carbon at the incinerator inlet and outlet is multiplied by the inlet volume to determine the exhaust volume flow rate.

4B - 74

74

**Method 2B**

**Equipment and Supplies**

- Same as Section 6.0 of Method 2A, Method 10, and Method 25A and/or Method 25B as applicable.
- In addition, the analyzer must meet the specifications set forth in Section 6.1.2 of Method 10, except that the span shall be 15 percent CO<sub>2</sub>

4B - 75

75

**Method 2B Exhaust Gas Volume Equation**

$$V_{es} = V_{is} \frac{K_i(HC_i)}{K_e(HC_e) + [(CO_2)_e - (CO_2)_a] + CO_e} \quad \text{Eq. 2B-1}$$

4B - 76

76

**Method 2B Exhaust Gas Volume Flow Rate Equation**

$$Q_{es} = \frac{V_{es}}{\theta} \quad \text{Eq. 2B-2}$$

4B - 77

77

**METHOD 2C—DETERMINATION OF GAS VELOCITY AND VOLUMETRIC FLOW RATE IN SMALL STACKS OR DUCTS (STANDARD PITOT TUBE)**

4B - 78

78

*1.0 Scope and Application*

1.1 This method is applicable for the determination of average velocity and volumetric flow rate of gas streams in small stacks or ducts. Limits on the applicability of this method are identical to those set forth in Method 2, Section 1.0, except that this method is limited to stationary source stacks or ducts less than about 0.30 meter (12 in.) in diameter, or 0.071 m<sup>2</sup> (113 in.<sup>2</sup>) in cross-sectional area, but equal to or greater than about 0.10 meter (4 in.) in diameter, or 0.0081 m<sup>2</sup> (12.57 in.<sup>2</sup>) in cross-sectional area.

4B-79

79

**METHOD 2C**

6.1 Standard Pitot Tube (instead of Type S). A standard pitot tube which meets the specifications of Section 6.7 of Method 2. Use a coefficient of 0.99 unless it is calibrated against another standard pitot tube with a NIST-traceable coefficient (see Section 10.2 of Method 2).

4B - 80

80

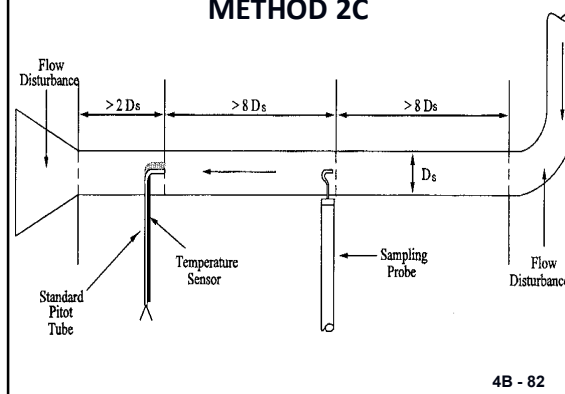
**METHOD 2C**

6.1 Standard Pitot Tube (instead of Type S). A standard pitot tube which meets the specifications of Section 6.7 of Method 2. Use a coefficient of 0.99 unless it is calibrated against another standard pitot tube with a NIST-traceable coefficient (see Section 10.2 of Method 2).

4B - 81

81

**METHOD 2C**



4B - 82

82

6.2 Alternative Pitot Tube. A modified hemispherical-nosed pitot tube (see Figure 2C-1), which features a shortened stem and enlarged impact and static pressure holes. Use a coefficient of 0.99 unless it is calibrated as mentioned in Section 6.1 above. This pitot tube is useful in particulate liquid droplet-laden gas streams when a "back purge" is ineffective.

4B - 83

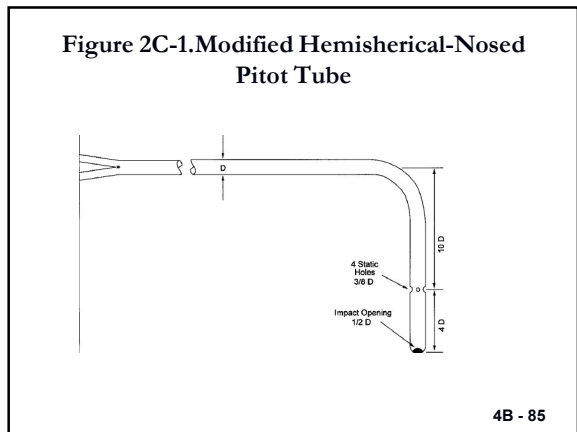
83

**Method 2C**

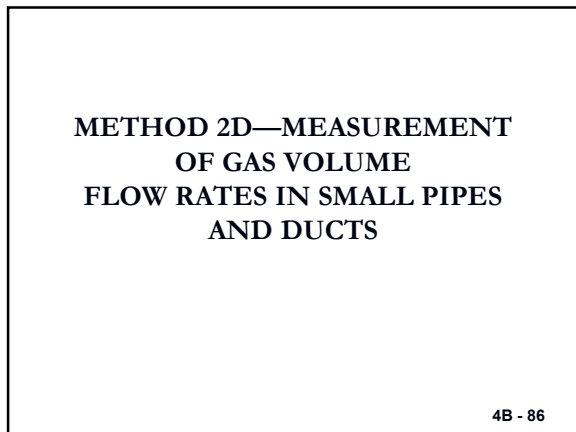
8.1 Follow the general procedures in Section 8.0 of Method 2, except conduct the measurements at the traverse points specified in Method 1A. The static and impact pressure holes of standard pitot tubes are susceptible to plugging in particulate-laden gas streams. Therefore, adequate proof that the openings of the pitot tube have not plugged during the traverse period must be furnished;

4B - 84

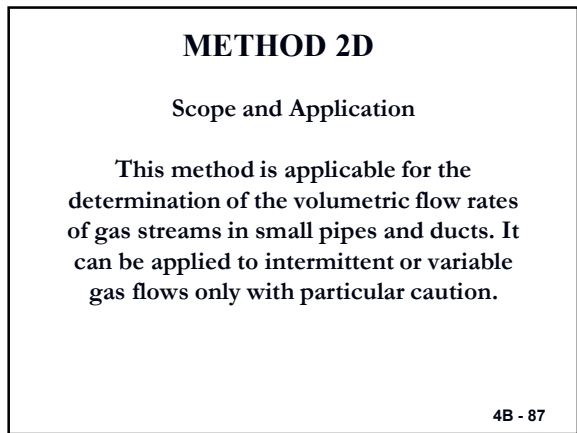
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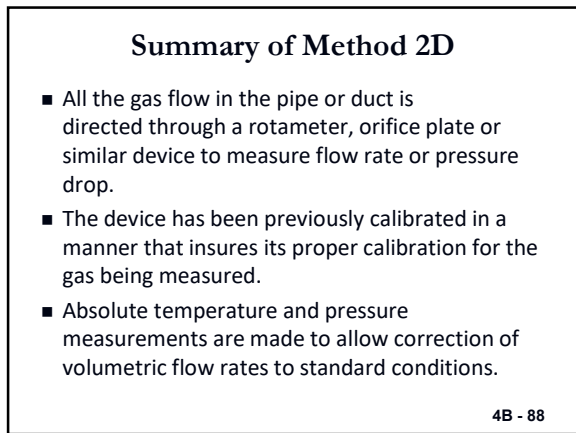
85



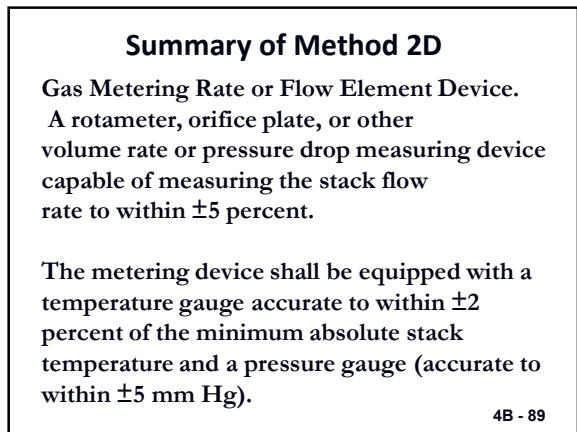
86



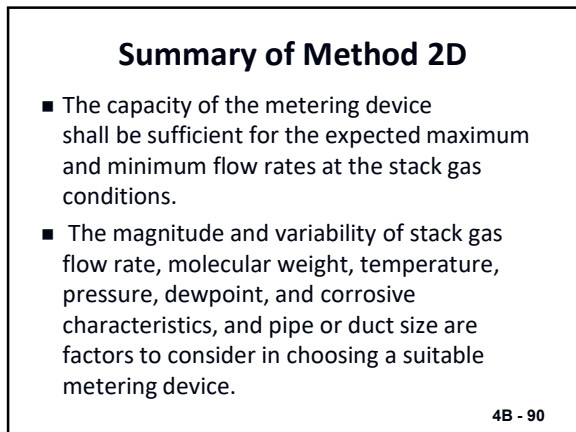
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88



89



90

**Method 2D Gas Flow Rate Equation**

$$Q_s = K_1 Y_m Q_m \frac{(P_{bar} + P_m)}{T_m} \quad \text{Eq. 2D-1}$$

4B - 91

91

Method 2D Test Meter Device Calibration Coefficient. Calculation for testing metering device calibration coefficient,  $Y_m$ .

$$Y_m = \frac{Q_r T_r P_{bar}}{Q_m T_m (P_{bar} + P_m)} \quad \text{Eq. 2D-2}$$

4B - 92

92

**METHOD 2E—DETERMINATION OF  
LANDFILL  
GAS PRODUCTION FLOW RATE**

4B - 93

93

**Method 2E**

- Applicability. This method applies to the measurement of landfill gas (LFG) production flow rate from municipal solid waste landfills and is used to calculate the flow rate of nonmethane organic compounds (NMOC) from landfills.
- Also applies to calculating a site-specific “k” value for waste decay.

4B - 94

94

**Summary of Method 2E**

- Extraction wells are installed either in a cluster of three or at five dispersed locations in the landfill.
- A blower is used to extract LFG from the landfill. LFG composition, landfill pressures, and orifice pressure differentials from the wells are measured and the landfill gas production flow rate is calculated.

4B - 95

95

**Method 2E**

**Equipment and Supplies**

- Well Drilling Rig. Capable of boring a 0.61 m (24 in.) diameter hole into the landfill to a minimum of 75 percent of the landfill depth.
- The depth of the well shall not extend to the bottom of the landfill or the liquid level. Gravel diameter should be appreciably larger than perforations and have a Bentonite seal
- Backfill Material. Clay, soil, and sandy loam have been found to be acceptable.

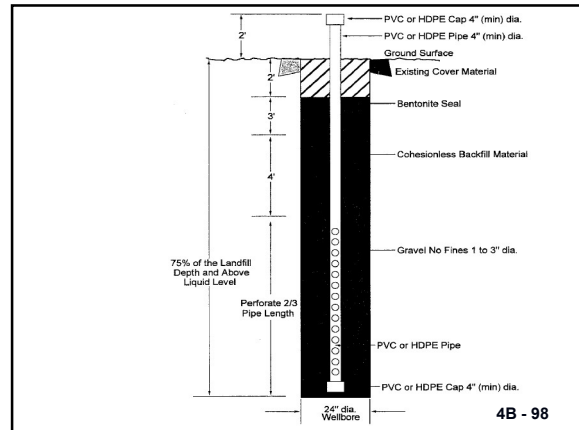
4B - 96

96



4B - 97

97



4B - 98

98

### Method 2E

- Extraction Well Pipe. Minimum diameter of 3 in., constructed of polyvinyl chloride (PVC), high density polyethylene (HDPE), fiberglass, stainless steel, or other suitable nonporous material capable of transporting landfill gas.

4B - 99

99



4B - 100

100



4B - 101

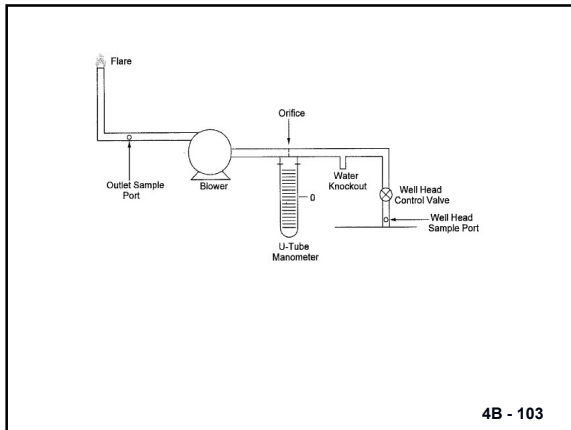
101

### Method 2E

- Above Ground Well Assembly. Valve capable of adjusting gas flow, such as a gate, ball, or butterfly valve; sampling ports at the well head and outlet; and a flow measuring device, such as an in-line orifice meter or pitot tube.

4B - 102

102



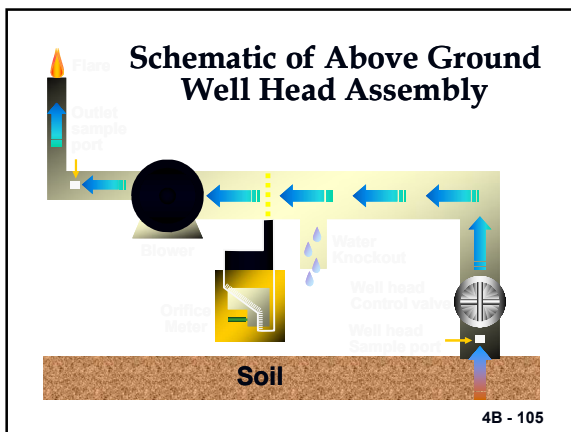
4B - 103

103



4B - 104

104



4B - 105

105

### Method 2E

- The landfill owner or operator may install a single cluster of three extraction wells in a test area or space five equal-volume wells over the landfill.
- The cluster wells are recommended, but may be used only if the composition, age of the refuse, and the landfill depth of the test area can be determined

4B - 106

106

### Method 2E

#### Calibration and Standardization

- For LFG Flow Rate Meter (Orifice) Calibration Procedure, locate a standard pitot tube in line with an orifice meter.
- Use the procedures in Method 2 to determine the average dry gas volumetric flow rate for at least five flow rates that bracket the expected LFG flow rates, except in Section 8.1, use a standard pitot tube rather than a Type S pitot tube.

4B - 107

107



4B - 108

108



### FRMs 2F, 2G, and 2H Newer Flow Test Methods

- Method 2F: calculates axial velocity (3-D Probes)
- Method 2G: calculates “near-axial” velocity (Type S or 3-D probes)
- Method 2H: Wall effects (Type S or 3-D probes or default wall effects adjustment factor)

4B - 109

109

### METHOD 2F—DETERMINATION OF STACK GAS VELOCITY AND VOLUMETRIC FLOW RATE WITH THREE-DIMENSIONAL PROBES

4B - 110

110

### Method 2F

- This method is applicable for the determination of yaw angle, pitch angle, axial velocity and the volumetric flow rate of a gas stream in a stack or duct using a three-dimensional (3-D) probe.
- This method may be used only when the average stack or duct gas velocity is greater than or equal to 20 ft/sec.
- When the above condition cannot be met, alternative procedures, approved by the Administrator shall be used to make accurate flow rate determinations.

4B - 111

111

### Method 2F

#### Summary of Method

- A 3-D probe is used to determine the velocity pressure and the yaw and pitch angles of the flow velocity vector in a stack or duct.
- The method determines the yaw angle directly by rotating the probe to null the pressure across a pair of symmetrically placed ports on the probe head.
- The pitch angle is calculated using probe-specific calibration curves.

4B - 112

112

### Method 2F

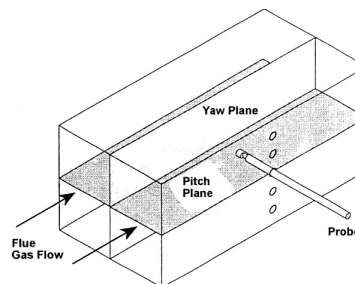
#### Summary of Method (continued)

- From these values and a determination of the stack gas density, the average axial velocity of the stack gas is calculated.
- The average gas volumetric flow rate in the stack or duct is then determined from the average axial velocity.

4B - 113

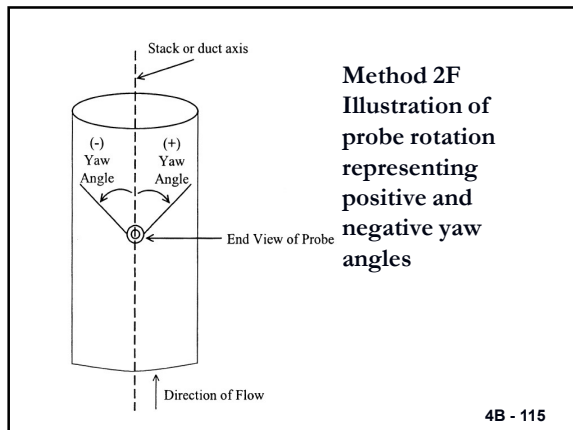
113

### Method 2F Illustration of yaw and pitch planes in stack or duct



4B - 114

114



115

**METHOD 2G—DETERMINATION OF STACK GAS VELOCITY AND VOLUMETRIC FLOW RATE WITH TWO-DIMENSIONAL PROBES**

4B - 116

116

**Method 2G**

**Scope and Application**

- This method is applicable for the determination of yaw angle, near-axial velocity, and the volumetric flow rate of a gas stream in a stack or duct using a two-dimensional (2-D) probe.

4B - 117

117

**Method 2G**

**Summary of Method**

- A 2-D probe is used to measure the velocity pressure and the yaw angle of the flow velocity vector in a stack or duct.
- Alternatively, these measurements may be made by operating one of the three-dimensional (3-D) probes described in Method 2F, in yaw determination mode only.
- From these measurements and a determination of the stack gas density, the average near-axial velocity of the stack gas is calculated.

4B - 118

118

**Method 2G**

**Summary of Method (continued)**

- The near-axial velocity accounts for the yaw, but not the pitch, component of flow.
- The average gas volumetric flow rate in the stack or duct is then determined from the average near-axial velocity.

4B - 119

119

**METHOD 2H—DETERMINATION OF STACK GAS VELOCITY TAKING INTO ACCOUNT VELOCITY DECAY NEAR THE STACK WALL**

4B - 120

120

### Method 2H

#### Scope and Application

- This method is applicable in conjunction with Methods 2, 2F, and 2G (40 CFR Part 60, Appendix A) to account for velocity decay near the wall in circular stacks and ducts.
- This method is not applicable for testing stacks and ducts less than 3.3 ft (1.0 m) in diameter.

4B - 121

121

### Method 2H

#### Summary of Method

- A wall effects adjustment factor is determined.
- It is used to adjust the averagestack gas velocity obtained under Method 2, 2F, or 2G of this appendix, to take into account velocity decay near the stack or duct wall.

4B - 122

122

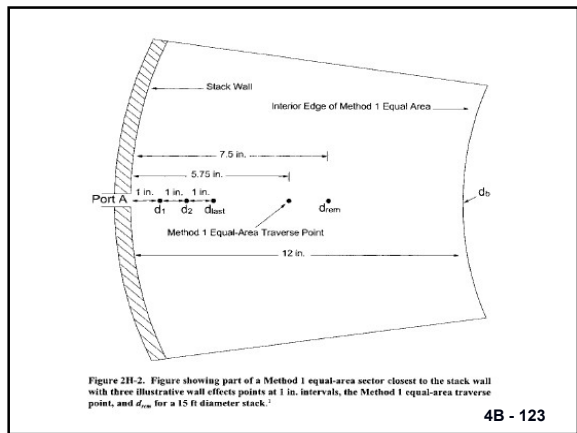


Figure 2H-2. Figure showing part of a Method 1 equal-area sector closest to the stack wall with three illustrative wall effects points at 1 in. intervals, the Method 1 equal-area traverse point, and  $d_{0m}$  for a 15 ft diameter stack.

4B - 123

123

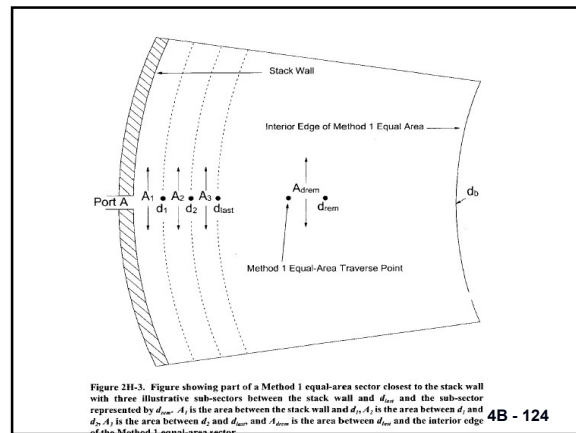


Figure 2H-3. Figure showing part of a Method 1 equal-area sector closest to the stack wall with three illustrative sub-sectors between the stack wall and  $d_{0m}$  and the sub-sector represented by  $d_{0m}$ .  $A_1$  is the area between the stack wall and  $d_1$ ,  $A_2$  is the area between  $d_1$  and  $d_2$ ,  $A_3$  is the area between  $d_2$  and  $d_{0m}$ , and  $A_{rem}$  is the area between  $d_{0m}$  and the interior edge of the Method 1 equal-area sector.

4B - 124

124

4B-125

1. Diameter of the stack or duct (D) = 24 Radius, r, of the stack or duct (in (1/2 diameter × D)) = 144  
 2. Location of center A<sub>1</sub>, measured and along velocities between B<sub>1</sub> and C<sub>1</sub>, and volumetric flow (Column G)  
 associated with each successive wall effects traverse point.

(A)	(B)	(C)	(D)	(E)	(F)	(G)
Distance (ft) from Wall	Measured Velocity (ft/min)	Distance (ft)	Intermediate Calculations	Area A <sub>i</sub>	Volumetric Flow in Sub-sector (G <sub>i</sub> )	
			$\frac{V_i + V_{i+1}}{2}$ None $V_i = 0$	$\frac{1}{2}A_i(d_i + d_{i+1})$	$\frac{1}{2}A_i V_i$	(Col. D × Col. E) (Col. C × Col. F)
0						
1	91.71 MW	20.85	76.286 05	18.960 59	225.41	0.287 47
2	91.71 MW	41.71	140.965 05	18.960 59	225.41	11.452 52
3	71.71	57.71	163.36 78	18.944 49	222.27	17.432 51
4	62.29	68.30	178.14 49	18.262 79	209.70	22.576 24
5	62.76	68.71	178.63 78	18.174 61	218.13	24.729 46
6	60.44	68.30	181.74 67	14.927 71	217.56	14.938 30
7	72.63	71.03	143.67 71	14.941 13	219.98	16.361 75
8	71.37	72.00	147.41 13	14.505 71	214.41	15.437 51
9	74.37	72.87	143.26 71	14.313 87	212.84	15.101 00
10	73.80	76.08	142.93 87	14.163 08	211.27	15.003 36
11	77.15	76.47	141.02 80	13.822 80	209.70	16.036 59
12	78.68	77.86	138.62 80	13.684 77	208.13	16.258 92
						184.037 08

4. Volumetric flow for remainder of the Method 1 equal-area sector: 175.430 64  
 a. Velocity measured in distance  $d_{0m}$  from stack wall ( $V_{0m}$ ) (24 ft) = 78.51  
 b. Total area in remainder of Method 1 equal-area segment ( $A_{rem}$ ). Subtract: 1.470 26  
 c. Multiply values on lines 4a and 4b. ( $G_{0m}$ ) 175.430 64  
 5. Wall effects adjustment velocity for the Method 1 equal-area sector: 205.522 02  
 a. Add the values on lines 3 and 4c. ( $G_0$ ) 205.522 02  
 b. Divide line 5a by  $\frac{1}{2}A_{rem}$ . The resulting value is one of four "replacement" point velocity values adjusted for wall effects,  $V_{0m}$ , as derived in Equation 2H-16. 68.85  
 6. Substitute the value shown in 5b for the unadjusted velocity value in the Method 1 sector. (See Eq. 2H-17)

4B - 125

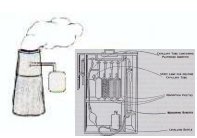
125

U.S. EPA APTI  
Compliance Test and  
Source Test Observation

Stack Test Basic Continued

**Method 3**

Determination of the dry molecular weight of flue gas  
(using Orsat apparatus measuring %O<sub>2</sub>, %CO<sub>2</sub>, and %CO)



5A - 1

1

**POLLUTANT MASS RATE**

$$\overline{PMR}_s = \bar{c}_s \bar{Q}_s$$

$$v_s = v_n \text{ for Isokinetic Conditions}$$

$$v_s = K_p C_p \sqrt{\frac{T_s \Delta p}{M_s P_s}}$$

Obtain  $C_p, T_s, \Delta p$   
 $M_s, P_s$

Obtain  $\Delta H_{@}, D_n$   
 $B_{ws}, B_{wm},$   
 $P_m, T_m$

5A - 2

2

Federal Reference  
Method 3 History

- 1970FRM 3 Promulgated
- 1986FRM 3A Instrumental
- 1990FRM 3B Orsat for Correction Factor and Excess Air ( $F_o$  - Factor)
- 1996FRM 3C Landfill Gas

5A - 3

3

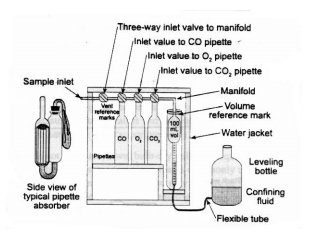
Federal Reference  
Method 3

- Gas analysis: measuring percent of O<sub>2</sub> and percent of CO<sub>2</sub> to determine the dry molecular weight of the flue gas (using Orsat Apparatus)

5A - 4

4

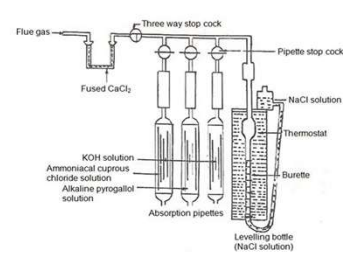
Orsat Analyser



5A - 5

5

Orsat Analyser



5A - 6

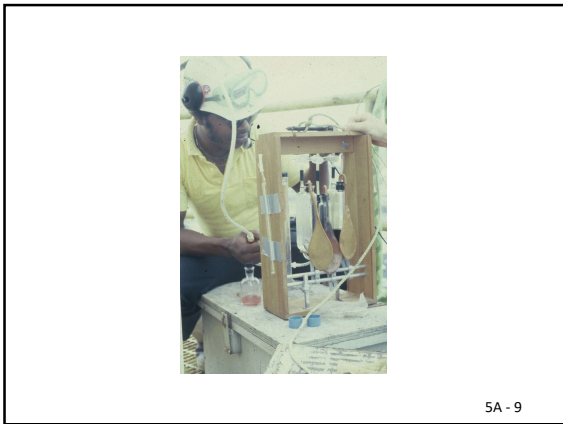
6



7



8



9



10



11

FRM 3 Sampling Techniques

- Single point grab sample
- Single point integrated sample
- Integrated multi-point sample

5A - 12

12

### Single-Point Grab Sampling Train

**Figure 3-1. Grab-Sampling Train.**

5A - 13

13

### Single-Point Integrated Sampling Train

**Figure 3-2. Integrated Gas-Sampling Train.**

5A - 14

14

### Multi-point Integrated Sampling Train

**Multi-Point Integrated Sampling**

5A - 15

15

### Multi-Point Continuous Integrated Sampling

- Particulate sample and variations
- Modified Method 5 sampling
- VOST sampling
- For concentrations given to specific conditions (i.e., 12 % CO<sub>2</sub>, 6 % O<sub>2</sub>)
- For emission rate calculations (F-factor)
- For molecular weight determination

5A - 16

16

### FRM 3 Calculation

**Dry Molecular Weight Equation**

$$M_d = 0.44(\%CO_2) + 0.32(\%O_2) + 0.28(\%N_2 + \%CO)$$

Where:  $M_d$  = dry molecular weight  
 %CO<sub>2</sub> = percent CO<sub>2</sub> by volume (dry basis)  
 %O<sub>2</sub> = percent O<sub>2</sub> by volume (dry basis)  
 %CO = percent CO by volume (dry basis)  
 %N<sub>2</sub> = percent N<sub>2</sub> by volume (dry basis)  
 0.44 = molecular weight of CO<sub>2</sub> divided by 100  
 0.32 = molecular weight of O<sub>2</sub> divided by 100  
 0.28 = molecular weight of N<sub>2</sub> divided by 100  
 0.28 = molecular weight of CO divided by 100

5A - 17

17

### Method 3 Data Uses

- Calculate molecular weight of the stack gas
- Emission rate correction
  - FRM 20 contains the equation to correct an emission rate to a % O<sub>2</sub> or % CO<sub>2</sub>

$$C_{adj} = C_d \left[ \frac{(20.9 - \%O_{2corr})}{(20.9 - \%O_{2meas})} \right]$$

5A - 18

18

### Method 3 Data Uses

- Emission rate calculation
  - FRM 19 contains the equation to determine a heat input based emission concentration

$$E = C_d F_d \left[ \frac{20.9}{(20.9 - \%O_{2dry})} \right]$$

5A - 19

19

### Problems with FRM 3

- Leak in pump or bag
- Process gives off CO<sub>2</sub> or O<sub>2</sub>
  - Cement plant- Cannot validate F<sub>o</sub>
  - FGD scrubber- Cannot validate F<sub>o</sub>
- Incomplete combustion cannot validate F<sub>o</sub>- Too low for fuel
- Processes removing CO<sub>2</sub> or O<sub>2</sub>

5A - 20

20

### FRM 3B Equations

*Fuel Factor*

$$F_o = \frac{(20.9 - O_2)}{CO_2}$$

*Excess Air*

$$\%EA = \frac{(\%O_2 - 0.5\%CO)}{(0.264\%N_2 - (\%O_2 - 0.5\%CO))}$$

5A - 21

21

### FRM 3B F<sub>o</sub> Factors

Coal: Anthracite	1.016-1.130
Coal: Bituminous	1.083-1.230
Oil: Distillate	1.260-1.413
Oil: Residual	1.210-1.370
Gas: Natural	1.600-1.836
Gas: Propane	1.434-1.586
Gas: Butane	1.405-1.553
Wood	1.000-1.120
Wood Bark	1.003-1.130

5A - 22

22

### FRM 3 Major Points

- Applicability (Sec. 1.2)
- Method modifications (Sec. 1.2)
  - A multi-point sampling method/ Orsat at each point
  - Using CO<sub>2</sub> or O<sub>2</sub> and stoichiometric calculations
  - Assigning value of 30.0

5A - 23

23

### FRM 3 Major Points

- Sampling approaches (Sec. 1.2)
- Leak-check Tedlar bags (Sec. 6.2.6)
- Sampling point in the stack for single point grab (Sec. 8.1)
- Multi-point integration (Sec. 8.3):  
>24 in. 12 Pts; <24 in. 8 Pts

5A - 24

24

### FRM 3 Major Points

- Sampling at constant rate and same time as FRM 5 (Sec. 8.2.5)
- Analysis time 8 hours (Sec. 8.2.4)
- Leak-check Orsat (Section 11.5)
- $F_o$  Factor (Method 3B)
- Can't use Fyrite (Method 3B)
- Triplicate trials

5A - 25

25

### FRM 3 Inspector Tools

- Field observation agency checklist
- Stack sampling nomographs for field estimations
- Fryite-type combustion gas analyzer

5A - 26

26

### FRM 3 Tips

- Don't forget to take into account correction for altitude location of sampling port (0.1 in./100 ft)
- Stack gas pressure also requires determination of stack static pressure ( $P_g$ ):  $P_g/13.6$

5A - 27

27

### FRM 3 Tips

- Leak check sampling bag
- Leak check sampling train lines before sampling
- Leak check Orsat analyzer
- Minimum 12 sampling pts. (>24 in.)
- Minimum 8 sampling pts. (<24 in.)

5A - 28

28

### FRM 3 Tips

- Validate analytical data
  - Analyze ambient air ( $O_2 = 20.9 \pm 0.3\%$ )
  - Analyze against protocol gases ( $\pm 0.2\%$ )
  - $F_o$  Calculation
  - Nomograph verification

5A - 29

29

### FRM 3 Tips

- Analyze bag sample within 4 hours
- No more than 20 separate analysis for a given set of reagents
- Three separate analysis for each bag
  - $\pm 0.3\%$  if  $CO_2 > 4\%$
  - $O_2 < 15\%$
  - then  $\pm 0.2\%$

5A - 30

30



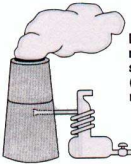
Dismiss FRM 3 Stack Test

- Failed to calibrate Orsat analyzer
- Tedlar bag found to be leaking
- $F_o$  outside of +/- 5 % of calculated value
- $O_2/CO_2$  outside of typical range

5A - 31

U.S. EPA APTI  
Compliance Test and  
Source Test Observation

Stack Test Basic Continued



**Method 4**  
Determination of  
moisture content of  
stack gas  
(by condensation  
method)

5B - 1

1

POLLUTANT MASS RATE

$$\overline{PMR}_s = \overline{c}_s Q_s$$

$Q_s = v_s A_s = v_n A_n$   
for  
Isokinetic Conditions

$$v_s = K_p C_p \sqrt{\frac{T_s \Delta p}{M_s P_s}}$$

Obtain  $C_p, T_s, \Delta p$   
 $M_s, P_s$

Obtain  $\Delta H_{@}, D_n$   
 $B_{ws}, B_{wm},$   
 $P_m, T_m$

5B - 2

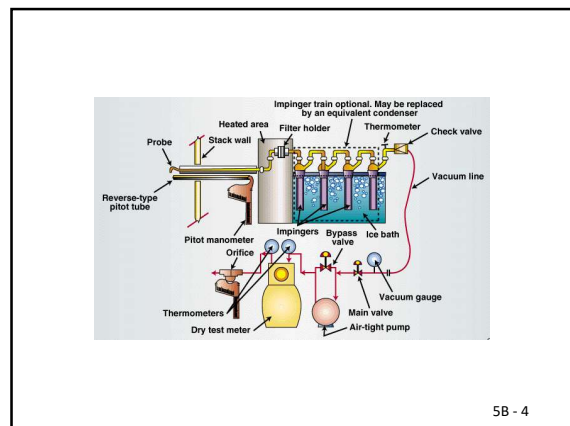
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Two Methods in FRM 4

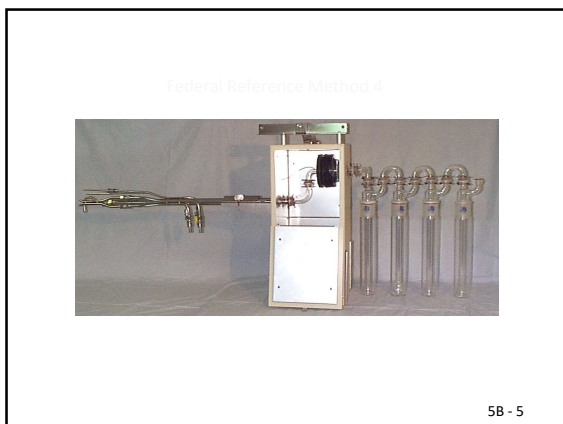
- Reference method  
(FRM 5 Condenser Methodology)
- Approximate Methodology
  - FRM 6 Impingers
  - Wet Bulb/Dry Bulb
  - Nomographs

5B - 3

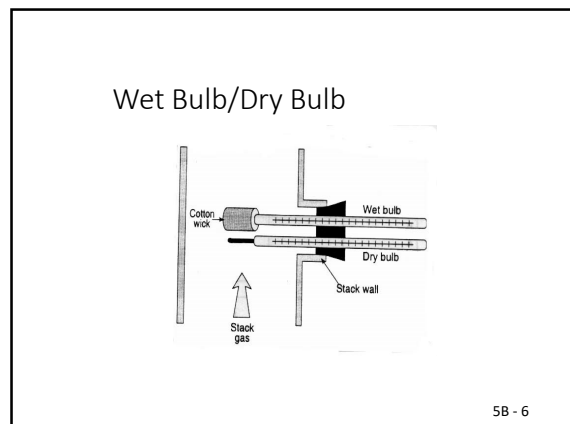
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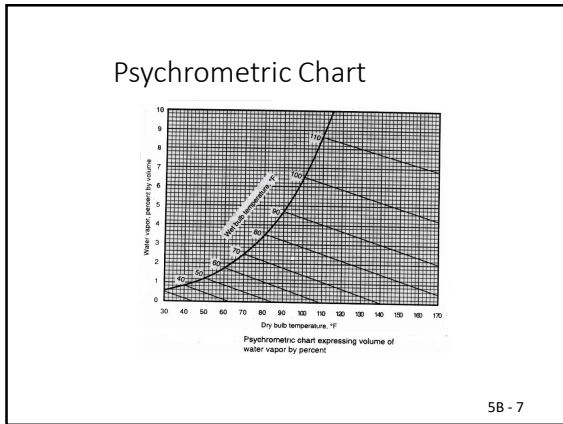
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5



6



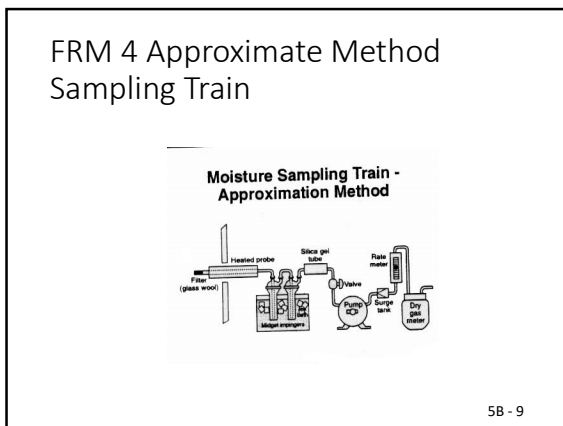
7

### Calculating % Moisture Under Saturated Gas Stream

$$\%H_2O = \frac{10 \left( 6.691 - \left( \frac{3144}{T_s + 39.86} \right) \right)}{(P_s \times 100)}$$

5B - 8

8



9

$B_{ws}$  = Proportion of water vapor in the gas stream.  
(by volume)

$$B_{ws} = \frac{V_{wc(std)}}{V_{m(std)} + V_{wc(std)}}$$

5B - 10

10

- ### FRM 4 Key Points
- Reference Method: Condenser Approach (Sec. 8.1)
  - Approximation Method: Method 6 impingers, wet bulb/dry bulb, charts (Sec. 6.1.1.2)
  - Saturated gas streams may give questionable results (Sec. 4.1)
- 5B - 11

11

- ### FRM 4 Key Points
- Design of train (Method 5, sec. 6.1.1.8)
  - Number of traverse points (sec. 8.1.1.1)
  - Minimum sample vol. (21 scf) and sampling rate (0.75 cfm) (Sec. 8.1.1.2)
  - Sampling at a "constant sampling rate" (Sec. 6.1.4)
- 5B - 12

12

### FRM 4 Key Points

- Leak rate determined from filter (Sec. 8.2.1)
- Approximate Method  
(Method 6, section 10.1 and Method 5, section 10.6, respectively)

5B - 13

13

### FRM 4 Key Points

- Two calculations for saturated/ moisture droplet gas stream
  - One measurement on saturation conditions
  - One measurement on impinger technique
- Lower of these two values used in calculations

5B - 14

14

### FRM 4 Inspector Tools

- Hand-held digital thermometer
- Field observation agency checklist
- Stack sampling nomographs for field estimations

5B - 15

15

### FRM 4 Tips

- Don't forget to wipe moisture from the outside of each impinger before weighing
- Do not weigh U-tube connectors
- Condensibles other than water leads to positive bias in results (i.e., acid aerosols and condensable organics)
- Stack gases that are supersaturated or no demisting

5B - 16

16

### FRM 4 Tips

- Typical moisture ranges
  - Coal: 5-15%
  - Oil: 8-10%
  - Gas: 8-10%
  - After wet scrubbers: 4-70%
  - Wood: 15-30%
  - Kilns: 30-40%
  - Sewage sludge incinerators: 5-30%
- Use wet/dry bulb and nomographs to verify moisture

5B - 17

17

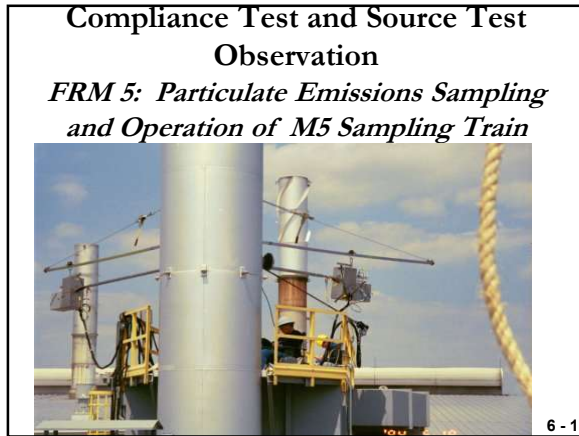
**SOURCE SAMPLING TITLE PAGE**  
**ALARMS EXIST !!! - Check Alarm Sheet**

Source Information			
<b>Plant Name</b>	Florida DEP		
<b>Sampling Location</b>	Bush Gardens		
<b>Fuel or Source Type</b>	Boiler		
<b>Fuel F-Factor</b>			

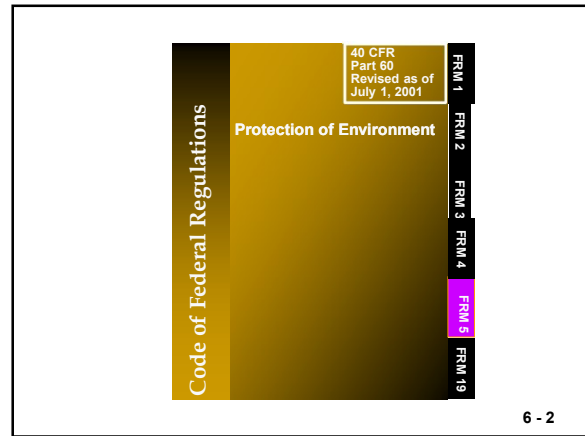
Test Information			
<b>Starting Test Date</b>		9/24/2018	
<b>Project #</b>		18-001 FL	
<b>Operator</b>		BF	
<b>Standard Temperature</b>		68	°F
<b>Standard Pressure</b>		30	in Hg
<b>Minimum required sample vol.</b>		30	scf
<b>Run Duration</b>		60	Minutes
<b>Base Run Number</b>		1	
<b># of Ports Available</b>		2	
<b># of Ports Used</b>		2	
<b>Port Inside Diameter</b>		25.00	in
<b>Circular Stack?</b>			<input checked="" type="checkbox"/>
<b>Rectangular Stack?</b>			<input type="checkbox"/>

Test Equipment Information			
<b>Meter Box Number</b>		m5	
<b>Meter Calibration Factor</b>	(Y)	0.998	
<b>Orifice Meter Coefficient</b>	( $\Delta H_{@}$ )	1.200	in H <sub>2</sub> O
<b>Pitot Identification</b>		p1	
<b>Pitot Tube Coefficient</b>	(C <sub>p</sub> )	0.840	
<b>Orsat Identification</b>		or2	
<b>Nozzle Number</b>		n3	
<b>Nozzle Diameter</b>	(D <sub>n</sub> )	0.3820	in
<b>Probe Number</b>		pr2	
<b>Probe Length</b>		60.00	in
<small>(SS, Glass ....)</small> <b>Liner Material</b>		steel	
<b>Sample Case / Oven Number</b>		111	
<b>Impinger Case Number</b>		123	
<b>Acetone Lot Number</b>		3	

Testing Company Information	
<b>Company Name</b>	Results R Us
<b>Address</b>	
<b>City, State Country Zip</b>	
<b>Project Manager</b>	
<b>Phone Number</b>	
<b>Fax Number</b>	



1



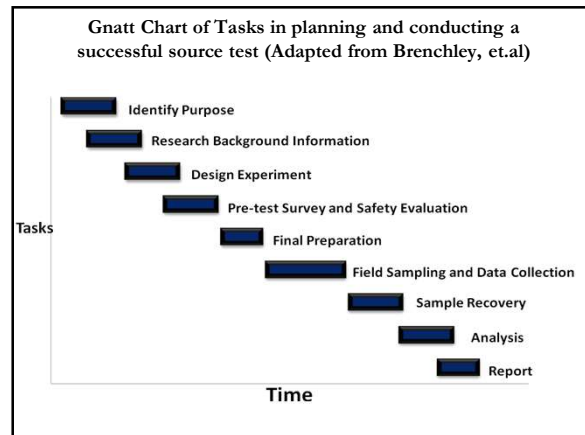
2

**Method 5**

- Source testing is a scientific experiment that requires an organized and methodical approach in order to achieve representative results.
- The source test is conducted to provide answers and valuable information, in regards to the air emissions from a specific source.
- This requires that objectives be decided before starting the test and that the procedures and equipment be designed to aid in reaching those objectives.
- After the test is completed, the results should be evaluated to determine whether the test objectives have been met

6 - 3

3



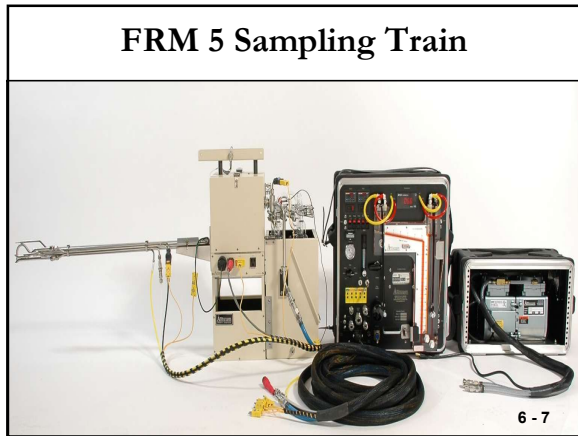
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6



7

**Basic Operation of FRM 5**

- Isokinetic Source Sampling
- “Iso” as denoting equality, similarity, uniformity.
- “Kinetic” is defined as of, pertaining to, or due to motion
- $\Delta H = K \Delta p$

6 - 8

8

**Simplified Isokinetic Rate Equation**

$$\Delta H = K \Delta P$$

6 - 9

9

**Isokinetic Sampling and Bias**

- To obtain average pollutant concentration, need parameters:
  - Quantity of mass emitted from stack
  - Total quantity of volume from stack

6 - 10

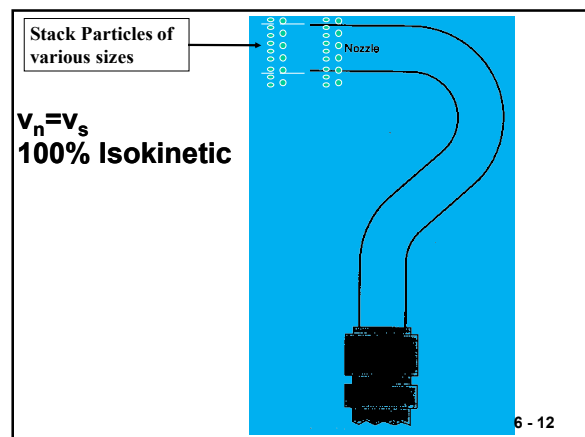
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**Isokinetic Sampling and Bias**

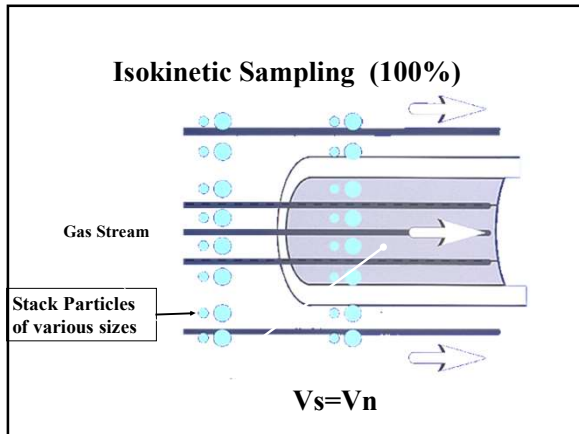
- Isokinetic sampling provides best approach for accurate data
- Pollutant mass rate (pmr)
  - $pmr_a$  (Ratio-of-areas:  $A_n$  ratio  $A_s$ )
  - $pmr_c$  (Ratio-of-conc.:  $m_n$  ratio  $A_n$ )

6 - 11

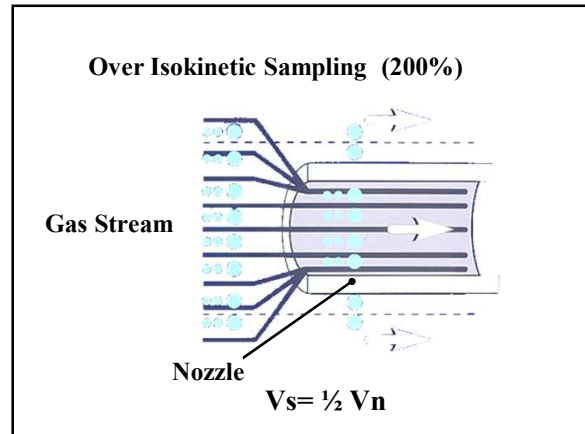
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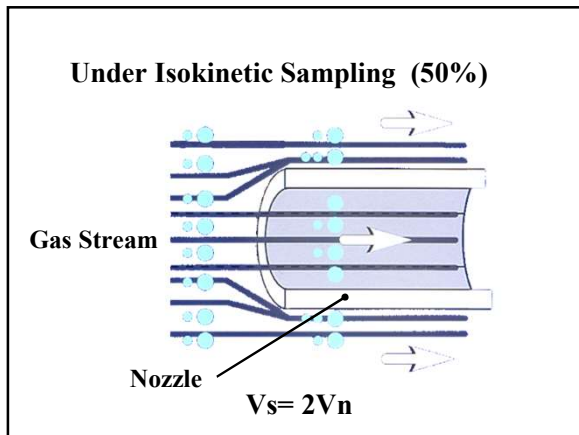
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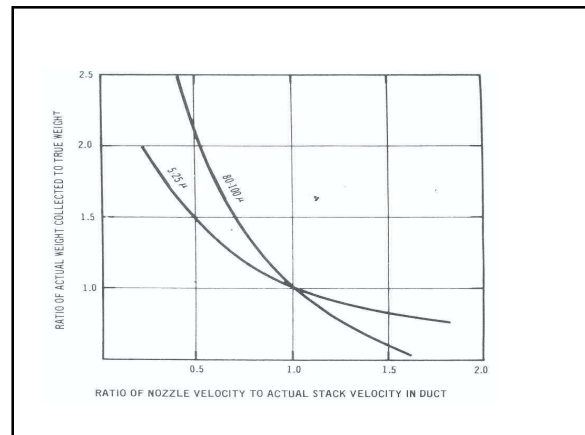
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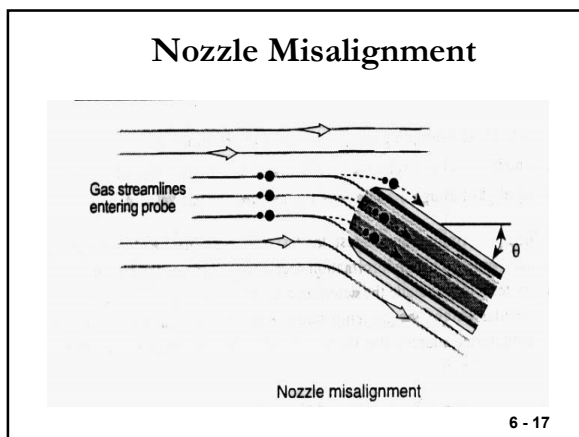
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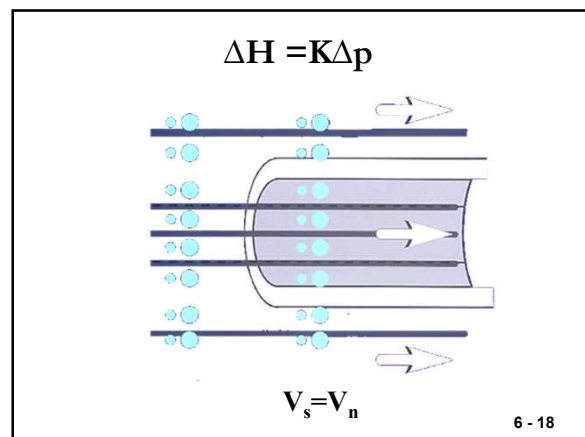
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16



17



18



### Isokinetic Sampling

$$\% \text{ Isokinetic} = \frac{V_n}{V_s} \times 100$$

6 - 19

19

### In Order To Take An Isokinetic Sample, We Must....

- Calculate the motion of the gas stream passing by the sampling system, and
- Recreate that motion in the sampling system

6 - 20

20

### FRM 5 Isokinetic Rate Equation

$$I_{int} = 100 \frac{T_s V_{m(std)} P_{std}}{T_{std} V_s \theta A_n P_s 60 (1 - B_{ws(est)})}$$

$$I_{final} = \frac{100 T_{s(avg)} \left[ K_3 V_{1c} + \left( \frac{V_{m(avg)}}{T_{m(avg)}} \right) P_{bar} + \frac{\Delta H}{13.6} \right]}{60 \theta V_{s(avg)} P_s A_n}$$

6 - 21

21

### FRM 5 Isokinetic Rate Equation (Simplified)

$$D_{n(est)} \sqrt{\frac{0.0358 Q_m P_m}{T_m C_p (1 - B_{ws(est)})}} \sqrt{\frac{T_s M_s}{P_s \Delta p_{est}}}$$

$$\Delta H = 846.72 D_n^4 \Delta H_{@} C_p^2 (1 - B_{ws})^2 \frac{M_d T_m P_s}{M_s T_s P_m} \Delta P$$

6 - 22

22

### FRM 5 Isokinetic Rate Equation

- The relationship between “ $v_s$ ” and “ $v_n$ ” is the core understanding of FRM 5 and isokinetic sampling
- Reading the “ $\Delta p$ ” from the pitot tube and setting the proper “ $\Delta H$ ” on the meter box allows one to sample isokinetically

6 - 23

23

### FRM 5 Nomograph

Nomograph

6 - 24

24

**FRM 5 Isokinetic Rate  
Equation**

$$\Delta H = \left\{ 846.72 D_n^4 \Delta H_{@} C_p^2 (1 - B_{ws})^2 \frac{M_d T_m P_s}{M_s T_s P_m} \right\} \Delta P$$

6 - 25

25

**FRM 5 Operation  
Setting  $\Delta H$  Based Upon  $\Delta p$   
Observation and Calculated K Factor**

$$K = \frac{\Delta H}{\Delta p} = K_6 D_n^4 \Delta H_{@} C_p^2 (1 - B_{ws})^2 \frac{M_d T_m P_s}{M_s T_s P_m}$$

6 - 26

26

6 - 27

27

**FRM 5 Causes for not Meeting 100%  
Isokinetics**

- Heavy grain loading, causing plugging of filter so can't achieve proper  $\Delta H$
- Large temperature variations not corrected in isokinetic rate equation

6 - 28

28

**FRM 5 Causes for not Meeting 100%  
Isokinetics**

- Moisture value wrong in setting preliminary isokinetic rate equation
- Inability to follow rapid fluctuations in  $\Delta p$  and corresponding calculating/setting  $\Delta H$

6 - 29

29

**FRM 5 Causes for not Meeting 100% Isokinetics**

- Leak in pitot or sampling lines (broken probe, lopsided filter, broken frit)
- Preliminary selection of wrong nozzle size

6 - 30

30

**Difficulty in  
Maintaining Isokinetics**

- Plugging of filter by particles
- Filter becoming wet:  
low box temperature
- Impinger stem too restricted

6 - 31

31

**Difficulty in  
Maintaining Isokinetics**

- Filter disc plugging
- Nozzle too small/large for  
velocity of stack gas

6 - 32

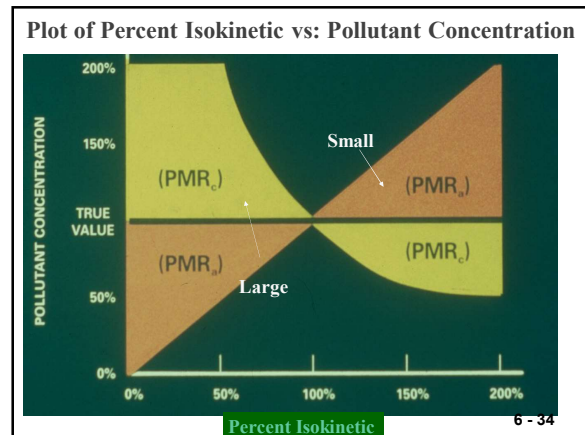
32

**Isokinetic Sampling and Bias**

- To obtain average pollutant concentration, need parameters:
  - Quantity of mass emitted from stack
  - Total quantity of volume from stack
- Isokinetic sampling provides best approach for accurate data
- Pollutant mass rate (pmr)
  - $pmr_a$  (Ratio-of-areas:  $A_n$  ratio  $A_s$ )
  - $pmr_c$  (Ratio-of-conc.:  $m_n$  ratio  $A_n$ )

6 - 33

33



34

**Error Percent in pmr  
Calculations Using FRM 5**

- $T_s$ : 1.4 %
- DGM: 1.0 %
- $P_s$ : 0.4 %
- $P_m$ : 0.4 %
- $P_b$ : 0.2 %
- $B_{ws}$ : 1.0 % Affects % Iso
- $\Delta H$ : 5.0 %
- $D_n$ : 1.0 %
- $\Delta H_{\phi}$ : 1.5 %

6 - 35

35

**FRM 5 Principle**

- Particulate matter is drawn isokinetically from an applicable source and collected on a glass fiber filter maintained at regulated temperature (usually  $120^{\circ}\text{C} \pm 14^{\circ}\text{C}$ )
- The particulate mass is determined gravimetrically after removal of uncombined water

6 - 36

36

### FRM Method 5 Limits

- Particulate matter (PM) target catch as a concentration or amount of an analyte that can be determined with a specific degree of confidence to be different from zero

6 - 37

37

### FRM 5

- “Front Half” is defined as particulate emissions
- Filter Temperature
  - 248°F
  - 320°F
- Isokinetic Sampling
  - $Velocity_{nozzle} = Velocity_{stack}$
  - 90% - 110%

6 - 38

38

### FRM Method 5 Limits

- Designed for PM catches of > 50 mg
- Limits for FRM 5
  - Practical quantitation limit (PQL) of 3 mg
  - Method detection limit (MDL) of 1 mg
- Target catch for FRM 5 must be no less than 3 mg; If less, go to FRM 5I

6 - 39

39

### Required Sampling

- Sampling duration: 60 –120 minutes
- Sampling rate: 0.50-0.75 dscfm
- Minimum sampling volume: 30 – 60 dscf
- Review 40CFR60/61 for minimum sampling duration, volumes and filter/gas temperatures
- Minimum sample volume dependent on analyte MDLs and expected concentrations

6 - 40

40

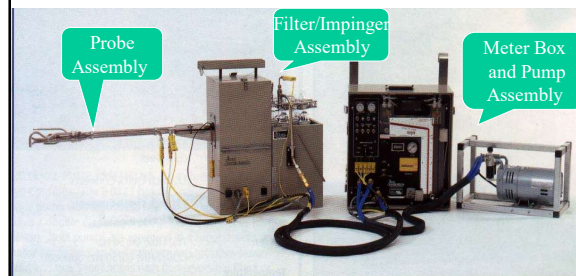
### Sampling Train Components

- The probe assembly
- The sample box
- The umbilical
- The meter box

6 - 41

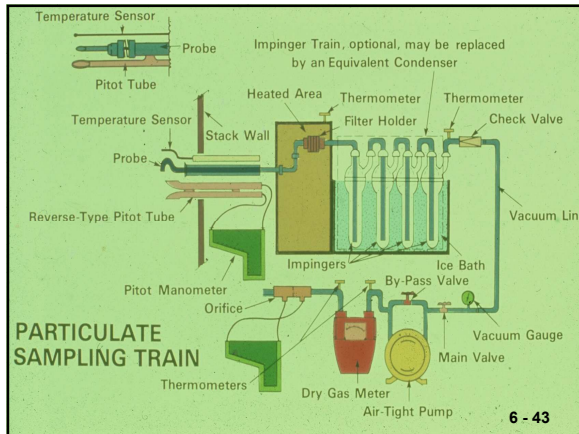
41

### FRM 5 Sampling Train



6 - 42

42



43

### FRM 5 Isokinetic Rate Equation

$$\%I_{int} = 100 \frac{T_s V_{m(std)} P_{std}}{T_{std} v_s \theta A_n P_s 60 (1 - B_{ws(est)})}$$

$$\%I_{final} = \frac{100 T_{s(avg)} \left[ K_3 V_{1c} + \left( \frac{V_{m(avg)}}{T_{m(avg)}} \right) \left( P_{bar} + \frac{\Delta H}{13.6} \right) \right]}{60 \theta V_{s(avg)} P_s A_n}$$

44

### FRM 5 Isokinetic Rate Equation (Simplified)

$$D_{n(est)} \sqrt{\frac{0.0358 Q_m P_m}{T_m C_p (1 - B_{ws(est)})}} \sqrt{\frac{T_s M_s}{P_s \Delta p_{est}}}$$

$$\Delta H = \left\{ 846.72 D_n^4 \Delta H_{@} C_p^2 (1 - B_{ws})^2 \frac{M_d T_m P_s}{M_s T_s P_m} \right\} \Delta P$$

45

An Isokinetic Calculation Example

46

### Simplified Isokinetic Rate Equation

$$\Delta H = K \Delta P$$

47

### The Basic Calculations

$$D_{n(est)} \sqrt{\frac{0.0358 Q_m P_m}{T_m C_p (1 - B_{ws(est)})}} \sqrt{\frac{T_s M_s}{P_s \Delta p_{est}}}$$

$$K = \left\{ 846.72 D_n^4 \Delta H_{@} C_p^2 (1 - B_{ws})^2 \frac{M_d T_m P_s}{M_s T_s P_m} \right\}$$

- $\Delta H = K \Delta P \quad T_s = t_s + 460$
- $T_m = t_m + 460$
- $M_s = M_d (1 - B_{ws(est)}) + B_{ws(est)}$

48

**Nozzle Selection Example**

- Given the following, solve for the nozzle diameter and for k in the isokinetic equation.

$B_{ws} = 12\%$	$Q_m = 0.75 \text{ cfm}$
$C_p = 0.85$	$\Delta H_{@} = 1.85$
$P_m = 30.0 \text{ in Hg}$	$P_s = 29.6 \text{ in Hg}$
$T_m = 80^\circ\text{F}$	$M_d = 29 \text{ lb/lb-mole}$
$T_s = 280^\circ\text{F}$	
$\Delta p = 0.80 \text{ in H}_2\text{O}$	

6 - 49

49

**Nozzle Selection Example (cont.)**

$$M_s = M_d (1 - B_{ws}) + 18 B_{ws}$$

$$M_s = 29 (1 - 0.12) + 18(0.12) = 27.7$$

$$D_n = \sqrt{\frac{(0.035 Q_m P_m)}{T_m C_p} \frac{1}{(1 - B_{ws})} \sqrt{\frac{T_s M_s}{P_s \Delta p}}}$$

$$D_n = \sqrt{\frac{(0.035 (0.75)(30.0))}{(460+80)(0.85)} \frac{1}{(0.88)} \sqrt{\frac{(280)(27.7)}{(29.6)(0.80)}}$$

$$D_n = 0.241 \text{ There choose a 0.25 in nozzle}$$

6 - 50

50

**Nozzle Selection Example (cont.)**

$$\Delta H = (846.72 D_n^4 \Delta H_{@} C_p^2 (1 - B_{ws})^2 \frac{(M_d T_m P_s)}{(M_s T_s P_m)}) \Delta P$$

$$\Delta H = (846.72 (0.25)^4 (1.85)(0.85)^2 (0.88)^2 \frac{29 \cdot 540 \cdot 29}{(27.7 \cdot 740 \cdot 30.0)}) \Delta P$$

$\Delta H = 2.59 \Delta P$  Where K in the isokinetic equation is equal to 2.59

What do you set  $\Delta H$  on the meter box manometer gauge to, when  $\Delta P = 1.0$  on the velocity manometer gauge.

6 - 51

51

**FRM 5 Isokinetic Rate Equation**

- The relationship between “ $v_s$ ” and “ $v_n$ ” is the core understanding of FRM 5 isokinetic sampling
- Reading the “ $\Delta p$ ” from the pitot tube and setting the proper “ $\Delta H$ ” on the meter box allows one to sample isokinetically


6 - 52

52

6 - 53

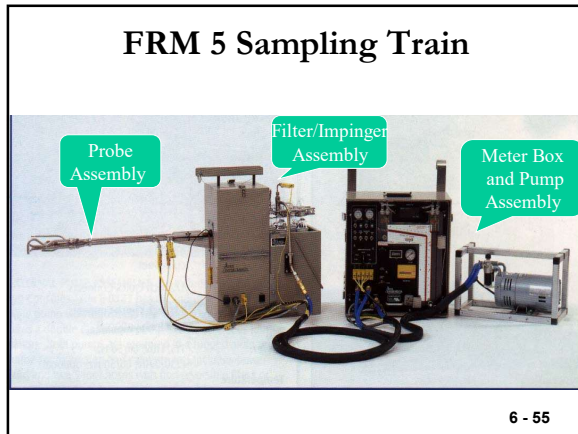
53

**FRM 5 Sampling Train**

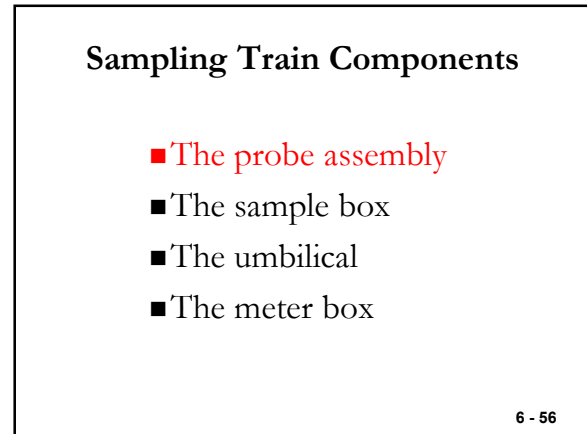


6 - 54

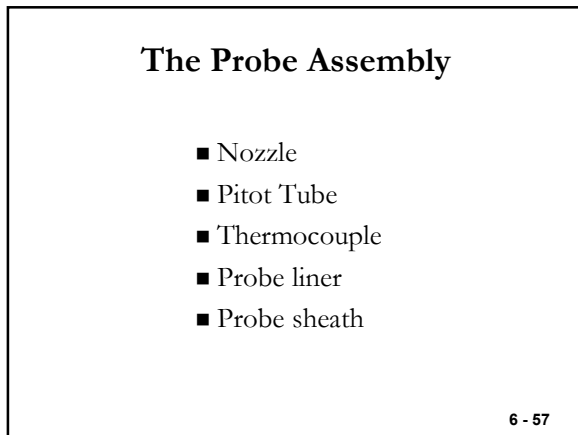
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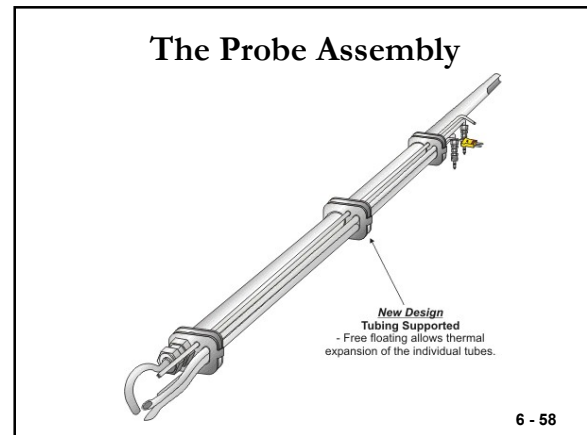
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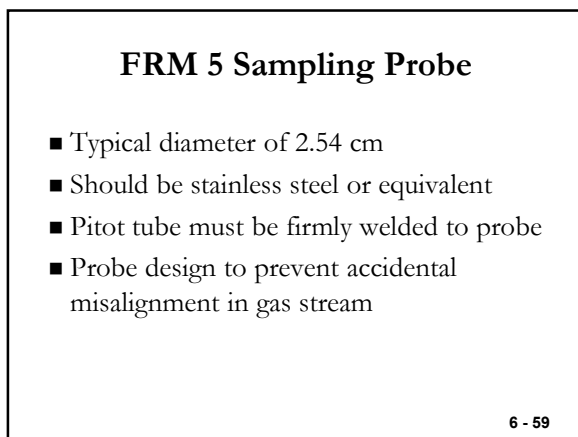
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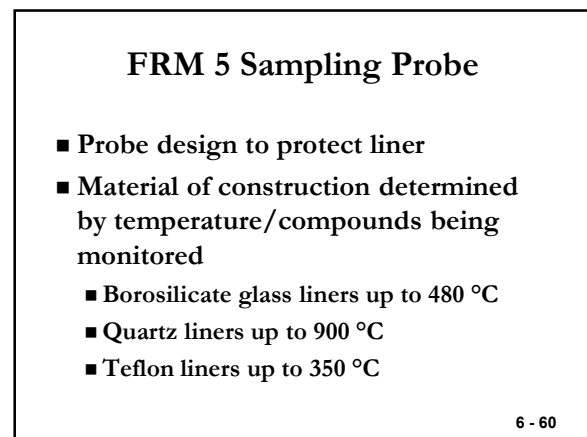
57



58



59



60

### Probe Liner

- Borosilicate or quartz glass
- Heating System to maintain exit gas temperature of 120 °C
- Borosilicate temperature to 480 °C
- Quartz glass temperature to 900 °C

6 - 61

61

### FRM 5 Sampling Probe

- Must have heating system capable of maintaining gas temperature of typically 120 °C +/- 14 °C
- Temperature must be calibrated

6 - 62

62

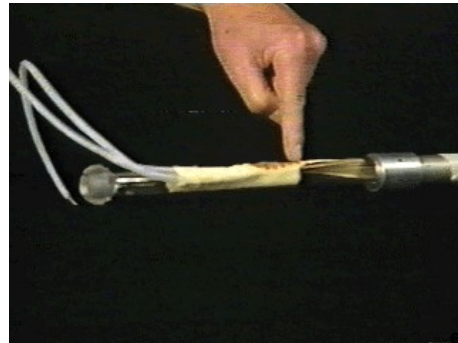
### Probe Sheath

- Usually stainless steel
- Pitot tube welded to sheath to prevent misalignment
- Protects liner from breakage

6 - 63

63

### Probe liner and sheath



64

64

### FRM 5 Ceramic Probe Heater



6 - 65

65



6 - 66

66





67



68

### FRM 5 Sample Nozzle

- Seamless stainless steel tubing or glass or Teflon
- Other materials approved by administrator
- Button-hook/elbow design
  - Sharp/tapered leading edge (<30 angle)
  - Constant internal diameter

6 - 69

69

### FRM 5 Sample Nozzle

- Range of nozzles (0.32-1.27 cm ID)
  - Nozzle must be calibrated
  - Measure 3 readings using micrometer (take average)
  - Low/high readings not exceed 0.004 inches

6 - 70

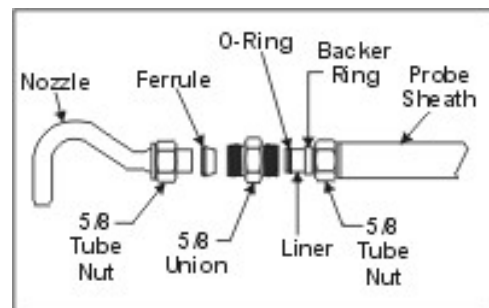
70

### FRM 5 Sampling Nozzle



71

### Sampling Nozzle



6 - 72

72



73



74



75



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77

**FRM 5 Sample Nozzle**

- Nozzles that have been nicked, dented, or corroded must be reshaped and recalibrated
- Each nozzle must have a permanent identification

78

### Nozzle Selection Equation

$$D_{n(est)} = \sqrt{\frac{K_5 Q_m P_m \sqrt{T_s M_s}}{T_m C_p (1 - B_{ws}) \sqrt{P_s \Delta p_{avg}}}}$$

6 - 79

79

### SIMPLIFYING

LET  $\Delta H@ = \frac{.9244}{(K_m)^2}$   
AND  $K_p = 85.49$

$\Delta H_\phi$  IS DEFINED AS THE ORIFICE PRESSURE DIFFERENTIAL THAT GIVES 0.75 CFM OF AIR AT 68° F AND 29.92" Hg.

$$\Delta H = \frac{Q_n^2 P_m M_n}{K_n^2 T_m}$$

$$\Delta H_\phi = \frac{(.75 \text{ cfm})^2 (29.92 \text{ Hg}) (29.0)}{(460 + 68) K_n^2}$$

$$\Delta H_\phi = \frac{.9244}{K_n^2}$$

6 - 80

80

### FRM 5 Isokinetic Rate Equation (Simplified)

$$D_{n(est)} = \sqrt{\frac{0.0358 Q_m P_m}{T_m C_p (1 - B_{ws(est)})}} \sqrt{\frac{T_s M_s}{P_s \Delta p_{est}}}$$

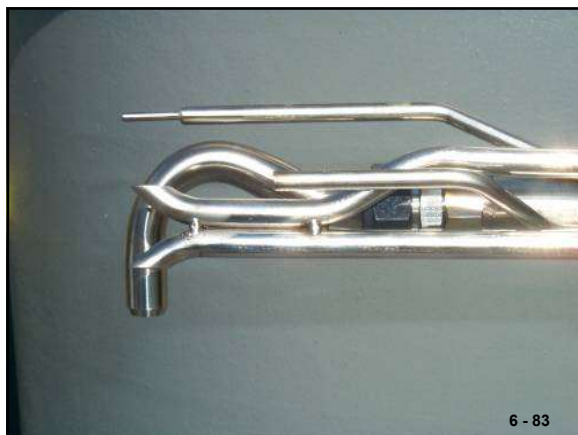
$$\Delta H = \left\{ 846.72 D_n^4 \Delta H_\phi C_p^2 (1 - B_{ws}) \frac{M_d T_m P_s}{M_s T_s P_m} \right\} \Delta P$$

6 - 81

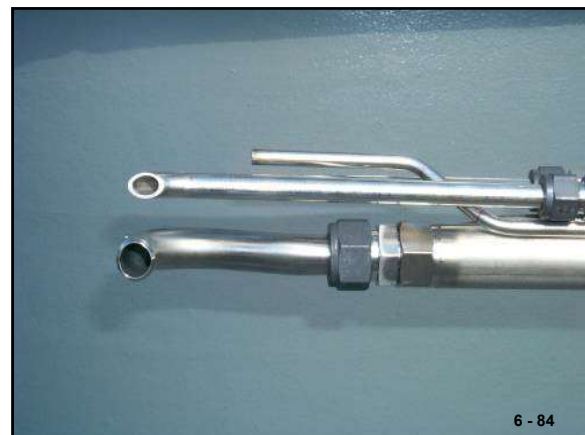
81

- ### FRM 5 Nozzle/Pitot Tube/Thermocouple Orientation
- Must meet certain design and configuration specifications
  - Inspect during each test to verify orientation
- 6 - 82

82



83



84

## Type S Pitot Tube

Design criteria for assigning

6 - 85

85

## Sampling Train Components

- The probe assembly
- **The sample box**
- The umbilical
- The meter box

6 - 86

86

## The Sample Box

### Heated Filter Box

- Heating element to maintain filter temperature of 120° C
- Filter Holder
- Flexibility for vertical and horizontal traverses
- Insulated

### Impinger Box

- Provide support and protection for glassware
- Insulated
- Holding container for ice to cool impingers

6 - 87

87

## FRM 5 Heated Filter Box

- Filter heating system capable of maintaining temperature typically 120 °C +/- 14 °C
- Temperature gauge capable of +/- 3 °C
- May be separate from impinger system for convenience

6 - 88

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6 - 90

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**FRM 5 Heated Filter Box  
Desired Features**

- Light weight, good insulation
- Positive probe alignment locking system
- Easy accessibility to all parts
- Good electrical system
- Durability/flexibility for vertical and horizontal stacks

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**FRM 5 Impinger System**

- Material of construction depends upon compounds being tested
  - Glass, Teflon, stainless steel
- Design should allow for additional space for impingers beyond FRM 5 requirements
- Need for water drain tap

94

**FRM 5 Impinger Assembly**

95



96



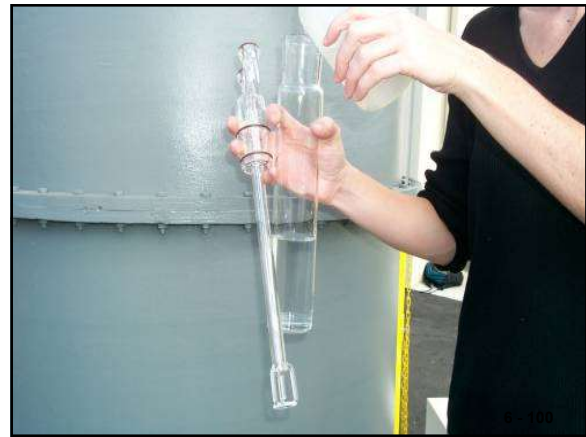
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100



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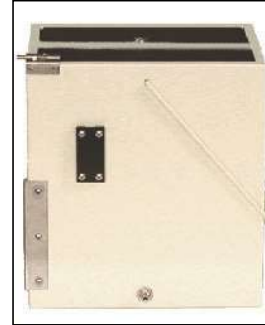
### FRM 5 Filter/Impinger Transport Case



6 - 103

103

### FRM 5 Impinger Case



6 - 104

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### Problems

- Leak in sampling train:  
low gas volume (correct or void)
- Filter/probe temperature  
not within specification
- Contamination during  
sampling/recovery  
(nozzle scraps on nipple,  
dust falls on filter)

6 - 105

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### Problems

- Non-Isokinetics
  - Range outside of  $90 < I < 110$ 
    - If  $< 90$ , bias high (large particles)
    - If  $> 110$ , bias low (high sample volume)
  - Multiply E by  $< 90$ : corrected does not  
pass limit: accept test
  - Multiply E by  $> 110$ : corrected not  
greater than limit: accept test

6 - 106

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### FRM 5 Train Components/pmr Error

- $P_{bar}$ : + 5.9%
- $\Delta p$ : + 2.4%
- Moisture: + 1.4%
- Nozzle diameter: - 2.0%
- Isokinetic rate: - 5.0%

6 - 107

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### Sampling Train Components

- The probe assembly
- The sample box
- **The umbilical**
- The meter box

6 - 108

108

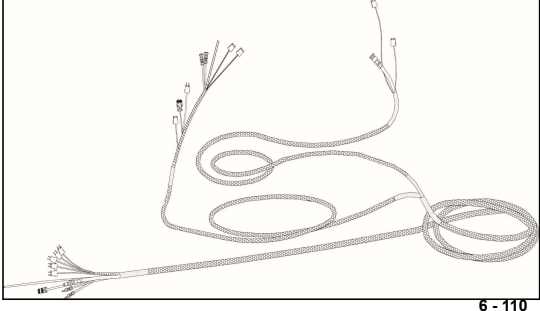
### The Umbilical Line

- Sample lines
- Pitot lines
- Electrical connections
- Covered in a protective sheath

6 - 109

109

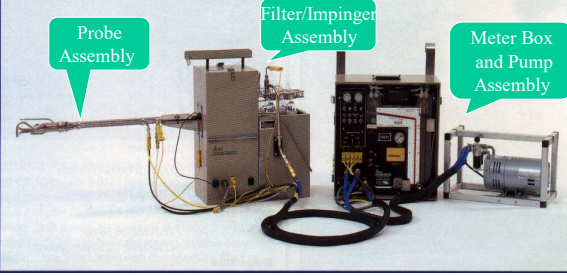
### FRM 5 Transfer Line



6 - 110

110

### FRM 5 Sampling Train



6 - 111

111

### The Meter Box

- Pump
- Dry gas meter
- Inclined manometer for  $\Delta p$  and  $\Delta H$  readings
- Flow control valves
- Ports for integrated gas sampling

6 - 112

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### FRM 5 Meter Console Desirable Features

- Light weight
- Reliable leak free pump
- Good temperature controls
- Rugged construction/  
good carrying handles

6 - 113

113

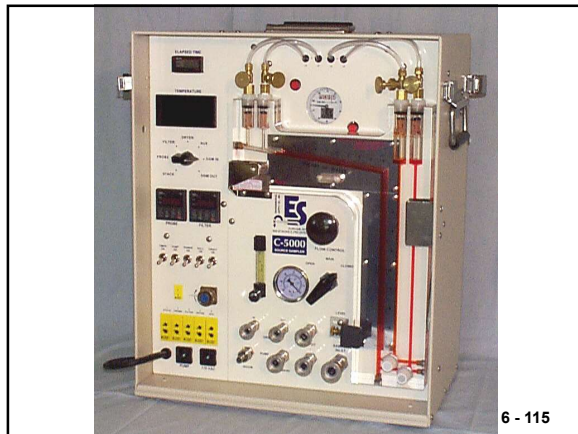
### FRM 5 Meter Console Desirable Features

- Accessibility to components  
and fuse compartment
- Communication system
- Easy to read digital readouts

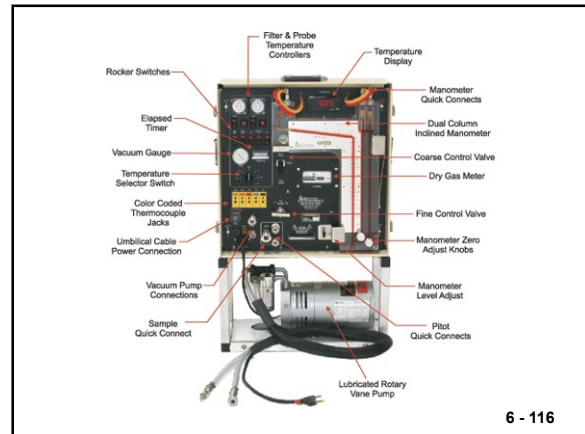
6 - 114

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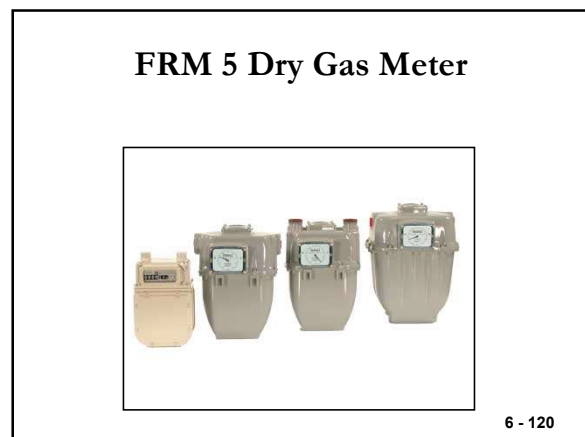
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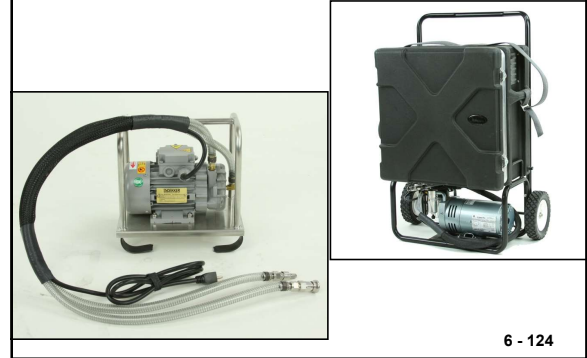
122

### FRM 5 Digital Meter Box



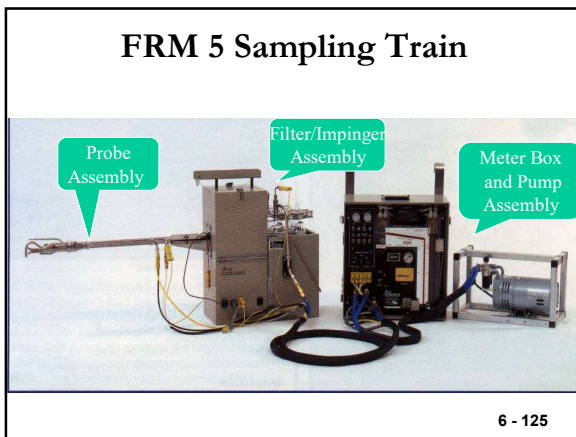
123

### FRM 5 Sampling Pump



124

### FRM 5 Sampling Train



125

### Errors in pmr Calculations Using FRM 5

- $T_s$ : 1.4 %
- DGM: 1.0 %
- $P_s$ : 0.4 %
- $P_m$ : 0.4 %
- $P_i$ : 0.2 %
- $B_{ws}$ : 1.0 % Affects % Iso
- $\Delta H$ : 5.0 %
- $D_n$ : 1.0 %
- $\Delta H_{\phi}$ : 1.5 %

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6 - 126

### What Are the Significant Errors With FRM 5?

- Before obtaining the answer, the tester or observer needs to know three things to determine what is important in significant errors with FRM 5:
  - What is the data to be used for (i.e., proof of compliance, proof of violation, engineering evaluation etc.)?

6 - 127

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### What Are the Significant Errors With FRM 5?

- Know three things (cont'd):
  - What are the direction and magnitude of any biases?
  - What is the acceptable bias that will be allowed before rejecting the results?

6 - 128

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### Source Compliance

- If test results show compliance:
  - Any magnitude of bias in the data that increases measured results (high bias), accepted as compliance
  - (10 % for high bias and 5 % low bias)
- If test results shows violation:
  - Any magnitude of bias in the data that shows violation of standard, then test data can contain any level of low bias
  - (10 % for low bias and 5 % for high)

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ERROR ANALYSIS OF SAMPLING PARAMETERS

Parameter	True value	Error	Erroneous value	Concentration (%)	Q <sub>1</sub>	Q <sub>2</sub>	Pollutant mass rate (lb/hr)	Requirement
P <sub>bar</sub>	30 in. Hg	1 in. Hg	31 in. Hg	+4.1	-1.6	+1.6	+5.9	>0.1 in. Hg
Q <sub>1</sub>	30 in. Hg	1 in. Hg	30.07 in. Hg	+0.2	-5	-5	+0.2	none
Q <sub>2</sub>	520°R	5°R	525°R	+0.9	-5	-5	+0.9	>5.0°R
P <sub>s</sub>	30 in. Hg	2 in. Hg	30.26 in. Hg	+0.1	+0.2	+0.2	+0.3	>1.06 in. Hg
t <sub>s</sub>	600°R	10°R	610°R	-0.4	+0.8	+0.8	-1.2	>1.55
Q <sub>p</sub>	1 in. H <sub>2</sub> O	0.1 in. H <sub>2</sub> O	1.1 in. H <sub>2</sub> O	-2.5	+4.9	+4.9	+5.4	>0.99 spec.
Moisture	10%	1%	11%	+0.1	-0.2	+1.3	+1.4	>1%
M <sub>d</sub>	29	15 CO <sub>2</sub>	29.15	+0.1	-0.3	+0.3	+0.4	>0.15
M <sub>d</sub>	29	15 O <sub>2</sub>	29.03	+0.1	-0.1	+0.1	+0.2	>0.15
M <sub>d</sub>	29	15 CO	29	-	-	-	-	>0.15
M <sub>n</sub>	100 mg	1 mg	101 mg	-1.0	-5	-5	-1.0	>0.5 mg
Time	120 min	1 min	121 min	-0.4	-5	-5	-0.4	none
Y	1.00	0.01	1.01	-1.0	-5	-5	-1.0	>2%
C <sub>p</sub>	0.04	0.01	0.05	-0.5	+1.2	+1.2	+0.6	>0.03
Nozzle diameter	0.250 in.	0.005 in.	0.255 in.	-2.0	-5	-5	-5.0	>0.002 in.
Isokinetic	10%	10%	10%	-5.0	-5	-5	-5.0	>10%
F Factor	55 O <sub>2</sub>	15 O <sub>2</sub>	65 O <sub>2</sub>	+6.7%	N/A <sup>a</sup>	N/A <sup>a</sup>	N/A <sup>a</sup>	>0.15 O <sub>2</sub>
F Factor	105 O <sub>2</sub>	15 O <sub>2</sub>	115 O <sub>2</sub>	+10.1%	N/A <sup>a</sup>	N/A <sup>a</sup>	N/A <sup>a</sup>	>0.15 O <sub>2</sub>
F Factor	155 O <sub>2</sub>	15 O <sub>2</sub>	165 O <sub>2</sub>	+10.4%	N/A <sup>a</sup>	N/A <sup>a</sup>	N/A <sup>a</sup>	>0.15 O <sub>2</sub>

Note: All errors are a theoretical calculation and it is assumed that a 2% error in isokinetics will cause a 1% error in both concentration and pollutant mass rate emissions. The percentage of error may vary slightly depending on the magnitude of the true value and the different assumptions made.

<sup>a</sup>Error due to calculation and combined isokinetic bias.

<sup>b</sup>Error due to calculation and combined isokinetic bias.

<sup>c</sup>No effect on the measured value.

<sup>d</sup>lb/10<sup>6</sup> Btu is actually a concentration standard.

<sup>e</sup>N/A - not applicable.

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### Example #1 Handout) (Stack Temperature)

- Asphalt plant with concentration standard of 0.04 g/scf
- Team measured stack temperature at 350 °F, but correct temperature was 320 °F
- Question: How much error?
  - From Table, -0.4 %/10 °F
  - Therefore, -1.2 % total error
  - Little effect!

6 - 131

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### Example #2 Handout (Orifice Meter)

- Dry dog food plant
- Allowable mass emissions 5 lbs/hr
- DGM "Y" determined to be 0.91, but tester using 0.97
  - From Table, 1.0 % error for each 0.10
  - Therefore, 6 % bias high error
  - May want to reject test!

6 - 132

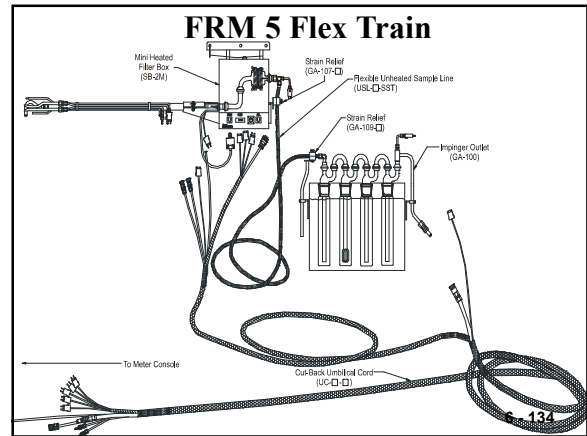
132

### Calibration Laboratory for DGM “γ” and Orifice Meter “ΔH@” Determinations



6 - 133

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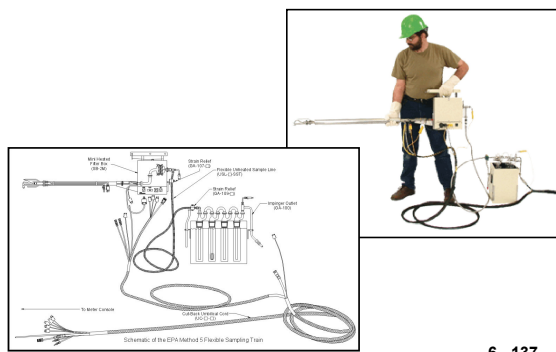
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6 - 136

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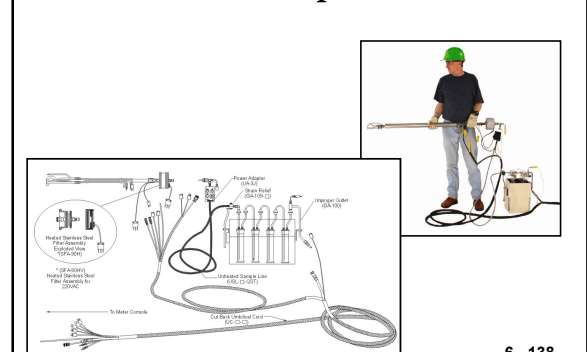
### FRM 5 Flex Train



6 - 137

137

### FRM 5 Compact Train



6 - 138

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### FRM 5 Recovery

- Note final DGM reading
- Leak check sampling system
- Remove probe from sampling train
- Sample train removed to recovery area
- Nozzle removed and brushed 3-6X with acetone into sample bottle

6 - 139

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### FRM 5 Recovery

- Probe brushed and rinsed with acetone 3-6X into sample bottle
- Front half of filter brushed and rinsed with acetone into sample bottle with nozzle/probe rinse
- Filter removed carefully and placed into petri dish. Filter disc scrapped to remove filter particles which are added to dish

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### FRM 5 Recovery

- Liquids in impingers measured either by weight or volume-normally discarded. Can be saved if further analysis required
- Silica gel weighed either in impinger or returned to sample jar

6 - 141

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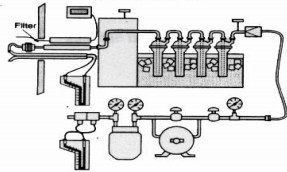
### FRM 5 Sample Recovery Items



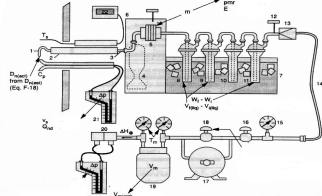
6 - 142

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### Method 17



### Method 5



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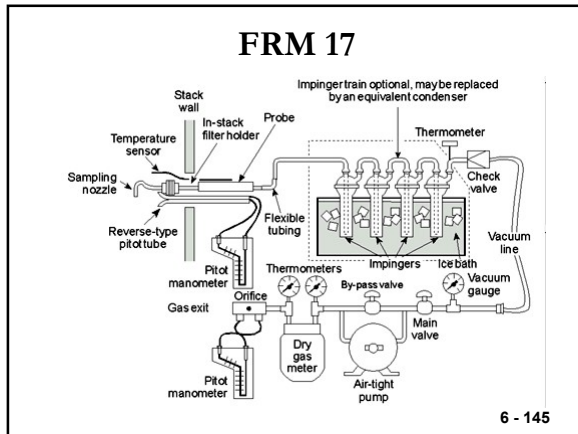
## Method 17

### In-stack Filter Applicability

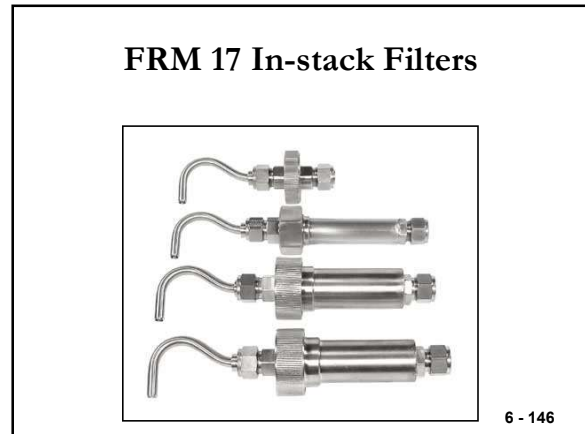
In sources where particulate matter concentration is independent of temperature

6 - 144

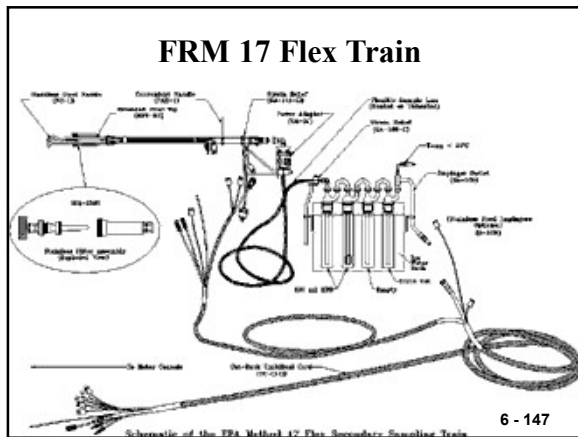
144



145



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### Method 5I Low PM Concentrations

- Initial Federal Register notice - December 30, 1997
- FRM 5I promulgation in 1999 with Maximum Achievable Control Technology (MACT) Hazardous Waste Incinerator (HWI) Rule
- EPA contact: Dan Bivins (919) 541-5244

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### Method 5I Low PM Concentrations

- Validated for Hazardous Waste Incinerators (HWI)
- Application - Calibrating PM CEMS
- Accuracy improved through:
  - Improved sampling handling procedures
  - Light weight sample filter assembly which is weighted entirely
  - Use of low residue grade acetone<sup>6</sup> - 149

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### Method 5I Low PM Concentrations

- Description
  - Isokinetic sampling using FRM 5 sampling equipment
  - Paired sampling trains
  - Lightweight out-of-stack filter (47 mm) assembly in FRM 5 hot box
  - Entire filter assembly weighing
  - Design for stack with < 50 mg PM (below 45 mg/dscm, ~0.02 gr/dscf)

150

**Method 5I Low PM Concentrations**

- Components:
  - Pyrex filter inlet
  - Viton seal ring
  - 47-mm filter paper
  - Stainless steel filter frit
  - 47-mm stainless steel clamp
  - Held together by Teflon tape seal
- Designed to be weighted as a single unit

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**Method 5I Low PM Concentrations**

- Limits for FRM 5
  - Practical quantitation limit (PQL) of 3 mg
  - Method detection limit (MDL) of 1 mg
- Therefore, the target catch must be > 3 mg by adjusting sampling time or sampling rate

6 - 152

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**FRM Method 5I Potential Interferences**

- Attention to filter housing during handling, sampling, and port changes
- Balance room conditions
  - Relative humidity < 50 %
  - Same person perform weighting before and after test
  - Electrostatic charges minimized during sample weighting

6 - 153

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**FRM Method 5I Quality Control (QC) Requirements**

- Same as FRM 5
- Recommended field bias blank train. Similar train, taken to field, prepared, leak checked, and recovered but no sampling of source emissions
- Relative standard deviation
  - $RSD = 100\% \cdot |C_a - C_b| / (C_a + C_b)$
  - Acceptable limits of < 10%

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**FRM 5 Sampling Train Questions?**



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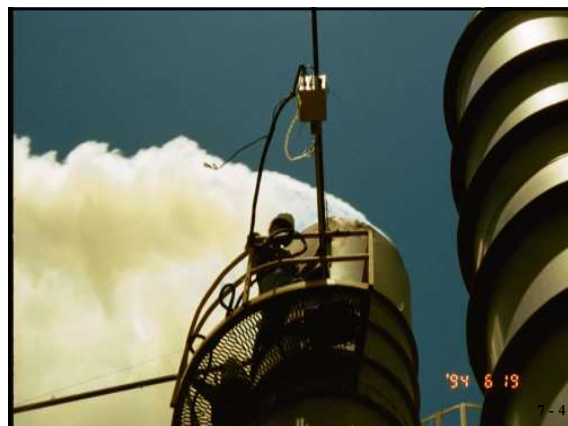
1



2



3



4

**The Source Test and Protocols**

- Dates/Times (timeliness of the submittal?)
- Facility Information
- Unit(s) to be Tested
- Operating and Control Information
- Stack Diagram
- Methods
- Modifications
  - Listed in the method as written
  - Proposed (who has the authority to approve?)

7-5

5

**Reviewing the Test Protocol**

- Rules/Regulations
- Permits
- Previous Testing History

<http://www.dep.pa.gov/BUSINESS/AIR/BAQ/BUSINESSSTOPICS/SOURCETESTING/Pages/default.aspx>

<http://www.epa.state.oh.us/portals/27/files/ITT.pdf>

7-6

6



**STACK TEST PROTOCOL - REQUEST FOR APPROVAL**

PROTOCOL (consisting of pages 1 through \_\_\_\_ ) IS APPROVED AS SUBMITTED.  
 PROTOCOL (consisting of pages 1 through \_\_\_\_ ) IS APPROVED WITH REVISIONS NOTED IN APPENDIX B.  
 Failure to conduct tests in accordance with the approved protocol may result in the test results being rejected by DEQ.  
 Approved by: \_\_\_\_\_ Date: \_\_\_\_\_

**I. Facility Information:**  
 Facility Name: \_\_\_\_\_ DEQ Registration Number: \_\_\_\_\_  
 Physical Location: \_\_\_\_\_  
 Emission Unit(s) to be tested: \_\_\_\_\_  
 Is an audit sample required? Yes  No  Please explain why: \_\_\_\_\_  
 If yes, is the Facility obtaining a sample in accordance with EPA requirements? Yes  No  Please explain why: \_\_\_\_\_

**II. Stack Testing Firm:**  
 Contact Name: \_\_\_\_\_ Phone: \_\_\_\_\_  
 Environmental Lab: \_\_\_\_\_ \*\*Virginia Laboratory ID: \_\_\_\_\_  
 Contact Name: \_\_\_\_\_ Phone: \_\_\_\_\_

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SIGNATURE: \_\_\_\_\_ DATE: \_\_\_\_\_  
Must be signed by a Responsible Official as defined in 9 VAC 5-20-220 of the Regulations for the Control and Abatement of Air Pollution, available at [www.dhs.gov](http://www.dhs.gov)

PRINTED NAME: \_\_\_\_\_ TITLE: \_\_\_\_\_  
Page \_\_\_\_ of \_\_\_\_ (number ALL pages, including attachments) Rev. 3/2010

**7 - 7**

7

**Reviewing the Test Protocol**

Protocol spells out the procedures to be followed by tuning the methods.

- Analyzer ranges
- Detection limits
- Sampling times
- etc.

**7 - 8**

8

**Reviewing the Test Protocol**

- Method specific tuning information
- Production Information
- Final report preparation details
- QA/QC Procedures
- Internal stack diameter
- Sampling port location(s)
  - diagram required
- Location(s) relative to disturbances
  - must meet minimum requirements
  - If not > 3D traverse required

**7 - 9**

9

**Pre-test Meeting/Conference**

- Smoother Testing , Less Procedural Problems
- Preview facility: emissions unit and control
- Discuss Testing – request changes

**7 - 10**

10

**Observing Testing – Be Prepared**

Have a Test Protocol Handy

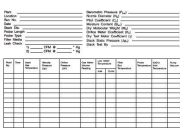
- PPE
- Observation Forms
- Camera (if allowed)
- Paperwork (copies)
- Methods
- Permits
- Rules


**7 - 11**

11

**Observing Testing – Take Notes**

- Field Data recorded
- INK
- Single-line cross out and initialed
- Computer Entered
- Equipment ID information
- Visual inspection of nozzle, pitot tube
  - Alignment in the stack
  - Nozzle diameter






**7 - 12**

12

### Observing Testing – Take Notes

- Calibration and span gases used
- Manometers to scale
- Meter Box Values :  $\Delta H$ ,  $\gamma$  and calibration dates
- Static and barometric pressures





7 - 13

13

### Observing Testing – Take Note

- Silica Gel
- Leak checks
- Probe and nozzle clean up
- Filter
- Instrumental Methods



7 - 14

14

### Observing Testing- What to be Aware of!!

- Umbilical cord crimping during leak check
- Adjusting impinger connections during leak checks
- Turning off the pump during leak check
- Not using highest vacuum during leak check
- Adjusting instrument based on readings
- Fabricating data on field data sheets
- Not traversing the stack or cyclonic flow check

7 - 15

15

### Types of Problems Found

- Unacceptable Sample Locations
- Port Locations
- Upstream & Downstream Diameters
- Equipment & Electrical Needs/Limitations
- Equipment Clearances
- Port Diameters
- Traversing needs (vertical)

7 - 16

16

### Types of Problems Found

- Equipment Errors
  - Operating ranges/calibration gases
  - Poor condition or not calibrated
  - Incorrect train components
  - Improper methods

7 - 17

17



7 - 18

18

**Types of Problems Found**

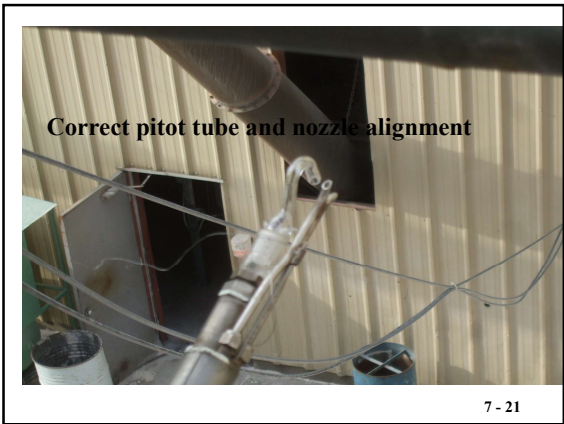
- **Procedural Errors**
  - Cyclonic flow checks
  - Leak checks
  - Traverse points
  - Isokinetics
  - Temperatures and ice downs
  - Recovery procedures

7 - 19

19



20



21

**Example of Guidelines**

FRM	Options	Responsible Party	Affects on Emissions
1	Circular Stack: Use of Particulate Traverse Not In Plane of Bend	Tester	Equal or Lower Emissions
2	Use of Standard Pitot Tube Rather than Type-S	Tester	Equal Values (Observe Possible Plugging)
3	Leak Check of Orsat Analyzer	Tester	Inaccurate O <sub>2</sub> and CO <sub>2</sub> Measurements
4	Use of Flexible Tubes Between Impingers	Tester	None
5	Nozzle Design Other Than Button-hook or Elbow	Administrator	None or Less

7 - 22

22

Hazardous Waste Combustion Unit Permitting Manual

COMPONENT 1  
How To Review A Trial Burn Plan

U.S. EPA Region 6 Center for Combustion Science and Engineering

[Hazardous Waste Combustion Unit Permitting Manual | Region 6 | US EPA](#)

7 - 23

23

Compliance Test and Source Test Observation

*Role of the Agency Inspector/Observer*

8 - 1

1

Why Compliance Stack Test and Observation Program ?

- Identify Air Pollutants
- Quantify
- Evaluate Test Results

*by prescribed EPA Federal Reference Methods (FRMs)*

2

Example of Typical Industries

- Coal-fired Power Plants
- Asphalt Plants
- Gas Turbines
- Gasoline Terminals
- Coating and Printing Facilities
- Secondary Aluminum
- Cement Plants

8 - 3

3

Groups Involved In A Compliance Test

- Officials of the facility being tested
- Consulting stack testing team
- Agency officials in which the facility is located (i.e., State Air Quality Division)

8 - 4

4

Source Test Time-line

Tasks

Time

- Identify Purpose
- Research Background Information
- Design Experiment
- Pre-test Survey and Safety Evaluation
- Final Preparation
- Field Sampling and Data Collection
- Sample Recovery
- Analysis
- Report

8 - 5

5

Step 1: Objectives, Protocols and Pre-site Survey

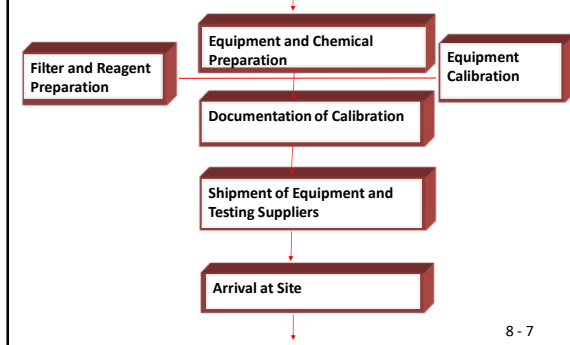
```

    graph TD
      A[Establish Test Objectives] --> B[Design Test Protocol]
      B --> C[Perform Pre-Site Survey]
      C --> D[Finalize Test Protocol]
      D --> E[Calculate Preliminary v_w, Q_w, B_ws, M_d, ΔH@ and D_n]
      A --- F[Research Liter./Regulations]
      B --- G[Submit Test Plan to Agency For Approval]
      E --- G
  
```

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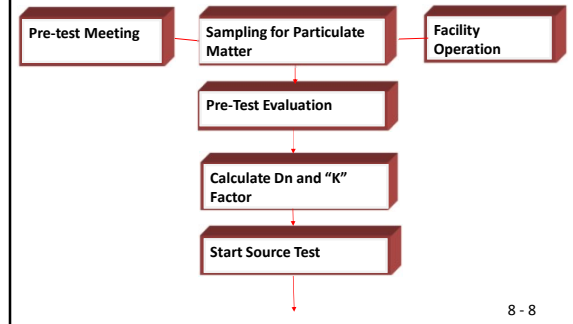
Step 2: Equipment Preparation



8 - 7

7

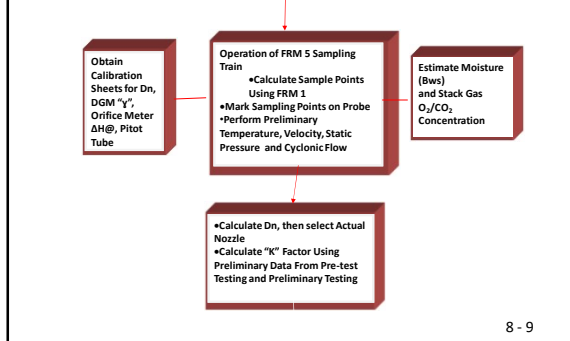
Step 3: Pre-test Conference and Evaluation



8 - 8

8

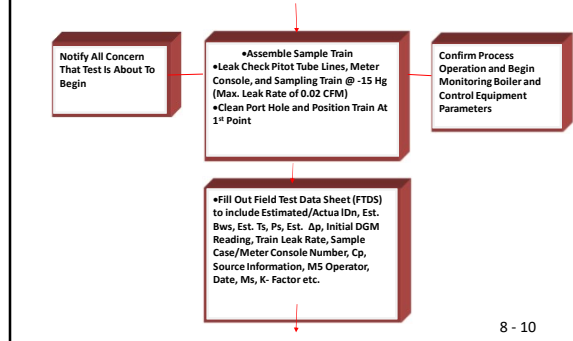
Step 4: The Test



8 - 9

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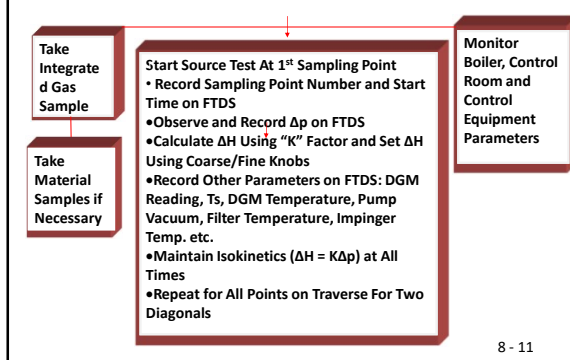
Step 4: The Test



8 - 10

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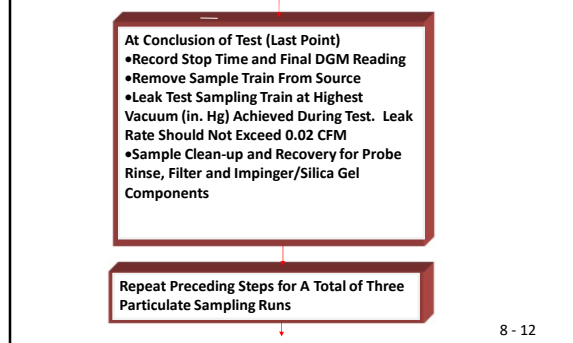
Step 4: The Test (Cont'd)



8 - 11

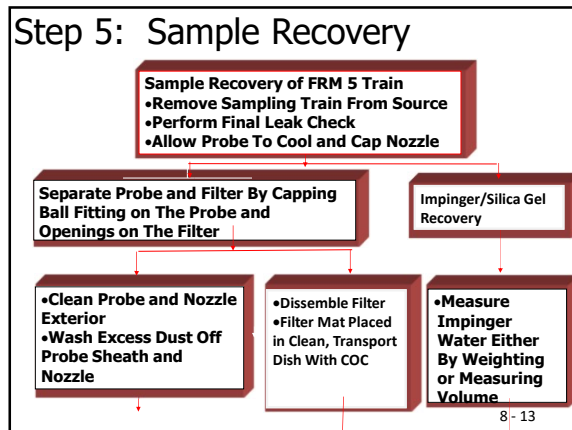
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Step 4: The Test (Cont'd)

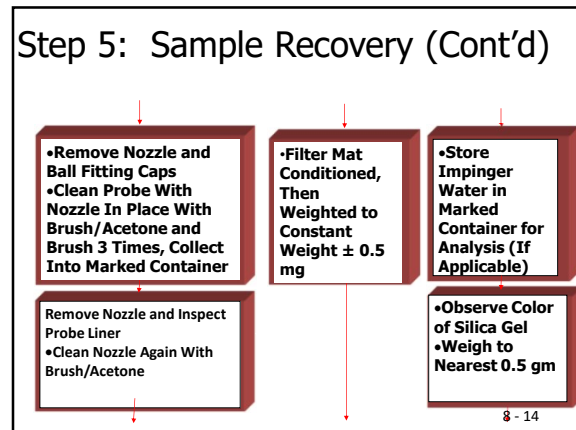


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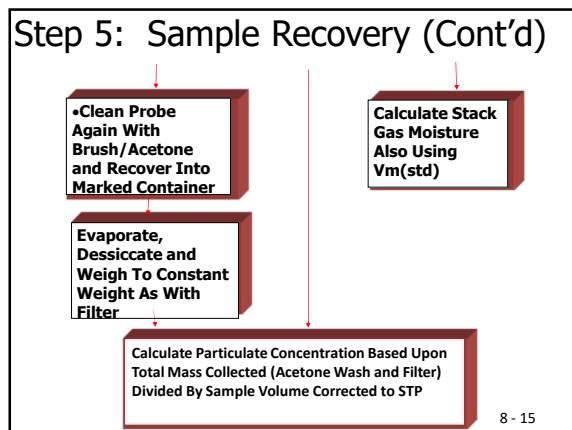
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14



15

### Function of Stack Test Observer

*“...the principal function of the stack test observer is to evaluate the representativeness of the compliance test in which emissions are sampled while the plant operates under typical conditions considered representative of day-to-day operations.”*

16

### The Inspector's/Observer's Role

- Be Present! (Phone insp. and windshield insp. are discouraged)
- Have a Plan, Follow the Plan!
- 3-Tier Inspection
- Observations – “familiar” with 40 CFR 60, App. A, Methods 1-4,5; 1.Velocity Profile, 2.Leak Check, 3.Clean-up 4. Observer Check-list
- Operations of facility
- Sample train recovery and data acquisition

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### Inspectors Do's and Don'ts

**DO**

- Ask intelligent questions that add value
- Become “familiar” with test methods rules and test plans
- Show Up! Presence is critical
- Be critical but reasonable
- Reward “quality testing”

**DON'T**

- “Umpire” a test
- Challenge a test w/o good cause
- Be unresponsive to requests
- Hesitant to say “I don't have an answer”
- Be Careless

18



19

### Seven Areas of Responsibility of Agency Personnel

- **Familiarize:** Agency observer establishes contact with the source and becomes familiar with operations, emissions, and applicable regulations.
- **Division of Air Quality Reviews Scheduled Source Test:** May be part of compliance test or annual test requirements
- **Division of Air Quality Establish Methodology:** Identify testing methodology as prescribed by regulations and receipt of testing plan from facility or contractor

8 - 20

20

### Seven Areas of Responsibility of Agency Personnel

- **Division of Air Quality Reviews Final Test Plan:** Pre-test meeting between Division personnel, test team leader and facility to finalize test plan.
- **Actual Compliance Test:** The facility Operations Personnel and Division of Air Quality Test Personnel observe testing methodology.

8 - 21

21

### Seven Areas of Responsibility of Agency Personnel

- **Review of Test Data:** Division of Air Quality determines compliance and official notification are determined.
- **Continuing Enforcement of Compliance:** Follow-up inspections are undertaken, using data generated from source test as a "baseline" for compliance purposes.

8 - 22

22

### Compliance Evaluation In Terms of Five Criteria

- Process and control equipment must be operated in such a manner as to produce representative atmospheric emissions
- Location of the sample port and sample points must provide samples representative of the atmospheric emissions

8 - 23

23

### Compliance Evaluation In Terms of Five Criteria

- The sample collected in the sample train must be representative of the sample points.
- The sample recovered and analyzed must be representative of the sample collected in the sample train
- The reported results must be representative of the sample recovered and analyzed

8 - 24

24

### Division of Air Quality Personnel Involved In The Testing

- Phase 1: Preparation and planning
- Phase 2: Conducting the test
- Phase 3: Recovery, transport (Optional), and analysis of the samples (Optional)
- Phase 4: The observer's compliance test report

8 - 25

25

### Role of The Observer

- Determine whether source test is required
- Coordinate process operation
- Coordinate control equipment operation
- Coordinate testing methodology
- Document all activities during the testing program
- Review test reports

8 - 26

26

### Role of The Observer

- Specify Division requirements
- Make decisions regarding test methodology, process and control equipment operation and reporting requirements
- Determine representativeness of process and control equipment operation

8 - 27

27

### Role of The Observer

- Determine acceptability of testing methodology
- Compile summary report of test
- Review test report and make recommendation

8 - 28

28

### Observer Behavior

- The observer should do all within his power to see that testing is successfully completed
- The observer should work cooperatively with the source and consultant
- The observer must be specific and forthright in his request
- The observer must be respectful of the positions of the other parties involved

8 - 29

29

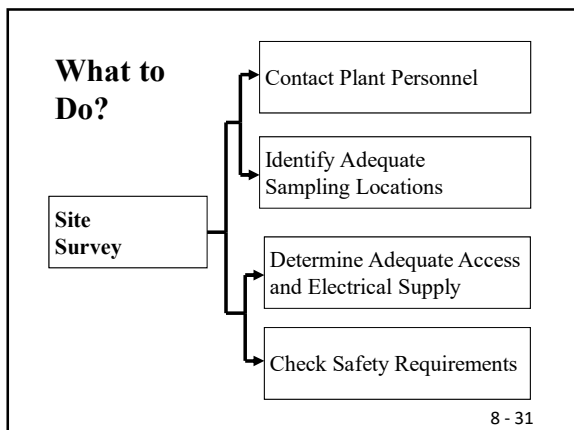
### Observer Techniques

- Do not write on process charts and graphs
- Do not turn knobs and dials
- Do not collect unnecessary data
- Do not touch or adjust testing equipment
- Do not question tester or interfere during critical times of the test
- Do not conceal unacceptable acts or procedures

8 - 30

30





31

**Phase 1: Preparation and Planning**

- Division of Air Quality must clarify for the plant representative and stack test team leader procedures to be followed (i.e., compliance test guidelines)
  - Identification of Federal Reference Methods (FRMs): PM, Condensibles, Filter Temp, Inorganics, Organics etc.
  - Operation level of process during testing (i.e. “baselining” the control equipment/source)
  - Data acquisition and reporting of process and test methodology parameters

8 - 32

32

**Phase 1: Preparing and Planning**

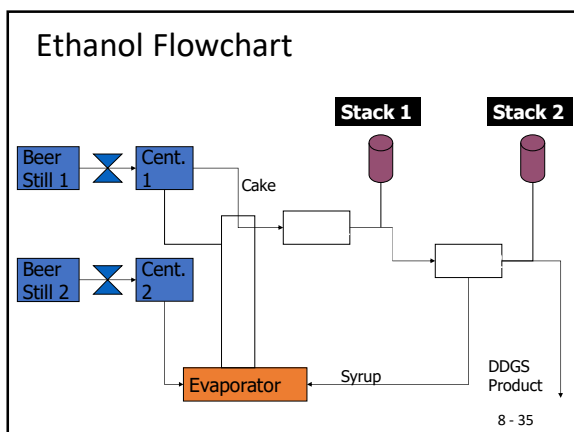
- Block-style flowchart is adequate for our needs for “baselining”
- Do not need design-oriented piping and instrumentation (P&I) engineering drawings
- Only system components need to be block-style rather than actual drawing of equipment

8 - 33

33



34



35

**Utility of Preparing a Block-Style Flowchart**

- Identifies health and safety hazards (i.e., high temperature, high positive pressure, fugitive leaks, slippery/wet surfaces etc.)
- Facilitates compliance evaluation
- Document operating conditions with reference to previous compliance test (“Baselining” the process!)
- Simplifies communications with plant personnel

8 - 36

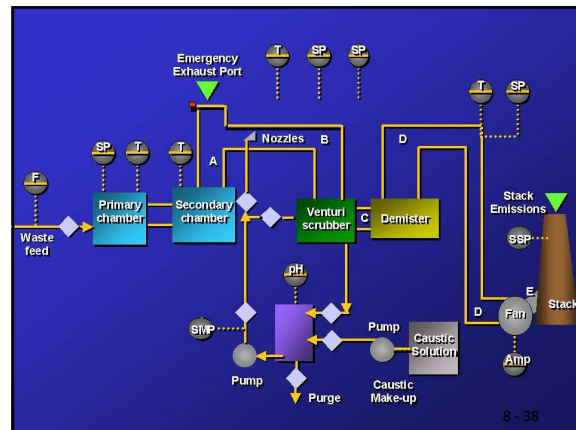
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### Symbols Used in Block-Style Flowcharts

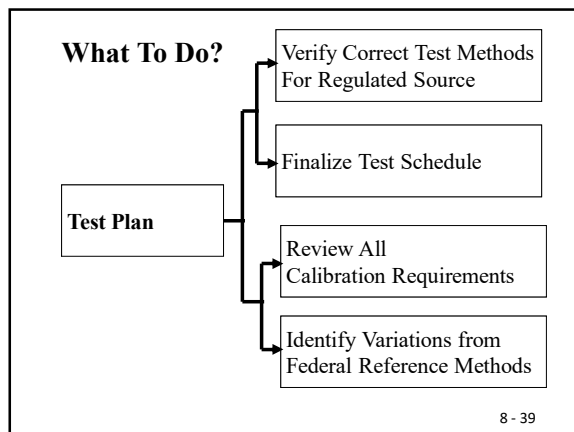
- Solid line.....Solid or liquid stream
- Two Parallel Solid Lines.....Gas stream
- Square or Rectangle.....Major equipment
- Reverse Triangle.....Gas emission point
- Circles with "T" inside...Actual temper.
- Circles with "SP" inside....Static pressure

8 - 37

37



38



39

### Phase 1: Preparing and Planning

- Division of Air Quality review of submitted test protocol
  - Deviation from standard sampling procedures
  - Operation of facility
  - Identification/discuss of test methods
  - Identification and discussion of sampling location
  - Calibration of all monitoring equipment

8 - 40

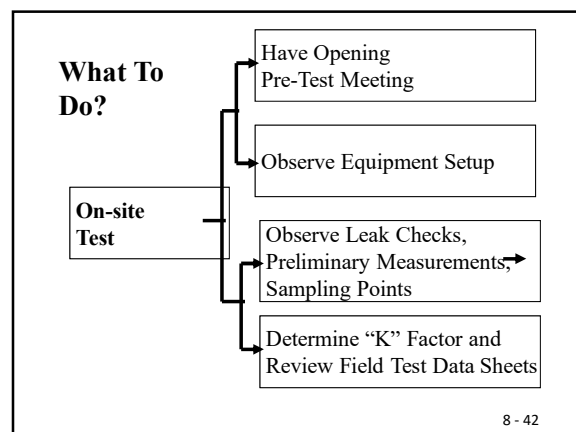
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### Phase 1: Preparing and Planning

- Observer's Needed Documentation
  - Checklist for Federal Reference Methods (FRMs) and SW-846 Methods (See Resource CD)
  - Checklist for air pollution control equipment
  - Checklist for facility operation parameters
- Pretest Meeting
  - Finalize sampling plan
  - Establish "Baseline" conditions
  - Coordinate testing schedule
  - Checklist for pretest meeting

8 - 41

41



42

### Observer Activities

- Observe preliminary velocity traverse and cyclonic flow check
- Observe nozzle size determination
- Review approximate molecular weight and moisture determination
- Review “K-factor” determination

8 - 43

43

### What To Do?

The Test

- Observe Locating Probe At 1st Point
- Observe Delta p and Calculate Delta H Using “K-factor”
- Observe setting Delta H with Fine Adjust Knob
- Observe Checking Stack Parameters/new “K-factors”

8 - 44

44

### What To Do?

The Test

- Observe 1st Test
- Observe 2nd Test
- Observe 3rd Test
- Observe Checking Stack Parameters/new “K-factors”

8 - 45

45

### Phase 2: Conducting The Test

- Observer’s Checklist (See Resource CD)
  - Health and safety requirements
  - Tentative testing schedule
  - Facility “baseline” conditions
  - Update stack test methodology checklist
  - Handling irregular situations, potential problems and their solutions
  - Calibration forms/checklist

8 - 46

46



47

### What to Watch

- Review records of equipment calibration (pre-test/QC)
- Watch cyclonic flow check and preliminary flow traverse

8 - 48

48

### Examine Probe Nozzle, Pitot, And Thermocouple Design

- Center of nozzle and pitot opening aligned
- Impact pressure sensor of pitot above nozzle opening

8 - 49

49

### Examine

- Type-S pitot tube offset 3/4 inch to side of nozzle
- Thermocouple offset 3/4 inch to side of pitot or set back 2 inches from center of pitot opening

8 - 50

50

### What to Watch

- Vacuum/pressure leak check
- Check traverse point marks, # is correct and within 1/2 inch

8 - 51

51

### What to Watch

- Nozzle ID calibrated; 3 measurements within +/- 0.004 inch
- Check dry gas meter with restricted orifice: also a gamma check

8 - 52

52

### What to Watch

- Pitot tube leak check; both (+) and (-) sides (check at pressure vacuum > 3 inches water and stable for at least 15 seconds)

8 - 53

53

### Sample Train Leak Check

- Pre-test should be at 15 inches Hg
- Post test at vacuum >= max. vacuum reached during the test

8 - 54

54

### Sample Train Leak Check

- Leak rate < 0.02 cfm acceptable
- Leak rate > 0.02 cfm; either record leak rate and correct sample volume or void the test run

8 - 55

55

### What to Watch

- Check sampling port is sealed
- Look to see that inclined manometer is level all the time
- Check that sampling train is being moved at the correct time and set at the correct traverse point

8 - 56

56

### What to Watch

- Check that the operator is recording temperatures and setting sampling rate at the proper times
- Reagents stored properly; i.e., at correct temperature and protected from sunlight

8 - 57

57

### What to Watch

- Sampling isokinetically; Is  $\Delta H$  on meter box equal to  $\Delta H$  on field data sheet?
- Check % Isokinetic rate equation at various points during the sampling scheme:  $\Delta H = k \Delta P$

8 - 58

58

### What to Watch

- Check that sampling system temperatures are within specifications:
  - Probe temperature
  - Filter temperature
  - Sorbent temperature
  - Impinger train temperature (iced?)

8 - 59

59

### What to Watch

- Watch sample recovery
  - Nozzle rinse
  - Probe rinse
  - Front half filter housing rinse
  - Filter recovery
  - Resin recovery
  - Proper labeling/storage of recovered samples

8 - 60

60

### What to Watch

- Samples properly identified and tied to specific sample runs
- Chain-of-custody properly prepared and maintained with samples

8 - 61

61

### What to Watch

- Field and trip blanks prepared properly and shipped with field samples
- Documentation retrieved and signed

8 - 62

62

### Phase 2: Conducting The Test

- Observe "First Test" Items
  - Configuration/preparation of train
  - Initial leak check
  - Positioning at 1st sampling point
  - Record initial data/operation meter box
  - Calculation of "K" factor
  - Verification of isokinetics
  - Movement of probe to other sampling points/ports
  - VE observations

8 - 63

63

### Phase 2: Conducting The Test

- Observe "First Test" Items
  - Facility Operation (i.e., "Baselining")
    - Fuel flow meters
    - Process monitors
    - Fuel consumption
  - Data from continuous emission monitors (CEMs)
  - Control equipment monitors
    - ESP (voltage, current, rapping rate etc.)
    - Bag houses (∅ p, bag failure logbook etc.)
    - Wet scrubbers (pH, flow rate etc.)

8 - 64

64

### Phase 2: Conducting The Test

- Observe "Second Test" Items
  - During second test, record and observe process and pollution control equipment data/operation
  - Verification of operation of Method 5 train and recorded data
  - Movement of probe to final sampling points
  - Final leak check/observation of filter condition
  - Sample recovery and "chain-of-custody (COC)" documentation
  - Final VE observation

8 - 65

65

### Phase 2: Conducting The Test

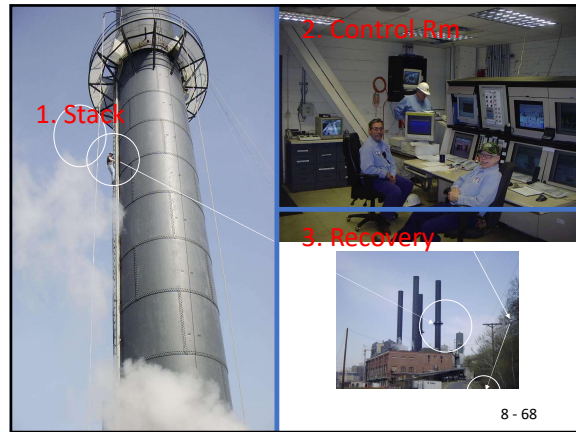
- Observe "Third Test" Items
  - During third test, record and observe process and pollution control equipment data/operation
  - Verification of operation of Method 5 and recorded data
  - Observation of continuous emission monitor systems (CEMs) and recorded information
  - Final leak check/train recovery of filter and impingers

8 - 66

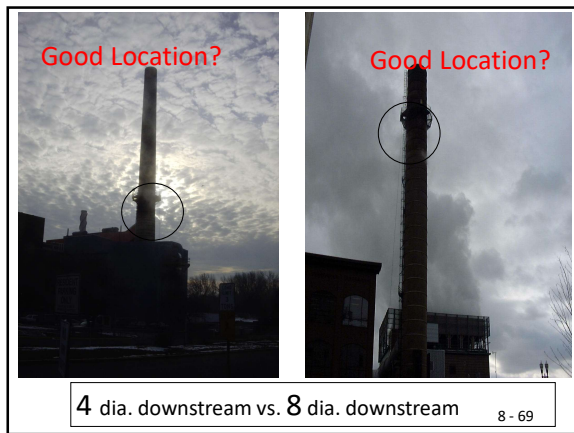
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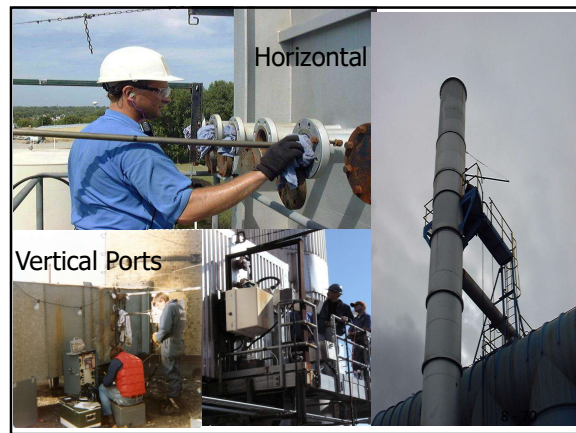
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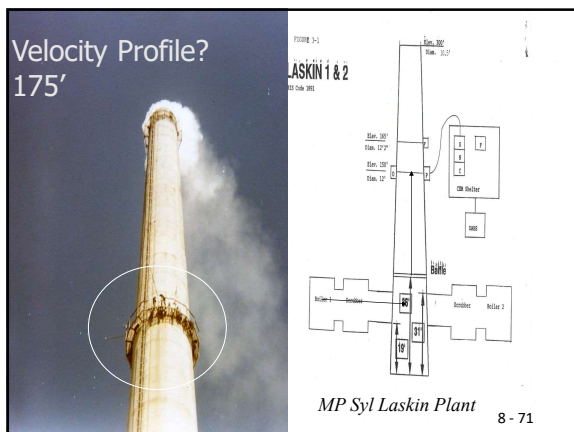
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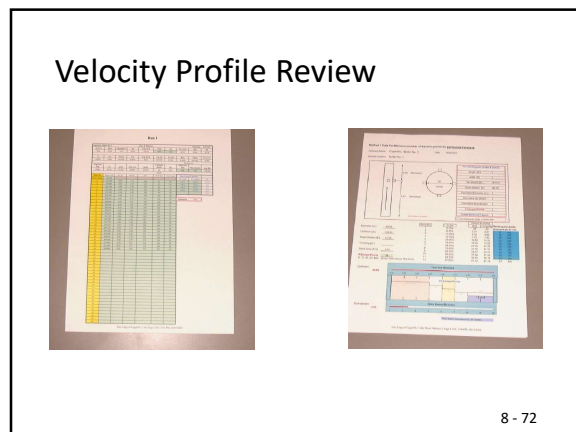
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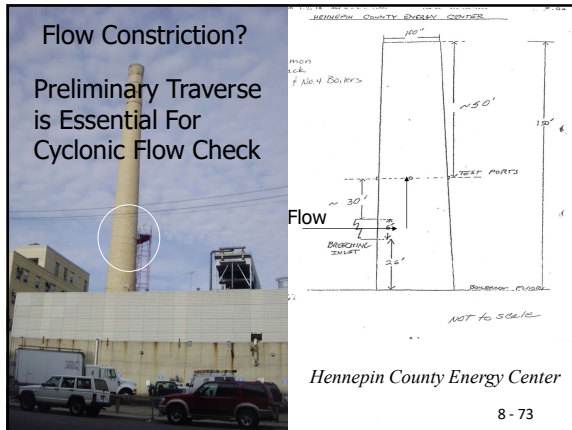
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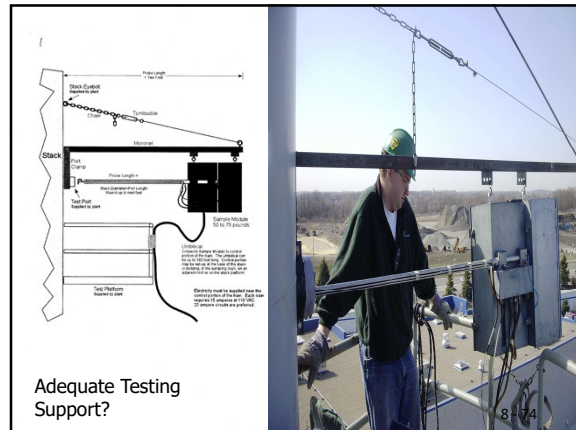
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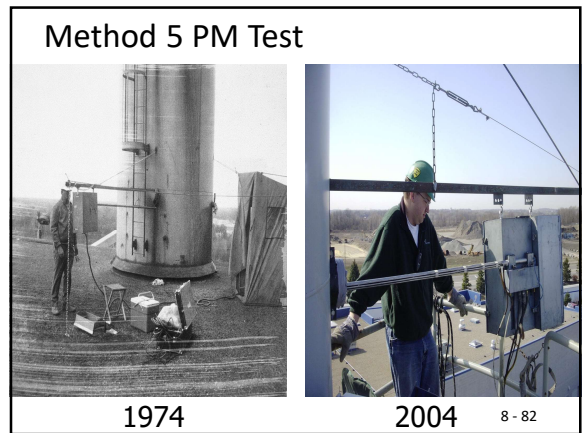
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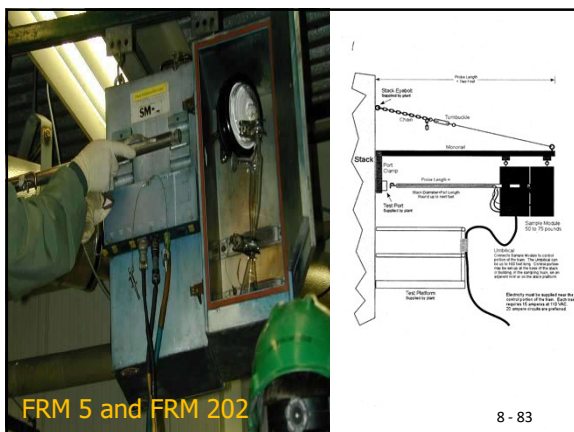
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81



82




83



84

*Inspector Presence*  
*"Be There"*



- Never circumvent Plant Safety Rules
- Adhere to Test Plan
- Communicate during testing
- Gather data, i.e. leak check

8 - 85

85




86


86

Times Have Changed...The Need to Test Hasn't

1974



2004

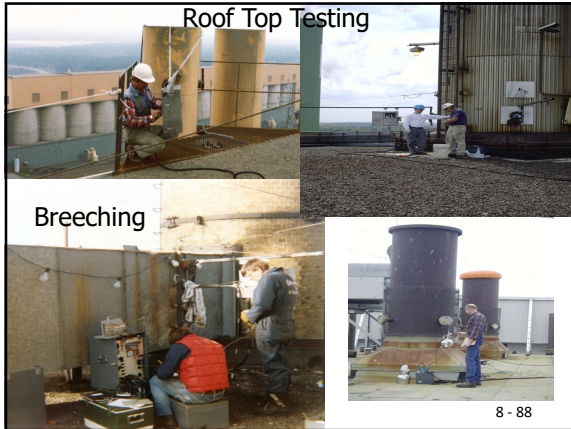


*On-site presence is essential!*

8 - 87

87


Roof Top Testing




Breaching

8 - 88

88



Roof Top Testing



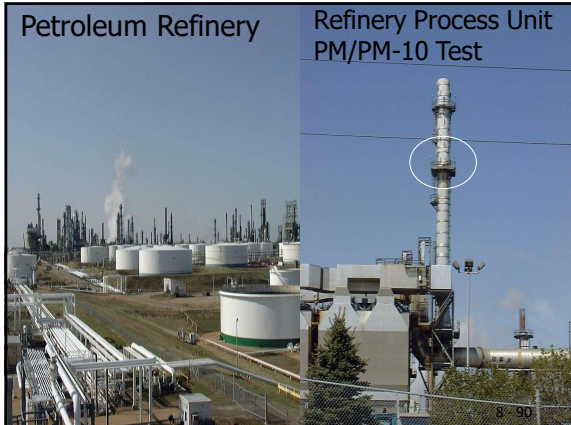
Mobile Lab

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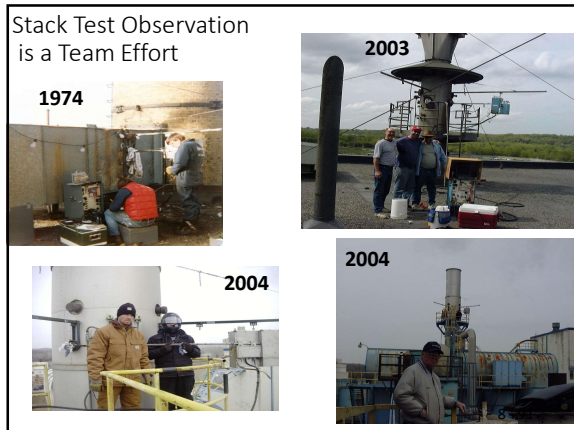
Petroleum Refinery

Refinery Process Unit  
PM/PM-10 Test



8 - 90

90



91



92



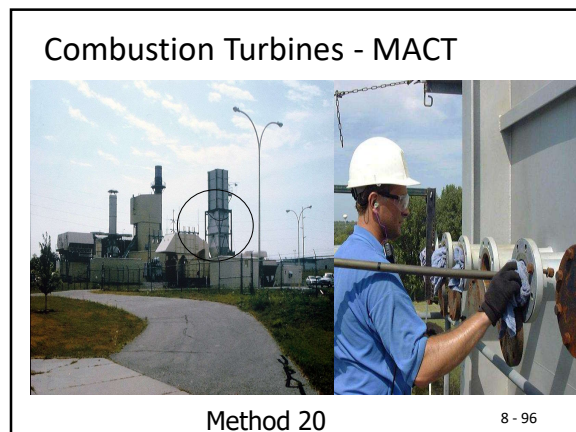
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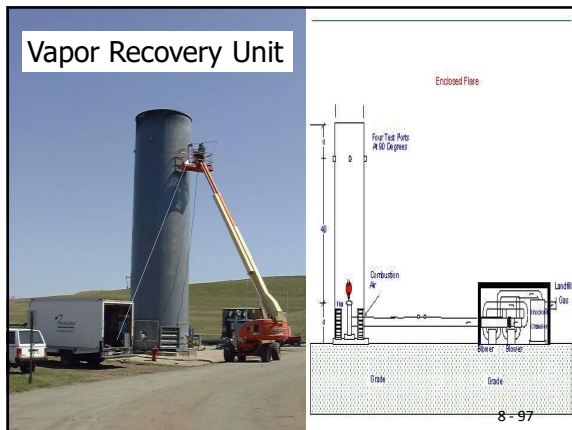
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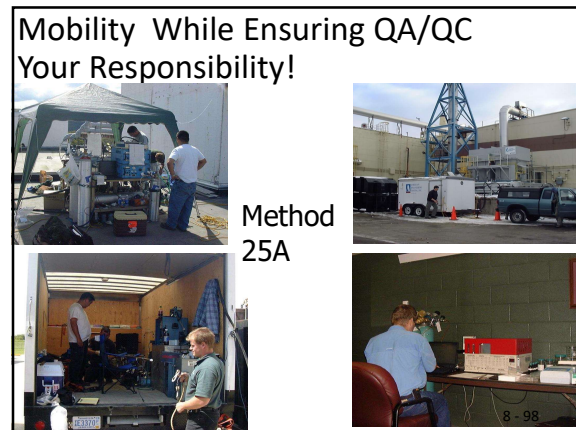
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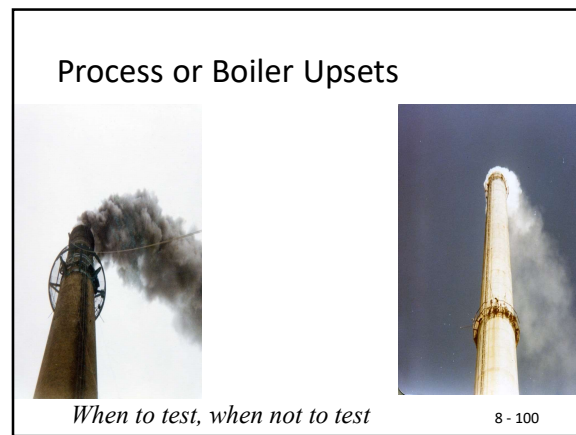
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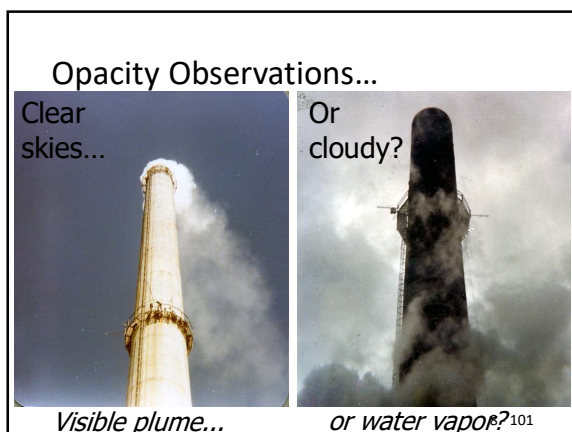
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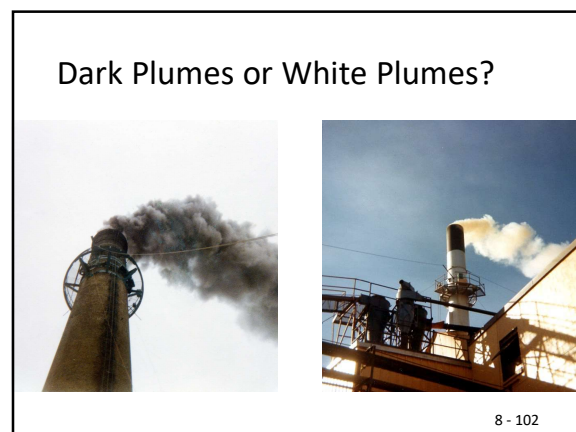
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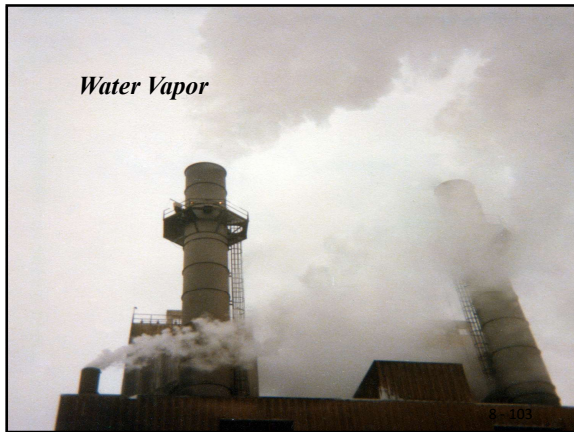
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101



102



103

**Testing Issues**

- Safety first – climbing, weather, platforms
- Port scrapping and stack liners
- Ethanol Plants – VOC Emissions
- Flow Disturbance (i.e. Cyclonic Flow)

8 - 104

104

Safety...

How do YOU stack up?

8 - 105

105

A hard hat?

Nomex suit?

Safety glasses?

Safety Shoes?

(OSHA 29 CFR 1910.23)

8 - 106

106

Distance up equals...

Distance down!

(OSHA 29 CFR 1910.23)

8 - 107

107

Be Prepared

Buckle Up...  
 Hook Up...  
 Lock Up!

8 - 108

108



109



110



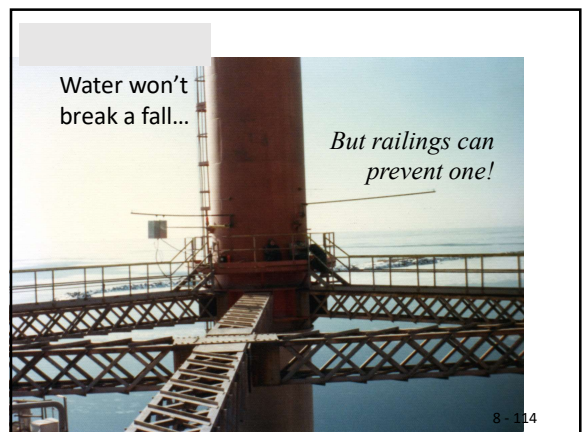
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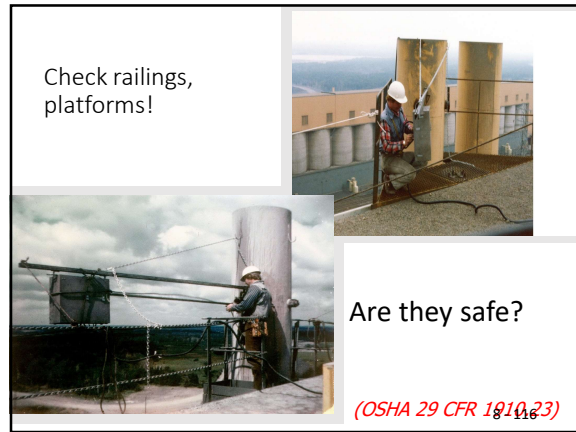
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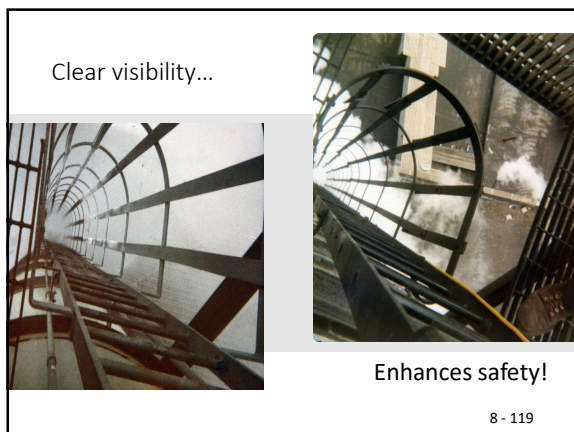
116



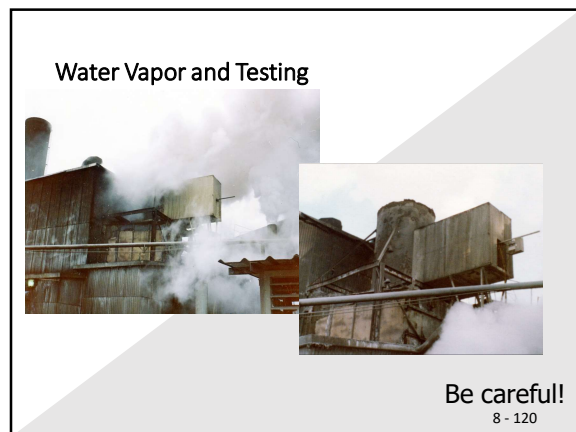
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120

Communications are Essential



Make time for **SAFETY!**

8 - 121

121

Testers use Harnesses!



State inspectors should too!

8 - 122

122

Respirators...



Are helpful!

8 - 123

123

Scaffolding or Ladders



Always Buckle Up!

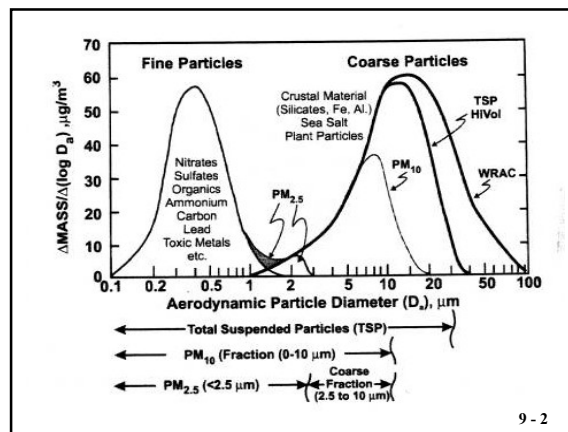
8 - 124

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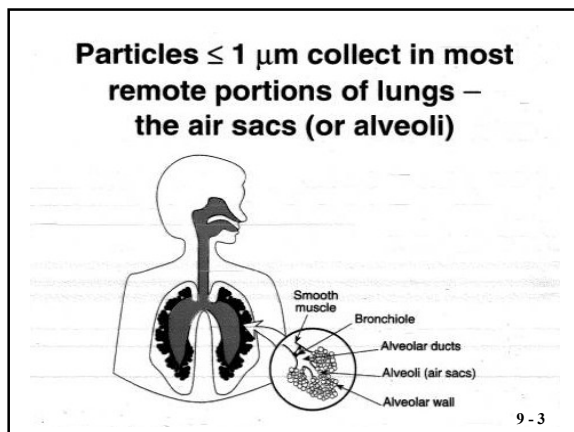




1



2



3

**FRM 201/201A**

**PROBLEM**

Since we are sampling particulate matter, we must stay isokinetically. If you are using cyclones, must use the flow rate design for the cyclone to maintain proper particulate cut size!

9 - 4

4

**FRM 201  
Exhaust Gas Recirculation (EGR)**

- 40CFR51, Appendix M
- $Q_c = Q_s + Q_r$  to maintain constant cut size
- Sample isokinetically at each sample point

9 - 5

5

**FRM 201  
Exhaust Gas Recirculation (EGR)**

- Must use cyclone, in-stack; probe pre-heated
- FRM 5 glassware can be used, so condensibles can be added by FRM 202
- EGR method uses new technology

9 - 6

6

### FRM 201 Exhaust Gas Recirculation (EGR)

- EGR method is recommended if:
  - A total particulate number is also needed because sampling is isokinetically.
  - Stack gas velocities fluctuate

9 - 7

7

### FRM 201 Exhaust Gas Recirculation (EGR)

- EGR modification of FRM 5
  - Nozzle has a recycle attachment
  - The recycle gas is heated to stack temperature
  - Adds in-stack cyclone to capture PM-10
  - Delete out-of-stack filter

9 - 8

8

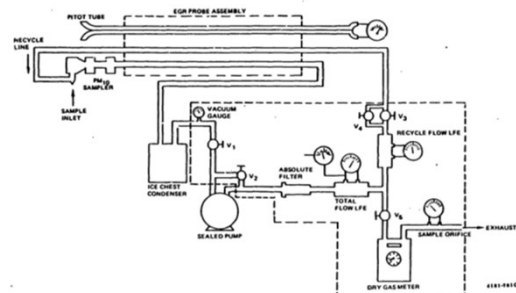
### FRM 201 Exhaust Gas Recirculation (EGR)

- Cyclone does have to be calibrated
- Must leak-check: positive and negative
- Can use condenser rather than FRM 5
- Each point isokinetically and same dwell time

9 - 9

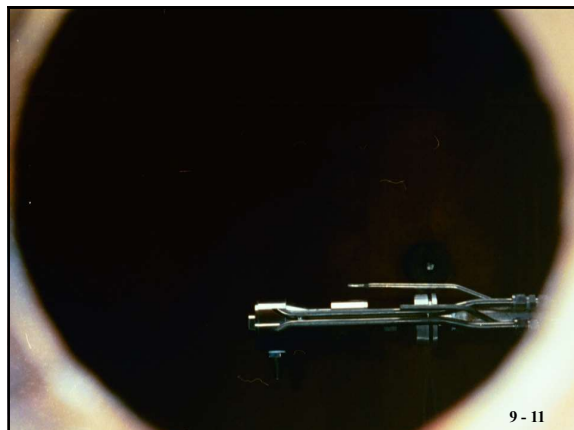
9

### Schematic of EGR Sampling Train



9 - 10

10



11

### FRM 201A Constant Sampling Rate (CSR)

- Uses available equipment
- Sample at constant sampling rate required by the PM-10 cyclone or impactor
- Relaxes FRM 5 +/- 10%, sample within 80 and 120 percent of isokinetic flow based upon stack gas velocity (Must keep sampling rate within delta p min and delta p max)

9 - 12

12

**FRM 201A  
Constant Sampling Rate (CSR)**

- Select nozzle based upon delta p min/max
- Interested in small particles, so isokinetic no as important as FRM 5.
- Dwell time at each point is proportional to stack gas velocity. (sec. 8.7.1)
- Assume a Reynolds number  $N_{RE}$  using Equation 10 in the described CFR method and an estimated sampling rate.

9 - 13

13

**FRM 201A  
Constant Sampling Rate (CSR)**

- Total catch may not be accurate as FRM 5
- Can use impactor or cyclone
- If using impactor, must be calibrated
- FRM 201A can also be used with FRM 202
- CSR is recommended if:
  - Particle sizing is desired
  - Low concentration of PM-10

9 - 14

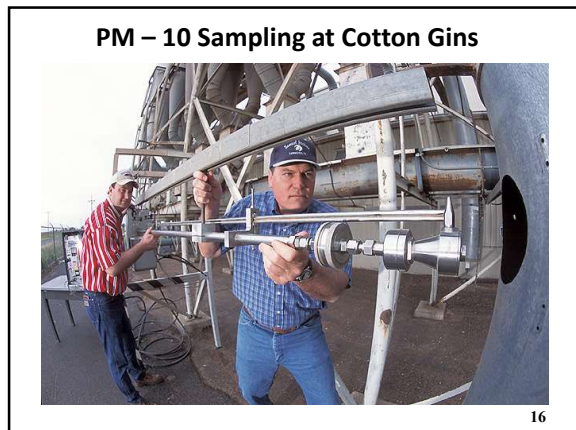
14

**FRM 201A  
Constant Sampling Rate (CSR)**

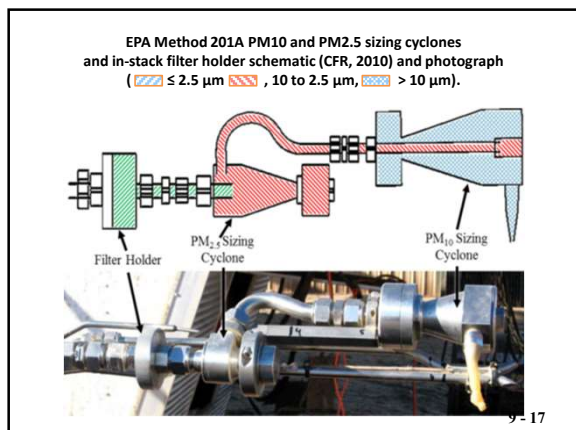
- A 4-inch port should be adequate for the single PM<sub>10</sub> or PM<sub>2.5</sub> sampling apparatus.
- A 4-inch diameter port cannot be use, in any circumstances, when the combined dimension of the cyclone and the exceeds the internal diameter of the port.

9 - 15

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16



17

**FRM 201/201A Review**

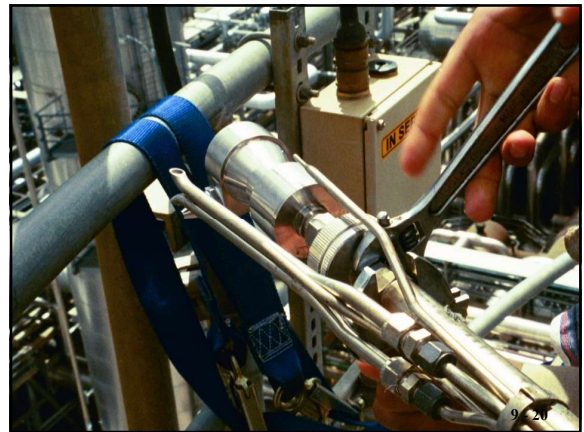
- Both methods measure PM-10 in-stack
- EGR new technology, CSR uses standard test equipment (i.e., FRM 5)

9 - 18

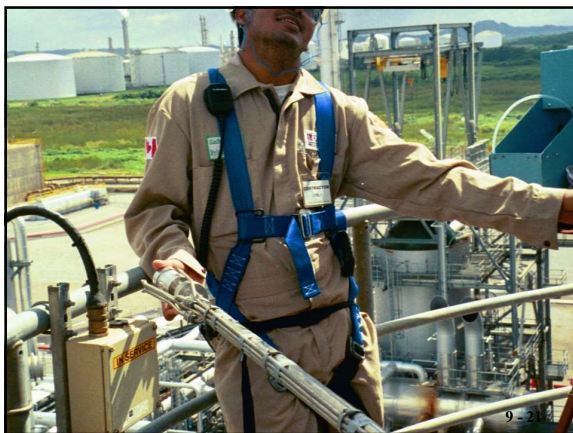
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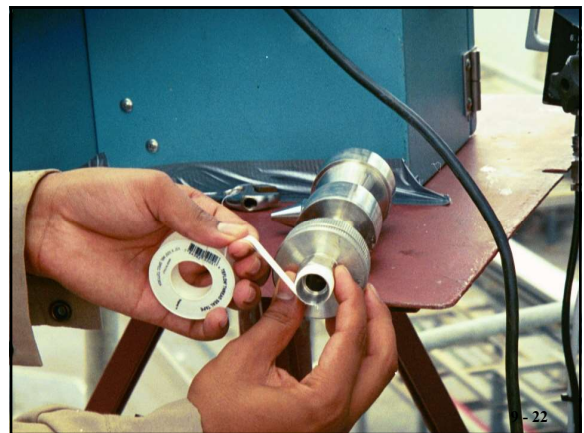
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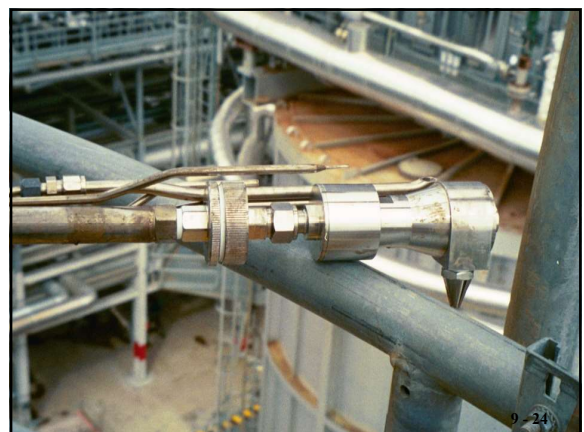
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23



24

### FRM 201/201A Review

- EGR uses a PM-10 cyclone. CSR can use either a cyclone or impactor
- EGR samples isokinetically, therefore total mass is accurate. CSR doesn't sample isokinetically, therefore mass not as accurate

9 - 25

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### FRM 201/201A Review

- If stack velocities fluctuate, the CSR may require more than one sample train
- PM-10 cyclones do not have to be calibrated if they meet design specification. Impactors (201A) must be calibrated

9 - 26

26

### FRM 201/201A Review

- CSR calibration of metering system and leak check procedures same as FRM 5
- CSR requires constant sampling rate and dwell time is proportional to stack gas velocity
- EGR is isokinetically and sampling time same as FRM 5

9 - 27

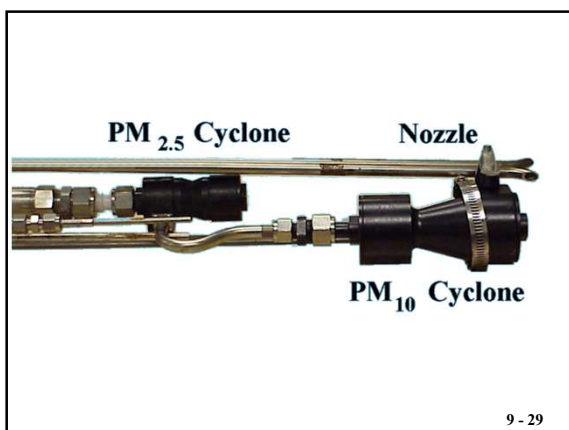
27

### FRM 201A previously CTM-040 Determination of PM-10/PM-2.5

- Predetermined constant sampling rate for combined PM-10 and PM-2.5
- In-stack cyclones used to capture PM-10 and PM-2.5
- Method used with FRM 202

9 - 28

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9 - 29

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### FRM 201A PM-10 and PM-2.5

- Method applies to in-stack measurement of particulate matter equal to or less than PM-10 and PM-2.5
- Use of optimum sampling rate (within limits of flows for PM-10 and PM-2.5 cyclones) near isokinetic conditions
- Methodology uses two in-stack cyclones (PM-10 followed by PM-2.5) followed by ultimate filter

9 - 30

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### FRM 201A PM-10 and PM-2.5

- Sampling train identical to FRM 201A PM-10 except a PM-2.5 cyclone is inserted between the PM-10 cyclone and the ultimate filter
- The particulate mass is determined gravimetrically for each size fraction (i.e., PM-10 cyclone, PM-2.5 cyclone, and < 2.5 filter) after removal of uncombined water

9 - 31

31

### Method for Determination of PM10/PM2.5

- Variations from isokinetic stack conditions maintained with well-defined flow rate
- Filter after PM-2.5 cyclone to trap final particulate matter
- Sampling train is similar to FRM 17
- Sampling rate selected for combined cyclone heads

9 - 32

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### FRM 201A: Method for Determination of PM10/PM2.5

- Flow rate determination for cyclones determined from manufacturer's graph

9 - 33

33

### FRM 201A: Method for Determination of PM10/PM2.5

- Sampling same as FRM 5 (i.e., sample points and time)
- PM-10/PM-2.5 software package available

9 - 34

34

### Cascade Impactors

- The following slide shows a cascade impactor sampling system that is designed for direct measurement of particle size ranges. The circular plates have different size slots or round holes that allow particles smaller than the impaction plate collection to pass through to the next plate, until they are distributed by size on all plates. These are directly weighed.
- The disadvantage for use in measuring PM from Cascade impactors is that it does not work well when the total PM catch is small.

9 - 35

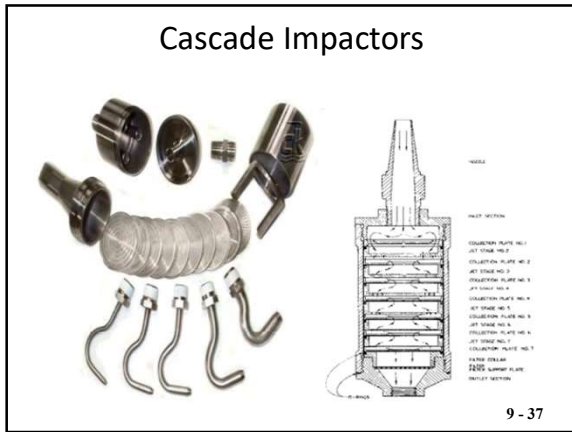
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### Cascade Impactors

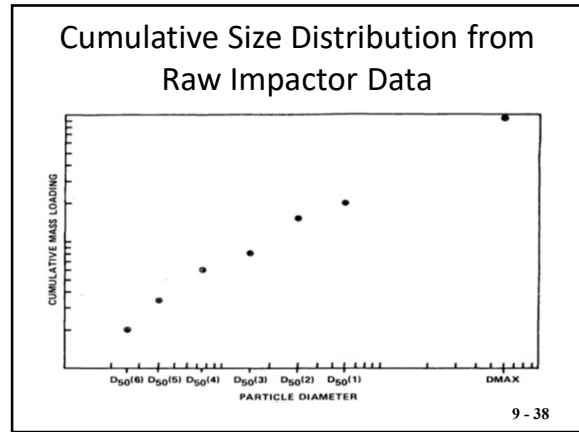
- Another primary alternative that could be used is employing a Method 5 PM train fitted with a polycarbonate filter instead of a glass fiber (the polycarbonate filter traps PM on its surface, whereas the glass fiber allows PM to penetrate into the fiber, making it difficult to see). Selective electron microscopy is then used to count the fraction of different PM size ranges.

9 - 36

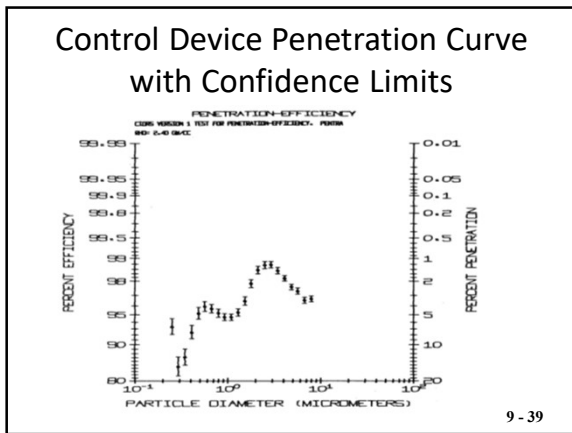
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**U.S. EPA APTI  
Compliance Test and Source Test  
Observation  
F-Factors and Units of the Standard**



10 - 1

1

**Emission Standards for Sources**

- Concentration of stack gas ( $C_s$ )
- Pollutant mass rate (pmr)
- Emission rate (E)
- Process weight rate (R)

10 - 2

2

**Concentration of Stack Gas ( $c_s$ )**

Can be expressed in:

- ppm
- g/dscm
- gr/dscf

10 - 3

3

**For example:**

The New Source Performance  
Standards (NSPS) for asphalt  
concrete plants is:

$0.04 \text{ gr/dscf} \Leftrightarrow 90 \text{ mg/dscm}$

10 - 4

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**Pollutant Mass Rate (pmr)**

Can be expressed in:

- lb/hr
- g/hr

10 - 5

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**Pollutant Mass Rate (pmr)**

$\text{pmr} = \text{Concentration} \times \text{Stack gas volumetric flow rate}$

$$= \frac{\text{lb}}{\text{dscf}} \times \frac{\text{dscf}}{\text{hr}}$$
$$= \frac{\text{lb}}{\text{hr}}$$

10 - 6

6



### Emission Rate (E)

#### Can be expressed in:

- lb/10<sup>6</sup> Btu heat input
- ng/joule heat input

10 - 7

7

The emission rate, in terms of the units given in the New Source Performance Standards (NSPS), is related to concentration and mass rate in the following manner:

$$E = \frac{pmr}{Q_H} = \frac{c_s Q_s}{Q_H}$$

Where:

Q<sub>s</sub> = the stack gas volumetric flow rate (units of ft<sup>3</sup>/hr, m<sup>3</sup>/hr)

Q<sub>H</sub> = the heat input rate, the rate at which combusted fuel supplies heat to the boiler or other heat utilization system (Btu/hr, Kcal/hr) <sup>10 - 8</sup>

8

By dimensional analysis, it can be seen that the units of E in terms of pollutant mass per unit of heat input are:

$$\blacksquare E = \frac{\text{lb/hr}}{10^6 \text{ BTU/hr}} = \frac{(\text{lb/ft}^3) (\text{ft}^3/\text{hr})}{10^6 \text{ BTU/hr}} = \frac{\text{lb}}{10^6 \text{ BTU/hr}}$$

10 - 9

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### For example:

The NSPS emission rate for fossil-fuel fired steam generators (FFFSG) is:

Particulate emissions limited to  
0.03 lb/10<sup>6</sup> Btu.

10 - 10

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#### Reporting In Units Of The Standard: F Factor Methods

To obtain emission rates in units of lb/10<sup>6</sup> Btu, it is necessary for the source sampler to obtain the following information:

1. Pollutant concentration, c<sub>s</sub>
  - a. Pollutant mass captured
  - b. Dry gas volume sampled
2. Effluent volumetric flow rate, Q<sub>s</sub>
  - a. Stack gas velocity
  - b. Stack temperature
  - c. Stack pressure

10 - 11

11

#### Reporting In Units Of The Standard: F Factor Methods

- d. Dry gas composition (Orsat) %CO<sub>2</sub>, %O<sub>2</sub>, %N<sub>2</sub>
- e. Moisture content
3. Heat input rate, Q<sub>H</sub>
  - a. Fuel input rate
  - b. Proximate analysis of fuel

10 - 12

12

**Process Weight Rate (E)**

Can be expressed in:

- lb/tons of product
- kg/metric tons of product

10 - 13

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$$\text{Combustion} = \frac{\text{Pollutant mass rate}}{\text{Heat input Rate}}$$

$$\text{Process} = \frac{\text{Pollutant mass rate}}{\text{Item of mass process rate}}$$

10 - 14

14

**For Example:**

The NSPS for sulfuric acid plants is:

SO<sub>2</sub> emissions limited to 2 kg

SO<sub>2</sub>/ metric ton H<sub>2</sub>SO<sub>4</sub> produced.

10 - 15

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**Concentration Corrected To  
Standard Conditions**

$$C_{\text{corr}} = C_S \frac{P_{\text{std}} T_s}{P_s T_{\text{std}}}$$

10 - 16

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**Correcting Concentration to 12% CO<sub>2</sub>**

$$\bar{C}_{S_{12\%CO_2}} = \bar{C}_S \frac{12}{\%CO_2}$$

10 - 17

17

**Correcting Concentration to 6% O<sub>2</sub>**

$$\bar{C}_{S_{6\%O_2}} = \frac{\bar{C}_S (20.9 - 6.0)}{20.9 - \%O_2}$$

10 - 18

18

Correcting Concentration to 3% O<sub>2</sub>

$$c_s (3\%O_2) = \frac{18c_s}{21 - \%O_2}$$

10 - 19

19

Excess Air Correction Factor

$$\%EA = \frac{\%O_2 - 0.5\%CO}{0.26\%N_2 - \%O_2 + 0.5\%CO} \times 100$$

$$c_s (\text{corr}) = c_s \left( \frac{150}{100 + \%EA} \right)$$

10 - 20

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Method 19  
F Factor Methods

10 - 21

21

Reporting in Units of Standard: F  
factor Methods

- The F factor is used in calculating particulate emission levels from new stationary sources.
- It was promulgated in the October 6, 1975
- The F factor is intended to reduce the amount of data necessary to calculate particulate emissions in terms of the standard expressed as pounds per million Btu heat inputs (lb/10<sup>6</sup> Btu).
- An F factor is the ratio of the gas volume of the products of combustion to the heat content of the fuel.

10 - 22

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Reporting in Units of Standard: F  
factor Methods

- The dry F factor (Fd) includes all products of combustion less water,
- The wet F factor (Fw) includes all products of combustion, and
- The carbon F factor (Fc) includes only carbon dioxide.

10 - 23

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Reporting in Units of Standard: F  
factor Methods

- All of the quantities for c<sub>s</sub> and Q<sub>s</sub> are obtained in a source test
- Q<sub>H</sub>, may not be easily obtained.
- The accuracy the source fuel flow and analysis representative may be difficult to determine
- F factors are based on simple principles of combustion

10 - 24

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**Reporting in Units of Standard: F factor Methods**

- Developed to avoid many of the problems involved in the calculation of E. By using the F factors, E may be obtained from a formula such as the following.
- $E = c_s F_d [20.9 / (20.9 - \%O_2)]$
- Where  $F_d$  is the dry F factor
- The F factor essentially replaces the ratio  $Q_s / Q_H$  and the term in brackets is merely a excess air correction.

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**Reporting in Units of Standard: F factor Methods**

- F factors are useful in calculating emissions for particulate matter.
- In their application to continuous monitoring instrumentation for gases, it is even more valuable.
- $F_d$  factors and its variants ( $F_c$  and  $F_w$  factors) are useful in reporting continuous monitoring data in terms of lb/10<sup>6</sup> Btu heat input

10 - 26

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**Reporting in Units of Standard: F factor Methods**

- F factors enables the source operator to monitor only the pollutant gas concentration and the oxygen or carbon dioxide concentrations.
- Without this method, it would be necessary to continuously monitor stack gas velocity, temperature, fuel input rate, and so on.
- This would be possible, but impractical and expensive

10 - 27

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**Reporting in Units of Standard: F factor Methods**

- Before proceeding with the derivation of the F factors, it is necessary to give a few definitions used in combustion analysis, namely those for proximate analysis, ultimate analysis, and gross calorific value. The definitions generally apply to the fuel "as received" at the plant.

10 - 28

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**Reporting in Units of Standard: F factor Methods**

- Proximate analysis is a fuel analysis procedure that expresses the principal characteristics of fuel as follows:
 

1. % moisture	}	Total 100%	5. % sulfur
2. % ash			6. Heating value (BTU/lb)
3. % volatile matter			7. Ash fusion temperature
4. % fixed carbon			

10 - 29

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**Reporting in Units of Standard: F factor Methods**

- Ultimate analysis is the determination of the exact chemical composition of the fuel. The analysis is generally given in terms of percent hydrogen, percent carbon, percent sulfur, percent nitrogen, and percent oxygen.
- Gross calorific value (GCV), also termed the "high heating value," is the total heat obtained from the complete combustion of a fuel, referred to a set of standard conditions. The GCV is obtained in the proximate analysis as the "heating value."

10 - 30

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### Reporting in Units of Standard: F factor Methods

- $Q_s = (\text{correction air excess}) \frac{V_t}{Q_H}$   
GVC

Dimensionally, this says

$$\frac{\text{ft}^3/\text{hr}}{\text{BTU/hr}} = \frac{\text{ft}^3}{\text{hr}}$$

$Q_s$  and  $Q_H$  can be determined at the source.  $V_t$  is obtained from the ultimate analysis of the fuel.

10 - 31

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### Reporting in Units of Standard: F factor Methods

- Remembering the first equation given in this lesson,
- $E = c_s Q_s / Q_H$
- and through substitution
- $E = c_s V_t \frac{1}{\text{GCV} (\text{excess air correction})}$

The quantity  $V_t/\text{GCV}$  is then defined as the  $F_d$  factor and the following simplified equation is obtained:  $E = (c_s F_d) 1/(\text{excess air correction})$

10 - 32

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### Reporting in Units of Standard: F factor Methods

- For Method 5, the oxygen concentration of the source must be determined simultaneously and at the same traverse. Since the excess air correction using percent oxygen is:
- $(20.9 - \% O_2) / 20.9$
- and the equation to be used for calculating emissions for Method 5 is:
- $E = (c_s F_d)(20.9/20.9 - \% O_2)$

10 - 33

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### Reporting in Units of Standard: F factor Methods

- Since there are different types of F factors (see Table below). The differences arise in the way in which the excess air corrections are determined.
- It should also be noted that the F factor method may be used with the percent  $O_2$  and  $c_{ws}$  determined on a wet basis if the moisture content  $B_{ws}$  of the stack is known:
- $E = (c_{ws} F_d) ((20.9/20.9(1 - B_{ws}) - \% O_2))$
- *Note:* The subscript w stands for measurements made on a wet basis.

10 - 34

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### F Factors Table

Factor	Excess Air Units	Measurement Required for Emissions Determination	Calculations	Comments
$F_d$	$\frac{\text{dscf}}{10^6 \text{Btu}}$	% $O_2$ (dry basis)	$E = c_s F_d \left[ \frac{20.9}{20.9 - \%O_{2d}} \right]$	$c_s$ determined on dry basis
$F_c$	$\frac{\text{dscf}}{10^6 \text{Btu}}$	% $CO_2$ (dry or wet basis)	$E = c_s F_c \left[ \frac{100}{\%CO_{2d}} \right]$	$c_s$ on dry or wet basis consistent with $CO_2$ measurement
$F_w$	$\frac{\text{wscf}}{10^6 \text{Btu}}$	% $O_2$ (wet basis)	$E = c_{ws} F_w \left[ \frac{20.9}{20.9(1 - B_{ws}) - \%O_{2w}} \right]$	The "wet" F factor, $c_{ws}$ and % $O_2$ on wet basis $B_{ws}$ = average moisture content of ambient air
$F_o$	---	---	$F_o = \frac{20.9 F_d}{100 F_c} = \frac{20.9 - \%O_2}{\%CO_2}$	Miscellaneous factor useful for checking Orsat data <b>10 - 35</b>

35

### Calculation and Tabulation of F Factors

The  $F_d$  factor method carries with it the assumption that  $V_t/\text{GCV}$ , the ratio of the quantity of dry effluent gas generated by combustion to the gross calorific value, is constant within a given category. This ratio, of course, is the  $F_d$  factor.

$V_t$  is determined from the stoichiometry of the combustion reaction. If a hydrocarbon is burned in air, gaseous products will result; the volumes of which can be calculated. For example,

$$\text{C}_3\text{H}_8 + \text{O}_2 + \text{N}_2 \rightarrow \text{CO}_2 \uparrow + \text{H}_2\text{O} \uparrow + \text{N}_2 \uparrow$$

propane      air              gases

For each pound of fuel undergoing perfect combustion, a known amount of gaseous products will result. Using the stoichiometric relationships resulting from chemical reactions (similar to the preceding example) and given the gross calorific value of the fuel per pound, the following relationships have been developed for the F factors.

10 - 36

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### Calculation and Tabulation of F Factors

- The  $F_d$  factor method based on the assumption that  $V_t/GCV$ , is constant within a given category.
  - $V_t$  is determined from the stoichiometry of the combustion reaction. When hydrocarbons are burned in air, gaseous products will result and the volumes can be calculated. For example,
  - $C_3H_8 + O_2 + N_2 \rightarrow CO_2 \uparrow + H_2O \uparrow + N_2 \uparrow$   
Propane Air Combustion Gases
- For each pound of fuel undergoing perfect combustion, a known amount of gaseous products will result. 10 - 37

37

### Calculation and Tabulation of F Factors

$$F_d = \frac{227.0 (\%H) + 95.7 (\%C) + 35.4 (\%S) + 8.6 (\%N) - 28.5 (\%O)}{GCV} \quad (\text{metric units})$$

$$F_d = \frac{10^6 [3.64 (\%H) + 1.53 (\%C) + 0.57 (\%S) + 0.14 (\%N) - 0.46 (\%O)]}{GCV} \quad (\text{English units})$$

$$F_c = \frac{20.0 (\%C)}{GCV} \quad (\text{metric units})$$

$$F_c = \frac{321 \times 10^6 (\%C)}{GCV} \quad (\text{English units})$$

$$F_w = \frac{347.4 (\%H) + 95.7 (\%C) + 35.4 (\%S) + 8.6 (\%N) - 28.5 (\%O) + 13.4 (\%H_2O)}{GCV_w}$$

$$F_d = \frac{10^6 [5.56 (\%H) + 1.53 (\%C) + 0.57 (\%S) + 0.14 (\%N) - 0.46 (\%O) + 0.21 (\%H_2O)]}{GCV_w} \quad 10 - 38$$

38

### Calculation and Tabulation of F Factors

If the source utilizes a combination of fossil fuels, a simple addition procedure can be used to compute the F factor.

$$F = xF_1 + yF_2 + zF_3$$

Where:  $x, y, z$  = the fraction of total heat input derived from gaseous, liquid, and solid fuels, respectively

$F_1, F_2, F_3$  = the value of F for gaseous, liquid, and solid fossil fuels, respectively

10 - 39

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### Calculation and Tabulation of F Factors

- Several F factors have been calculated for various types of fossil and waste fuels. It has been found that for a given type of fuel the F factor does not vary over a significantly large range. In general, it has been reported that the  $F_d$  factor can be calculated to within a  $\pm 3\%$  deviation and the  $F_c$  factor can be calculated to within a  $\pm 5.9\%$  deviation. The calculated factors are given in the Table below.

10 - 40

40

### F Factors for Various Fuels

Fuel Type	$F_d$		$F_w$		$F_c$	
	dscm/j	dscf/10 <sup>6</sup> Btu	wscm/j	wscf/10 <sup>6</sup> Btu	scm/j	scf/10 <sup>6</sup> Btu
Coal:						
Anthracite <sup>2</sup> .....	2.71x10 <sup>-7</sup>	10,100	2.83x10 <sup>-7</sup>	10,540	0.530x10 <sup>-7</sup>	1,970
Bituminous <sup>2</sup> .....	2.63x10 <sup>-7</sup>	9,780	2.86x10 <sup>-7</sup>	10,640	0.484x10 <sup>-7</sup>	1,800
Lignite .....	2.65x10 <sup>-7</sup>	9,860	3.21x10 <sup>-7</sup>	10,950	0.513x10 <sup>-7</sup>	1,910
Oil <sup>3</sup> :	2.47x10 <sup>-7</sup>	9,190	2.77x10 <sup>-7</sup>	10,320	0.383x10 <sup>-7</sup>	1,420
Gas:						
Natural .....	2.43x10 <sup>-7</sup>	8,710	2.85x10 <sup>-7</sup>	10,610	0.287x10 <sup>-7</sup>	1,040
Propane .....	2.34x10 <sup>-7</sup>	8,710	2.74x10 <sup>-7</sup>	10,200	0.321x10 <sup>-7</sup>	1,190
Butane .....	2.34x10 <sup>-7</sup>	8,710	2.79x10 <sup>-7</sup>	10,390	0.337x10 <sup>-7</sup>	1,250
Wood .....	2.48x10 <sup>-7</sup>	9,240			0.492x10 <sup>-7</sup>	1,830
Wood bark .....	2.58x10 <sup>-7</sup>	9,600			0.516x10 <sup>-7</sup>	1,920
Municipal .....	2.57x10 <sup>-7</sup>	9,570			0.488x10 <sup>-7</sup>	1,820
Solid waste .....						

<sup>1</sup> Determined at standard conditions: 20°C (68°F) and 760 mmHg (29.92 in. Hg)

<sup>2</sup> As classified according to ASTM D388-77

<sup>3</sup> Crude, residual, or distillate

10 - 41

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### Calculation and Tabulation of F Factors

- Three important points that should be made regarding application of the F factor to Method 5 are:
- 1. Only the dry F factor using percent O<sub>2</sub> for the excess air correction may be used in the calculation. The  $F_c$  and  $F_w$  factors may not be used.

10 - 42

42

### Calculation and Tabulation of F Factors

- 2. The oxygen sample is to be obtained simultaneously with the Method 5 run at the same traverse points. This essentially requires that an additional probe be placed along with the Method 5 probe and an additional pump be used to obtain an integrated bag sample over the duration of the run. However, only 12 sample points are required. If there are more than 12 traverse points determined by Method 1, an independent integrated gas sampling train could be used to traverse 12 points in the duct simultaneously with the particulate run.

43

### Calculation and Tabulation of F Factors

- 3. The procedures in 40 CFR Part 60.46 apply to new fossil-fuel fired steam generators (new sources are those constructed or modified after August 17, 1971). For existing fossil fuel steam generators, which are regulated by state standards, the state or local regulations should be checked for application of the F factor method.

10 - 44

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### Other Uses for F Factors

- 1. If values for  $Q_s$  (the stack gas volumetric flow rate), and  $Q_H$  (the heat input rate), are obtained during the source test, as they often are, several cross-checks can be made by comparing various calculated F factor values with the tabulated values. Equations that can be used to do this are as follows.

10 - 45

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### Other Uses for F Factors

$$F_d (\text{calc}) = \frac{Q_s (20.9 - \%O_2)}{Q_H 20.9}$$

$$F_w (\text{calc}) = \frac{Q_{sw} 20.9 (1 - B_{wa}) - \%O_{2w}}{Q_H 20.9}$$

$$F_c (\text{calc}) = \frac{Q_s \%CO_2}{Q_H 100} = \frac{Q_{sw} \%CO_{2w}}{Q_H 100}$$

10 - 46

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### Other Uses for F Factors

- If after calculating  $F_d$ ,  $F_c$ , or  $F_w$ , a large discrepancy exists between the calculated value and the corresponding value in the table, the original data for  $Q_s$ ,  $Q_H$ , and the Orsat data should be checked. This is an easy way of conducting a material balance check.
- 1. Using a tabulated value for  $F_d$ ,  $F_c$ , or  $F_w$  and the data obtained during the stack test for  $Q_s$  and  $\%O_2$ , a value of  $Q_H$  may be obtained from the equations.

10 - 47

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### Other Uses for F Factors

- 2. If ultimate and proximate analyses are available, they may be used to calculate an F factor using one of the equations. The calculated value can then be checked with the tabulated values and should be within 3 to 5% agreement, depending on the type of fuel and F factor.
- The  $F_0$  factor is the ratio
- $F_0 = (20.9/100)(F_d/F_c)$
- $F_0 = (20.9 - O_2)/\%CO_2$
- A value differing from those tabulated would necessitate a recheck of the Orsat data.

10 - 48

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### Errors and Problems in the Use of F Factors

- The following factors may contribute to errors in reporting emissions by using F factors:
- Deviations in the averaged or “midpoint” F factor value itself.
- Errors in the Orsat analysis and the consequent %O<sub>2</sub> and %CO<sub>2</sub> values.
- Failure to have complete combustion of the fuel (complete combustion is assumed in the derivation of all of the F factor methods).

10 - 49

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### Errors and Problems in the Use of F Factors

- Loss of carbon dioxide when wet scrubbers are used affecting the F<sub>d</sub>, F<sub>c</sub> and F<sub>w</sub> factors.
- Addition of carbon dioxide when lime or limestone scrubbers are used, affecting the F<sub>c</sub> factor.
- 

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### Errors and Problems in the Use of F Factors

- Since the F factors given are averaged values, differences in the ultimate analysis between fuel samples could easily account for the deviation. Also an error of a few percent in the oxygen concentration could cause a relatively large error in the value of E, or more importantly, could mean the difference between compliance and noncompliance. A publication by Mitchell and Midgett (1976) entitled “Field Reliability of the Orsat Analyzer,” states:

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### Errors and Problems in the Use of F Factors

- “The results from five collaborative tests of the Orsat method indicate that the use of Orsat data to determine the molecular weight of flue gases is a valid procedure, but the use of such data routinely to convert particulate catches to such reference conditions as 12% CO<sub>2</sub> and 50% excess air may introduce sizeable errors in the corrected particulate loading...”

10 - 52

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### Errors and Problems in the Use of F Factors

- Complete combustion is assumed for the derivation of all F Factor Methods.
- For incomplete combustion when carbon monoxide, are present in the effluent stream, the volume of effluent gas and carbon dioxide per pound of fuel burned will differ from the values used in calculating the F Factors.
- Adjustments to the measured CO<sub>2</sub> or O<sub>2</sub> concentration can be made, which would minimize this error, if the % CO is determined in the flue gas.

10 - 53

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### Errors and Problems in the Use of F Factors

- $(\%CO_2)_{adj} = \%CO_2 + \%CO$
- $(\%O_2)_{adj} = \%O_2 - 0.5 \%CO$
- With these adjustments, the error amounts to minus one-half the concentration of carbon monoxide present.
- Thus, if 1% CO (an extreme case) is present, an error of minus 0.5% is introduced. Without adjusting the CO<sub>2</sub> or O<sub>2</sub> concentration, a combustion source having 11% CO<sub>2</sub>, 1 % CO, and 6% O<sub>2</sub> will result in about plus 9% error for the F<sub>c</sub> Factor Method and about plus 3% for the F<sub>d</sub> Factor and F<sub>w</sub> Factor Methods.

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**Errors in Source Sampling and F factor Examples**

- See Handouts

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**Example F Factor Problem**

- The Bradshaw Furniture Company has an industrial steam generating unit of greater than  $250 \times 10^6$  Btu/hr heat input. The unit fires Bituminous coal and has an extractive CO<sub>2</sub> monitor. Recent testing showed an effluent SO<sub>2</sub> concentration of 750 ppm (wet basis) and 12.8 % CO<sub>2</sub>(dry basis). The average stack moisture content is 7% H<sub>2</sub>O.
- What is the emission rate in lb/10<sup>6</sup> BTU

10 - 56

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**What is the emission rate in lb/10<sup>6</sup> BTU**

- Use F<sub>C</sub> and convert C<sub>SO<sub>2</sub></sub> from ppm to lb/dscf

$$(750 \text{ ppm}) \times \frac{10^{-6} \text{ ft}^3 \text{ SO}_2}{\text{ft}^3 \text{ air/ppm}} \times \frac{(64 \text{ lb SO}_2)}{\text{lb-mole}} \times \frac{(\text{lb-mole})}{392.75 \text{ ft}^3} = 1.22 \times 10^{-4} \text{ lb/dscf}$$

$$1.22 \times 10^{-4} \text{ lb/dscf} \times \frac{(1 \text{ ft}^3 \text{ wet})}{(1 - 0.07) \text{ ft}^3 \text{ dry}} = 1.31 \times 10^{-4} \text{ lb/dscf}$$

$$E = C_s F_C \frac{100}{\text{CO}_2} = 1.31 \times 10^{-4} \text{ lb/dscf} \left( \frac{1800 \text{ ft}^3}{10^6 \text{ BTU}} \right) \left( \frac{100}{12.8} \right)$$

$$= 1.85 \text{ lb SO}_2/10^6 \text{ BTU}$$

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**Concentration Correction Equation Handout & Example Problems**

**APPENDIX D. CONCENTRATION CORRECTION EQUATIONS**

**Introduction**

After a value for the concentration of a pollutant in a flue gas stream is obtained by a reference method test, it is often necessary to correct the value to some standard set of conditions, which is done to compare the data from one source to that of another. Different stack temperatures and different amounts of excess air would make a comparison of the *actual* concentrations almost meaningless. Therefore, terms such as SCFM for "Standard Cubic Feet per Minute" instead of ACFM ("Actual Cubic Feet per Minute") and  $c_s$  (corr. 50% EA) instead of  $c_a$  are generally used when reporting data. Note that in reporting data in units of the standard, E (lbs./10<sup>6</sup> Btu heat input), the pollutant concentration is expressed as pounds per dry *standard* cubic foot and an excess air correction is included in the F factor equation (Chapter 7). In this section, derivations for correcting a concentration to standard conditions, 50% excess air, 12% CO<sub>2</sub>, and 6% O<sub>2</sub> will be given.

10 - 58

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U.S. EPA APTI  
Compliance Test and Source Test  
Observation  
FRM 202 Condensable Particulate  
Matter (CPM)

11 - 1

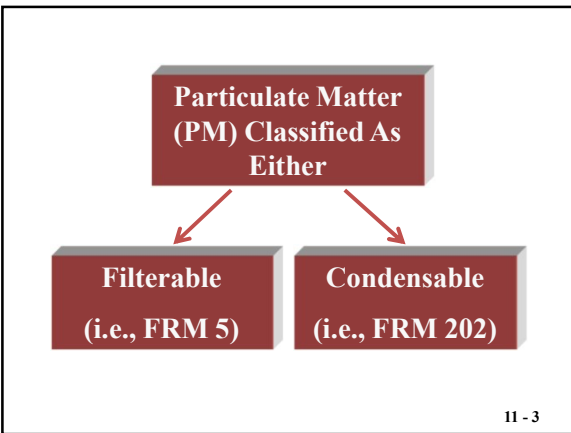
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EPA's Defines Emitted Particulate Matter  
(PM) in 40CFR51.100

*"Particulate matter emissions mean all finely divided solid or liquid materials, other than uncombined water, emitted to the ambient air as measured by an applicable reference method, or an equivalent or alternative method, specified in the regulations, or by a test method specified in an approved State Implementation Plan (SIP)."*

11 - 2

2



3

Basic Measurement Methods for  
Particulate Matter (PM)

- External Heated Filter: Total particulate matter as measured by FRM 5 at defined temperature
- In-stack Filtration: Total particulate matter as measured by FRM 17 at stack temperature and pressure
- In-stack Cyclone: PM<sub>10</sub>/PM<sub>2.5</sub> particulate matter using FRM 201/201A

11 - 4

4

Basic Measurement Methods for  
condensables

- FRM 6: Determination of Sulfur Dioxide Emissions from Stationary Sources
- FRM 8: Determination of Sulfuric Acid Mist and Sulfur Dioxide Emissions from Stationary Sources
- FRM 202: Determination of Condensable particulate Emissions from Stationary Sources

11 - 5

5

Basic Measurement Methods for  
condensables

- Method 315 - Particulate and Methylene Chloride Extractable Matter from Aluminum Production Facilities
- Other Test Method 37 (OTM-37): Measurement of Direct PM<sub>2.5</sub> and PM<sub>10</sub> Emissions at Low Concentrations by Dilution Sampling (Constant Sampling Rate Procedure)

11 - 6

6

Regulatory Background  
CPM

- FRM 8 (1971): New source measurement method for SO<sub>3</sub>/H<sub>2</sub>SO<sub>4</sub> emissions
- PM<sub>10</sub> NAAQS (1987): EPA acknowledges the effect of PM<sub>10</sub> on human health
- FRM 201/201A (1990): New source measurement methods for PM<sub>10</sub> for quantifying emissions

11 - 7

7

Regulatory Background  
CPM

- FRM 202 (1991): EPA acknowledges that some emissions in the vapor phase at stack conditions are converted to the condensed phase (as a liquid or solid) immediately upon discharge into the ambient air and those compounds are not captured on a particulate filter during stack testing

11 - 8

8

Regulatory Background  
CPM

- PM<sub>2.5</sub> NAAQS (1997): EPA acknowledges that effect of fine particulate matter (i.e., PM<sub>2.5</sub>) on human health
- Conditional Test Method 039 (2004): Measurement of PM<sub>2.5</sub> and PM<sub>10</sub> Emissions by Dilution Sampling (Constant Sampling Rate Procedures)

11 - 9

9

Regulatory Background  
CPM

- Conditional Test Method 040 (2004): EPA proposes test method for combined PM<sub>10</sub> and PM<sub>2.5</sub>, now incorporated into Method 201/201A
- Other Test Method 37 (May 2018): Measurement of Direct PM<sub>2.5</sub> and PM<sub>10</sub> Emissions at Low Concentrations by Dilution Sampling (Constant Sampling Rate Procedure)

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Condensable Particulate Matter

- Condensable particulate matter (CPM) consists of species that are emitted from a source in the vapor phase at stack gas temperature but condenses into a liquid or solid aerosol at ambient temperature

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Historical Measurement Methods for  
CPM

- Condensable Particulate Matter by FRM 202: Particulate matter captured in the back half of the FRM 5 sampling train, including water and organic soluble extraction components
- Total Particulate: The sum of the filterable particulate (i.e., front half of the FRM 5 sampling train) and the condensable particulate matter (i.e., the back half of the FRM 5 sampling train, including water and organic soluble extractions)

11 - 12

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### Recent History

- Pre - PM<sub>10</sub> & PM<sub>2.5</sub> NAAQS
  - Recognized condensable PM impact
    - Dust PM was cause of most non-attainment areas for TSP
    - Condensable PM was a small consideration
  - Condensable PM method proposed 1990
    - Was a “Consensus Method” addressing several State specific compliance test methods
    - Incorporates several analytical options

11 - 13

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### Why A Condensable Test Method?

- New NAAQS for particulate matter (PM<sub>2.5</sub>)
- New emission inventories required
- More comprehensive emission factors required

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### Why A Condensable Test Method?

- More comprehensive test methods now required to address non-attainment questions
- Expanded use of dispersion models
- Expanded use of receptor models

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### Components of Direct PM<sub>2.5</sub>

- Filterable PM<sub>2.5</sub>
  - Solid or liquid material at stack temperature and higher (measured at ~250° to 320° F)
  - Stable in atmosphere and collected on ambient sampler
- Condensable PM<sub>2.5</sub>
  - Vapor or gas at stack temperature
  - Condenses to liquid or solid at stack exit
  - Stable in atmosphere and collected on ambient sampler

11 - 16

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### Precursors to Condensables

Ammonia	Nitrates
HCl	Organics
HF	Chlorides
Sulfates	

11 - 17

17

### List of Precursors Reactions to Condensables

- |                                     |   |
|-------------------------------------|---|
| • Condensable Organics              | • $H_xC_y(g) = H_xC_y(a)$                       |
| • SO <sub>3</sub>                   | • $SO_3(g) + H_2O(g) = H_2SO_4(a)$              |
| • SO <sub>3</sub> w/NH <sub>3</sub> | • $SO_3(g) + H_2O(g) + 2NH_3 = (NH_4)_2SO_4(s)$ |

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### List of Potential Precursors Reactions to Condensables

- HCl                      •  $\text{HCl(g)} + \text{H}_2\text{O(g)} = \text{HCl(l)}$
- HF                        •  $\text{HF(g)} + \text{H}_2\text{O(g)} = \text{HF(l)}$
- Trace Metals        •  $\text{M(g)} = \text{M(l)}$  or  $\text{M(s)}$
- Nitrates                •  $\text{NO}_3\text{(g)} + \text{H}_2\text{O(g)} = \text{HNO}_3\text{(l)}$

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### FRM 202 for Measurement of CPM

- Needed to measure CPM instead of solid PM
- Allows the determination of both filterable and Condensable PM simultaneously

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### Condensable Test Method

- Allow for speciation of collected particulate
  - Elements Al through Pb
  - Major Ions (Sulfates, Nitrates, Ammonium, Sodium, Potassium etc.)
  - Total Mass, Carbon (Elemental and Organic)
  - Others (Semi-volatiles, Ds/Fs, PCBs, Volatiles etc.)

11 - 21

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### Reasons to Consider Condensable PM<sub>2.5</sub> Emissions

- Condensable fraction of direct PM<sub>2.5</sub> can be significant
  - 10 to 50 percent of PM<sub>2.5</sub> emissions depending on control measures, temperature, other source-specific conditions

11 - 22

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### Reasons to Consider Condensable PM<sub>2.5</sub> Emissions

- Combustion, metallurgical & wood product sources emit large quantities of vapors that condense to form PM<sub>2.5</sub>
  - Acids (e.g., sulfuric acid from coal combustion)
  - Neutralized acids (e.g.,  $[\text{NH}_4]_2[\text{SO}_4]$ ,  $\text{NH}_4\text{Cl}$ )
  - Organic materials (e.g., alkanes, PAHs, PCBs, PCDDs, acids)
  - Metals (e.g., As, Se, Sb, Pb Compounds)

11 - 23

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### Reasons to Consider Condensable PM<sub>2.5</sub> Emissions

- A small fraction of point sources are responsible for the majority of condensable PM emissions

11 - 24

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### Inventories and PM<sub>2.5</sub> Emissions

- Filterable PM
  - Historically only PM included in databases
  - Some States include filterable PM<sub>10</sub> or PM<sub>2.5</sub>
- Condensable PM
  - Current knowledge is spotty
  - Some SIP databases fail to include PM<sub>cond</sub> (even when required)
  - When PM<sub>cond</sub> included - calculated from emissions factors (e.g., AP-42) that are often based on incorrect test methods

11 - 25

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### Inventories and PM<sub>2.5</sub> Emissions

- Inventories reflect database errors
  - Federal inventory includes some adjustments
  - Underestimate some sources' contributions, overestimate others

11 - 26

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### Issues to Consider for CPM

- Most current regulations do not address PM<sub>cond</sub> Effect on SIP Regulations
  - Focus on filterable PM
  - Force control technology towards filterable PM
- Some regulations do include PM<sub>cond</sub>, but with incorrect test methods

11 - 27

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### Issues to Consider for CPM

- Final rule creates a transition period
  - Regulations addressing PM<sub>cond</sub> encouraged but not required
  - Develop more precise and accurate PM<sub>cond</sub> emissions for inventories and rules

11 - 28

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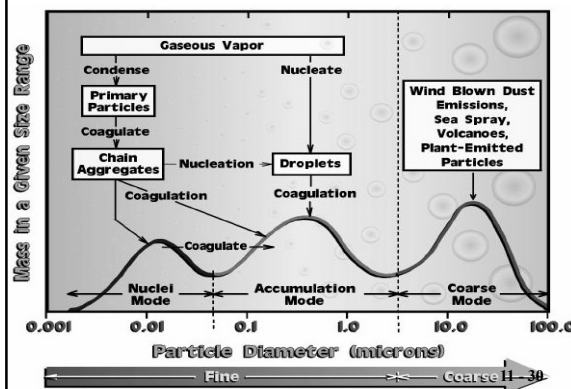
### CPM in Relation to Air Quality Issues

- Potential impacts on PSD review applicability for PM<sub>10</sub> and PM<sub>2.5</sub> (Threshold levels: Rural vs. urban)
- Potential impacts on dispersion modeling analysis
  - Current NAAQS and PSD increments (Class I areas)
  - Monitoring *de minimis* levels
- Visibility impairment (VISCREEN vs. MESOPUFF-II models)
- Human health issues

11 - 29

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### Size Distribution and Sources of Atmospheric Particles.



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### Biases from Condensables

#### Positive

- Some condensables that are not intended to be regulated condense below stack temperature and are collected on heated filter

11 - 31

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### Biases from Condensables

#### Negative

- Some condensables that are to be regulated do not condense at filter temperature and pass through the filter and are not counted

11 - 32

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### Steps to Handle Condensables

- Determine if condensables are to be regulated by applicable emission regulations
- Design proper sampling and analytical procedures to match intention of the regulation

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### Cautions on Condensable Sampling Techniques

- EPA Reference Method 5 sample box temperature may not be an accurate indication of sample gas temperature
- Condensed particulate matter may change its chemical composition after condensation

11 - 34

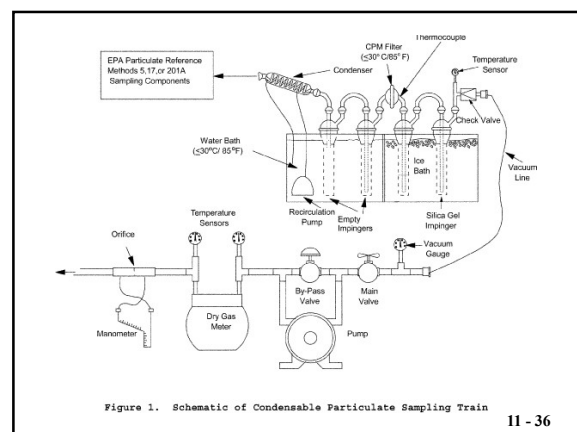
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### Cautions on Condensable Sampling Techniques

- Although temperature is major parameter for collection of condensables, several other factors can greatly affect condensables (i.e., moisture content, dilution air, presence of other compounds)

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### EPA FRM 202

- Used with filterable PM method
- Requires post sample conditioning in field
- Uses existing methodology and equipment
- Is used by several State agencies

11 - 37

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### FRM 202 CPM Sampling Program

- Impinger portion of a FRM 17 type sampling train
- Nitrogen purge to remove dissolved SO<sub>2</sub>

11 - 38

38

### FRM 202 CPM Sampling Program

- 8.5.4.2 CPM Container #1, Aqueous liquid impinger contents. Quantitatively transfer liquid from the dropout and the backup impingers prior to the CPM filter into a clean, leak-proof container Rinse all sampling train components twice with water.

11 - 39

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### FRM 202 CPM Sampling Program

- 8.5.4.3 CPM Container #2, Organic rinses. Follow the water rinses of the back half with an acetone rinse. " Then repeat the entire rinse procedure with two rinses of hexane, and save the hexane rinses in the same container as the acetone rinse.

11 - 40

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### FRM 202 CPM Sampling Program

- 8.5.4.4 CPM Container #3, CPM filter sample. Use tweezers and/or clean disposable surgical gloves to remove the filter from the CPM filter holder. Place the filter in the Petri dish labeled with test identification and "CPM Container #3, Filter Sample."

11 - 41

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### FRM 202 CPM Sampling Program

- 8.5.4.5 CPM Container #4, Cold impinger water. You must weigh or measure the volume of the contents of CPM Container #4 either in the field or during sample analysis (see Section 11.2.4). If the water from the cold impinger has been weighed in the field, it can be discarded.

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### EPA FRM 202

- Requires post sample separation in field
- Requires post sample adjustments in lab
- Limited speciation

11 - 43

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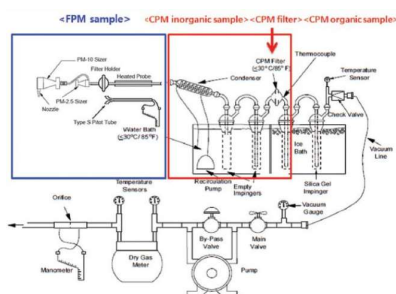
### FRM 202

- FRM 202 is subject to false positive bias because of conversion of non-particulate species into CPM in the method's sampling train

11 - 44

44

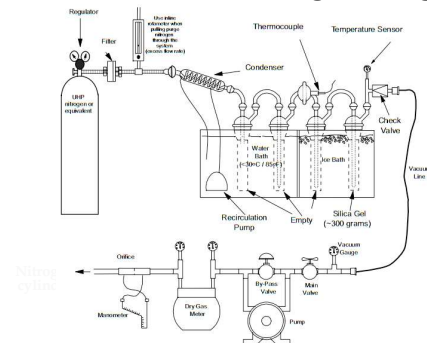
### FRM 202 Sampling Train



11 - 45

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### FRM 202 Post Nitrogen Purge



11 - 46

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### FRM 202 Biases

- Normally noncondensable gases may react with other gases or condensables to form condensable PM
- Oxidation of dissolved  $\text{SO}_2$  in the impinger water to form  $\text{H}_2\text{SO}_4$
- Stabilization of  $\text{H}_2\text{SO}_4$  with  $\text{NH}_4\text{OH}$  when pH of the impinger solution is  $> 4.5$

11 - 47

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### FRM 202 Biases

- Use of water impingers to concentrate condensibles has bias given the potential to affect chemical reaction rate. Chemical reaction rates generally increase with concentration

11 - 48

48

### % Condensable Particulate Matter (FRM 202)

Source Category	% of Total Catch in Back Half
Fossil fuel fired gen.	50
Incinerator	20-30
Asphalt Plant	40-85
Smelters	35-85

11 - 49

49

### Results of FRM 202 For Condensables

- Coal-burning Boilers: condensables were ~76 % of the total PM<sub>10</sub> stack emissions
- Oil/Natural Gas/Kerosene Combustion Turbines: condensables were ~ 68 % of the total PM<sub>10</sub> stack emissions
- Oil/Natural Gas Boilers: condensables were ~ 49 % of the total PM<sub>10</sub> stack emissions

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### FRM 202 Testing Conclusion

- Condensable particulate matter (CPM) is composed mostly of inorganic matter, independent of source type (boiler or turbine) or fuel burned (coal, oil or natural gas)
- Inorganic matter is composed of mostly sulfate associated compounds

11 - 51

51

### FRM 202 Testing Conclusion

- Close relationship between ambient sulfate concentrations and fine PM (i.e., PM)
- Based on review of FRM 202 stack tests, the condensable PM emissions can make a significant contribution PM constitutes a portion of the total PM<sub>10</sub> emissions from Fossil Fuel-Fired Steam Generators (FFSGs)

11 - 52

52

### Special Considerations When Using Method 202

- May not be applicable at sources that emit high levels of ammonia
- If SO<sub>2</sub> is present, the sample must be purged with N<sub>2</sub>, but recent studies indicate that not all the SO<sub>2</sub> is purged from the impingers

11 - 53

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### EPA Activities to Resolve PM<sub>cond</sub> Test Methods Issues

- Recommending use of Method 202 with purge and use of condensable PM<sub>2.5</sub>

<https://www.epa.gov/sites/production/files/2016-06/documents/m-202.pdf>

- Assessing “improvements” to Method 202
  - Apply technologies tested in Canada and US
  - Reduce artifacts from ~10 mg to >2 mg

11 - 54

54

EPA Activities to Resolve  
PM<sub>cond</sub> Test Methods Issues

- Revise M202 in Appendix M
  - More precise (no options)
  - More accurate (reduce artifacts)
  - Post on EPA/EMC web site in July 2007
  - Propose in 2007/2008
  - Promulgate 2008/2009

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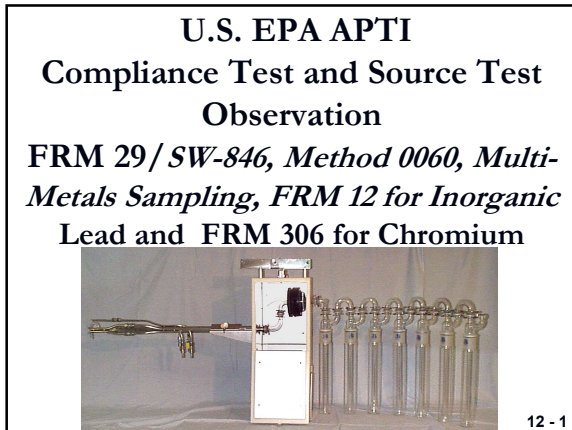
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EPA Updated Method 202

- Recommending use of Method 201A (existing filterable PM<sub>10</sub> test method) with supplemental hardware for filterable PM<sub>2.5</sub> added to updated 202
- Revise Method 202 in Appendix M
  - Add filterable PM<sub>2.5</sub> measurement
  - Add condenser followed by dry impingers
  - First two impingers in water
  - Second two impingers in ice water
  - Promulgate 2008/2009

11 - 56

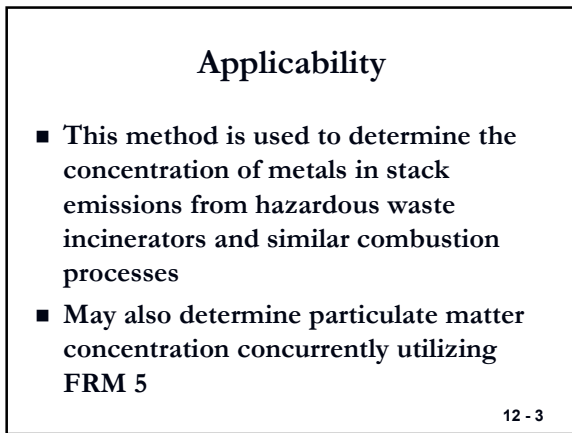
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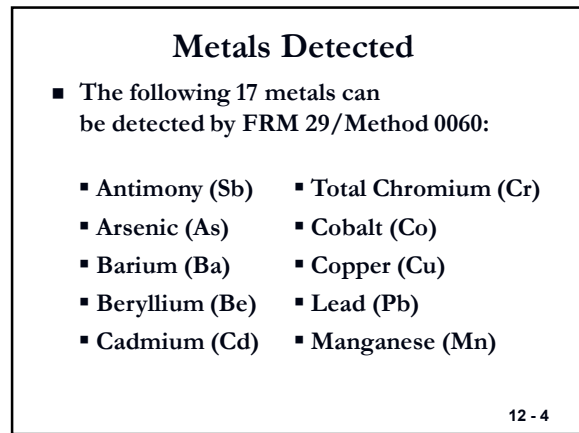
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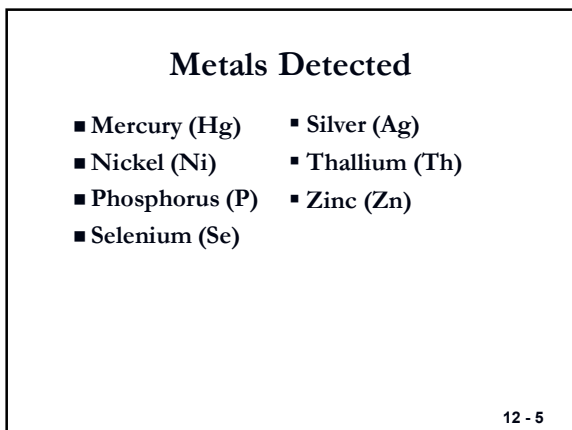
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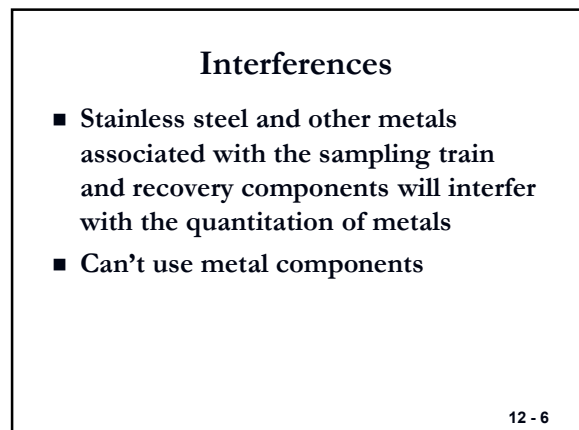
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5



6

**Interferences**

- Spectral interferences can be minimized through the proper selection of analytical methodology
- “Dated” reagents may provide high metal background concentration, thus, high bias

12 - 7

7

**FRM 29/Method 0060 Design Requirements**

- Gas flow measurement system (FRM 2-4)
- Modified Method 5 sampling train
- Addition of three more impingers

12 - 8

8

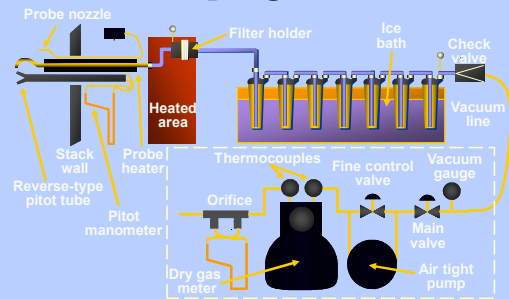
**FRM 29/Method 0060 Sampling Train**

- Probe with quartz nozzle and liner
- Pitot tube/temperature sensor array
- Heated filter assembly
- Seven impingers
- Pump/dry gas meter/orifice assembly

12 - 9

9

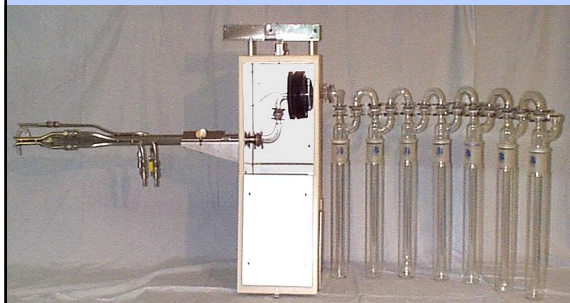
**FRM 29/Method 0060 Sampling Train**



12 - 10

10

**FRM 29/Method 0060 Sampling Train**



12 - 11

11

**FRM 29/Method 0060 Operational Requirements**

- See Field Observation Checklist
- Multi-point integrated sampling
- Isokinetic sampling rate
- 2-hr sample with minimum sample volume of 45 cf

12 - 12

12

**FRM 29/Method 0060  
Operational Requirements**

- Probe/filter at 120°C (248°F)
- PM metals (and FRM5 PM) collected in front half, gaseous metals collected in back half

12 -13

13

**FRM 29/Method 0060  
Operational Requirements**

- Recovery of front half and back half separate
- Samples are acid digested to dissolve inorganics and remove organic constituents
- If stack gas moisture < 100 mL, then can eliminate first impinger

12 - 14

14

**FRM 29/Method 0060  
Impinger Arrangement**

- 1st Impinger- empty (Optional)
- 2nd & 3rd Impinger- 5% HNO<sub>3</sub>/10% H<sub>2</sub>O<sub>2</sub> (vapor multi-metals)
- 4th Impinger- empty

12 - 15

15

**FRM 29/Method 0060  
Impinger Arrangement**

- 5th & 6th Impinger- 4% KMnO<sub>3</sub>/10% H<sub>2</sub>SO<sub>4</sub> (For mercury vapor)
- 7th Impinger- Silica gel

12 - 16

16

**FRM 29/Method 0060  
Glassware Preparation**

- Hot tap water rinse
- Wash with hot soapy water
- Rinse 3 times with tap water, then 3 times with cleaned, DI water
- Soak in 10% HNO<sub>3</sub> for 4 hours

12 - 17

17

**FRM 29/Method 0060  
Glassware Preparation**

- Rinse 3 times with cleaned, DI water
- Rinse with acetone and air dry
- All openings covered with paraffin until used

12 - 18

18

**FRM 29/Method 0060  
Sample Train Requirements**

- Glass or Teflon® nozzle
- Nonmetallic probe line
- Nonmetallic brushes

12 - 19

19

**FRM 29/Method 0060  
Sample Train Requirements**

- Daily preparation of  $\text{KMnO}_4$  solution
- Polypropylene tweezers
- Storage bottles of glass with Teflon lined caps

12 - 20

20

**FRM 29/Method 0060 Operation**

- Preliminary field determination (sample location, nozzle size, probe length) same as FRM 5
- Sample train preparation (charging of impingers etc.) same as FRM 5

12 - 21

21

**FRM 29/Method 0060 Operation**

- Prevent  $\text{KMnO}_4$  from contacting other glassware and prevent  $\text{H}_2\text{O}_2$  from mixing with  $\text{KMnO}_4$
- Leak check in accordance with FRM 5
- Sample collection in general accordance with FRM 5

12 - 22

22

**FRM 29/Method 0060 Operation**

- No metal components in the sample train and during sample recovery

12 - 23

23

**FRM 29/Method 0060 Sample  
Train  
Recovery Containers**

- 1- Petri Dish (Filter)
- 2- Acetone rinse from probe nozzle/liner, and front half of filter holder (exactly 100 mL)
- 3-  $\text{HNO}_3$  rinse of probe nozzle/liner, and front half of filter holder (exactly 100 mL)

12 - 24

24

**Sample Train  
Recovery Containers**

4- Combined impingers 1, 2 and 3 (measured) and HNO<sub>3</sub> acid rinse of impingers and back half of filter holder (exactly 100 mL)

12 - 25

25

**Sample Train  
Recovery Containers**

5A- Impinger 4 (measured) and HNO<sub>3</sub> rinse of impinger 4 (100 mL)  
5B- KMnO<sub>4</sub> impingers contents (measured) and KMnO<sub>4</sub> (100 mL) + water (100 mL)

12 - 26

26

**Sample Train  
Recovery Containers**

5C- 8 M HCl (25 mL) rinse of the two impingers and transferred to container containing water (200 mL)

12 - 27

27

**Sample Train  
Recovery Containers**

6- Silica gel contents (note color, weigh)  
7- Acetone blank (100 mL)  
8A- HNO<sub>3</sub> reagent blank (300 mL)  
8B- Water reagent blank (100 mL)

12 - 28

28

**Sample Train  
Recovery Containers**

9- 5 % HNO<sub>3</sub>/10% H<sub>2</sub>O<sub>2</sub> reagent blank (200 mL)  
10- KMnO<sub>4</sub> reagent blank (100 mL)  
11- 8 M HCl reagent blank (200 mL of water + 25 mL of 8 M HCl)  
12- Filter blank

12 - 29

29

**Analysis**

- Weigh filter if need FRM 5 PM
- Acid digestion of filter and sample train recovery reagents
- Analysis by Inductively Coupled Argon Plasma (ICAP) for all metals (except mercury)
- Aliquots taken of recovery reagents for mercury analyzed by Cold Vapor Atomic Absorption Spectroscopy (CVAAS)

12 - 30

30



**Calculation**

- $M(i) = (C)(F)(V)$   
where:
  - C = concentration of metal from calibration curve, ug/mL
  - F = dilution factor
  - V = total volume of digested sample

12 - 31

31

**Calculation**

- Total metal concentration in sample train:  
 $M(f) = [M(ifah)-M(fhb)] + [M(ibh)-M(bhb)]$
- where:
  - M(f) = total mass of each metal in complete sample train
  - M(ifah) = total mass of each metal in front half (fh) of sample train

12 - 32

32

**Calculation**

$M(f) = [M(ifah)-M(fhb)] + [M(ibh)-M(bhb)]$

- M(fhb) = total metal found in front half blank
- M(ibh) = total metal found in back half of sampling train
- M(bhb) = total metal found in back half blank

12 - 33

33

**Calculation**

- Stack gas concentration is calculated:
  - $C(\mu\text{g}/\text{m}^3) = M(\mu\text{g}) / (\text{Std. volume of gas sampled, m}^3)$

12 - 34

34

**FRM 29/Method 0060 Key Points**

- All active sample train components must be made of glass or Teflon® (no metal components)
- All active sample train components must be cleaned through a detailed clean-up scheme

12 - 35

35

**FRM 29/Method 0060 Key Points**

- FRM 5 PM can also be determined concurrent with Method 0060
  - Front half of train: particulate metals
  - Back half of train: gaseous metals
- If not sampling for mercury, do not need impingers 4, 5 & 6 in the sample train

12 - 36

36

**FRM 29/Method 0060**

**Key Points**

- Storage containers must be made of glass with Teflon®-lined caps
- Front half of train captures particulate metals while back half captures gaseous metals
- Imperative to use exactly 100 mL of rinsing solutions for blank correction in final concentration calculation

12 - 37

37

**FRM 29/Method 0060**

**Key Points**

- If sampling for total metals only (not FRM 5 PM), then filter does not have to be desiccated or weighed
- Do not need 1st impinger if water is determined to be < 100 mL
- Impinger reagents made daily
- Must use exact volume of rinses for background correction

12 - 38

38

**FRM 29/Method 0060**

**Key Points**

- Special cleaning of glassware
- Exact blank volumes/composition must be acquired for blank correction

12 - 39

39

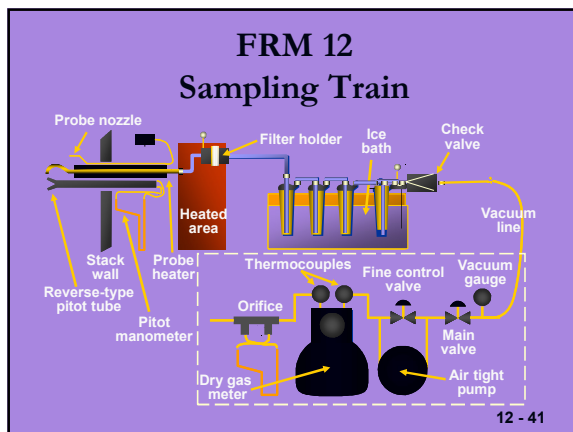
**U.S. EPA APTI  
Compliance Test and Source Test  
Observation  
Course #468**

**FRM 12, Inorganic Lead**

12 - 40

40

**FRM 12  
Sampling Train**



12 - 41

41

**40CFR63, Subpart X: National  
Emission Standards for  
Secondary Lead Smelters**

- 06/09/94: Proposed rule
- 06/23/95: Final rule for new and existing secondary lead smelters
- 06/13/97: Direct final rule (Amendments to final rule)
- 08/18/99: Proposed amendments Title V
- 12/14/99: Final rule

12 - 42

42

### Test Methods Identification

- FRM 1: Port location
- FRM 2: Volumetric flow rate
- FRM 3 or 3A: Correct conc. meas.
- FRM 4: Moisture content
- FRM 12: Determination of inorganic lead

12 - 43

43

### FRM 12 Applicability

- This method is used to determine the concentration of particulate matter (PM) lead and gaseous lead emissions from stationary sources
- Sources comprise mostly of 23 smelters (15 major and 8 area sources) located in 13 states

12 - 44

44

### Summary of Method

- FRM 5 sample train with glass nozzle and probe liner
- Filter temperature maintained @ 248°F
- Particulate lead caught on filter while gaseous lead caught in impingers
- Analysis by acid digestion followed by flame atomic absorption (FAA)

12 - 45

45

### FRM 12 Design Requirements

- Gas flow measurement system (FRM 1-4)
- FRM 5 sampling train
- Operated isokinetically

12 - 46

46

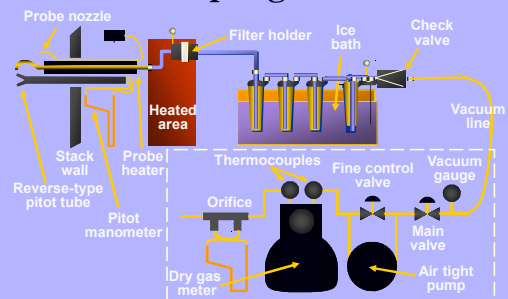
### FRM 12 Sampling Train

- Probe with quartz nozzle and liner
- Pitot tube/temperature sensor array
- Heated filter assembly
- Standard FRM 5 impingers with impingers 1 and 2 containing 100 mL of 0.1 HNO<sub>3</sub>
- Pump/dry gas meter/orifice assembly

12 - 47

47

### FRM 12 Sampling Train



12 - 48

48

### Sample Recovery

- FRM 12 Recovery
  - Container #1: Recover filter for lead PM same as FRM 5
  - Container #2: Front-half 0.1 N HNO<sub>3</sub> rinse up to front-half filter compartment
  - Container #3: Note color of silica gel to determine whether it has been completely spent. Transfer the silica gel to its original container, weigh on site or transport back to laboratory for weighting

12 - 49

49

### Sample Recovery

- FRM 12 Recovery
  - Container #4: Measure and collect the impinger nitric acid solutions from first three impingers; Rinse twice with 30 mL 0.1 N HNO<sub>3</sub> each impinger and collect in container #4
  - Container #5: Reagent blank of 200 mL of 0.1 N HNO<sub>3</sub>

12 - 50

50

### Sample Analysis

- Container #1: Filter cut into strips and digested with 10 mL of 50% of HNO<sub>3</sub>, heat on hot plate, add 10 mL of 3 % H<sub>2</sub>O<sub>2</sub> and 50 mL of DI water, heat for 20 minutes. Filter and dilute to 100 mL. Also must determine filter blank (FB) with 2 unexposed filters from same lot following same procedure

12 - 51

51

### Sample Analysis

- Containers #2 and #4: Transfer to Erlenmeyer flask, heat on hot plate to dryness, add 30 mL of 3 % H<sub>2</sub>O<sub>2</sub> and 50 mL of hot DI water, heat for 20 minutes. Filter and dilute to 250 mL

12 - 52

52

### Sample Analysis

- Container #3: Weigh silica gel to nearest 0.5 grams ( $B_{ws}$ )
- Container #5: Dry the 200 mL on a steam bath to dryness, add 15 mL of 50 % H<sub>2</sub>O<sub>2</sub> and 50 mL of hot DI water, dilute to a total volume of 100 mL

12 - 53

53

### Sample Analysis

- Flame Atomic Absorption (FAA)
  - Calibration of FAA using standard solutions
  - Check matrix effects by using the method of additions
    - Spiked sample vs. unspiked sample
  - Stability of calibration curve
    - Run a blank and standard after every 5<sup>th</sup> sample

12 - 54

54

### FRM 12

#### Operational Requirements

- See Field Observation Checklist for FRM 5
- Multi-point integrated sampling
- Isokinetic sampling rate
- 1-hr sample with minimum sample volume of 45 cf

12 - 55

55

### FRM 12

#### Operational Requirements

- Probe/filter at 120°C (248°F)
- Lead PM collected on front-half of sampling train, while gaseous lead collected in impingers

12 - 56

56

### FRM 12

#### Impinger Arrangement

- 1<sup>st</sup> and 2<sup>nd</sup> Impinger- 100 mL 0.1 N HNO<sub>3</sub>
- 3<sup>rd</sup> Impinger- Dry
- 4<sup>th</sup> Impinger- 200-300 g silica gel

12 - 57

57

### FRM 12 Operation

- See Field Observation Checklist for FRM 5
- Preliminary field determination (sample location, nozzle size, probe length) same as FRM 5
- Sample train preparation (charging of impingers etc.) same as FRM 5

12 - 58

58

### FRM 12 Operation

- Pre-/post leak check in accordance with FRM 5
- Sample collection in general accordance with FRM 5
- Sample recovery in general agreement with FRM 5 except rinsing with 0.1 N HNO<sub>3</sub>

12 - 59

59

### FRM 12 Key Points

- All active sample train components must be made of glass (no mention of Teflon components)
- All active sample train components must be cleaned

12 - 60

60

### FRM 12 Key Points

- FRM 5 PM can be determined concurrent with FRM 12
  - Front half of train: particulate matter (PM) with acetone rinse
  - Impinger solution: 0.1 N HNO<sub>3</sub>
  - Use of glass fiber filter with low background lead concentration
  - Treat and analyzes the entire sample train contents, including the impingers, for lead

12 - 61

61

### FRM 12 Key Points

- FRM 17 may be used provided that:
  - Use of glass-lined probe and at least 2 impingers each containing 100 mL of 0.1 N HNO<sub>3</sub> after the in-stack filter
  - Recovery of probe and impinger contents for lead. Recovery of sample from the nozzle with acetone if a PM determination is to be made

12 - 62

62

### U.S. EPA APTI Compliance Test and Source Test Observation

Federal Reference Method 306:  
Sampling and Analysis for Chromium  
Emissions from Decorative and Hard  
Chromium Electroplating/Anodizing  
Operations

12 - 63

63

### Principle

- Gaseous and particulate chromium pollutants are withdrawn isokinetically from the source and collected in a unheated FRM 5 sample train without filter
- Gaseous and particulate chromium pollutants are collected in the impingers containing 0.1 N NaOH or 0.1 N NaHCO<sub>3</sub>

12 - 64

64

### FRM 306 Summary

- Chromium extracted isokinetically from the source
- FRM 5 sampling train except:
  - Unheated quartz probe/nozzle; No SS
  - No heated filter box
  - Replacement of water in impingers with 0.1 N NaOH or 0.1 N NaHCO<sub>3</sub>
  - Don't have to brush probe for recovery

12 - 65

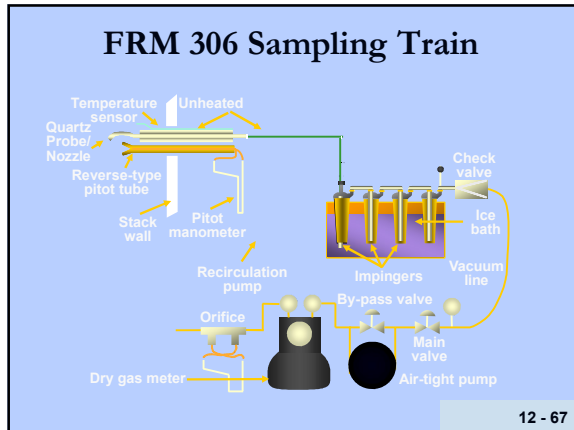
65

### FRM 316 Summary

- 2-hour sample run
- Options for analysis
  - Total chromium: Collect all impinger
  - Cr<sup>+6</sup>: Evaluate pH of first impinger; Should be > 8.5 pH
- Audit sample required

12 - 66

66



67

### Discussion

- Sampling Train: Tradition FRM 5 Without Heating; No Filter or Filter Component; All Quartz Components
- Sampling: Isokinetic, FRMs 1-4, Sample Time > 2 Hrs
- Analytical Finish: Inductively Coupled Plasma Emission Spectrometry (ICP); Cr<sup>+6</sup> by Ion Chromatography (IC)

12 - 68

68

### Discussion

- Cr<sup>+6</sup> Emissions?
  - If Cr<sup>+6</sup> emissions, then at end of sampling run, 1<sup>st</sup> impinger must have pH of >8.5 or must discard sample run (No requirement for total chromium)
  - Must store samples at 4 °C until analysis (Total chromium can store samples at room temperature)
  - Samples must be analyzed within 14 days (60 days for total chromium)
  - Analysis by ion chromatography equipped with post-column reactor (IC/PCR)

12 - 69

69

### Discussion

- Total Chromium (TC) Emissions?
  - High Concentrations: Inductively coupled plasma emission spectrometer (ICP) @ 267.72 nm
  - Low concentrations: Digestion with HNO<sub>3</sub>, then graphite furnace atomic absorption spectroscopy (GFAAS) @ 357.9 nm

12 - 70

70

### Discussion

- Interferences: Stack and ICP Interferences
  - High SO<sub>2</sub> Concentrations reduces 0.1 N NaOH concentration in impingers
  - Spectral: Overlapping of spectral lines (Fe, Mn, U)
  - Physical: Dissolved solids in sample
  - ICAP background interferences
- Concentration: No Blank Correction

12 - 71

71

### Discussion

- GFAA Interferences
  - Spectral: CN<sup>-</sup>
  - Chemical: Ca and PO<sub>4</sub><sup>-</sup>
- IC/PCR
  - Compounds which cause Cr<sup>+6</sup> to Cr<sup>+3</sup> etc.
  - Coeluting compounds

12 - 72

72

### Sampling

- Must traverse the stack to each sampling point determined by FRM 1 (may need probe extension)
- Sample a minimum of 2 minutes per point and required minimum sample time of > 2 hrs
- Must follow all FRM 5 QC requirement (i.e., leak checks, nozzle selection, isokinetic sampling maintained etc.)

12 - 73

73

### Sampling

- Assemble sampling train, but keep all openings covered with Teflon or aluminum foil (0.1 N NaOH in impingers)
- Clean portholes prior to test run
- If stack is under negative pressure, one may start pump prior to putting filter into stack at 1<sup>st</sup> sampling point
- Block off opening around the probe to prevent in-leakage

12 - 74

74

### Sampling

- Add ice to condenser impinger to maintain exit temperature < 68 °F
- Sample isokinetically and make adjustments if variable change by 10 %
- At end of run, wipe off particulate matter on outside of probe nozzle and perform final leak check

12 - 75

75

### Recovery

- Recover impinger solutions and measure for moisture determination and place in labeled container along with completed COC
  - Option #1: Total Cr Sample Option
  - Option #2: Cr<sup>+6</sup> Sample Option

12 - 76

76

### Recovery

- Option #1: Total Cr Sample Option
  - Measure volume of liquid in first, second, and third impingers
  - Rinse nozzle, probe liner, connecting glassware and all three impingers with ~ 200-300 mL of 0.1 N NaOH
  - Do not have to refrigerate
  - Must be analyzed within 60 days
  - Retain the silica gel for follow-up weighting for moisture determination

12 - 77

77

### Recovery

- Option #2: Cr<sup>+6</sup> Sample Option
  - Measure volume of liquid in first, second, and third impingers
  - Measure pH with indicator strip of 1<sup>st</sup> impinger. Must be > 8.5 for 0.1 N NaOH or > 8.0 for NaHCO<sub>3</sub>. If not, discard and redo test

12 - 78

78



**Recovery**

- **Option #2: Cr<sup>6+</sup> Sample Option**
  - Rinse nozzle, probe liner, connecting glassware and all three impingers with ~ 200-300 mL of 0.1 N NaOH
  - Refrigerate @ 4 °C until analysis
  - Must be analyzed within 14 days
  - Retain the silica gel for follow-up weighting for moisture determination

12 - 79

79

**Recovery**

- Prepare a field reagent blank for analysis (i.e., 0.1 N NaOH) into a second bottle
- Seal all bottles and store properly until analysis
- Complete chain-of-custody (COC)

12 - 80

80

**In-stack Detection Limits**

- 1.4 µg Cr/dscm for ICAP
- 0.15 µg Cr/dscm for GFAAS
- 0.015 µg Cr<sup>6+</sup>/dscm for IC/PCR with preconcentration

12 - 81

81

U.S. EPA APTI  
Compliance Test and Source Test  
Observation

*FRMs 26/26A and SW-846,  
Methods 0050/0051  
Determination of HCl and Cl<sub>2</sub>*

13 - 1

1

Applicability

- SW-846, Method 0050 and FRM 26A are both isokinetic methods which provide procedures for the determination of HCl/Cl<sub>2</sub> from hazardous waste incinerators and municipal waste combustors, especially suited for those sources with wet scrubbers emitting acid particulate matter (e.g., HCl dissolved in water droplets)

13 - 2

2

Applicability

- A typical analytical detection limit for HCl is 0.2 µg/ml (sec. 13.3)
- SW-846, Method 0050 and FRM 26A is for water-droplet stack gas environments requiring isokinetic sampling. Additionally, FRM 5 can be performed concurrent with FRM 26A and SW-846, Method 0050

13 - 3

3

Interferences

- Volatile material which produces chloride ions upon dissolution during sampling
- Diatomic chlorine (Cl<sub>2</sub>) for sampling HCl (Cl<sub>2</sub> disproportionate to HCl and Hypochlorous acid (HClO) in water)

13 - 4

4

FRM 26A/Method 0050  
Design Requirements

- Gas flow measurement system (FRMs 2-4)
- Modified Method 5 sampling train
  - All glass/Teflon filter assembly
  - Can't use stainless steel
- Addition of two more impingers to the traditional FRM 5 sampling train

13 - 5

5

FRM 26A/Method 0050  
Sampling Train

- Glass lined probe and nozzle
  - Can't use stainless steel unions in probe assembly
  - If stack gas >210°C, must use one piece nozzle/probe made of quartz
- Pitot tube/temperature sensor array
- Optional glass cyclone

13 - 6

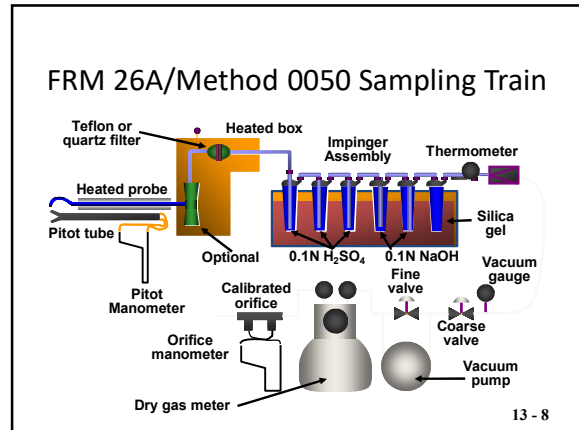
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### FRM 26A/Method 0050 Sampling Train

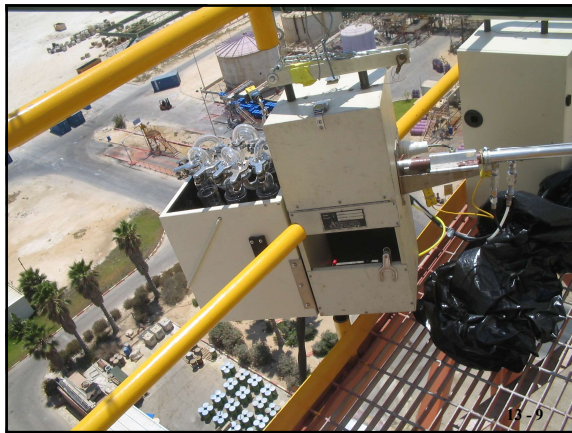
- Heated filter assembly
  - Filter and filter gaskets must be Teflon
- Condensing impingers (glass)
- Pump/dry gas meter/orifice assembly

13 - 7

7



8



9

### FRM 26A/Method 0050 Operational Requirements

- Multi-point integrated sampling
- Isokinetic sampling rate
- 2-hr sample at an anticipated rate of 0.75 cfm
- Probe/cyclone/filter at 120°C (248°F)

13 - 10

10

### FRM 26A/Method 0050 Operational Requirements

- Post-sampling purge: If there is any possibility that liquid has collected in the glass cyclone and/or on the filter (30 minutes) to remove trapped HCl/Cl<sub>2</sub> from filter to impingers (Method 0050) (sec. 7.5.13)

13 - 11

11

### FRM 26A/Method 0050 Operational Requirements

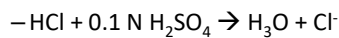
- Leak-free system
- Performance Evaluation (PE) sample required

13 - 12

12

### FRM 26A/Method 0050 Chemistry

- Impingers 1,2 &3 remove HCl from sample gas stream by the following equation

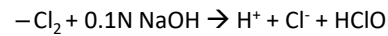


13 - 13

13

### FRM 26A/Method 0050 Chemistry

- Impingers 4 & 5 remove Cl<sub>2</sub> from the stack gas stream by the following equation



- Must keep basic to prevent Cl<sub>2</sub> losses

13 - 14

14

### FRM 26A/Method 0050 Impinger Arrangement

- 1st Impinger(Optional)-  
50 mL of 0.1 N H<sub>2</sub>SO<sub>4</sub>
- 2nd and 3rd Impingers-  
100 mL of 0.1 N H<sub>2</sub>SO<sub>4</sub>

13 - 15

15

### FRM 26A/Method 0050 Impinger Arrangement

- 4th and 5th Impingers-  
100 mL of 0.1 N NaOH
- 6th Impinger-  
200-300 g of Silica Gel

13 - 16

16

### FRM 26A/Method 0050 Operation

- Preliminary field determination (sample location, nozzle size, probe length) same as FRM 5
- Sample train preparation (charging of filter and impingers) same as FRM 5

13 - 17

17

### FRM 26A/Method 0050 Operation

- Pre-leak check (optional) in accordance with FRM 5
- Sample collection in general accordance with FRM 5  
(should be 2-hr sample run Method 0050)

13 - 18

18

### FRM 26A/Method 0050 Operation

- The last impinger of the 0.1 N NaOH must be maintained strongly basic during sampling. Monitor pH of solution frequently during the run to prevent loss of Cl<sub>2</sub>

13 - 19

19

### FRM 26A/Method 0050 Operation

- If solution PH drops, resolve by:
  - Use stronger base (0.5 N)
  - Add volume to impinger (~200 mL)
  - Recharge impinger during sampling
  - Halfway through run, check pH of last impinger to validate basic nature of absorbing solution

13 - 20

20

### FRM 26A/Method 0050 Operation

- Leak check before/after component changes during sample run
- Post-sampling Ascarite purge of system (30 minutes per Method 0050)
- Post-leak check in accordance with FRM 5
  - Leak rate must be <0.02 cfm

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### Sample Train Recovery Containers

- 1- Petri dish (filter) – Optional; for PM
- 2- Acetone rinse from probe nozzle/liner and front half of filter holder - Optional; for PM

13 - 22

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### Sample Train Recovery Containers

- 3- Combined impingers 1, 2 and 3 (measured) and water rinses
- 4- Combined impingers 4 and 5 (measured) and water rinses (add 2 mL of Na<sub>2</sub>S<sub>2</sub>O<sub>3</sub>)  
The addition of Na<sub>2</sub>S<sub>2</sub>O<sub>3</sub> keeps the hypochlorous acid from dissociating

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### Sample Train Recovery Containers

- 5- Silica gel contents (note color, weigh)

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### Analysis

- Weigh filter, Optional; FRM 5 PM
- Analysis of recovery reagents for Cl<sup>-</sup> by SW-846, Method 9057, ion chromatography

13 - 25

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### FRM 26A/Method 0050 Key Points

- Sampling system uses FRM 5 sampling train, so can also quantitate PM
- Sampling is isokinetic, total sampling time should be two hours (0050 sec. 7.2.4)
- Methodology quantitates HCl from Cl<sub>2</sub> emissions

13 - 26

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### FRM 26A/Method 0050 Key Points

- Complete Performance Evaluation (PE) sample prior to test
- The in-stack limit for HCl for the method is approximately 0.02 mg/dscm of stack gas. The method has a negative bias below 20 ppm HCl

13 - 27

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### FRM 26A/Method 0050 Key Points

- Post-sampling purge to move HCl from the cyclone/filter to impingers for 30 minutes at average  $\Delta H$  (Method 0050)

13 - 28

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### FRM 26A/Method 0050 Key Points

Must maintain a basic solution in the last impinger of NaOH at 0.1 N by

- Using stronger base
- Using more volume in impinger
- Changing impinger during run
- Checking frequently during run

13 - 29

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### FRM 26A/Method 0050 Key Points

- Can't change nozzle during sampling to maintain isokinetics
- Can't use stainless steel in probe assembly
- If stack gas >210°C, then must use one piece nozzle/probe assembly
- Filter analyzed for particles, but not for Cl<sub>2</sub>/HCl

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**FRM 26A/Method 0050  
Key Differences**

- Method 0050
  - allows a filter temperature of 248 ± 25 °F
  - Ambient conditioning is required
  - High post leak rate – void sampling run
- FRM 26A
  - requires a filter temperature > 248 °F
  - Ambient conditioning is optional
  - High Leak Rate – allows one to follow FRM 5, Seciton 12.3 (allows for correction)

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**FRM 26/SW-846  
Method 0051  
Sampling and Analysis for  
HCl and Cl<sub>2</sub> Emissions  
  
(Constant Rate Approach)**

13 - 32

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**Applicability**

- This method provides procedures for the determination of gaseous HCl and Cl<sub>2</sub> from hazardous waste incinerators and municipal waste incinerators

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**Interferences**

- This method is designed to collect gaseous HCl and Cl<sub>2</sub> in relatively dry, particulate-free gas streams
- Must use FRM 26A/SW-846, Method 0050 (Isokinetic) with sources controlled by wet scrubbers that emit acid particulate matter and have water droplets

13 - 34

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**FRM 26/Method 0051  
Design Requirements**

- Modified Method 6 sampling train
- Addition of 3-way stopcock and two more impingers to Method 6 sampling train
- 3-way stopcock used to purge probe

13 - 35

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**FRM 26/Method 0051  
Sampling Train**

- Glass lined probe and Teflon elbow inlet
  - nozzle points downstream
- Heated Teflon mat Pallflex filter and three-way stopcock valve
  - can't use glass wool as particle control due to bias effects

13 - 36

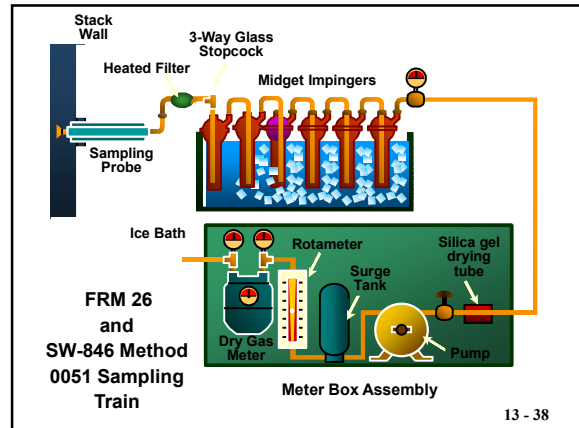
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FRM 26/Method 0051  
Sampling Train

- Midget impinger system (5 midget + 1 Mae West/drying tube)
- Pump/rotameter/dry gas meter

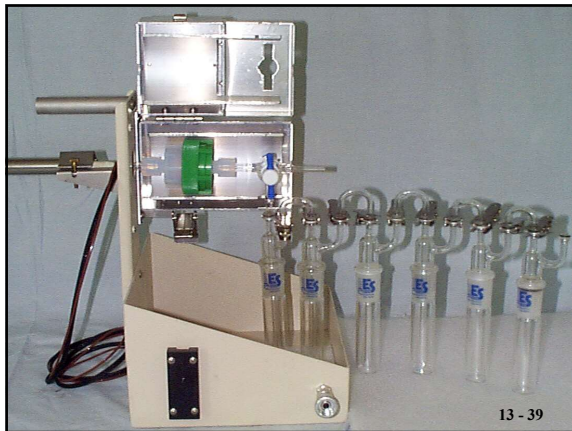
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Operational Requirements

- Single point (> 1 meter from stack wall) integrated sampling
- Purging of probe for 5 minutes prior to sampling

13 - 41

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Operational Requirements

- Probe/filter at 120°C (248°F)
- Sampling at 2 L/min for 60 minutes
  - 120 liters total sample volume

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### Operational Requirements

- Leak-free system
- Performance evaluation (PE) sample

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### Two Tier Leak Check

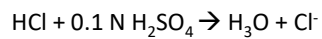
- Stopcock, probe and filter
- Impingers and meter box assembly

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### FRM 26/Method 0051 Chemistry

- Impinger #1 empty
- Impingers #2 & #3 remove HCl from sample gas stream by the following equation:

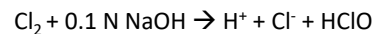


13 - 45

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### FRM 26/Method 0051 Chemistry

- Impingers #4 & #5 remove Cl<sub>2</sub> from the stack gas stream by the following reaction:



13 - 46

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### FRM 26/Method 0051 Impinger Arrangement

- 1st impinger (Optional)
  - empty
- 2nd and 3rd impingers
  - 15 mL of 0.1 N H<sub>2</sub>SO<sub>4</sub>

13 - 47

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### FRM 26/Method 0051 Impinger Arrangement

- 4th and 5th Impingers
  - 15 mL of 0.1 N NaOH
- 6th Impinger/drying tube
  - 30 g silica gel

13 - 48

48

### FRM 26/Method 0051 Operation

#### Field Observation Checklist

- Preliminary field determination (sample location, recovery area) same as FRM 6
- Sample train preparation (charging of filter and impingers) same as FRM 6

13 - 49

49

### FRM 26/Method 0051 Operation

#### Two Tier Leak Check

- Pre-leak check (-10 in. Hg) stopcock, probe, and filter prior to inserting probe into stack
- Pre-leak check (-10 in. Hg) impinger and meter box assembly before testing

13 - 50

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### FRM 26/Method 0051 Operation

- Purge probe/filter assembly at 2 L/min for 5 minutes
- Position probe/Teflon®-elbow pointing downstream
- Sample collection in general accordance with FRM 6
- Sample at 2 L/min for 60 minutes
  - 120 liters total sample volume

13 - 51

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### FRM 26/Method 0051 Operation

- The last impinger of the 0.1 N NaOH must be maintained strongly basic during sampling
- Monitor pH of solution frequently

13 - 52

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### FRM 26/Method 0051 Operation

- To resolve
  - Use stronger base (0.5 N)
  - Add volume to impinger (30 mL)
  - Recharge impinger during sampling
  - Half-way through run, check pH of last impinger to validate basic nature

13 - 53

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### FRM 26/Method 0051 Operation

- Leak check before/after component changes during sample run
- Post-leak check in accordance with FRM 5

13 - 54

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### Sample Train Recovery Containers

- 1- Combined impingers #1, #2 and #3 (measured) and water rinses
- 2- Combined impingers #4 and #5 (measured) and water rinses (add 2 mL of Na<sub>2</sub>S<sub>2</sub>O<sub>3</sub> to prevent hyperchlorous acid from dissociating)

13 - 55

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### Sample Train Recovery Containers

- 3- Silica gel contents (note color; not weighted)

13 - 56

56

### Analysis

- Analysis of recovery reagents for Cl<sup>-</sup> by SW-846, Method 9057, Ion Chromatography (IC)

13 - 57

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### FRM 26/Method 0051 Key Points

- System uses a modified FRM 6 sampling train
- Sampling is performed at 2 L/min for 60 minutes

13 - 58

58

### FRM 26/Method 0051 Key Points

- Methodology quantitates HCl from Cl<sub>2</sub> emissions
- Must maintain last impinger of NaOH strongly basic
  - Use stronger base (0.5 N NaOH)
  - Add more volume to impingers
  - Change out during sample run

13 - 59

59

### FRM 26/Method 0051 Key Points

- Two tier pre-test leak check (-10 in. Hg):
1. Stopcock, probe, and filter
  2. Impinger and meter box assembly
- Can also determine moisture of stack gas

13 - 60

60

FRM 26/Method 0051  
Key Points

- Glass lined probe/Teflon® elbow and Teflon® filter assembly only
- Methodology limited to relatively dry, particulate-free gas streams
- Weigh filter, but can't analyze for HCl/Cl<sub>2</sub>

13 - 61

61

**U.S. EPA APTI  
Compliance Test and Source Test  
Observation**

Defining Volatile Organic Compounds  
(VOCs)

14 - 1

1

**How Do We Define HAPs**

- Clean Air Act Amendment (CAAA) of 1990, Title III now contains a list of 187 HAPs containing both organic and inorganic analytes

14 - 2

2

**CAAA of 1990 Number of HAPs in  
Each Volatility Class**

Volatility Class	Number of HAPs in Class
<b>Volatile (VV/V)</b>	<b>106 (56%)</b>
<b>Semi-Volatile (SV)</b>	<b>65 (35%)</b>
<b>Non-Volatile [Particles] (NV)</b>	<b>17 (9%)</b>

14 - 3

3

**Organic Compounds**

- Organic compounds (OCs) are those compounds which have a carbon-carbon bond
- Toxic air pollutants are those pollutants known or suspected to cause cancer or other serious health effects
- Many organic compounds are toxic air pollutants

14 - 4

4

**Testing for VOCs Difficulties**

- Some State and Federal Regulations are based upon VOC emissions, not TOC or TNMOC
- The terms TOC, VOCs, NMOCs etc. are often erroneously applied interchangeably
- There is no straightforward way to measure the VOC emissions since there is no way to separate all VOCs by vapor pressure

14 - 5

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**Testing for VOCs Difficulties**

- All of the reference methods for organic compounds have inherent limitations that restrict their applicability
- There is no one method that can satisfy characterization of organic emissions from an industrial source

14 - 6

6

### Historical Definition of VOCs

- 1970-1980's: Vapor pressure > 77 mm Hg. CAA of 1970 provided for NAAQS for HCs
- 1971: EPA's develop SIP program including definition for VOCs (~ 77 mm Hg)

14 - 7

7

### Historical Definition of VOCs

- Late 1980's: Photochemical reactivity (40CFR51.100) and excluding Freon's
- 1990's: CAAA of 1990 definition of hazardous air pollutants (HAPs), including VOCs

14 - 8

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### 40CFR51.100

- "Volatile organic compounds (VOC) means any compound of carbon, excluding carbon monoxide, carbon dioxide, carbonic acid, metallic carbides or carbonates, and ammonium carbonate, which participates in atmospheric photochemical reactions. This includes any such organic compound other than the following:
  - Methane, ethane, methylene chloride, CFCs, HCFCs, HFCs, etc.

14 - 9

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### Organic Chemistry

- "...*Organic chemistry is the chemistry of the compounds of carbon.*"
- Historically, chemical compounds were divided into two groups:
  - Inorganic compounds were those obtained from minerals;
  - Organic compounds were those obtained from animal sources, that is, from materials produced by living organisms. They all contain the element carbon.

14 - 10

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### Historical Definition of VOCs

- 2000's: Various state agencies define VOCs (0.1 mm Hg to 77 mm Hg) by:
  - Vapor Pressure (in mm Hg at 25°C)
  - Boiling Point Temperature (°C)

14 - 11

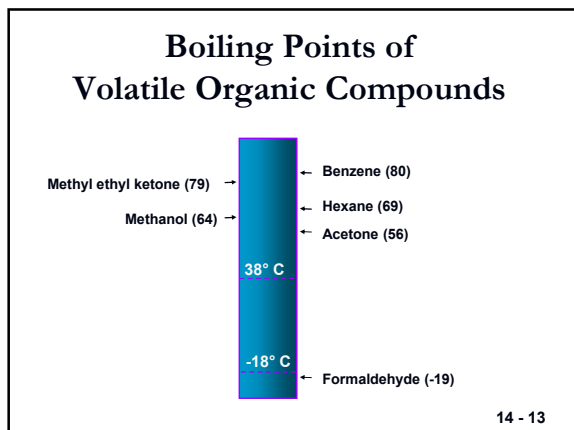
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### General Classification of VOCs

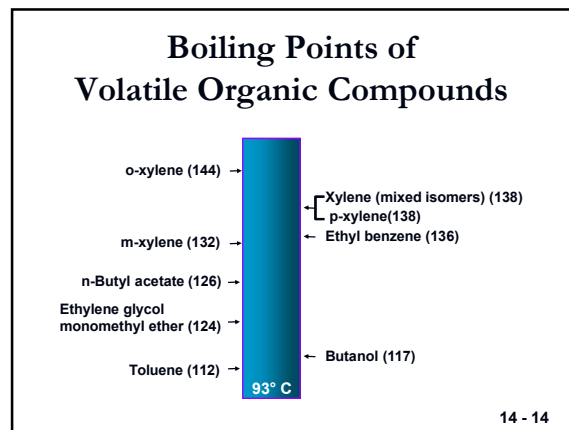
Classification	Vapor Pressure mm Hg	Boiling Point °C
Volatiles (VVV)	> 10 <sup>-1</sup>	200°C
Semi-volatiles (SV)	10 <sup>-1</sup> to 10 <sup>-7</sup>	200 - 500°C
Particles (NV)	< 10 <sup>-7</sup>	500°C

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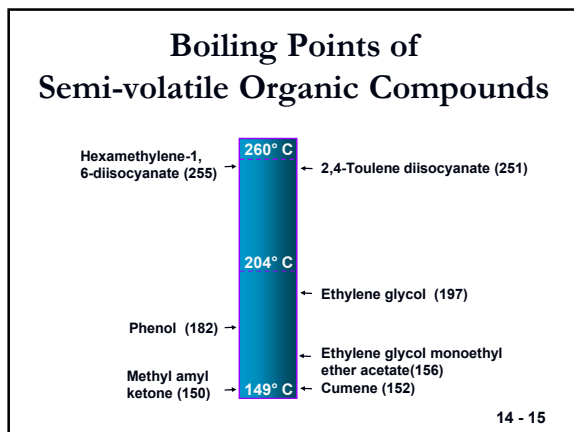
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- ### Six (6) Key Factors to Consider in Test Method Selection
1. The chemical composition of the VOCs being tested
  2. The expected concentration range of the VOCs being emitted
  3. The chemical properties (i.e., vapor pressure, boiling point, solubility etc.) of the emitted VOCs
- 14 - 16

16

- ### Six (6) Key Factors to Consider in Test Method Selection
4. The characteristics of the effluent (i.e., temperature, moisture, %CO<sub>2</sub> etc.)
  5. The advantages and disadvantages of each of the test methods
  6. The state and federal testing requirements documented in their regulations
- 14 - 17

17

- ### Methods Associated with Monitoring VOCs
- FRM 18: Individual Organic Compounds by Gas Chromatography
  - FRM 25: Measurement for Total Gaseous Non-methane Organic Emissions
  - FRM 25A: Total Gaseous Organic Concentration by Flame Ionization Analyzer
- 14 - 18

18

### Methods Associated with Monitoring VOCs

- FRM 25B: Total Gaseous Organic Concentration by Non-Dispersive Infrared Analyzer (NDIR)

14 - 19

19

### Methods Associated with Monitoring VOCs

- SCAQMD Method 25.3/EPA's CTM 035: Low-level Concentration of VOCs
- SW-846, Method 0010 and 0030: Semi-volatiles and volatile organic compounds respectively
- FRM 315: Polycyclic Organic Matter (POM) by MCEM

14 - 20

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### Definitions

- Volatile Organic Compounds (VOCs): Organic compounds that participate in atmospheric photochemical reactions and have vapor pressure (vp)  $> 10^{-1}$  mm Hg
- An organic compound that participates in atmospheric photochemical reactions. The exempt compounds are listed in 40CFR51.100

14 - 21

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### Definitions

- Semi-volatile Organic Compounds (SVOCs): Organic compounds with v.p.  $10^{-1}$  to  $10^{-7}$  mm Hg and b.p 200-500 °C
- Those organic compounds which can be quantified by SW-846, Method 0010 and analyzed by SW-846, Method 8270D

14 - 22

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### Definitions

- Polycyclic Aromatic Hydrocarbons (PAHs) or Polycyclic Organic Matter (POM): Organic compounds with more than one benzene ring and which have a boiling point  $> 200$  °C
- Methylene Chloride Extractable Matter (MCEM): Organic compounds which are extracted by  $\text{MeCl}_2$

14 - 23

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### Definitions

- Total Hydrocarbons (THCs): Sum of total organic compounds containing only C and H
- Total Non-Methane Organic Compounds (TNMOCs): Sum of all VOCs and all exempt compounds excluding methane
- Total Non-Methane/Non-Ethane Organic Compounds (TNM/NEOCs): Sum of total VOCs and exempt compounds excluding methane and ethane

14 - 24

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### Definitions

- FRM 18 results can be converted to mass emission rates since this method reports concentrations in terms of the actual organic compounds. We know the molecular weight of each analyte along with volumetric flow rate to get VOC mass flow rate.
- Total Organic Compounds (TOCs): Organic compounds detected by a flame ionization analyzer (FIA)

14 - 25

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### Definitions

- Hazardous Air Pollutants (HAPs): Those compounds identified in the Clean Air Act Amendments of 1990, Title III list of 187 HAPs

14 - 26

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### Applicability of Organic Sampling Methods

FRM	Conc. Range
FRM 25 B	0.5-10 %
FRM 25	50 ppm-10 %
FRM 18	1 ppm – 1 %
FRM 25 A	50 ppm – 1 %
Method 25C	< 1 ppm

(CTM 035) SCAQMD < 50 ppm(C) or 25 ppm(C) in trap

14 - 27

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### Applicability of Methods

	FRM 18	FRM 25	FRM 25A
Measures...	VOCs	TGNMO	THC
Principle...	GC/MD	GC/FID	FID
Carbon Resp...	1:1	1:1	Var.
Results Exp As..	VOC	As C	Cal Gas

14 - 28

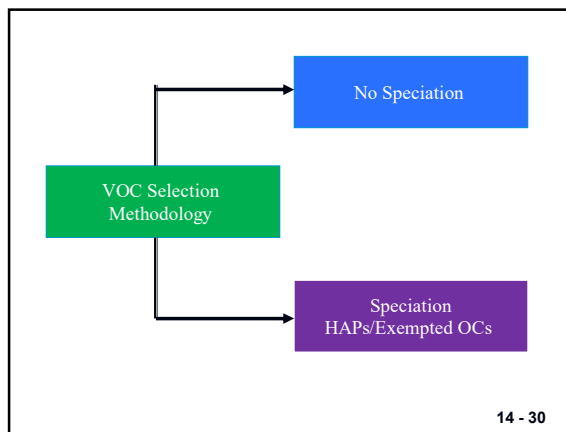
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### Applicability of Methods

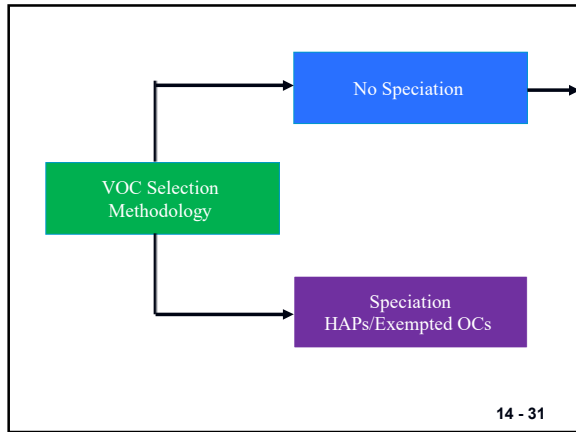
Nature of Emission	Report Emission As	Affected Facility
VOCs unknown/variable	Propane	Asphalt Plants Cement Plants Resource Recovery Bakeries
Single VOC > 75 %	That single VOC	SOCMI
Single VOC < 75 %	Surrogate	Surface Coat Graphite Art

14 - 29

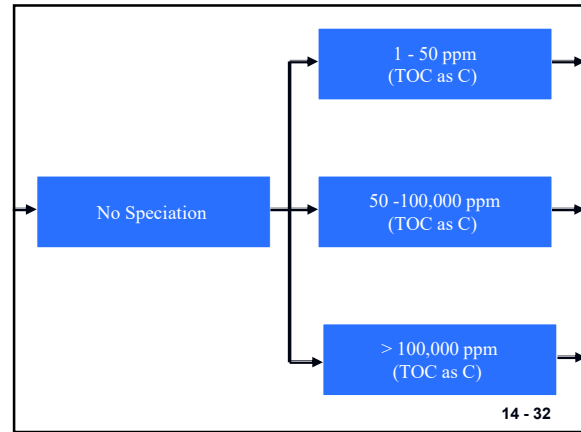
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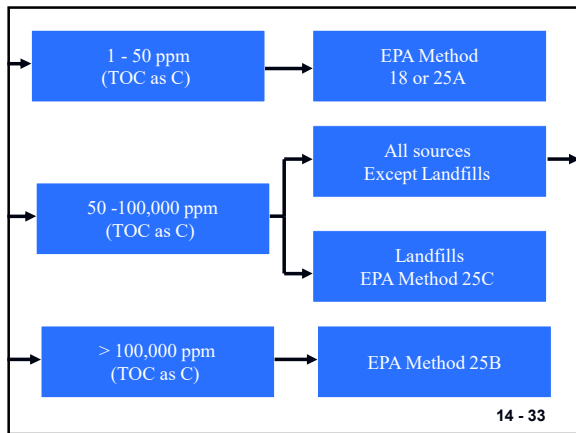
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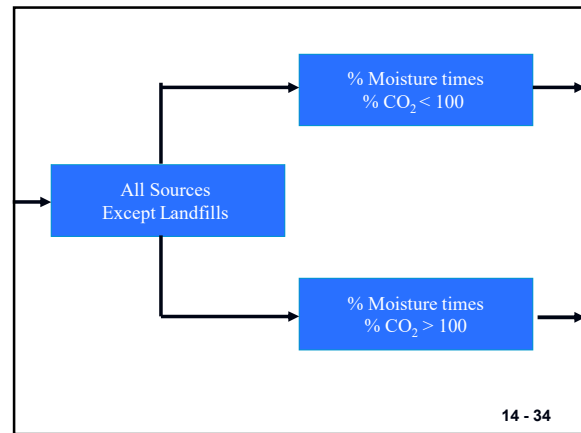
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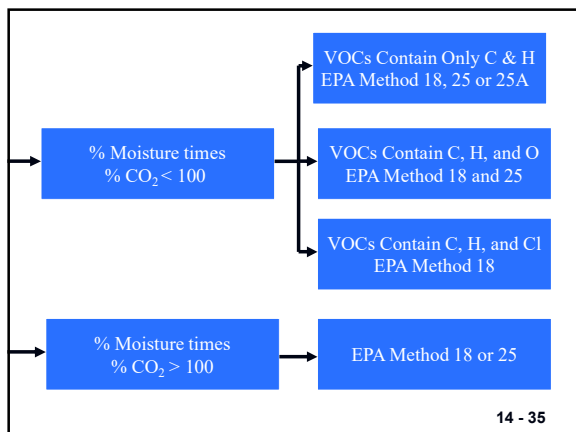
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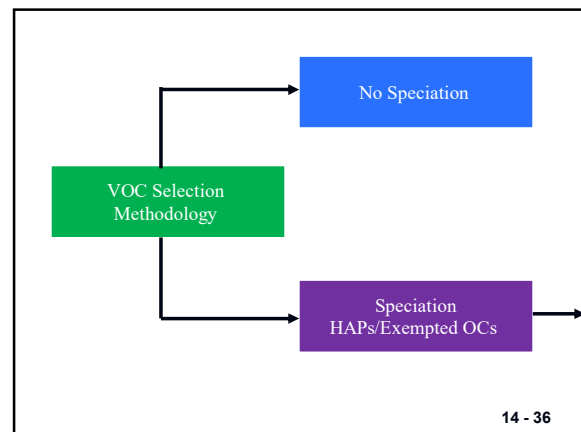
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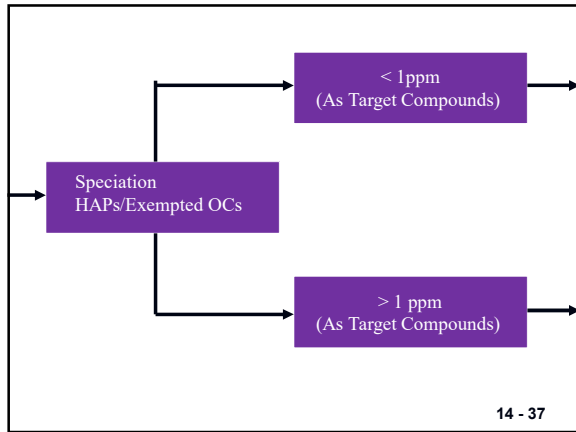
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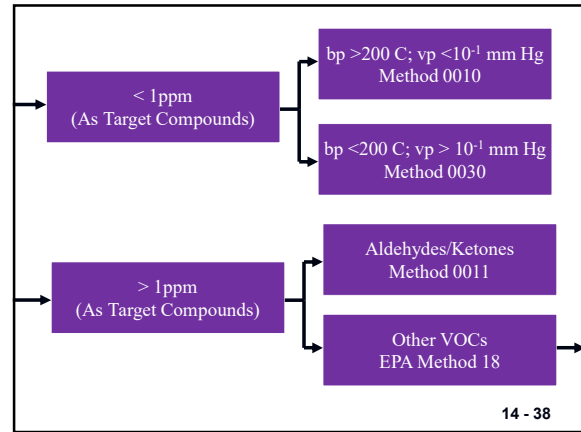
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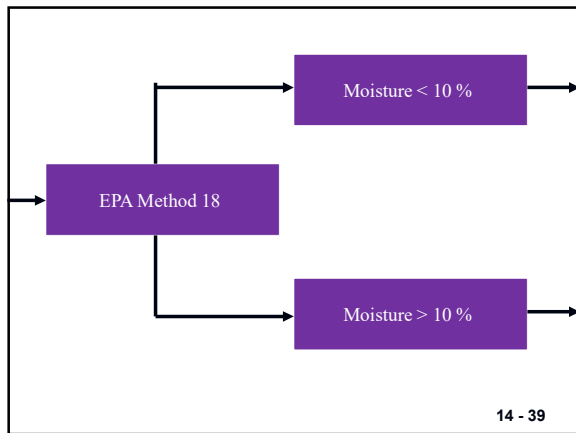
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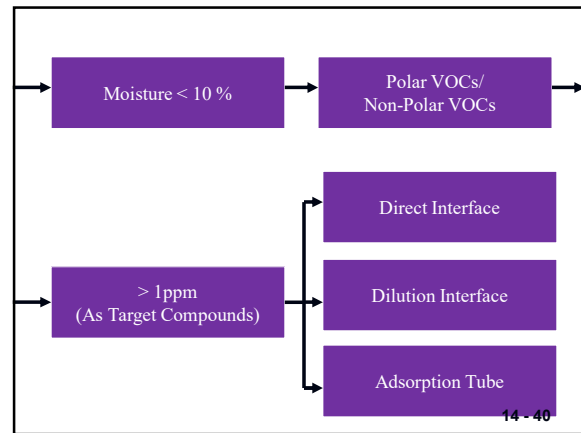
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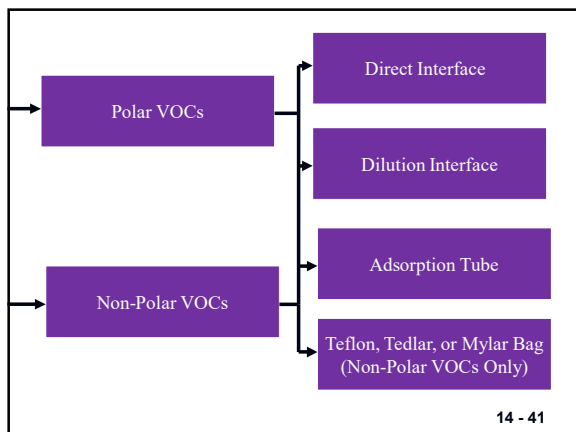
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41

### Reporting of Emissions?

- “As Carbon?”
- “As TGNMOCs?”
- “As Propane?”
- “As VOCs?”
- “As THC’s?”
- “As.....What?”

42

### Reporting of Emissions

- FRM 18, because of the GC/MS analysis, reports results in terms of the concentration of specific organics
- FRM 25 is a method for measuring total gaseous nonmethane organic compounds (TGNMOCs) with a GC column and FID. Therefore, a one-to-one response of all carbon atoms in the sample are as methane (i.e., carbon counter) .

14 - 43

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### Reporting of Emissions

- FRM 25A involves determining total hydrocarbons concentrations by introduction of the sample directly into the FID without a GC step to speciate. Results are expressed in terms of the gas used to calibrate the FID (usually methane or propane). FRM 25A does not provide a one-to-one response for all of the carbon atoms present in the sample.

14 - 44

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### Reporting of Emissions

- FRM 18 results can be converted to mass emission rates since this method reports concentrations in terms of the actual organic compounds. We know the molecular weight of each analyte along with volumetric flow rate to get VOC mass flow rate.

14 - 45

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### Reporting of Emissions

- For FRM 25, we need to know the VOC-to-carbon weight ratio to get VOC mass emission rate.
  - Methanol molecular weight = 32
  - Carbon molecular weight = 12
    - $32/12 = 2.67$  VOC to carbon weight ratio. We would multiply everything by 2.67 to calculate VOC mass emission rate

14 - 46

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### Reporting of Emissions

- Converting FRM 25A results to “as VOCs” mass flow is similar to FRM 25 except one must take into account not only the molecular weight factor, but also the relative response factor (RRF) for the FID between the analytes in the gas stream and the calibration gas.

14 - 47

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### Relative Response Factors

VOC	C:O Ratio	RRF
Methane	1:0	1.00
Propane	1:0	1.00
Formalde	1:1	0.00
Methanol	1:1	0.40
Ethanol	2:1	0.70
MEK	4:1	0.75
Ethy. Ox	2:1	0.50
CO	1:1	0.00

14 - 48

48

### Suggested Reporting of Emissions

- For federally regulated source (i.e., NSPS, NESHAPs, MACT etc.), report VOC emissions according to the specific subpart
- If VOC emissions are unknown, highly variable nature, the results should be reported in terms of propane (i.e., Incinerators, boilers, asphalt plants, cement plants, and recovery boilers etc.)

14 - 49

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### Suggested Reporting of Emissions

- If composition of the effluent is known and a single VOC > 75%, then emissions reported in terms of that compound (i.e., SOCOMI facilities etc.)
- If composition of the effluent is known and a single VOC < 75%, then emissions reported in terms of a surrogate compound (i.e., surface coatings, graphic arts etc.)

14 - 50

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### Suggested Reporting of Emissions

- If testing is for control device efficiency, then emissions can be reported “as carbon” or “as VOCs.”
- If testing is to determine if a source is subject to a regulation whose applicability is based upon VOC emission rates, to determine compliance with VOC emission rate standard, or to set permit fees, then the results must be reported “as VOCs” rather than “as carbon.”

14 - 51

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### Suggested Reporting of Emissions

- This means one has to take into account molecular weight (MW) and for FRM 25A, relative response factor (RRF) in determining VOC emission rate.
  - Reporting as carbon in such circumstances would understate the impact of the emissions on the environment and therefore, would lead to incorrect conclusions regarding compliance or rule applicability.

14 - 52

52

### Reporting of Emissions

#### Example Calculation 1

Calculating the VOC mass emission rate from a source emitting mostly ethanol (C<sub>2</sub>H<sub>5</sub>OH) using EPA Method 25A data in terms of propane...

$$\left( \frac{\text{ppmvw as C}_2\text{H}_5}{(1 - B_{\text{w}})} \right) \left( \frac{\text{K}_{\text{min}}}{385.3 \times 10^{-6}} \right) (MW_c)(Q_{\text{st}}) \left( \frac{MW_{\text{C}_2\text{H}_5\text{OH}}}{(\# \text{ C atoms}_{\text{C}_2\text{H}_5\text{OH}})(MW_c)} \right) \left( \frac{\text{RRF}_{\text{C}_2\text{H}_5}}{\text{RRF}_{\text{C}_2\text{H}_5\text{OH}}} \right) = \text{lbs C}_2\text{H}_5\text{OH} \text{ hour}$$

$$\left( \frac{\text{ppmvw as C}_2\text{H}_5}{(1 - B_{\text{w}})} \right) (3)(12.01)(Q_{\text{st}}) \left( \frac{46.07}{(2)(12.01)} \right) \left( \frac{1.00}{0.70} \right) = \text{lbs C}_2\text{H}_5\text{OH} \text{ hour}$$

14 - 53

53

### Reporting of Emissions

#### Example Calculation 2

Calculating the VOC mass emission rate from a source emitting mostly ethanol (C<sub>2</sub>H<sub>5</sub>OH) using EPA Method 25 data in terms of carbon...

$$\left( \frac{\text{ppmvw as C}}{(1 - B_{\text{w}})} \right) (MW_c)(Q_{\text{st}}) \left( \frac{MW_{\text{C}_2\text{H}_5\text{OH}}}{(\# \text{ C atoms}_{\text{C}_2\text{H}_5\text{OH}})(MW_c)} \right) = \text{lbs C}_2\text{H}_5\text{OH} \text{ hour}$$

$$\left( \frac{\text{ppmvw as C}}{(1 - B_{\text{w}})} \right) (12.01)(Q_{\text{st}}) \left( \frac{46.07}{(2)(12.01)} \right) = \text{lbs C}_2\text{H}_5\text{OH} \text{ hour}$$

14 - 54

54

**U.S. EPA APTI**  
**Compliance Test and Source Test**  
**Observation**  
**Overview and Comparison FRMs 18, 25,**  
**25A and CTS 035**



15-1

1

**Lecture Objectives**

- ➔ Compare the Methods
- ➔ Discuss Their Advantages and Disadvantages
- ➔ Describe Current EPA Guidance on Their Use

15-2

2

**Background**

- FRM 25 - measures total VOC
- FRM 25A - measures total hydrocarbons (THC)
- FRM 18 - measures individual organic compounds

15-3

3

**Background**

- Generally, “stack testing” is performed using FRM 25A or FRM 18
- FRM 25/25A were created in order to determine the removal efficiency of
- VOC's for control devices

15-4

4

**Background**

- Typically, once a method is promulgated (and sometimes before it is) the method will be used for a variety of purposes including functions that it was not designed to perform
- FRM 25 and FRM 25A are not applicable to mass emission rate

15-5

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**Background**

- FRM 25
  - Samples are time integrated
  - Analysis is completed off site
- FRM 25A
  - Sampling is continuous
  - Analysis is done on site

15-6

6

### Background

- FRM 18
  - Samples can be time integrated or semi-continuous
  - Analysis can be on site or off site

15 - 7

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### Background

- FRM 25 - All compounds are converted to methane before measuring with an FID
- FRM 25A - All compounds are measured directly, as a whole, with an FID

15 - 8

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### Background

- FRM 18 - Each compound is separated and measured individually with an FID

15 - 9

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### FRM 25 & 25A

- The FID can be applied to the determination of the mass concentration of the total molecular structure of the organic emissions under any of the following limited conditions

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### FRM 25 & 25A

- Where only one compound is known to exist
- When the organic compounds consist of only hydrogen and carbon

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### FRM 25 & 25A

- Where the relative percentages of the compounds are known or can be determined, and the FID responses to the compounds are known

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### FRM 25 & 25A

- Where a consistent mixture of the compounds exists before and after emission control and only the relative concentrations are to be assessed
- Where the FID can be calibrated against mass standards of the compounds emitted (solvent emissions, for example)

15 - 13

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### Advantages: FRM 25

- Measures only VOC (excludes Methane)
- Responds equally to all VOC

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### Disadvantages: FRM 25

- Potential positive bias that may vary according to source category
- Relatively poor precision

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### Advantages: FRM 25A

- Very good precision
- Real time analysis
- Relatively low detection limit

15 - 16

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### Disadvantages: FRM 25A

- Does not respond equally to all VOC
- Requires a separate measurement of Methane to convert THC to VOC

15 - 17

17

### Advantages: FRM 18

- Good precision
- Low detection limits
- Can exclude methane

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### Disadvantages: FRM 18

- Measures individual organic compounds - not total VOC
- Requires calibration standards for all measured compounds

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### General Guidance

- Use FRM 25 for unknown mixtures with concentrations greater than 50 ppm
- Use FRM 25A for unknown mixtures with concentrations less than 50 ppm

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### General Guidance

- Use any of the methods for known mixtures with the following conditions
  - FRM 25 should only be used for concentrations greater than 50 ppm

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### General Guidance

- Use any of the methods for known mixtures with the following conditions
  - FRM 25A should be calibrated with the known mixture or the results mathematically corrected for varying response factors

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### General Guidance

- Use any of the methods for known mixtures with the following conditions
  - FRM 18 must be calibrated for each of the compounds in the mixture

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### Summary

- None of the existing methods for measuring VOCs are perfect
- Because their problems can be source specific, we may have to approve alternative methods for some sources
- We must continue to improve the existing methods

15 - 24

24

### Reporting VOCs

- Many state agencies require reporting “as VOCs;” or as “carbon, methane; or propane” or “make up your own!”
- One must know how the state wants data reported for VOC emissions
- Volatile organic compounds as defined in 40 CFR 51.100

15 - 25

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### Reporting VOCs

- The reporting format of the data must be known prior to accepting test data
  - Mass emission rates - lb/hr as carbon, methane, or propane?
  - Mass emission rates - lb/hr “as VOC”

15 - 26

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### Case Study Molecular Weight - FRMs 25 & 25A

- Emissions testing was performed and submitted in support of a permit application
- Gas Stream consisted of ~ 100 VOCs
- Total VOCs per FRM 25A = 2.5 lb/hr as carbon

15 - 27

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### Case Study

- One speciated compound per a compound specific test was emitted at 5 lb/hr
- Outcome
  - Facility adjusted the reported VOC emission rate using a MW that was considered ‘average’ for the pollutant gas stream (avg MW of the VOCs)

15 - 28

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### Case Study

- Using the MW of carbon for mass emission rate calculation
- Consider Propylene Glycol ( $\text{CH}_3\text{CH}(\text{OH})\text{CH}_2\text{OH}$ )
- Molecular Weight is 76.10
- Assume: Concentration = 100ppm
- Qsd of 100,000 dscfm

15 - 29

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### Case Study

- lb/hr “as carbon” ( $\text{MW}=12$ ) = 18.7 lb/hr.
- lb/hr “as VOC” ( $\text{MW}=76.1/3$ ) = 39.57 lb/hr.
- An error in excess of 100% due only to MW

15 - 30

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### Case Study

- Identification of a major concern with the reporting of VOCs when using FRMs 25 & 25A
- Propose using a molecular weight adjustment
- Every organic will weigh more than just carbon

15 - 31

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### Other Errors Involving FRM 25 & 25A

- “Response factor” error associated with FRM 25A
- The flame ionization detector (FID) used in FRM 25A does not give a 1:1 response with all organics

15 - 32

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### FRM 18 Reporting of VOCs

- FRM 18 measures specific VOCs
- Requires knowledge of the pollutant gas stream
- Can only measure VOCs for which the GC/specific detector has been calibrated

15 - 33

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### FRM 18 Reporting

- Difficulties
  - Sources claim that they only need to measure “total VOCs” - not speciated
  - What to do with a “soup” of VOCs?

15 - 34

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### Summary VOC Methods

- FRM 25 - Measures Total VOC (> 50 ppm)
- FRM 25A - Measures Total Hydrocarbons (THC) (10-100 ppm)
- FRM 18 - Measures Individual Organic Compounds (Sub-ppm)

15 - 35

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### EPA’s Conditional Test Method (CTM) 035



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### ◆ VOC Test Methods

- SCAQMD Former Draft Method 25.2 - removed from consideration
- SCAQMD Method 25.3 - for low concentrations only
- EPA's Conditional Test Method (CTM)-035

15 - 37

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### Applicability

- ◆ EPA's CTM-035 for combustion exhausts < 50 ppmC
- ◆ Continue to use FRM on inlets or higher concentrations (> 50 ppm)
- ◆ SCAQMD M25.3 replaces former draft M25.2
- ◆ Has a provision for deleting trap when no elevated moisture present (ambient)

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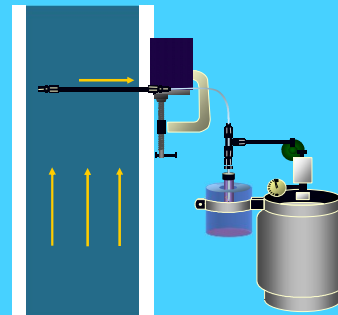
### EPA's CTM-035 Sampling

- ◆ Simple self contained sampler
  - No power, no heaters, no adjustments
  - Analysis is completed off-site
- ◆ Duplicate sampling
  - ◆ Probes are placed flush with port entrance

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### ◆ Sampling Apparatus



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### Duplicate Samplers



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### Trap Assembly



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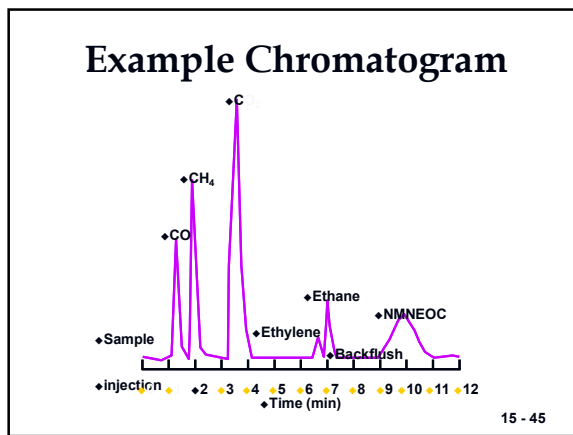
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### Analysis

- ◆ Condensate by infrared total organic carbon analyzer
  - Lower detection limit 1 ppmC
- ◆ Canister by Method 25.1 modified for low concentration
  - GC/oxidation/reduction/FID
  - Lower detection limit 1 ppmC

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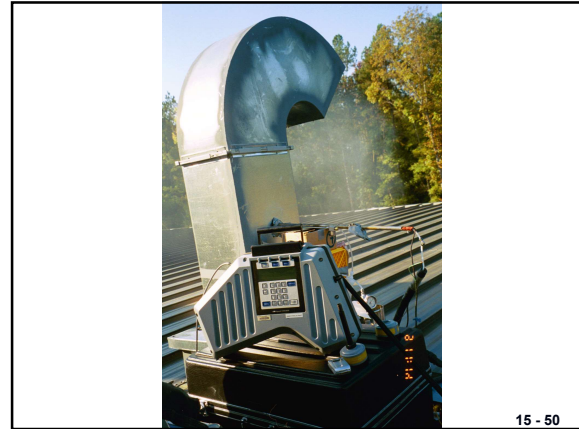
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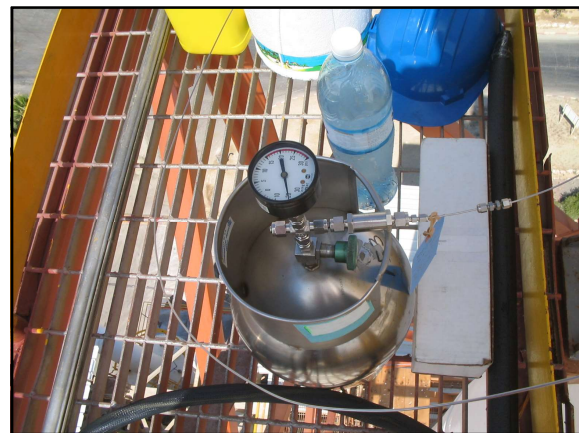
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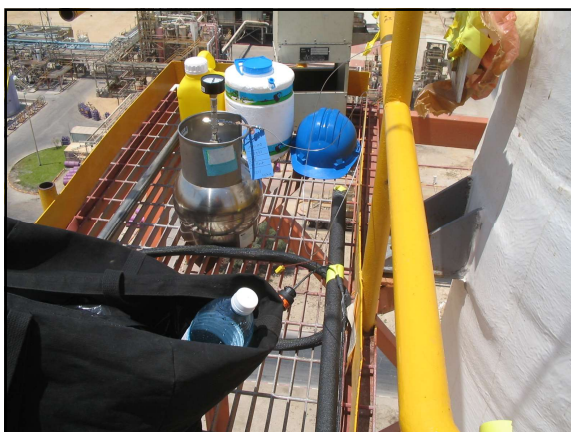
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**Method Development**

- ◆ Various improvements made
  - Trap volume, connector line recovery, trap purge for CO<sub>2</sub>, cleaning and handling
- ◆ EPA Method 301 validation needed however
- ◆ Recent test indicate 92% spike recovery, 20% COV (0.5 ppm)
- ◆ Deemed validated by EPA giving CTM status

15 - 54

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### Implementation Issues

- ◆ In interim, distributing CTM-035 for comments
- ◆ Have been allowing use of draft method subject to protocol review
- ◆ Requires determination for MW/C ratio
  - Draft method contains guidelines for MW/C

15 - 55

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### ◆Conclusions

- Method is thought to have superior accuracy and precision than existing methods (i.e., FRM 25 or FRM 25A)
  - Next phase – comparison to Method 25A
- Well received by industry and source test firms
- Not accurate above 50 ppmC

15 - 56

56

### NCASI Impinger and Canister Method

- National Council for Air and Stream Improvement (NCASI)
  - IM/CAN/WP-99.01
  - “Impinger/Canister Source Sampling Method for HAPs at Wood Products Facilities
  - Publications@ncasi.org

15 - 57

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### NCASI Impinger and Canister Method

- Sampling train consist of three chilled impingers/pump/canister
- Flow through impingers is ~ 400 cc/mL
- Single point sampling for 60 minutes

15 - 58

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### NCASI Impinger and Canister Method

- Ketones/phenols-Water Impinger: GC/FID
  - Acetaldehyde
  - Acrolein
  - Methanol
  - Methyl Ethyl Ketone
  - Methyl Isobutyl Ketone
  - Propionaldehyde
  - Phenol

15 - 59

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### NCASI Impinger and Canister Method

- Formaldehyde-Water Impinger: Acetylacetone Reagent
  - Measure absorption at 412 nm

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**NCASI Impinger and Canister  
Method**

- Organic Analysis-Canister: Cryogenic trapping followed by GC/MSD EPA's Compendium Method TO-14
  - Acetaldehyde
  - Acetone
  - Acrolein
  - Methanol
  - Methyl Ethyl Ketone (2-Butanone)
  - Methyl Isobutyl Ketone
  - Propionaldehyde
  - Phenol

15 - 61

61

**NCASI Impinger and Canister  
Method**

- Terpene Analysis-Canister: Direct Injection GC/FID
  - Camphene
  - p-Mentha-1,5-Diene
  - 3-Carene
  - p-Cymene
  - Limonene
  - $\alpha$ -Pinene
  - $\beta$ -Pine

15 - 62

62

**NCASI Impinger and Canister  
Method**

- Total Hydrocarbons-Canister: Direct Injection GC/FID
- Bacharach Gas Analyzer For CO/O<sub>2</sub>/CO<sub>2</sub>-Canister: Direct Analysis By Bacharach Gas Analyzer

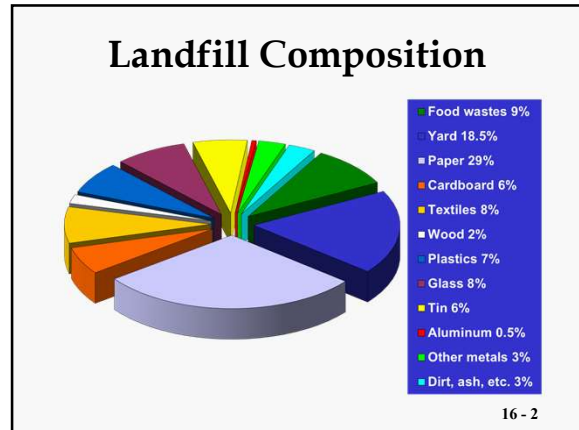
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**What is Landfill Gas(LFG)?**

- ◆ Landfill gas generated by the decomposition of organic municipal solid waste such as garbage, garden waste, and paper products

16-3

3

**At Near Steady-state Conditions LFG Is Typically Composed Of:**

- ◆ 45 - 58% methane ( $CH_4$ )
- ◆ 35 - 45% carbon dioxide ( $CO_2$ )
- ◆ <1 - 5% oxygen ( $O_2$ )
- ◆ <1 - 20% nitrogen ( $N_2$ )

16-4

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**At Near Steady-state Conditions LFG Is Typically Composed Of:**

- ◆ <1 - 5% hydrogen ( $H_2$ )
- ◆ 1 - 5% water vapor
- ◆ <1 - 3% trace constituents

16-5

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**LFG is typically composed of:**

- ◆ Small amounts of nonmethane organic compounds (NMOCs)
  - Benzene
  - Vinyl chloride
  - Chloroform
  - 1,1-dichloroethene
  - Carbon tetrachloride

16-6

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### LFG is typically composed of:

- ◆ Nonorganic species
  - Hydrogen sulfide
  - Mercury
  - Particulate matter

16 - 7

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### Landfill Gases

- ◆ Methane
  - By-product of anaerobic decomposition
  - Colorless, odorless, tasteless gas
  - Lighter than air, relatively insoluble in water
  - Highly explosive in concentrations of 5 to 15% in air

16 - 8

8

### Landfill Gases

- ◆ Carbon Dioxide (CO<sub>2</sub>)
  - By-product of both aerobic and anaerobic decomposition
  - Colorless, odorless gas
  - Heavier than air, noncombustible
  - Soluble in water and decreases water pH

16 - 9

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### Landfill Gases

- ◆ Oxygen (O<sub>2</sub>) and Nitrogen (N<sub>2</sub>)
  - Not common constituents of LFG
  - Present as result of air intrusion (i.e., through cover, through recovery/control system)
  - Typically combined volumes of oxygen and nitrogen < 10% with same ratios in air

16 - 10

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### Landfill Gases

- ◆ Hydrogen (H<sub>2</sub>)
  - Typically produced during aerobic decomposition and early stages of anaerobic decomposition
  - Should have only trace concentrations in a mature landfill

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### Landfill Gases

- ◆ Water Vapor (H<sub>2</sub>O)
  - LFG typically saturated with water vapor
  - Water in landfill entrained in the gas

16 - 12

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### Landfill Gases

- ◆ Trace Constituents
  - Usually originate from waste within the landfill, but some may be present as a result of natural decomposition processes (H<sub>2</sub>S)
  - Nonmethane organic compounds (NMOCs) usually < 1%

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### Landfill Gases

- Over 150 different organic gases have been identified
- Contaminants of potential concern (COPCs) in LFG

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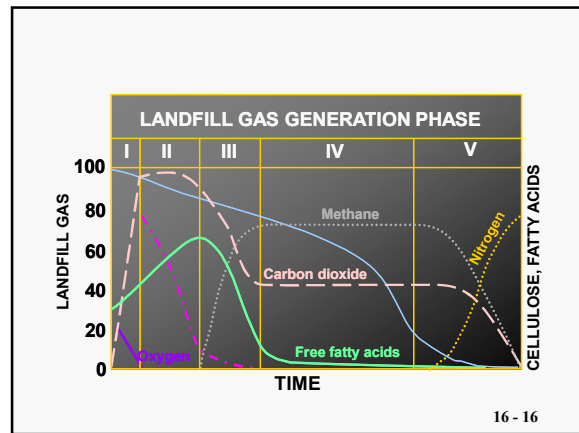
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### Landfill Gas Generation Stages

- ◆ Mainly methane and carbon dioxide produced by microorganisms within the landfill under anaerobic conditions

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### Four Characteristic Phases of Gas Generation at Landfills

- ◆ Phase I: Aerobic
- ◆ Phase II: Anaerobic/Acid Generation
- ◆ Phase III: Transition to Anaerobic
- ◆ Phase IV: Anaerobic
- ◆ Phase V: Transition to Stability

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### Factors Affecting LFG Formation

- ◆ Refuse composition
  - Typically, 50% of the residential and commercial refuse is decomposable
  - Inert materials such as concrete, ash, dirt, metals, and plastic retard LFG generation
  - High percentage of food waste leads to faster LFG generation

16 - 18

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### Factors Affecting LFG Formation

- ◆ **Moisture content**
  - Higher the moisture, greater the LFG generation rate
  - Landfill moisture content affected by:
    - Surface water infiltration
    - Groundwater inflow

16 - 19

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### Factors Affecting LFG Formation

- Release of water as a result of refuse decomposition
- Seasonal variation of moisture content of the waste

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### Factors Affecting LFG Formation

- ◆ **Refuse compaction**
  - Less compaction of refuse, the faster rate of decomposition
  - Shredded refuse generates faster LFG generation

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### Factors Affecting LFG Formation

- ◆ **Age of waste**
  - Lag time is the period from waste placement to the start of the methane generation (start of Phase III)
  - Conversion time is the period from waste placement to end of methane generation (end of Phase V)

16 - 22

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### Factors Affecting LFG Formation

- Yard waste has short lag/conversion times
- Leather/plastic has very long lag/conversion times

16 - 23

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### Factors Affecting LFG Formation

- ◆ **pH**
  - Optimum pH range for most anaerobic bacteria (methanogens) is near neutral (pH = 6.6-7.4)
  - Most landfills tend to have slightly acidic environments

16 - 24

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### Factors Affecting LFG Formation

- Extreme pH movement in either direction reduces the LFG generation rate

16 - 25

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### Factors Affecting LFG Formation

- ◆ Other factors
  - Biological activity-inhibiting industrial waste
  - Absence/presence of nutrients
  - Landfill temperature which affects the microbial activity within the landfill

16 - 26

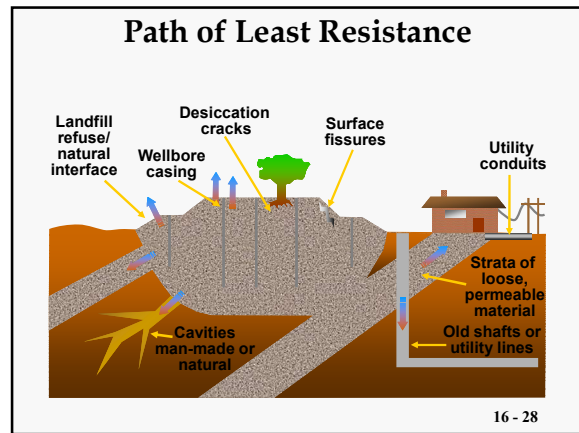
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### Primary Pathways to Human Exposure?

- ◆ Indoor vapor infiltration from contaminated groundwater below buildings (Vapor Intrusion)

16 - 27

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### Depends Upon the Path of Least Resistance

- ◆ To the atmosphere through the landfill surface
- ◆ Migrate laterally into surrounding soils
- ◆ Enter groundwater and follow water path
- ◆ Through LFG extraction systems

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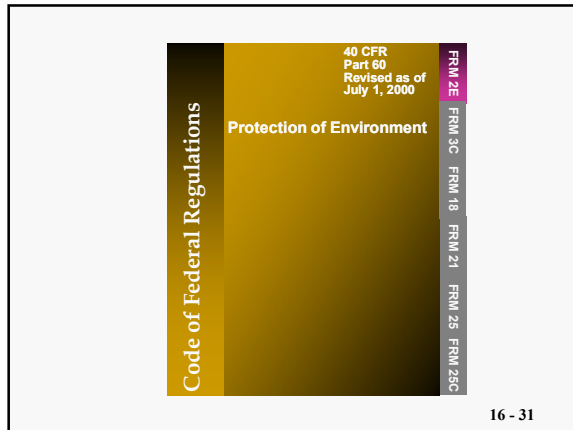
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### Federal Reference Method 2E

#### Determination of Landfill Gas Production Flow Rate

16 - 30

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### Applicability

- ◆ Applies to measurement of landfill gas (LFG) production flow rate from municipal solid waste (MSW) landfills
- ◆ Used to calculate the flow rate of nonmethane organic compounds (NMOC) from landfills
- ◆ Also applies to calculating a site-specific “k” value

16 - 32

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### Principle

- ◆ Extraction wells are installed in a cluster of three, or at five locations dispersed throughout the landfill
- ◆ A blower is used to extract LFG from the landfill

16 - 33

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### Principle

- ◆ LFG composition, landfill pressures near the extraction well, and volumetric flow rate are measured and landfill gas production flow rate determined

16 - 34

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### Apparatus

- ◆ Well drilling rig
- ◆ Material
  - Gravel
  - Bentonite
  - Backfill material

16 - 35

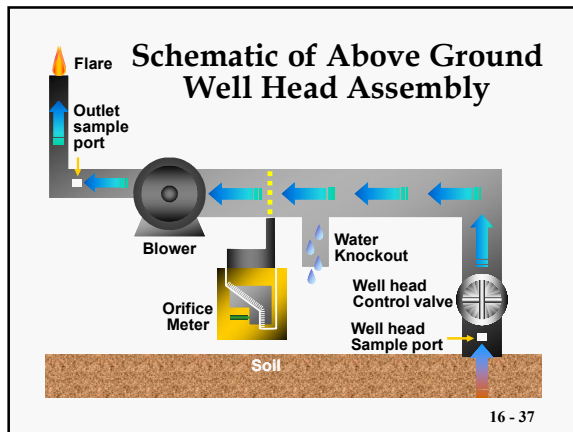
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### Apparatus

- ◆ Wellhead assembly
  - Control valve
  - Orifice meter/manometer
  - Blower
  - Sampling ports (Well head/outlet)

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### Placement of Extraction Wells

- ◆ Single cluster of three (3) extraction wells in a test area (Waste known)
  - Near perimeter of site
  - Depth equal to or greater than the average depth of the landfill
  - Waste 2-10 years old

16 - 38

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### Placement of Extraction Wells

- ◆ Five (5) wells spaced over the landfill (waste unknown)
  - Divide landfill into five (5) equal areas and place extraction well at centroid of each area

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### Extraction Well Pipe Configuration

- ◆ PVC, HDPE, fiberglass, stainless steel or other materials of construction
- ◆ Minimum diameter of 0.075 meters

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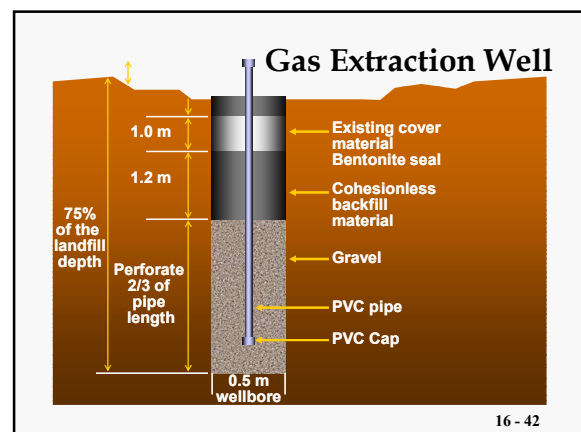
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### Extraction Well Pipe Configuration

- ◆ Bottom two-thirds of the pipe perforated
  - Holes/slots 1.0 centimeter diameter
  - Spaced 90 degrees apart every 0.1 to 0.2 meters

16 - 41

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### Extraction Well Pipe Placement

- ◆ Place in center of hole
- ◆ Backfill with gravel to 0.3 meters above perforation
- ◆ Add backfill material 1.2 meters thick
- ◆ Add layer of bentonite 1.0 meters thick
- ◆ Remainder cover material

16 - 43

43

### Pressure Probe

- ◆ Pressure probes are used in the check for infiltration of air into the landfill and radius of influence
  - Shallow pressure probes used for determination of infiltration of air into landfill
  - Deep pressure probes used to determine the radius of influence

16 - 44

44

### Pressure Probe Configuration

- ◆ PVC or stainless steel, 0.025 meter
- ◆ Bottom two-thirds of pipe perforated
  - Four 6-mm diameter holes
  - Placed 90 degrees apart
  - Every 0.15 meters

16 - 45

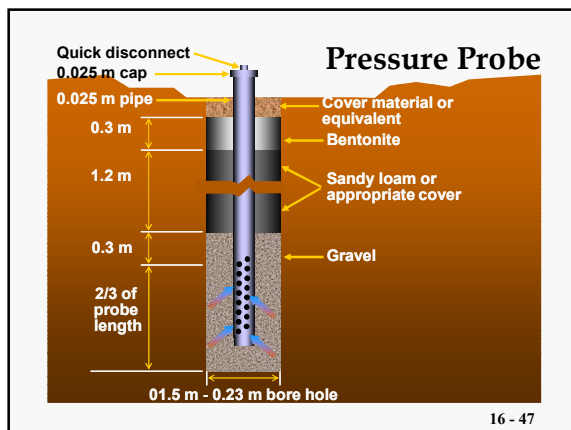
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### Pressure Probe Placement

- ◆ Shallow pressure probes placed in close proximity to cluster well
- ◆ Deep pressure probes
  - Along three radial arms from the extraction wells
  - Approximately 120 degrees apart
  - Distances of 3, 15, 30, and 45 meters from extraction wells

16 - 46

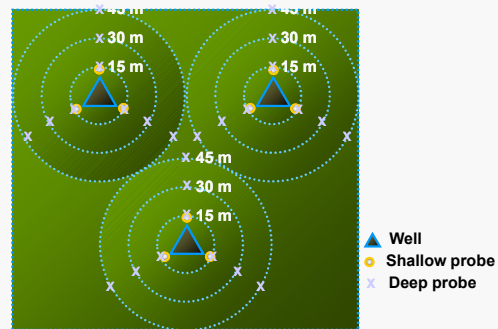
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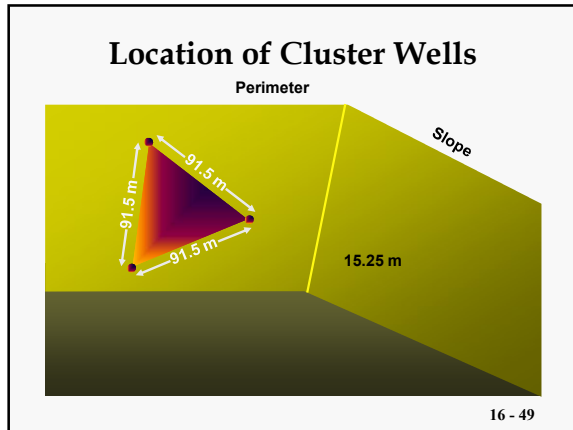
### Cluster Well Configuration



16 - 48

48





49

### LFG Flow Rate Measurement

- ◆ **Leak Check System:**  
Measure nitrogen using FRM 3C at the well head and downstream of the flow measuring device. System is leak tight if difference is < 10,000 ppm

16 - 50

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### LFG Flow Rate Measurement

- ◆ **LFG Flow Rate:**  
Measure LFG flow rate using orifice meter and manometer continuously during testing

16 - 51

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### LFG Static Testing

- ◆ **Purpose:** Determine the initial condition of the landfill
- ◆ **Procedure:** Close the control valve on the well. Measure the gauge pressure ( $P_g$ ) at each deep pressure probe and barometric pressure ( $P_{bar}$ ) every 8 hours for 3 days

16 - 52

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### LFG Static Testing

- ◆ **Calculate:**  $P_i = P_{bar} + P_g$
- ◆ **Average all 8 hours reading for each well to record  $P_{ia}$**

16 - 53

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### Well Temperature and Static Flow Rate

- ◆ **Measure the LFG temperature at each well head**
- ◆ **Measure static flow rate using Type S pitot tube at each well head**

16 - 54

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### Short Term Testing

- ◆ The purpose of short term testing is to determine the maximum vacuum that can be applied to the wells without infiltration of air into the landfill
  - Use blower to extract LFG from single well (others capped) at a rate at least twice the static flow rate

16 - 55

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### Short Term Testing

- Check for infiltration of air into the landfill by measuring the temperature of the LFG at the wellhead, the gauge pressures of the shallow pressure probes, and LFG nitrogen using FRM 3C
- ◆ LFG concentration of nitrogen is  $> 20\%$
- ◆ Any shallow probes have a negative gauge pressure

16 - 56

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### Short Term Testing

- ◆ LFG temperature  $> 55^{\circ}\text{C}$
- ◆ Increase the blower vacuum by 4 mm Hg, wait 24 hours, and repeat infiltration test
- ◆ Continue increasing blower vacuum by 4 mm Hg until infiltration occurs

16 - 57

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### Short Term Testing

- ◆ Then reduce blower vacuum until nitrogen  $< 20\%$ , shallow probes are positive, or LFG temperature  $< 55^{\circ}\text{C}$
- ◆ This is the maximum vacuum at which infiltration does not occur
- ◆ At this maximum vacuum, measure  $P_{\text{bar}}$  every 8 hours for 24 hours
- ◆ Record LFG flow rate:  $Q_s$

16 - 58

58

### Short Term Testing

- ◆ Deep probe gauge pressures for all probes every 8 - hours:  $P_f$
- ◆ Average 8 hour readings of deep probes:  $P$
- ◆ Compare initial average pressure ( $P_{\text{ia}}$ ) to final average pressure ( $P_{\text{fa}}$ )

16 - 59

59

### Short Term Testing

- ◆ Determine furthestmost point from the wellhead along each radial arm where  $P_{\text{fa}} < P_{\text{ia}}$

16 - 60

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### Short Term Testing

- ◆ This is the distance of maximum radius of influence (ROI)
- ◆ Average ROIs to determine the average maximum radius of influence ( $R_{ma}$ )
- ◆ Calculate depth ( $D_{st}$ ) affected by the extraction well:
  - $D_{st} = WD + R_{ma}^2$

16 - 61

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### Short Term Testing

- ◆ Calculate void volume (V)
  - $V = (0.40)(R_{ma}^2)(D_{st})$
- ◆ Calculate total void volumes ( $V_v$ )
  - Sum of all V

16 - 62

62

### Long Term Testing

- ◆ The purpose of long term testing is to determine the methane generation rate constant, k
  - Set blower vacuum to previously determined highest vacuum rate acceptable without infiltration
  - Every 8 hours, sample LFG, measure gauge pressure at shallow pressure probes, the blower vacuum, the LFG flow rate, and check for infiltration

16 - 63

63

### Long Term Testing

- Calculate  $V_t$ , the total volume of landfill gas extracted:

$$V_t = \sum_{i=1}^n 60(Q_i)(T_{vi})$$

16 - 64

64

### Calculating NMOC mass emission rate

$$Q_t = \frac{2kL_0 C_{NMOC}}{5.256 \times 10^{11}} \sum_{i=1}^n M_i e^{-kt_i}$$

16 - 65

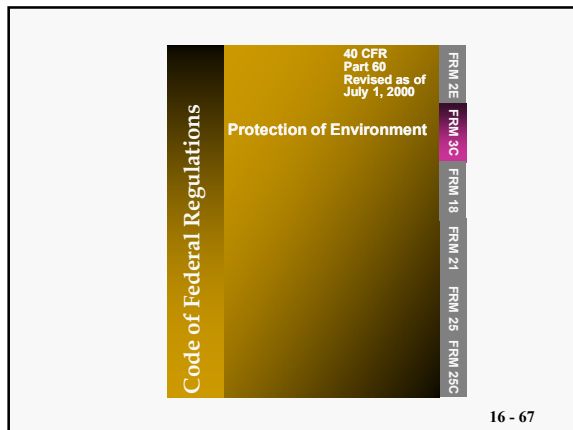
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### Federal Reference Method 3C

Determination of Carbon Dioxide, Methane, Nitrogen, and Oxygen from Stationary Sources  
(40 CFR 60, Appendix A)

16 - 66

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### Applicability

- ◆ This method applies to the analysis of carbon dioxide (CO<sub>2</sub>), methane (CH<sub>4</sub>), nitrogen (N<sub>2</sub>), and oxygen (O<sub>2</sub>) in samples from municipal solid waste landfills and other sources when specified in an applicable subpart

16 - 68

68

### Principle

- ◆ A portion of the sample is injected into a gas chromatograph (GC) and the CO<sub>2</sub>, CH<sub>4</sub>, N<sub>2</sub>, and O<sub>2</sub> concentrations are determined by using a thermal conductivity detector (TCD) and integrator

16 - 69

69

### Apparatus

- ◆ Gas Chromatography equipped with separation column, sample loop, conditioning system, and thermal conductivity detector
- ◆ Recorder, tubing, regulators and adsorption tubes to remove any oxygen in the carrier gas

16 - 70

70

### GC System and Analytical Apparatus

16 - 71

71

### Calibration and Linearity Gases

- ◆ Standard cylinder gas mixtures for each compound of interest with at least three (3) concentration levels spanning the range of sample concentration

16 - 72

72

### Sample Collection

- ◆ Direct Injection
- ◆ Tedlar® Bag
- ◆ Whole Air Flask/Canister

16 - 73

73

### Whole Air Flask/canister at Extraction Well



16 - 74

74

### Analytical System Standardization

- ◆ Optimize GC system according to manufacturer's specifications
- ◆ Linearity Check and Calibration
  - Three calibration gases over the range of suspected sample concentration (This initial check may also serve as the initial instrument calibration)

16 - 75

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### Analytical System Standardization

- Plot linear regression of concentration vs. area values to obtain relative response to each compound

16 - 76

76

### Analytical System Standardization

- ◆ Single Point Calibration Check
  - Use standard calibration gas which is within 20% of the sample component concentration

16 - 77

77

### Sample Analysis

- ◆ Purge sample loop with sample
- ◆ Analyze each sample in duplicate
  - Peak areas should agree within 5% of their average

16 - 78

78

### Method 3C Calculations

- ◆ Moisture content in the sample
  - $B_w = P_w/P_{bar}$
- ◆ Compound concentration
  - $C = A/R(1-B_w)$

16 - 79

79

### Concentration of Sample Components

$$C = \left( \frac{\left( \frac{P_{tf}}{T_{tf}} \right)}{\left( \left( \frac{P_t}{T_t} \right) - \left( \frac{P_{ti}}{T_{ti}} \right) \right)} \right) * \left( \frac{A}{R(1 - B_w)} \right)$$

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### Federal Reference Method 25C

16 - 81

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16 - 82

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### Applicability

- ◆ This method is applicable to the sampling and measurement of nonmethane organic compounds (NMO) as carbon in MSW landfill gases

16 - 83

83

### Principle

- ◆ In operation, a sample probe that has been perforated at one end is driven or augured to a depth of 1.0 meter below the bottom of the landfill cover
- ◆ A sample of the landfill gas is extracted with an evacuated cylinder

16 - 84

84

### Principle

- ◆ The NMOC content of the gas is determined by injecting a portion of the gas from the evacuated cylinder into a gas chromatographic column to separate the NMOC from CO, CO<sub>2</sub>, and CH<sub>4</sub>

16 - 85

85

### Principle

- ◆ The NMOC from the separation is oxidized to CO<sub>2</sub>, reduced to CH<sub>4</sub>, and measured by a flame ionization detector (FID)

16 - 86

86

### FRM 25C Sampling System

- ◆ Probe: Stainless steel with the bottom third perforated. Must be long enough to go a minimum of 1 meter below landfill cover
- ◆ Rotameter: With flow control valve (< 500 mL/min)
- ◆ Sampling valve: Stainless steel

16 - 87

87

### FRM 25C Sampling System

- ◆ Pressure gauge: U-tube mercury manometer
- ◆ Purge pump: Capable of purging probe
- ◆ Vacuum pump: Capable of evacuating to an absolute pressure of 10 mm Hg

16 - 88

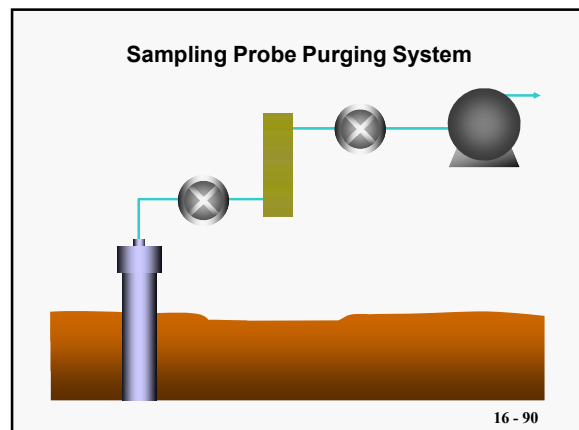
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### FRM 25C Sampling System

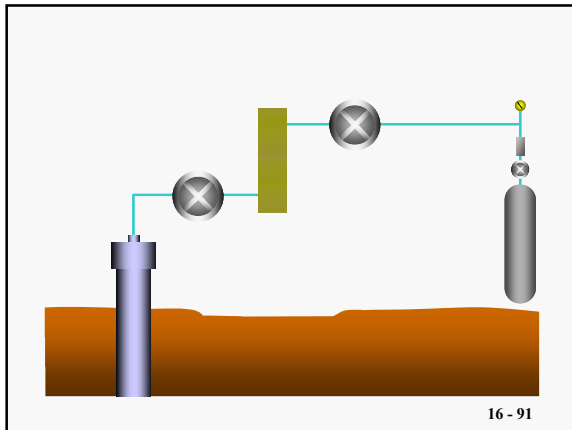
- ◆ Sampling tank: Stainless steel or aluminum cylinder with a minimum volume of 4 liters and equipped with a stainless steel sample tank valve

16 - 89

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### Tank Sampling Procedure

- ◆ **Sample Tank Evacuation:** Evacuate to 10 mm Hg absolute (field/laboratory), set aside for 60 minutes, check vacuum, no change; acceptable

16 - 94

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### Tank Sampling Procedure

- ◆ **Sampling**
  - Evacuate/pressurize sampling tank three time with final vacuum of 325 mm Hg; set aside
  - Assemble sample probe, flow control valve, rotameter and purge pump

16 - 95

95

### Pilot Probe Sampling Procedure

- ◆ **Sample Probe Installation**
  - **Pilot Probe Procedure:**
    - Use post driver to 1 meter below landfill cover
    - Insert sample probe
    - Seal with bentonite
    - Cap

16 - 96

96



### Pitot Probe Sampling Procedure

- Purge at least 2 probe volumes at flow rate of 500 mL/min
- Replace purge pump with sample tank

16 - 97

97

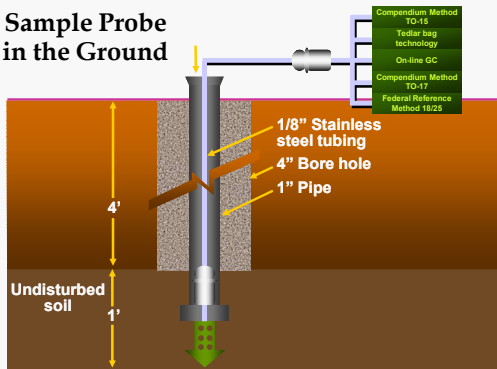
### Pilot Probe Sampling Procedure

- Auger Procedure:
  - Drill hole to 1 meter below landfill cover
  - Place sample probe in hole
  - Backfill with pea gravel to level of 0.6 meters from the surface
  - Seal around probe with bentonite
  - Equilibrate for 24 hours before sampling

16 - 98

98

#### Sample Probe in the Ground



16 - 99

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16 - 100

100

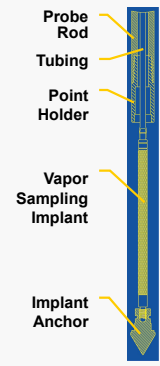
#### Geoprobe on Truck



16 - 101

101

#### Soil Gas Sampling



11 - 102

102

### Sampling Procedure

- ◆ Sampling
  - Open the sampling valve and tank valve
  - Sample at a flow rate of 500 mL/min until sample tank gauge is zero
  - Disconnect from sampling system
  - Pressurize to 1,060 mm Hg with helium

16 - 103

103

### Sampling Procedure

- Record final pressure (may also be pressurized in the laboratory)
- Landfill gas sample is acceptable if N<sub>2</sub> is < 20%

16 - 104

104

### Federal Reference Method 25C Analysis

- ◆ FRM 25C: Oxidation, reduction and measurement of NMOC
- ◆ Initial NMOC analyzer performance test:
  - Oxidation catalyst efficiency check
  - Reduction catalyst efficiency check
  - Analyzer linearity check (not CO<sub>2</sub>)

16 - 105

105

### Federal Reference Method 25C Analysis

- ◆ NMO Analyzer daily calibration
- ◆ NMO response factor

16 - 106

106

### NMOC Concentration

$$C_t = \frac{P_{tf}}{T_{tf}} \cdot \frac{1}{\left(\frac{P_t}{T_t} - \frac{P_{ti}}{T_{ti}}\right) \cdot ((1 - B_w) - C_{N_2})} \cdot \sum_{j=1}^r C_{tm^{(j)}}$$

11 - 107

107

**EPA** United States Environmental Protection Agency  
EPA/600/R-07/043 April 2007

### Field Test Measurements at Five Municipal Solid Waste Landfills with Landfill Gas Control Technology

*Final Report*



16 - 108

108

### Purpose of Field Test Measurement at Five MSW Landfills

- ◆ The purpose of this field test program is to generate data that may be used to update EPA's factors for quantifying landfill gas emissions from municipal solid waste (MSW) landfills.
- ◆ EPA issued in 1996, 2014 and 2020 (RRTR) for New Source Performance Standards (NSPS) and Emission Guidelines (EGs) for new and existing MSW landfills. These regulations require that large landfills collect and control landfill gas emissions.

16 - 109

109

### Purpose of Field Test Measurement at Five MSW Landfills

Landfills are listed as a source for residual risk evaluation as part of EPA's Urban Air Toxic Strategy and are also subject to New Source Review under Title V of the Clean Air Act.

The data being used for issuing air permits, developing estimates for emission inventories and environmental or risk assessments, are obtained from EPA's emission factors found in Chapter 2.4 of AP-42 (U.S. EPA, 1997).

Factors for evaluating uncontrolled emissions and also combustion by-products are included in AP-42. 16 - 110

110

### Target Analytes for the Raw Landfill Gas Samples collected at the Gas Header

Target Analytes in AP-42 List of Landfill Gas Constituents		
Methane	Acrylonitrile	t-1,2-Dichloroethene
Ethane	Benzene	Tetrachloroethene
Propane	Bromodichloromethane	Toluene
Butane	Carbon disulfide	Trichloroethylene
Pentane	Carbon tetrachloride	Vinyl chloride
Hexane	Chlorobenzene	Vinylidene chloride
Carbonyl sulfide	Chloroform	Ethanol
Chlorodifluoromethane	Dimethyl sulfide	Methyl ethyl ketone
Chloromethane	Ethyl mercaptan	2-Propanol
Dichlorodifluoromethane	Ethylene dibromide	1,4-Dichlorobenzene
Dichlorofluoromethane	Ethylene dichloride	Ethylbenzene
Ethyl chloride	Methyl chloroform	Xylenes
Fluorotrichloromethane	Methyl isobutyl ketone	
1,3-Butadiene	Methyl mercaptan	Non-methane organic compounds
Acetone	Methylene chloride	Hydrogen sulfide
Acetone	Propylene dichloride	

16 - 111

111

### Target Analytes for the Raw Landfill Gas Samples collected at the Gas Header

Target Analytes Not Previously Included in AP-42		
Acetaldehyde	Mercury	Gases
Formaldehyde	Organo-mercury compounds	Carbon dioxide
Polycyclic aromatic hydrocarbon <sup>a</sup>	Elemental	Oxygen
Polychlorinated biphenyls <sup>a</sup>	Total	Moisture

16 - 112

112

### Testing Methods for Raw LFG

Procedure	Description	Organization Performing Analysis
EPA Method 1	Selection of traverse points	ARCADIS G&M
EPA Method 2	Determination of gas velocity and volumetric flow rate	ARCADIS G&M
EPA Method 3C	Determination of CO <sub>2</sub> , CH <sub>4</sub> , nitrogen (N <sub>2</sub> ), and O <sub>2</sub> in raw LFG	Triangle Environmental Services
EPA Method 11	Determination of H <sub>2</sub> S	Oxford Laboratories (Landfills A, B, C, D) Enthalpy Analytical (Landfill E)
EPA Method 23	Determination of: PCDDs/PCDFs by Method 8290, PAHs by Method 8270 PCBs by Method 1668	ALTA Analytical Perspectives
EPA Method 25C	Determination of raw LFG NMOCs	Triangle Environmental Services
EPA Method 40/TO-15	Determination of VOCs	Research Triangle Park Laboratories
SW-846 Method 0100/TO-11	Determination of carbonyls (formaldehyde, acetaldehyde)	Resolution Analytics
LUMEX instrument	Determination of elemental mercury (Hg <sup>0</sup> )	ARCADIS G&M
Organic mercury methods	Determination of: monomethylmercury, dimethylmercury, and total mercury.	Frontier Geosciences (Landfills A, B, C, D, E) Studio Geochimica (Landfill E)

16 - 113

113

### Testing Methods for Control Technology Exit Gas

Procedure	Description	Organization Performing Analysis
EPA Method 1	Selection of traverse points	ARCADIS G&M
EPA Method 2	Determination of stack gas velocity and volumetric flow rate	ARCADIS G&M
EPA Method 3A	Determination of O <sub>2</sub> and CO <sub>2</sub> for flare stack gas molecular weight calculations	ARCADIS G&M
EPA Method 4	Determination of stack gas moisture	ARCADIS G&M
EPA Method 6C	Determination of SO <sub>2</sub>	ARCADIS G&M
EPA Method 7E	Determination of NO <sub>x</sub>	ARCADIS G&M
EPA Method 10	Determination of CO	ARCADIS G&M
EPA Method 23	Determination of: PCDDs/PCDFs by Method 8290, PAHs by Method 8270 PCBs by Method 1668	ALTA Analytical Perspectives
EPA Method 25A	Determination of flare stack gas NMOCs, as THCs when total organic concentration was less than the 50 ppm Method 25C applicability threshold	ARCADIS G&M
EPA Method 26A	Determination of HCl	Resolution Analytics
EPA Method 29	Determination of toxic heavy metals	First Analytical Laboratories
LUMEX instrument	Determination of elemental mercury (Hg <sup>0</sup> )	ARCADIS G&M

16 - 114

114

### Raw LFG Major Constituents

	Constituent		Landfill A	Landfill B	Landfill C	Landfill D	Landfill E
Method 25C	Methane (% v/v)	Range	48.0 – 49.8	37.7 – 40.6	54.6 – 57.7	57.4 – 59.5	46.7 – 50.9
		Average	48.8	39.2	56.0	58.6	49.5
	Carbon Dioxide (% v/v)	Range	38.1 – 39.4	29.5 – 31.9	45.2 – 47.2	40.2 – 41.7	33.3 – 36.3
Method 3C	Methane (% v/v)	Range	43.5 – 45.4	35.2 – 37.3	47.4 – 49.1	54.3 – 55.6	46.8 – 51.7
		Average	44.5	36.1	48.0	55.1	49.5
	Carbon Dioxide (% v/v)	Range	35.2 – 36.9	28.2 – 29.9	35.4 – 36.9	37.6 – 38.5	30.2 – 31.9
Method 23	Methane (% v/v)	Range	1.6 – 1.8	6.0 – 6.6	1.4 – 1.9	0.01 – 0.02	2.1 – 3.4
		Average	1.7	6.4	1.6	0.02	2.6
	Oxygen (% v/v)	Range	12.7 – 13.4	24.4 – 26.2	13.5 – 18.9	9.5 – 12.8	11.9 – 16.4
Method 23	Methane (% v/v)	Range	11.6 – 12.3	1.8 – 2.1	NM	NM	NM
		Average	12.0	2.0			

16 – 115

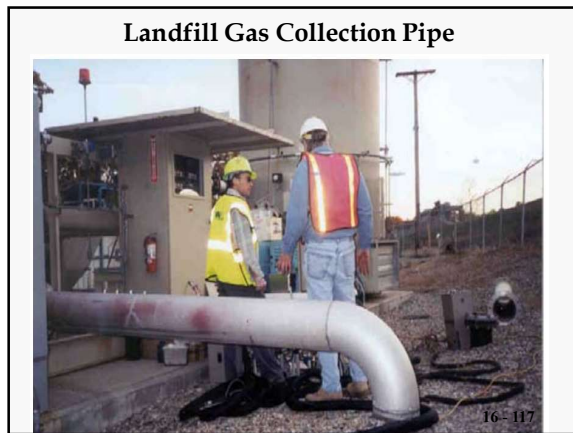
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### Control Equipment Exit Stack Flow Rate and Temperature

		Landfill A	Landfill B	Landfill C	Landfill D	Landfill E
Control Technology		Reciprocating IC Engine	Enclosed Flare	Reciprocating IC Engine	Enclosed Ground Flare	Boiler
Unit Model		Caterpillar 3412	Perennial Energy	Caterpillar 3516	John Zink Model 72	Combustion Engineering 33-7KT-10 A Type
Size or Capacity		1649 cu. in displacement, 470KW	10.8 to 54 MMBtu/hr	4210 cu. in displacement, 800KW	4.0 to 20.9 MMBtu/hr	80,000 lb/hr 250 psi steam
LFG Flowrate into Equipment (scfm)		150	1500	300	400	2430
Exit Flowrate (dscfm)	Range	1290 – 1340	19700 – 22000	1890 – 2000	7830 – 8290	26820 – 30400
	Average	1310	20700	1950	8080	28690
Exit Gas Temperature (°F)	Range	732 – 738	1359 – 1419	997 – 1038	1412 – 1446	476 – 488
	Average	735	1389	1016	1437	479

16 – 116

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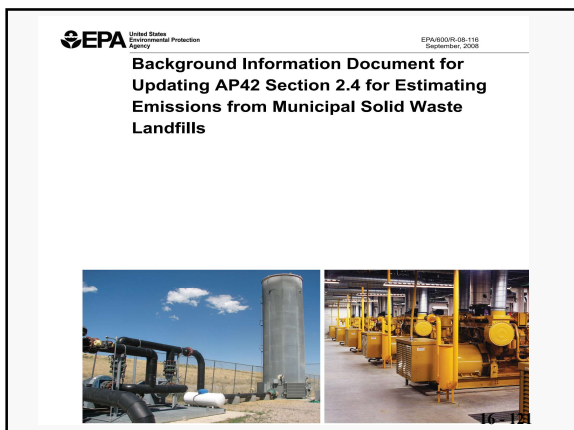
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119



120



121

U.S. EPA APTI  
Compliance Test and Source Test  
Observation

Federal Reference  
Method 18  
General GC Methodology  
(Work Horse for VOCs Speciation Detection)

17A - 1

1

Direct Interface  
Direct Interface/Dilution  
Solid Adsorbent  
Tedlar Bags



17A - 2

2

Survey Canister Sampling



17A - 3

3

Applicability

- Provides concentration data on approximately 90% of total gaseous organic mass emitted from an industrial source
- Does not include techniques to identify and measure trace amounts of organic compounds (< 1 ppm), such as those found in building air and fugitive air emission sources

17A - 4

4

Applicability

- FRM 18 is a generic method which is wide open for quantifying speciated organic compounds
- FRM 18 is a “self-certifying” method....”performance-base” method! Most all other VOC methods are “procedure-base!”
- “Regulatory science” vs. “measurement science!”

17A - 5

5

Applicability

- FRM 18 will not determine compounds that are
  - Polymeric (high molecular weight)
  - Analytes that can polymerize before analysis
  - Analytes that have very low vapor pressure at stack or instrument conditions (< 10<sup>-3</sup> mm Hg)

17A - 6

6

Principle

- Based on separating components of a gas mixture in a gas chromatographic column and measuring separated components with suitable detector (i.e., FID, ECD, PID, MS, IT etc.)
- Uses retention time (RT) as the identification technique compared to standards

17A - 7

7

Overview Items

- FRM 18 requires analysis of an EPA audit cylinder prior to sample analysis
- FRM 18 strongly suggest/requires performing pre-survey to help identify analytes/column/detector [All tentatively identified compounds (TICs) with peaks > 5%]
- FRM 18 requires conducting a recovery study to meet 70-130 %

17A - 8

8

Overview Items

- FRM 18 provides concentration (usually in terms of "ppm") for speciated organics
- Mass emission rate can be provided as long as FRM 1 and 2 are incorporated into the monitoring program

17A - 9

9

Overview Items

- FRM 18 identifies only those analytes for which sampling and analysis is specifically conducted
- FRM 18 can't be used if emissions are unknown
  - FRM 18 ( $\text{CH}_3\text{OH}$ , MW=32) 100 ppm x 32 = 3200
  - FRM 25 (C, MW=12) 100 ppm x 12 = 1200
  - Error: 62 %

17A - 10

10

Overview Items

- FRM 18 requires calibration of analytical system with 3 standards which bracket the concentration of the analyte in the source
  - Commercial cylinders
  - Gas cylinder dilution (FRM 205)
  - Flash vaporization
- FRM 18 requires determination of response factor for each analyte

17A - 11

11

Overview Items

- FRM 18, for tube sampling, requires determination of collection efficiency (CE). Tubes (800/200 mg) with no more than 10% of analyte concentration on back portion

17A - 12

12

Overview Items

- FRM 18 requires determination of recovery study for all methodologies
  - Direct interface: Mid-level gas at probe then analyzer/2 injections ( $\pm 10\%$ )
  - Bags: Of the 3 sample bags, choose one and spike all analytes into bag (40-60 % of avg. conc. of 3 bags). Recovery 70-130 %
  - Adsorbent tubes: Two sampling trains: Spiked/40-60 % of expect conc. and unspiked; three runs; 70-130 % recovery

17A - 13

13

Overview Items

- FRM 18 pushes you to using direct injection, Tedlar bags or adsorbents as sampling options
- FRM 18 allows correction of emissions to "Recovery Study" results: Reported emissions = FRM 18 Conc./R
- For solid adsorbent, no more than 10% of analyte found on back tube

17A - 14

14

Overview Items

- All tubing used in the sampling train must be Teflon...no Tygon tubing allowed
- Aluminized Mylar bags are recommended for low concentration bag sampling because of low permeation rate
- Canister sampling can only be used during survey, **NOT** for compliance application

17A - 15

15

Method Criteria

- Range: 1 ppm to an upper limit of GC detector (saturation of detector limiting factor; upper limit can be extended by dilution)
- A lower range may be achievable by concentrating the sample, thus lowering the limit of detection below the 1
- Sensitivity: minimum detection limit or signal-to-noise ratio 3:1

17A - 16

16

Method Criteria

- Precision: 5 to 10% relative standard deviation(RSD) of mean value (usually 5% with experience GC operator)
- Accuracy: Within 10% audit sample value
- Must conduct recovery study
  - 70-130 % recovery criteria

17A - 17

17

Method Criteria

- Audit Samples are required
- Candace Sorrell (919-541-1064), email: [sorrell.candace@epa.gov](mailto:sorrell.candace@epa.gov)
- As of July 2021, the requirement to obtain these audit samples is no longer in effect until such time as another independent AASP has audit samples available for purchase.

17A - 18

18



Interferences

- Resolution interferences  
(may be eliminated by GC column selection and column physics)
- Contamination of analytical system  
(checked by periodic analysis of blanks)

17A - 19

19

Interferences

- Cross-contamination from analysis of high to low concentration (prevented by purging system between analysis)
- Water vapor  
(correction factor developed)

17A - 20

20

FRM 18 Overview

- To determine the concentration of discrete volatile organic compounds (VOCs) in the sample
- Generic GC method
- Pre-survey recommended/required
  - Confirms identity of target analytes and concentration > 5 % peak height
  - Qualitative by RT, quantitative by internal/external calibration technique

17A - 21

21

FRM 18 Overview

- For speciated VOCs
- Any combination of
  - Sampling techniques, GC Columns, and detectors can be used (Wide open method)
  - Source decides combination provide the recovery criteria are met (70-130%)
  - Recovery performed once per source

17A - 22

22

FRM 18 Sampling Methods

- Integrated bag
  - Glass sampling flask
  - Adsorbent tubes
    - Charcoal
    - Silica Gel
    - Florisil®
    - CarboTrap® 300
    - Tenax® TA
- (Must perform recovery study for each sampling approach)

17A - 23

23

FRM 18 Sampling Methods

- Liquid Trapping Media
  - Sulfuric acid for amines
  - Cadmium hydroxide for reduced sulfurs compounds
  - 2,4-Dinitrophenylhydrazine for aldehydes and ketones

17A - 24

24

FRM 18 Sampling Methods

- Direct Interface: Sample continuously pumped to gas chromatographic (GC) by heated line
  - Analysis conducted on discrete gas samples from sample loop ( ~ 1mL)
  - All compounds must be separated by one column/detector combination

17A - 25

25

FRM 18 Sampling Methods

- Dilution Interface: Same as direct interface, but used with extremely high concentrations of target analytes

17A - 26

26

Using FRM 18

- Know The Characteristics of the Source (Pre-Survey)
  - Specific analytes known
  - Chemical and physical properties of emissions known (i.e., BP, VP etc)
  - Matrix of source known (i.e., % H<sub>2</sub>O, stack temperature, part. loading etc.)
  - Perform survey with direct injection, Tedlar bags or canisters and identify all TICs with peaks > 5 %

17A - 27

27

Using FRM 18

- Select Sampling and Analytical Finish for Targeted Analytes
  - State of PA flow chart
  - Determine analytical finish for TICs
  - For solid adsorbents, select through literature resin and tube design
    - Breakthrough volume, desorption efficiency, capacity of adsorbent, design of 800 mg/200 mg
- Perform laboratory evaluation for analyte recovery (Not required by FRM 18)

17A - 28

28

Using FRM 18

- Perform An Audit of EPA's Gas Cylinder for Target Analytes (This is a Performance Evaluation [PE] Audit)
  - Analysis must agree within 10 % of certified gas values
  - Three analysis must agree within 10 % of each other
- Calibrate all Sampling Components
  - Dry gas meters, flow meters, thermocouples etc.

17A - 29

29

Using FRM 18

- Conduct Recovery Study (Once/source) For Selected Methodology
  - Direct Interface: Mid-level gas at entrance of probe; Must meet 5 % recovery
  - Tedlar Bag: Spike 1 bag at 40-60 % of emission standard; Must meet 70-130 % recovery
  - Tube Sampling: Two sample trains, 3-runs, one train spiked (40-60% mass); Must meet 70-130 % recovery

17A - 30

30

Using FRM 18

- Sampling
  - Verify non-cyclonic flow at sampling location
  - If mass emission required, perform FRM 1 and 2
- Sample
  - Assemble sample train, Leak check, Purge probe, Sample at constant rate/single point, Take necessary data during sampling, Post leak check, Fill out COC, Chill samples if applicable

17A - 31

31

Using FRM 18

- Calibration of Analytical System and Analysis
  - Calibrate system using minimum of 3 standards that bracket the concentration of analyte in source
  - Determine relative response factor for each target analyte
  - Must identify all TICs > 5 %
  - Determine collection efficiency of 1 tube by analyzing back section. No more than 10 % on back section
  - Correct data to recovery study value

17A - 32

32

Sampling Flask/Canister

- Samples can be collected in pre-cleaned 250 mL double-ended sampling flask or canisters
  - Cleaning of flask: methylene chloride, soap solution, furnace (500 °C for 1 hour)
- Sampling performed by either:
  - Evacuated flask procedure
  - Purged flask procedure

17A - 33

33

Evacuated Flask/Canister  
Sampling Procedure

- Flasked/canister cleaned
- Attach "T-connection" to inlet of flask/canister
- Attach 6 mm O.D. borosilicate sampling probe with 12 mm O.D. enlargement at end containing glass wool plug for particle control
- Probe placed > 1 meter from side wall of stack

17A - 34

34

Evacuated Flask  
Sampling Procedure

- Use rubber suction bulb to purge probe
- Open stopcock to fill flask/canister
- Heated canister used by NCASI for quantifying methanol, xylenes, acetone, benzene and methyl ethyl ketone (MEK)
- SCAQMD Method 25.3 applicable also

17A - 35

35

Purge Flask  
Sampling Procedure

- Attach end of flask to a rubber suction bulb
- Attach probe used in evacuated flask procedure to inlet of flask

17A - 36

36

Purge Flask  
Sampling Procedure

- Purge flask, then close stopcock near suction bulb
- Close stopcock near probe
- Tape stopcocks to prevent leakage

17A - 37

37

Flexible Bag  
Sampling Procedure

- Pre-survey samples collected in Tedlar® or aluminized Mylar flexible bags
- Flexible bag certification
  - Use new bag
  - Leak check all bags

17A - 38

38

Flexible Bag  
Sampling Procedure

- Check for contamination by filling with nitrogen
- Analyze 24 hours later with GC

17A - 39

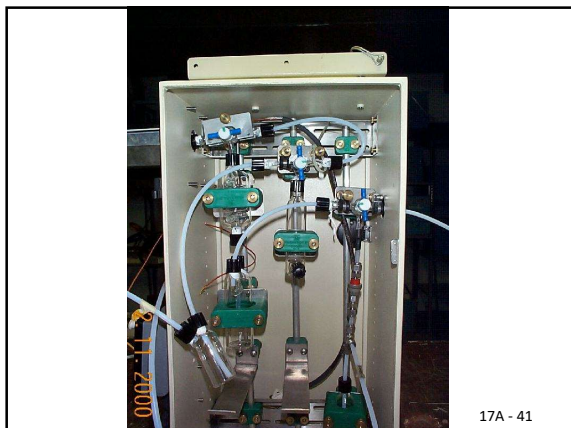
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Bag Sampling

- Assemble sampling train
- Leak check both the bag and container
- Place probe > 1 meter from inside wall
- Purge probe line
- Evacuate container containing flexible bag

17A - 40

40



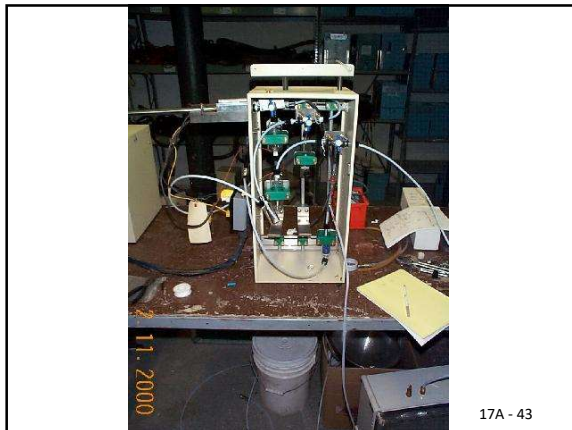
17A - 41

41

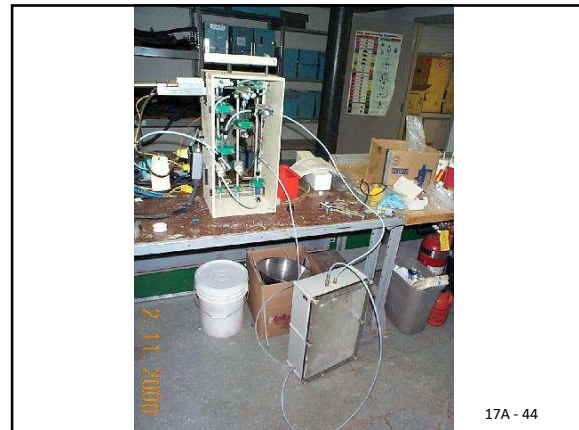


17A - 42

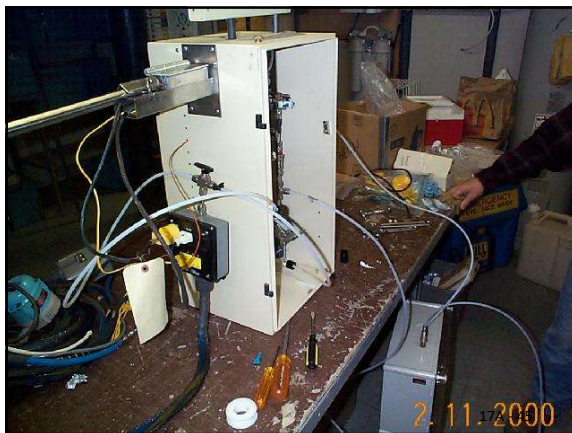
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43



44



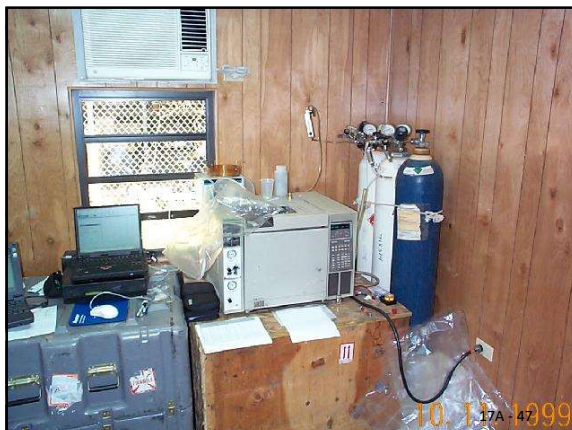
45

#### Bag Sampling

- Sample three bags (proportional sampling to stack flow, single point sampling)
- Analyze bag in triplicate
- Spike one of the bags for recovery determination
- Store for hold time period
- Analyze in triplicate

17A - 46

46



47

#### Recovery Study For Bag Sampling

- Recovery must be 70-130%; Field values adjusted to recovery value
- Must analyze performance evaluation (PE) sample (EPA Audit Sample) prior to analysis of stack gas sample
- Audit analyses must agree with the audit concentrations within 10%

17A - 48

48

Bag Sampling with High Condensation  
Stacks

- Heat sampling box containing sample bag to stack temperature
- Maintain temperature of bag until analysis (Similar to heated canister approach)
- Add dropout impinger to collect condensate (must be analyzed for VOCs along with bag analysis)

17A - 49

49

Direct Interface  
Sampling and Analysis

- Apparatus: Sample probe (~ 6.4 mm), sample line, sample pump, sample valve, flow meters, and heated box
- Assemble equipment and leak check
- Heat sample probe, line, and sample box to 1 to 3°C above stack temperature

17A - 50

50

Direct Interface  
Sampling and Analysis

- Perform analysis of mid-level calibration gas through the sample line behind probe outlet.
- Response should be  $\pm 10\%$  of true value and two readings must be within  $\pm 5\%$

17A - 51

51

Direct Interface  
Sampling and Analysis

- Response to calibration gas analysis should be accurate to within 10 %
- Reconnect probe, analyze stack gas
- Analysis of stack gas must agree with the two analyses to within 5 %

17A - 52

52

Direct Interface/Dilution Sampling  
and Analysis

- Same apparatus as direct interface except a dilution system is added between heated sample line and the gas sampling valve
- Apparatus arranged so either a 10:1 or 100:1 dilution of source gas can be directed to the GC analyzer

17A - 53

53

Direct Interface/Dilution Sampling  
and Analysis

- Verify accuracy of dilution system by analyzing calibration gas with agreement within 10 % of expected value
- Analyze low concentration calibration gas into analyzer twice
- Analysis should be within 5 % of each other

17A - 54

54

#### Adsorbent Tube Procedure

- Samples are collected in adsorbent tube containing specific amounts of adsorbents packed as primary and secondary sections (Dual bed tubes)
  - 800/200 mg for charcoal tubes
  - 1040/260 mg for silica gel tubes

17A - 55

55

#### Adsorbent Tube Procedure

- Tube design left up to user and selection of resin as long as:
  - Breakthrough volume determined;
  - Desorption efficiency determined; and
  - Capacity of adsorbent determine under stack conditions (i.e., temperature, moisture etc.)

17A - 56

56

#### Adsorbent Tube Design

- Adsorbents such as Tenax<sup>®</sup> GC or XAD-2<sup>®</sup> can also be used
- Typical tube design is 90 mm X 6 mm
- Dual sampling trains
- Dual components of tubes (< 10% in back tube)
- Audit analysis of  $\pm 10\%$

17A - 57

57

#### Nature of Ideal Adsorbents

- Very high surface area
- Irregular shape
- Non-polar
- Non-reactive
- Granular

17A - 58

58

#### Nature of Ideal Adsorbents

- High capacity
- Inert
- Non-corrosive
- Readily activated
- Easy release

17A - 59

59

#### Advantages of Adsorbent Technology

- Small sample configuration
- First element in sampling train
- Large selection of adsorbents
- Better water management
- Large database

17A - 60

60

Typical Adsorbents

- Organic polymer adsorbent
- Inorganic adsorbent
- Carbon adsorbents

17A - 61

61

Classification of Adsorbents

- Weak (50 m<sup>2</sup>/g)
  - Tenax<sup>®</sup>, Carbopack C<sup>®</sup>, Anasorb<sup>®</sup>
- Medium (100-500 m<sup>2</sup>/g)
  - Carbopack B<sup>®</sup>, chromosorbs
- Strong (> 1000 m<sup>2</sup>/g)
  - Carbosieve S-III<sup>®</sup>, Carboxen<sup>®</sup>

17A - 62

62

Typical Organic  
Polymeric Adsorbents

- Tenax-GC<sup>®</sup> or Tenax-TA<sup>®</sup>
- Porapak Q<sup>®</sup>
- Carbon molecular sieve
- XAD<sup>®</sup> series

17A - 63

63

Weaknesses of  
Tenax<sup>®</sup> Adsorbent

- Poor desorption of highly polar compounds
- Possibly retains O<sub>2</sub> leading to sample oxidation
- Limited to specific range of VOCs

17A - 64

64

Weaknesses of  
Tenax<sup>®</sup> Adsorbent

- Possible background contamination
- Low breakthrough volume for many of the analytes of interest

17A - 65

65

Weaknesses of  
XAD<sup>®</sup> Series Adsorbent

- Thermal stability questionable
- Breakthrough extensive for < C7

17A - 66

66



Inorganic Adsorbents

- Silica gel
- Alumina
- Fluorisil
- Carbon molecular sieves

17A - 67

67

Weaknesses of  
Silica Gel Adsorbent

- Limited use in high moisture stacks
- Thermal breakdown of silica gel
- Solvent extraction means dilution of sample

17A - 68

68

Weaknesses of Carbon Molecular  
Sieve Adsorbent

- Holds onto very volatile compounds
- Solvent extraction means dilution
- Desorption efficiency decreases with analytes that have boiling points (BP) > 100°C

17A - 69

69

Carbon Adsorbent

- Activated carbon
- Carbon molecular sieve
- Carbonaceous polymeric adsorbents

17A - 70

70

Limitation of  
Carbon Base Adsorbents

- High surface area causes artifact formation
- High background contamination possible
- Very high affinity for water High catalytic activity

17A - 71

71

Limitation of  
Carbon Base Adsorbents

- Incomplete sample recovery during solvent extraction
- Impurities in solvents used during extraction
- Solvent extraction means dilution

17A - 72

72

Common Adsorbents Used in Air  
Pollution Studies

- Carbon
- Tenax-TA®
- Porapak Q®
- Polyurethane foam

17A - 73

73

Common Adsorbents Used in Air  
Pollution Studies

- Carbon molecular sieve
- XAD® Series
- Carbosieve S-III® /Carbotrap® /Carbotrap C® (Carbotrap 300®)

17A - 74

74

Adsorbent Selection-Capture Process  
(Analyte Boiling Point)

- Carbosieve S-III® for VOCs with boiling points between -15°C to 80°C
- Carbotrap® for VOCs with boiling points between 0°C to 100°C
- Carbotrap C® for VOCs with boiling points between 80°C to 250°C

17A - 75

75

Adsorbent Selection-Capture Process  
(Analyte Boiling Point)

- Tenax-TA® for VOCs with boiling points from 30°C to 200°C
- XAD-2® for VOCs with boiling points from 120°C to 350°C

17A - 76

76

Supelco Carbotrap® 300

Carbotrap C·	Carbonaceous material	Heavy Organics (> C <sub>12</sub> )
Carbotrap	Carbonaceous material	C <sub>5</sub> to C <sub>12</sub>
Carbosieve S-III·	Carbon molecular sieve	C <sub>2</sub> to C <sub>6</sub>

17A - 77

77

Adsorbent Recovery  
Two Process Recoveries

- Thermal Desorption
  - Entire sample analyzed
  - More readily automated
  - Only one analysis

17A - 78

78

Adsorbent Recovery Solvent  
Extraction

- Solvent Extraction
  - Able to adjust concentration
  - Replicate analysis
  - No thermal desorption breakthrough products
  - However, dilute sample

17A - 79

79

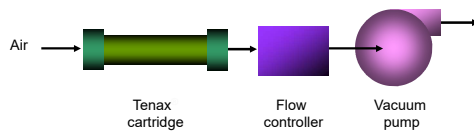
Adsorbent Tube  
Sampling Train

- Heated probe (~ 6 mm I.D.), in-stack or out-of-stack filter (heated), flexible tubing, leakless sample pump, rotameter, and adsorption tube
- All temperature and flow measuring devices must be calibrated

17A - 80

80

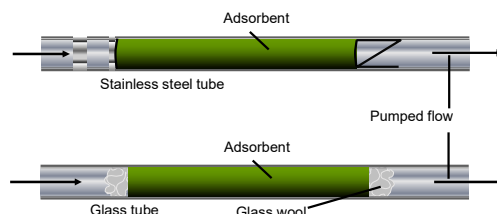
Active Sampling System Utilizing Solid  
Adsorbents



17A - 81

81

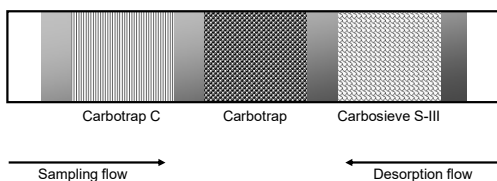
Single Tube Design-Glass/Stainless  
Steel



17A - 82

82

Multi-bed Adsorbent Trap



17A - 83

83

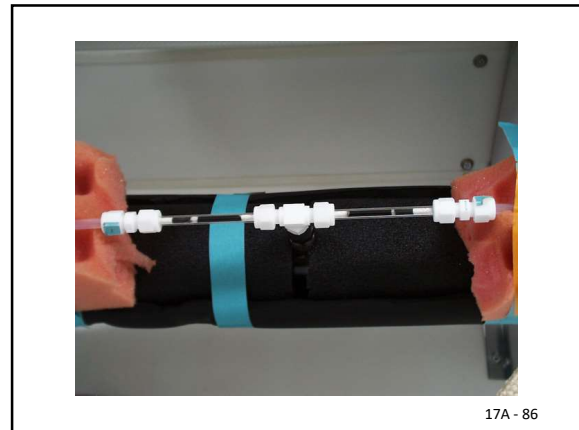


17A - 84

84



85



86



87

Adsorbent Tube Sampling

- Strengths
  - Sample compact and easy to use
  - Sample returned to laboratory for analysis
  - Good sample storage time

17A - 88

88

Adsorbent Tube Sampling

- Weaknesses
  - Quantitative recovery poor
  - Breakthrough possible of interested analytes
  - Moisture may affect sample recovery

17A - 89

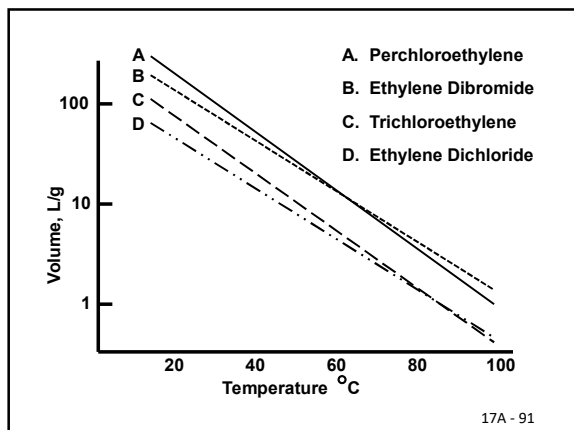
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Breakthrough Volume

- Breakthrough volume is when the analyte entering the adsorbent bed is also leaving the adsorbent bed at the same rate

17A - 90

90



91

Published Breakthrough Volumes  
(at 20°C)

- Vinyl Chloride 0.6 L/g
- p-Dichlorobenzene 820 L/g
- Chlorobenzene 184 L/g
- Benzene 36 L/g
- Carbon Tetrachloride 27 L/g

17A - 92

92

Safe Sample Volume

- Safe sample volume is the published breakthrough volume (liters/gram of adsorbent) divided by 1.5 times the weight of the adsorbent used in the system

17A - 93

93

Published Safe Sample Volumes

- Vinyl Chloride <1.0 L/g
- p-Dichlorobenzene 290.0 L/g
- Chlorobenzene 74.0 L/g
- Benzene 14.0 L/g
- Carbon Tetrachloride 11.0 L/g

17A - 94

94

Adsorbent Tube Sampling

- Determine "breakthrough volume" in order to calculate sampling time and volume
- Perform recovery study of the analytes of interest during the actual field test
  - Two identical sampling trains collocated in stack

17A - 95

95

Adsorbent Tube Sampling

- Recovery study (Two sampling trains)
  - One train spikes (all compounds of interest) and the other unspiked train
  - Amount of analyte spiked should be 40-60% of mass expected to be collected by unspiked train
  - Field data adjusted with recovery value (R)

17A - 96

96

#### Adsorbent Tube Sampling

- Sample the stack gas with the collocated sampling trains for a total of 3 runs
- Determine the fraction of spiked compound recovered (R)
- Criteria of  $70 < R < 130\%$  must be met in order for sampling technique to be used for specific analyte
- $< 10\%$  in back half of adsorbent tube
- Audit analysis agrees within  $\pm 10\%$

17A - 97

97

#### Direct Interface Sampling

- Strengths
  - Sampling provides for immediate analysis
  - Minimize loss or alteration to analytes during sampling
  - Method of choice for steady state processes when duct temperature is below  $100^{\circ}\text{C}$  and organics suitable for GC analysis

17A - 98

98

#### Direct Interface Sampling

- Weaknesses
  - GC at site, can't integrate sample, non-steady state, poor recovery

17A - 99

99

#### Tedlar® Bag Sampling

- Strengths
  - Sample collected over time and has same compounds and concentrations as stack emissions
  - Sample may be returned to laboratory for analysis
  - Multiple analysis

17A - 100

100

#### Tedlar® Bag Sampling

- Weaknesses
  - Tedlar® bags awkward and bulky for shipment, stability of compounds, can't do polar

17A - 101

101

#### Recovery Studies

- Direct Interface: Mid-level calibration point for 1 analysis ( $\pm 10\%$ ) repeated twice ( $\pm 5\%$ )
- Bags: After three analysis, choose bag, spike at 40-60% of avg. concentration (70-130 % recovery), field data adjusted to R value
- Solid Adsorbent: Two identical sampling trains, one spiked and one unspiked, 70-130 % recovery, field data adjusted to R value

17A - 102

102

Which Sampling  
Technique Should Be Used?

- Direct Interface: Excellent, provides real-time data if all analytes can be separated by one column/detector combination
- Dilution Interface: Same benefits as direct interface; excellent if high concentrations of target compounds are present in stack gas

17A - 103

103

Which Sampling  
Technique Should Be Used?

- Adsorbent Tube: Excellent if concentrations of target compounds are sub-ppm levels
- Bag Sampling: Everybody's favorite; cheap; excellent when more than one detector is needed; excellent for explosive environments

17A - 104

104

FRM 18  
Adsorbent Tube Sampling

- Any commercially available adsorbent is allowed
- May use water knockout impinger before adsorbent

17A - 105

105

FRM 18  
Adsorbent Tube Sampling

- Must perform dual sampling trains, one spiked and one unspiked
- Three dual-sampling trains constitutes a test

17A - 106

106

FRM 18  
Adsorbent Tube Sampling

- Desorption/analysis usually performed in lab
- May perform solvent or thermal desorption
- If solvent desorption, analyze each in triplicate

17A - 107

107

FRM 18  
Adsorbent Tube Sampling

- If thermal desorption, analyze each sample once
- Recovery of PE must be 70-130%

17A - 108

108

FRM 18  
Adsorbent Tube Sampling

- Method applicable to most sampling programs when
  - 10 or less compounds
  - compounds are known
  - fairly high vapor pressure at room temperature

17A - 109

109

FRM 18  
Adsorbent Tube Sampling

- ppb to ppm levels dependent on use of adsorbent or Tedlar® bag
- mass balance around system is required
- should not be used after combustion source unless compounds identifiable

17A - 110

110

FRM 18 Pre-survey Requirements

- A pre-survey shall be performed on each source to be tested to obtain all information necessary to design emission test
- Pre-survey optional if target compounds are known

17A - 111

111

FRM 18 Pre-survey Requirements

- Only place where canister sampling is allowed
- Typically grab sample, qualitative analysis, GC/MS for identification
- Canisters can be used during pre-survey

17A - 112

112

FRM 18 Pre-survey Requirements

- Obtain stack temperature and temperature range
- Obtain approximate particulate concentration
- Obtain static pressure and water vapor content

17A - 113

113

FRM 18 Pre-survey  
Sample Train Selection

- 250 mL double-ended glass sampling flask (specified cleaning procedures provided)
- Method 7 evacuated flask
- Tedlar® or aluminized Mylar flexible bag
- Adsorption tubes
- Specially-treated canisters

17A - 114

114





115



116



117



118

FRM 18 Pre-survey  
Sample Analysis

- Select GC columns based upon manufacturer's recommendation
- Select GC conditions for good resolution by varying conditions after 1st injection

17A - 119

119

FRM 18 Pre-survey  
Sample Analysis

- Heat pre-survey sample to duct temperature
- Analyze pre-survey samples using retention time (RT) compared to calibration standards

17A - 120

120

Criteria for Pre-survey  
and Sample Analysis

- Prepare calibration standards by proper technique
- Determine optimum GC settings
- Obtain retention times with repeatability of  $\pm 0.5$  seconds

17A - 121

121

Criteria for Pre-survey  
and Sample Analysis

- Use smaller sample loop or dilution if necessary
- Identify all peaks  $> 5\%$  of the total area (i.e., tentatively identified compounds [TICs])

17A - 122

122

Preparation of  
Calibration Standards

- Liquid standard in desorbing solution
- Direct analysis of NIST reference gases or commercial certified gas mixtures

17A - 123

123

Preparation of  
Calibration Standards

- Gas dilution from high concentration of gas cylinder using calibrated rotameters
- Direct syringe-bag dilution for known quantity volatile liquid material

17A - 124

124

Preparation of  
Calibration Standards

- Indirect syringe-bag dilution for known quantity of less volatile liquid materials

17A - 125

125

FRM 18 Final Sampling  
and Analysis Procedure

- Consider safety and source conditions, select appropriate sampling and analysis procedures (use direct interface if source  $< 100^\circ\text{C}$  and organics suitable for detection)

17A - 126

126

FRM 18 Final Sampling  
and Analysis Procedure

- If source has high concentration (> 100 ppm), then select direct dilution interface technique

17A - 127

127

FRM 18 Compliance Test  
Direct/Dilution Interface

- On-line, on-site GC
- Real-time analysis
- Triplicate injections, three concentrations of each target compound for generation of calibration curve

17A - 128

128

FRM 18 Compliance Test  
Direct/Dilution Interface

- Calibration gas must be certified to 2% accuracy by manufacturer
- Method 205 allowed

17A - 129

129

FRM 18 Compliance Test  
Direct/Dilution Interface

- Recovery study basically leak check, 70-130% recovery
- Five consecutive samples equals a run

17A - 130

130

FRM 18 Compliance Test  
Direct/Dilution Interface

- Post-test calibration check
  - If > 5% difference, use both curves
  - If < 5% difference, use first curve generated

17A - 131

131

FRM 18 Summary

- Source has great flexibility in choosing sampling/analytical methodology (as long as recovery criteria are met)
- Encourage direct/dilution interface: real-time data, less chance of sampling loss

17A - 132

132

FRM 18 Summary

- Any detector, including mass spectrometer, may be used
- Any adsorbent is allowed as long as recovery met
- Analyte recovery performed once per source
- Canisters are not allowed as a compliance test technique

17A - 133

133

FRM 18 Reporting Results

- Reported Results = (Measured concentration, ppm) / R
- R = Recovery =  $(m_v)(V_s)/S$ 
  - S = Theoretical mass

17A - 134

134

U.S. EPA APTI  
Compliance Test and Source Test  
Observation  
FRM 25: TGNMOs as C



17B - 1

1

Family of Method 25s

- FRM 25: Total VOCs
- FRM 25A: Instrumental FID
- FRM 25B: Instrumental NDIR
- FRM 25C: Landfill Gases
- FRM 25D: VOC Waste Sample
- FRM 25E: VOC Waste Sample

17B - 2

2

Applicability

- Method 25 applies to the measurement of volatile organic compounds (VOCs) as total gaseous nonmethane organics (TGNMO), condensable and non-condensable, as carbon in source emissions
- This method is not applicable for the determination of speciated VOCs or organic particulate matter

17B - 3

3

Method 25

- Applicability
  - Originally developed for determining the percent reduction of VOC emissions achieved by emission control devices for automobile and light-duty truck surface coating operations
- Concerns
  - Complex method
  - Use as last resort
  - Use FRM 18 first as survey tool

17B - 4

4

FRM 25 Timeline

- Original Proposed 10/05/79
- Promulgated 10/03/80
- Amendment 11/07/86
  - Added filter heating system
  - Redesigned condensate trap
  - Specified oxidation catalyst
  - Specified new separation column
- Corrections 04/07/88

17B - 5

5

Method 25 Applicability

- Concerns
  - Not applicable for measuring concentrations of VOCs or mass emissions of VOCs from sources whose concentrations are < 50 ppm
  - Possible bias when:
    - % CO<sub>2</sub> X % H<sub>2</sub>O > 100
  - As water freezes in the trap, CO<sub>2</sub> is trapped out prematurely. The CO<sub>2</sub>, when reduced to methane, is counted as VOCs in the analytical system

17B - 6

6

### Method 25 Applicability

- Concerns
  - Not applicable for measuring emissions from sources whose principal solvents are chlorinated hydrocarbons
  - Generally, for any situation were a simpler procedure is more accurate
  - High organic droplets in gas stream can cause high bias or data variability

17B - 7

7

### Method 25 Applicability

- Concerns
  - Source which has a complex flue gas flow
  - Moisture content of the exhaust gas is much higher than what is found in the audit sample
  - The presence of organic and inorganic particulates in concentrations larger than those found in the audit sample
  - Presence of droplets, tar, and wax aerosols

17B - 8

8

### Historical Method 25 Common Problems

- High gas sample moisture content and freezing of trap
- Probe exit and filter temperatures not within specifications
- Non-constant sample flow rate
- Use of Method 25 for measuring low levels of VOCs from source
- Measurement in ducts containing organic droplets

17B - 9

9



10

### Method 25 Principle

- A gas sample is withdrawn from the stack at a constant rate through a chilled condensate trap (dry ice temperature) by means of an evacuated sample tank (> 4 L)
- Condensate trap is 3/8 " stainless steel packed with glass wool
- TGNMO are determined by combining the analytical results obtained from independent analysis of the condensate trap and sample tank fraction

17B - 11

11

### Method 25 Applicability

- Applicable to all sources where VOC emissions are to be expressed as carbon (C)
  - To be used where there are too many solvents being emitted simultaneously
  - No speciation is required

17B - 12

12

### Method 25 Applicability

- After a combustion source where compound conversion takes place and identification is difficult
- A mass balance is not required (i.e., capture efficiency is not determined)

17B - 13

13

### Method 25 Interference

- Organic particulate matter will interfere with the analysis; therefore, a particulate filter may be required (i.e., in-stack or out-of-stack)

17B - 14

14

### Method 25 Advantages

- Gives constant results from source to source whether sample composition is known or not
- Sample train does require heated probe and filter, but is less complicated than FRM 5 hardware

17B - 15

15

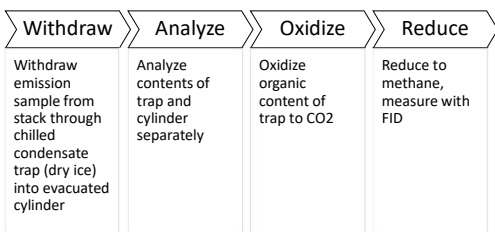
### Method 25 Disadvantages

- Will not yield true mass emission rate
- No real time data (sample must be returned to laboratory for analysis)
- High moisture and CO<sub>2</sub> together can cause interference
  - $(\%CO_2) \times (\%H_2O) > 100$  gives potential high bias (EPA Guidelines)

17B - 16

16

### Method 25 Summary



17B - 17

17

### Method 25 Summary

- Inject portion of cylinder sample into GC to separate non-methane organics, oxidize NMO to CO<sub>2</sub>, reduce to methane, and measure with FID
- Combine results (condensable and non-condensable) and report as total gaseous nonmethane organics (TGNMO)

17B - 18

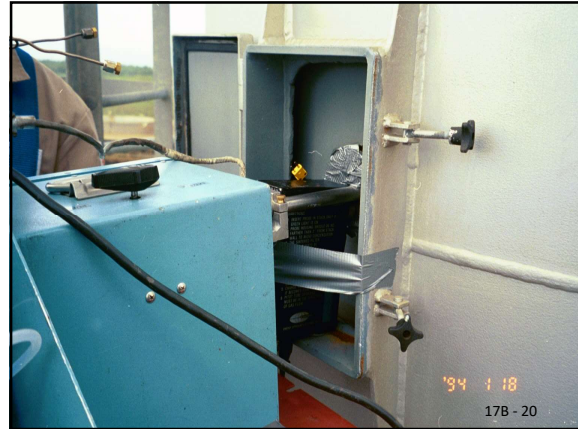
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### Method 25 Apparatus

- Sampling System
  - Probe (260 °C)
  - Filter (250 °C c 5 °C)
  - Condensate trap (-78 °C) for condensables
  - Flow control system
  - Sample tank for non-condensables

17B - 19

19



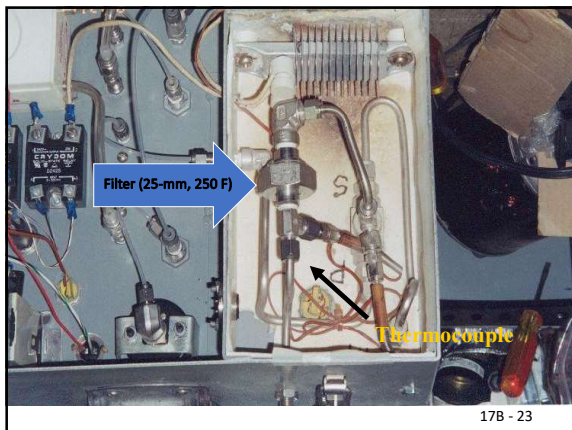
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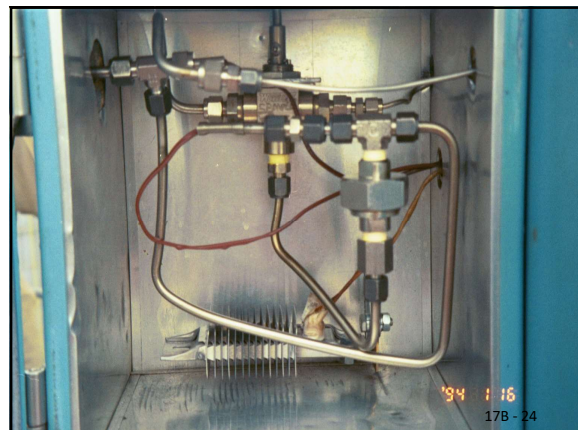
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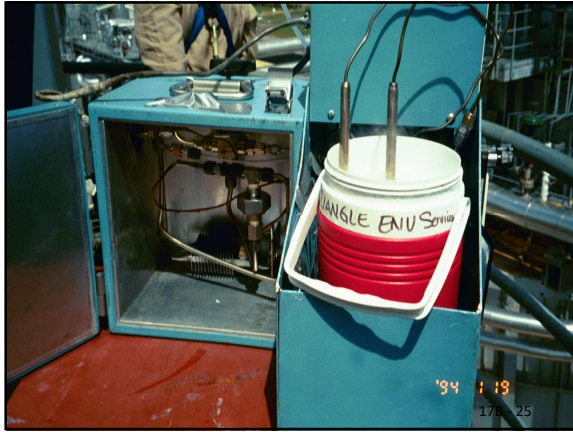


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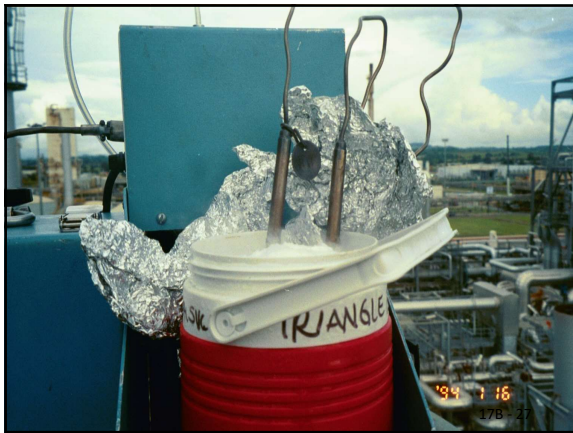




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31



32



33



34



35

**Calibration of Sampling System**

- Sample tank volume (Measure to nearest 5g of water or 5 mL)
- Volume of sampling train from probe tip to sample tank valve (This volume maximum should be 100 mL)

17B - 36

36

### Calibration of Sampling System

- Sample tank: to the nearest 5 g (if using deionized water) or to the nearest 5 mL
- Sample train volume: No limits (< 100 mL)
- Rotameter: Not calibrated
- Thermometers: Within 3°C of true value
- Barometer: Within 0.1 in. Hg of mercury-in-glass barometer

17B - 37

37

### Method 25 Sampling Train Preparation

- Leak check the tank (#1)
- Assemble the sampling train
- Leak check the entire sampling train

17B - 38

38

### Method 25 Train Preparation

- Evacuate sample tank to 10 mm Hg. Record on field test data sheet (FTDS). Set aside and recheck within 1 hour. Should be within 2 mm of previous reading
- Just before train assembly, measure tank vacuum

17B - 39

39

### Method 25 Train Preparation

- Assemble sampling system; immerse condensate trap in dry ice ~ 30 minutes before sampling
- Plug probe tip

17B - 40

40

### Method 25 Train Preparation

- Evacuate sampling system from probe tip to valve to 10 mm Hg
- Close purge valve, turn off pump, wait 10 minutes
- Record  $\Delta P$ . Vacuum should not change more than 2 mm to be acceptable

17B - 41

41

### Method 25 Train Preparation

- Calculate maximum allowable pressure change based on leak rate of 1% and compare to measured  $\Delta P$
- Record findings on FTDS

17B - 42

42

### Method 25 Sampling

- Mark probe for point of average stack gas velocity (probe  $\leq$  36 in. as specified in FRM 25)
- Check dry ice level (Maintain as high level as possible)
- Calculate flow rate, record time, set flow rate, probe temp, and filter

17B - 43

43

### Method 25 Sampling

- Attach trap to sampling train
- Position probe tip perpendicular to stack gas flow (Take plug off end)
- Purge sampling train, then adjust flow rate

17B - 44

44

### Method 25 Sampling

- Record sample tank vacuum, flow meter settings, and temperatures at 5 - minute intervals on FTDS
- Adjust the flow rate as necessary to maintain a constant rate,  $\pm 10\%$  over duration
- Sampling rate between 60-100 mL/min (i.e., 3.6 to 6.0 L of total sample acquired)
- After sampling, record final readings

17B - 45

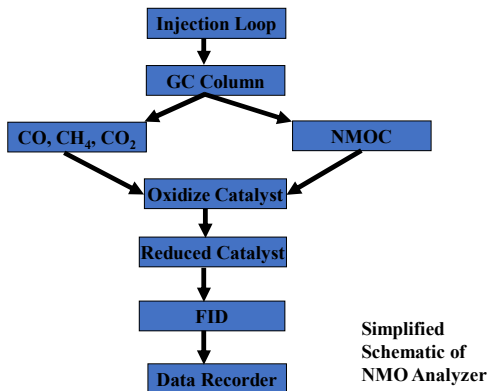
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### Method 25 Sampling

- Recover components, disconnect sample tank, record tank vacuum
- Disconnect condensate trap, seal both ends with brass fittings
- Record final readings on FTDS and chain-of-custody
- Pack trap in dry ice during storage and shipping

17B - 46

46



17B - 47

47

### Method 25 Sample Analysis

- Condensable organics in the trap are vaporized and oxidized to  $\text{CO}_2$  and collected in a separate (#2) evacuated tank
- The  $\text{CO}_2$  (which are the original condensable organics from sampling) in #2 tank is then injected into the NMO analyzer, reduced to methane, and detected with an FID

17B - 48

48

### Method 25 Sample Analysis

- Non-Condensable Organics
  - The non-condensable sample in the original field sample tank (#1) is injected into the analyzer
  - Methane, CO, CO<sub>2</sub>, and NMOC are separated, and the NMOC fraction is then back-flushed, oxidized to CO<sub>2</sub>, reduced to methane and detected with an FID

17B - 49

49

### Method 25 Apparatus

- Analytical System
  - Oxidation system for recovery and conditioning of condensate trap contents
    - Heat source
    - Oxidation catalyst (chromia @ 650 °C)
    - Non-dispersive infrared analyzer (NDIR)
    - Intermediate evacuated canister (#2)

17B - 50

50

### Method 25 Apparatus

- NMO Analyzer
- GC with back-flush capability
- Oxidizing/reducing catalyst (Ni @ 400 °C)
- FID

17B - 51

51



52



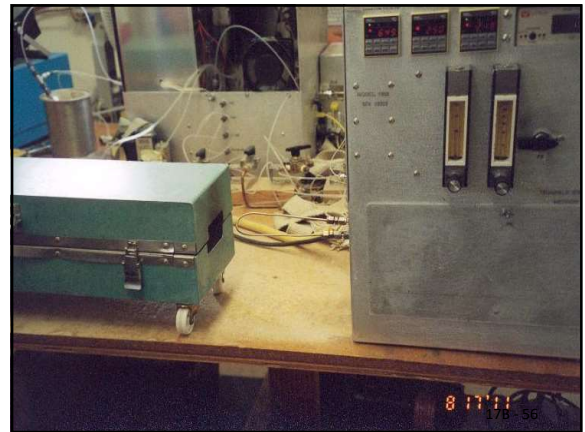
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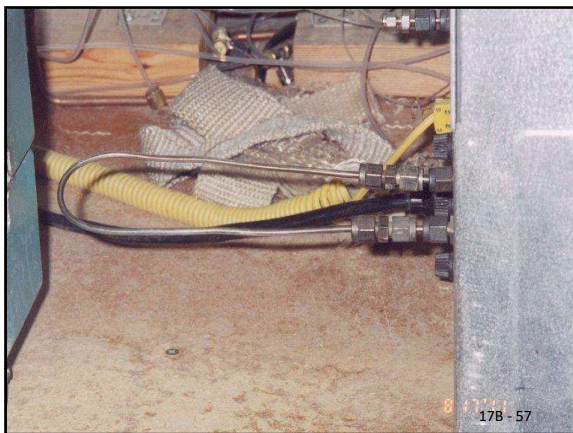
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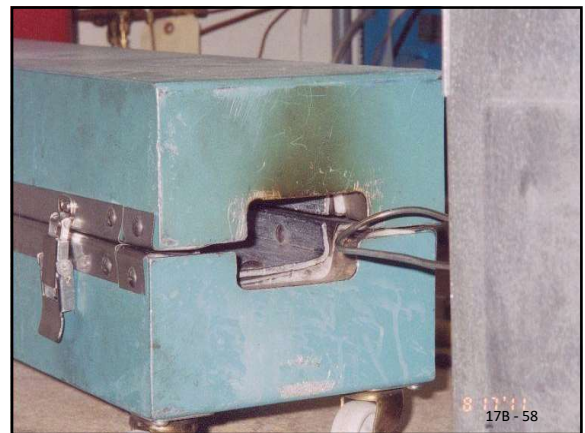
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58



59



60



61



62

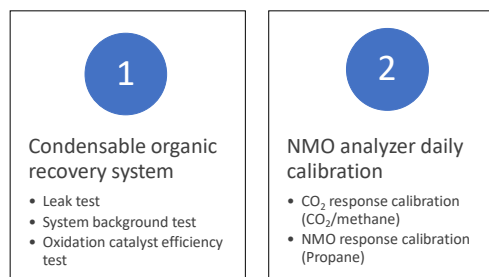
### Initial Performance Check of Condensate Recovery and Conditioning Apparatus

- Carrier gas and auxiliary oxygen blank (< 5 ppm contaminants)
- Catalyst efficiency check with 1% methane ( $\pm 2\%$ )
- System performance check
  - Hexane, toluene, methanol ( $\pm 5\%$ )

17B - 63

63

### Daily Performance Tests



17B - 64

64

### Condensable Organic Fraction Recovery

- Recovery of condensable organics is accomplished in two stages
  - Condensate trap is purged of CO<sub>2</sub> (< 5ppm) while cooling the trap in dry ice and put into original field tank (#1)
  - Condensate organics are volatilized and converted catalytically to CO<sub>2</sub> which is collected in an intermediate collection vessel (ICV or #2) for analysis

17B - 65

65

### Condensable Organic Fraction Recovery

- Trap purge and sample tank pressurization
  - Obtain sample tank and condensate trap
  - Set zero air flow to 100 mL/min
  - Attach the sample tank (#1) to the condensate trap recovery system

17B - 66

66

### Condensable Organic Fraction Recovery

- Measure sample tank pressure
- Immerse the condensate trap in crushed dry ice
- Observe IR response to CO<sub>2</sub> to minimum level of < 5 ppm
- Pressurize sample tank (#1) to 1060 mm Hg absolute pressure and detach

17B - 67

67

### Condensable Organic Fraction Recovery

- Recovery of condensable organics
  - Attach an ICV (i.e., #2 tank) to the trap recovery system and evacuate to 10 mm Hg
  - Set auxiliary oxygen flow to 150 mL/min
  - Switch 4-port valve to collect position

17B - 68

68

### Condensable Organic Fraction Recovery

- Remove condensate trap from dry ice and allow to warm to room temperature
- Heat trap by placing it in a furnace at 200 °C

17B - 69

69

### Condensable Organic Fraction Recovery

- Recovery of condensable organics
  - After NDIR analyzer indicates a CO<sub>2</sub> concentration of < 10,000 ppm, begin heating the tubing that connects the condensate trap to the oxidation catalyst with a heat gun

17B - 70

70

### Condensable Organic Fraction Recovery

- Continue trap heating and purging until the CO<sub>2</sub> concentration is below 10 ppm
- Pressurize the ICV (i.e., #2) to approximately 1060 mm Hg

17B - 71

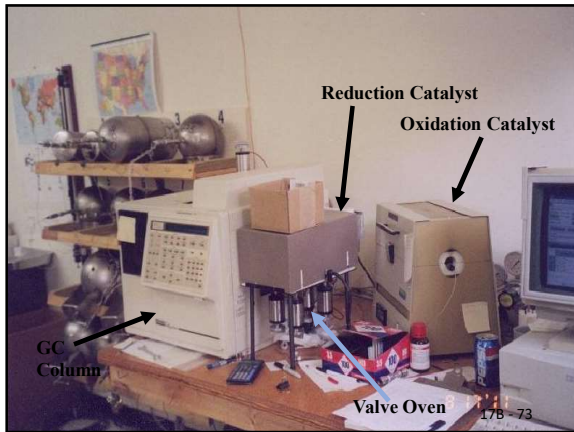
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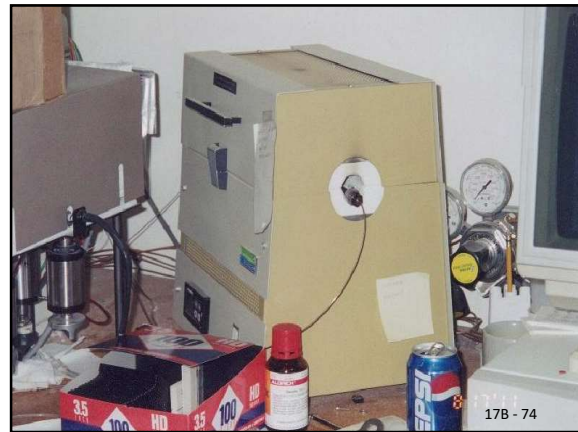
17B - 72

72

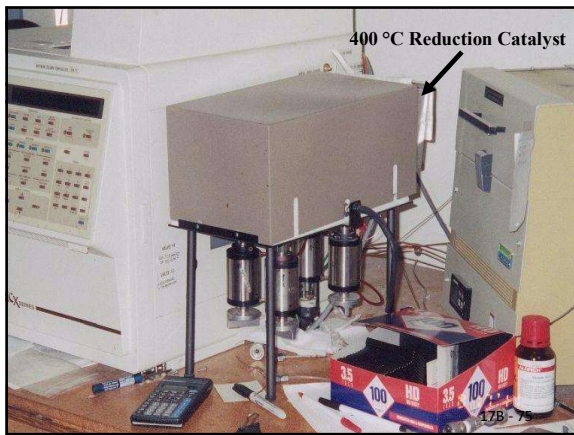




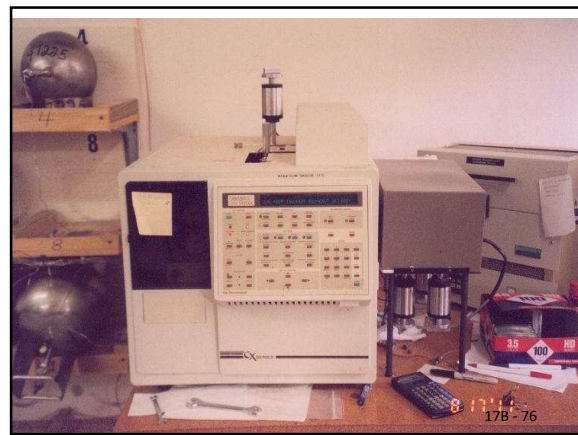
73



74



75



76



77



78

### Method 25 Apparatus

- Method 25 NMO Analyzer Apparatus
  - GC with back-flush capability
  - Oxidizing catalyst (19 % chromia on alumina @ 650 °C)
  - Reducing catalyst (Ni @ 400 °C)
  - FID

17B - 79

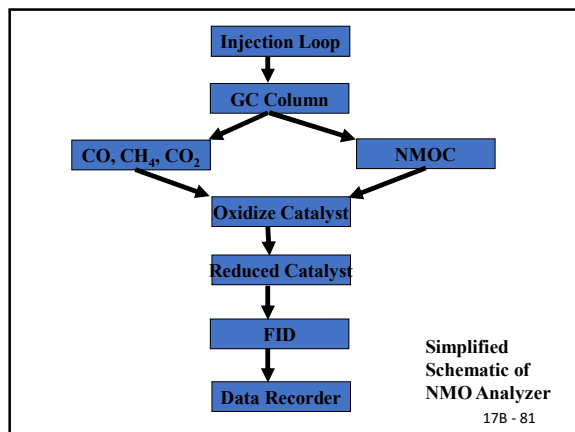
79

### Method 25 Sample Analysis

- Both Tanks (#1: Sample) and #2 (ICV)
  - Sample in both tanks (#1 and #2) are injected into the NMO analyzer
  - Methane, CO, CO<sub>2</sub>, and NMOC are separated, and the NMOC fraction is then back-flushed, oxidized to CO<sub>2</sub>, reduced to methane, and detected with an FID
  - Original tank (#1) only NMO quantified

17B - 80

80



81

### Method 25 Analysis

- ICV (i.e., #2) Analysis
  - Attach the ICV (#2) to the 10-port gas sampling valve
  - Purge sample loop
  - When detector response returns to near baseline after CO<sub>2</sub> peak, back-flush and increase column oven temperature

17B - 82

82

### Method 25 Analysis

- After detection of any NMOC, return column oven temperature to 85 °C
- Record the CO<sub>2</sub> peak area and NMO peak area
- Repeat analysis two additional times

17B - 83

83

### Method 25 Analysis

- Sample Tank (#1): Same as ICV (#2)
  - Inject triplicate samples from the sample tank and record the values obtained for nonmethane organics only
  - Perform three analyses and average the NMO values

17B - 84

84

Method 25 Calculations

- Sample volume
- Noncondensable organics
- Condensable organics
- Total gaseous nonmethane organics
- Percent recovery
- Relative standard deviation
- EPA provides audit sample

17B - 85

85



86



87



88



89



90

### Method 25 QC Checks

#### 1. Oxidation Catalyst Efficiency Test

1 % CH<sub>4</sub>

Oxid./Red. Cat. Unheated (R1)

Oxid Cat. Heated (R2)

Oxid. Cat. Eff. =  $R1 - R2/R1 \times 100$

17B - 91

91

### Method 25 QC Checks

#### 2. Reduction Catalyst Efficiency Test

1 % CH<sub>4</sub>

Oxid. Cat. Unheated + Red. Cat. Heated (R4)

Oxid./Red. Cat. Heated (R3)

Red. Cat. Eff. =  $R4/R3 \times 100$

17B - 92

92

### Method 25 QC Checks

#### 3. NMO Response Linearity Test

20, 200, 3000 ppm propane standard

Response Factor (RF) within 2.5 % over range, then linear response

17B - 93

93

### Method 25 QC Checks

#### 4. CO<sub>2</sub> Response Linearity Test and Initial Calibration

50, 500, 10,000 ppm CO<sub>2</sub> standard

Response Factor (RF) within 10 % over range, then linear response

17B - 94

94

### Method 25 QC Checks

#### 5. NMO Analyzer Performance (ppmC)

Std #1: 50 ppm CO, 50 ppm CH<sub>4</sub>, 2 % CO<sub>2</sub>, 20 ppm Propane

Std #2: 50 ppm Hexane

Std #3: 20 ppm Toluene

Std #4: 100 ppm Methanol

Criteria: ± 5%

17B - 95

95

### Method 25 QC Checks

#### 6. Condensible Organic Recovery System Check

Stage #1: Carrier Blank Check (< 5 ppm)

Stage #2: Oxidizing Catalyst

Stage #3: Known Organic Concentration

17B - 96

96

### Method 25 Daily QC Checks

1. Leak test of condensable recovery system (< 10 mm Hg for 10 minutes)
2. System background check (Syringe of gas < 10 ppm CO<sub>2</sub>)
3. Oxidation catalyst efficiency check
4. CO<sub>2</sub> analyzer response
5. NMO response check

17B - 97

97

### Method 25 Guide

- Make sure tanks, traps, and sample trains are clean (< 1 ppm)
- Analyze confirmation preferred
- Leak check sampling trains in the field, even though they are checked in the lab

17B - 98

98

### Method 25 QC Checks

#### EPA Audit Sample (2)

Between 50 % below standard and 100 % above standard ± 20% of known concentration

17B - 99

99

### Method 25 Guide

- Leak check cold (minimize heating/re-cooling system)
- Leak check before adding trap
- Leak check canisters before use in field
- Leak check with rotameter completely open

17B - 100

100

### Method 25 Guide

- Setup sampling train properly
- DO NOT over-tighten the filter or the swage fittings
- If there is a leak, go to last fitting disturbed
  - Use logical approach to find leak
  - Isolate specific areas in the sample train

17B - 101

101

### Method 25 Guide

- Get most accurate pre-test and post-test barometric pressures, tank vacuums, and temperature possible
- Used in sample volume

17B - 102

102

### Method 25 Guide

- Use small pellets of dry ice around the trap to increase contact to trap organics
  - This will generate better results (esp. oxygenated organics)

17B - 103

103

### Method 25 Guide

- Monitor both sample flow and tank vacuum with the rotameter and gauge on the unit
- Vacuum gauge is not accurate, but used as an indicator of proper sampling

17B - 104

104

### Method 25 Guide

- Take care that the brass caps from the traps don't come into contact with pump oil, vacuum grease, or other contaminants
- Use tags to identify the tank/trap pairing, as well as noting the pairings on the sample data sheet

17B - 105

105

### Method 25 Guide

- Seal both arms of the trap with the brass caps and pack the cooler with sufficient dry ice to ensure the temperature is maintained until receipt at the labs

17B - 106

106

### Method 25 Guide

- Perform Method 25 gas audits prior to field sampling to minimize carryover of contaminants from a dirty sampling train (Audit through sample train)
- If sampling blanks are part of the program, a preferred method is to collect a clean air sample over a one-hour period using the project sampling train components (i.e., blank train)

17B - 107

107

### Method 25 Guide

- If high concentrations are expected, then collect only 3.5 L sample
- If low concentrations are expected, then collect larger volume of gas (Increase trapped sample volume)

17B - 108

108

### Method 25 Guide

- If very high moisture is expected, then add an ice water second trap in front of the cryogenic trap to prevent freezing water from plugging the sample flow

17B - 109

109

### Method 25 Guide

- However, this increases analytical cost and may increase the positive bias from trapping CO<sub>2</sub>
- This approach does appear to limit sampling problems

17B - 110

110

### Observations

- Obtain the most accurate pre-test and post-test barometric pressure, tank vacuums, and temperatures. This data determines the volume of gas sampled. Don't use gauge on control box for tank vacuum measurement...it isn't accurate enough and effects final volume sampled
- Do not over tighten swage-lock fittings as part of the sample train

17B - 111

111

### Observations

- A pre-test leak check is required. Suggest set-up everything and leak check without the dry ice and condensate trap. This limits the number of components that might leak
- Method suggest purge the probe for 10 minutes at 60-100 cc/min. If the source has high moisture, then purge only for 5 minutes to minimize possible freezing of trap

17B - 112

112

### Observations

- FRM 25 requires you to evacuate the sample tank to <10 mm Hg absolute. Need laboratory pump and may take several attempts and 5 minutes to reach that value
- Purchase dry ice in small pellets. Pack the condensate trap to top of weld and cover dry ice during sampling with aluminum foil

17B - 113

113

### Observations

- Make sure that the sample canister and condensate trap are both labelled properly with the same sample run. The VOCs are determined from both components for that single sample run
- If sampling a high particulate source, then change the filter after each run to minimize potential biases in the analysis

17B - 114

114

### Observations

- If you are sampling a source with high moisture (> 20%) and high CO<sub>2</sub> (>20%), then there is a real possibility that your trap will freeze at the very top of the trap.
  - Use hair dryer to unfreeze trap
  - Remove foil and let the sun melt the plug at the top of the trap
  - Add a dry water impinger in front of the condensate trap. However, must analyze content of that trap also

17B - 115



U.S. EPA APTI  
Compliance Test and Source  
Test Observation

Federal Reference  
Method 25A

Determination of Total Gaseous  
Organic Concentration Using A Flame  
Ionization Detector (FID)

17C - 1

1

Family of Method 25s

- FRM 25: Total VOCs
- FRM 25A: Instrumental FID
- FRM 25B: Instrumental NDIR
- FRM 25C: Landfill Gases
- FRM 25D: VOC Waste Sample
- FRM 25E: VOC Waste Sample

17C - 2

2

Method 25A Timeline

- Proposed 12/17/80
- Promulgated 08/18/83

17C - 3

3

FRM 25A

- Originally developed to determine compliance with VOC emission standards for bulk gasoline terminals
- FRM 25A not recommended for high moisture (> 40 % by volume)
- High organic droplets in gas stream can cause high bias or data variability

17C - 4

4

FRM 25A Uses

- Incinerators
- Carbon Adsorption Units
- Coating and Printing Operations
- Web Offset Presses
- Method 25A measures total hydrocarbons (THCs) (i.e., non-compound specific)

17C - 5

5

Applicability

- This method is applicable to the measurement of total gaseous organic concentration of vapors consisting primarily of alkanes, alkenes, and/or arenes (aromatic hydrocarbons)
- Only measures C-H bond very well and analytes that can generate a response factor (RF)

17C - 6

6

### Applicability

- Results from the use of FRM 25A are expressed in terms of volume concentration of propane (or other appropriate organic calibration gas) or in terms of carbon

17C - 7

7

### Applicability

- Results from FRM 25A are measured on a wet basis and the concentration must be adjusted for the percent moisture in the sample gas stream for the purpose of emission calculations

17C - 8

8

### Applicability

- FRM 25A *"...can only be used where an appropriate response factor for the stack gas can be determined"*

17C - 9

9

### Instrument Response Factors (RF)

- The instrument response factor for the compound of interest is determined by:
  - Response Factor (RF) = (Act. Conc.) / (Instru. Observ. Conc.)
  - Typical RF:
    - Benzene: 0.29
    - Chloroform: 9.28
  - M25A requires RF determination

17C - 10

10

### Agency Example RF Application (Surface Coating Operation)

- Four analytes which you know % of solvent used in mixture
- Standard prepared with that same percent ratio in mixture in gas std.
- Response of analyzer in ppm as carbon
- Concentration of gas stream is determined by dividing by RF

17C - 11

11

### Applicability

- The concentration is expressed in terms of propane (or other appropriate organic calibration gas) or in terms of carbon
- Measurement is made on a wet bases and emissions must be adjusted accordingly to dry bases
- Span value of the analyzer is usually 1.5 to 2.5 times the applicable emission limit

17C - 12

12

### FRM 25A Items

- Calibration for FRM 25A should be done using EPA Traceability Protocol gas standards, preferably propane
- The sample line should be heated ( $\geq 110^{\circ}\text{C}$ ) to prevent any condensation. Heating above 400 F is not required.

17C - 13

13

### FRM 25A Items

- A system bias check is required and is performed by introducing the bias check standard directly into the FID and then through the entire sampling system, excluding the probe. Results must agree within 5 % to be acceptable

17C - 14

14

### FRM 25A Items

- The bias check standard must be representative of the effluent (i.e., boiling point, solubility, chemical reactivity etc.). Propane may be used if effluent is unknown.

17C - 15

15

### FRM 25A Items

- For the bias test, propane should be used at the following processes:
  - Incinerators, boilers, asphalt plants, cement plants and resource recovery facilities.
- For the bias test, propane should NOT be used at the following processes:
  - Bakeries (using yeast), ethylene oxide sterilizers, chemical manufacturing facilities (HON/SOCMI), surface coating operations, and graphic arts operations

17C - 16

16

### FRM 25A Items

- Calibration error test must be performed within 2 hours of start of testing
  - Introduce zero and high level standard, adjust
  - Introduce low and mid level standard, no adjustment. Criteria of 5 %
- Perform response time test at same time as calibration error test for zero and high level standard. Repeat 3 times and record. Typically  $< 1$  minute

17C - 17

17

### FRM 25A Items

- Drift determination is determined each hour during the test
  - Introduce zero and mid-level gas standards
  - Criteria:  $< 3$  %
- FRM 25A sampling system must be leak checked prior to monitoring
- Location of sampling point can be a single point ( $> 1.5$  meters from inside wall of stack) or raked probe (16.7, 50, 83.3 %)

17C - 18

18

### Wet Bases to Dry Bases

- Wet bases measurement emissions to dry bases measurement emissions:

$$C_{s(dry)} = \frac{C_{s(wet)}}{(1-BWS)}$$

$$C_{s(dry, STP)} = \frac{C_{s(wet)}}{(1-BWS)} \times \frac{(T_s)(P_{std})}{(T_{std})(P_s)}$$

17C - 19

19

### Principle

- A gas sample is extracted from the source through a heated sample line and filter to a total hydrocarbon analyzer (THC) containing a flame ionization detector (FID)
- All sampling components leading to the analyzer shall be heated  $\geq 110^\circ\text{C}$  ( $220^\circ\text{F}$ )
- The flame ionization detector block shall be heated  $>120^\circ\text{C}$  ( $250^\circ\text{F}$ ).

17C - 20

20

### Principle

- Sampling is performed on a continuous, real-time basis with results proportional to the carbon content of the sample stream passing through the detector on a wet bases
- FID is linear from 0-10,000 ppm (If higher concentrations, then use dilution system)
- Method 25A is good up to about 40 % moisture in the stack gas

17C - 21

21

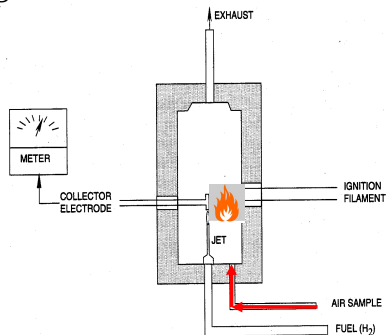
### FID Theory

- Basic Theory:
  - Sample is introduced into an ionization chamber and burned
  - Process separates free ions
  - Free ions are attracted to a collecting electrode
  - Collection of the ions results in an increased current which is proportional to the concentration of the compound
  - By-products are  $\text{H}_2\text{O}$  and  $\text{CO}_2$

17C - 22

22

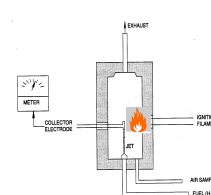
### Diagram of FID



17C - 23

23

### Flame Ionization Detection

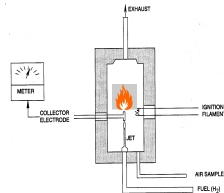


- Advantages
  - Wide dynamic and linear range (0-10,000 ppm)
  - Highly sensitive to hydrocarbon vapors
  - Very stable and repeatable
  - Unaffected by ambient levels of  $\text{CO}$ ,  $\text{CO}_2$  and water vapor

17C - 24

24

### Flame Ionization Detection



- Disadvantages
  - Requires oxygen > 16% to operate
  - Total hydrocarbon detector - not specific

17C - 25

25

### Principle

- FRM 25A results are measured on a wet basis and the concentration must be adjusted for the percent moisture in the sample gas stream for purposes of emission calculations

17C - 26

26

### Principle

- In general alkanes, alkenes, and aromatics are the most appropriate compound groups for FRM 25A sampling and analysis
- May also be used on C, H & O compounds. Ethanol gives ~ 60% signal to that of propane, but can still be used for ethanol

17C - 27

27

### FRM 25A Limitations

- Sensitivity greatest for the alkane, alkene, and aromatic organic compounds
- FRM 25A can only be used in situations where an appropriate response factor for the stack gas constituents can be determined

17C - 28

28

### FRM 25A Limitations

- Gas streams with high moisture (> 40%) can affect response of the FID
- Limitations of the FID. FID response is different for different analytes
- Large quantities of methane present gives questionable results
- Sample gas needs O<sub>2</sub> (> 16 %) for combustion in the FID

17C - 29

29

### FRM 25A Sampling System

- Sample Probe: A heated (> 250°F) stainless steel, three-hole rake type probe. Holes should be 4 mm diameter or smaller and located at 16.7, 50, and 83.3% of the equivalent stack diameter
- Alternatively, a single opening probe may be used so that a gas sample is collected from the centrally located 10% area of the stack cross-section

17C - 30

30

### Options for Sampling Point

- Single point in centroid of stack
- Single point at average velocity of stack gas
- Rake probe (i.e., 16.7%, 50%, and 83.3% of the equivalent stack diameter)
  - Therefore, FRM 2 needed to determine cyclonic flow and velocity of stack gas

17C - 31

31

### FRM 25A Sampling System

- Sample Line: Heated (> 250°F) stainless steel or Teflon® tubing
- All components must be heated > 250°F so moisture and organics don't drop out of the gas stream
  - Check unions for cold spots
  - Check for unheated transfer line
  - Check for sudden spiking at steady state conditions
  - Check for unheated filter

17C - 32

32

### Sampling System

- Calibration Valve Assembly:  
A heated (> 250°F) three-way valve at exit of probe assembly to direct the zero and calibration gases to the analyzer
- Particulate Filter: An in-stack or an out-of-stack heated (> 250°F) glass fiber filter assembly
- Pump: A heated (> 250°F) leak-free diaphragm type

17C - 33

33

### Sampling System

- Organic Concentration Analyzer:  
A heated (> 250°F) total hydrocarbon analyzer (THC) with a flame ionization detector (FID)
- Recorder: A strip-chart, digital recorder, or computer for recording measurement data

17C - 34

34

### FRM 25A Gases

- Fuel: 40% H<sub>2</sub>/60% He or 40% H<sub>2</sub>/60% N<sub>2</sub>
- Zero Air: High purity air with less than 0.1 ppmv of organic material (propane or carbon equivalent)
  - Most systems use 100% H<sub>2</sub> as the fuel which makes for a hotter flame

17C - 35

35

### Gases

- Calibration Gases (i.e., propane in air/N<sub>2</sub>)
  - Low-level calibration gas: An organic calibration gas with a concentration equivalent to 25 to 35% of the applicable span value
  - Mid-level calibration gas: An organic calibration gas with a concentration equivalent to 45 to 55% of the applicable span value

17C - 36

36

### Gases

- High-level calibration gas: An organic calibration gas with a concentration equivalent to 80 to 90% of the applicable span value

(Note: Use hydrocarbon/air standards; Propane/N<sub>2</sub> may yield inaccurate results!)

17C - 37

37

### Steps to Perform An Analysis

- Analysis of PE sample not mandatory, but suggested, due to calibration gases are NIST traceable!
- Leak Check System not mandatory, but suggested!
- Calibration Error Test (With Propane):  $\pm$  5% of calibration gas value

17C - 38

38

### Steps to Perform An Analysis

- Response Time Test: 1-2 minutes; traditionally < 1 min; No specifications in FRM 25A
- Calibration Drift (Zero/Mid-span Gas)Test (No adjustments allowed to analyzer):  $\pm$  3% of span value

17C - 39

39

### Pre-test Requirements

- Sampling Site: Located as required by the specific regulations (i.e., exhaust stack, inlet line etc.)
- At a minimum, 1.5 to 2 equivalent stack diameters upstream of the gas discharge to the atmosphere

17C - 40

40

### Pre-test Requirements

- Assemble the sampling system following manufacturer's specification
- Prepare sample interface from stack to extraction system
- Make system operable

17C - 41

41

### Pre-test Requirements

- All delivery pressures of the gases to the THC/FID system must be maintained at the same value used during calibration and sampling

17C - 42

42

### First Step To Perform An Analysis

- Leak Test of System: Perform both positive and negative leak check of sampling and analytical system
  - 1. Vacuum: Attach manometer to probe inlet, pull 2 in. of Hg vacuum; no leak for 1 minute
  - 2. Pressure: After pump, apply pressure and use soapy water to determine leaks at all joints/connections

17C - 43

43

### Pre-test Requirements

- After leak test of system, place probe at centroid of stack, pipe, or duct and is sealed tightly

17C - 44

44

### Remember Sampling Point Options!

- Single point in centroid of stack
- Single point at average velocity of stack gas
- Rake probe (i.e., 16.7%, 50%, and 83.3% of the equivalent stack diameter
  - Therefore, FRM 2 needed to determine cyclonic flow and velocity of stack gas

17C - 45

45

### Calibration of M25A

- Calibration of THC/FID Analytical System: Generate a series of high, mid, and low range calibration gases of known concentrations spanning the linear range of the FID and introduce at the calibration valve assembly to the THC/FID
  - The analytical range must be chosen so that the source THC limit is 10 to 100% of the range
  - Calibration must be done on-site to determine RFs

17C - 46

46

### Second Step To Perform An Analysis

- Calibration Error Test (Response to True Value):  
Perform a calibration error test (within 2 hours of the start of the test) by introducing the zero and high-level calibration gases to the analyzer

17C - 47

47

### Pre-test Calibration Error

- Calibration
  - The calibration gases are usually propane in air, propane in nitrogen, or methane in air or nitrogen
  - Perform three injections each of the calibration gases
  - Calibration gases must be NIST traceable; Therefore, no method does not require a PE sample

17C - 48

48



### Pre-test Calibration Error

- Calibration
  - Generate calibration curve from the three injections performed in the calibration of the analytical system
  - Develop a "calibration factor" for each level of the injected calibration gases (the calibration factor should fall between 0.95 and 1.05 to be acceptable)

17C - 49

49

### Pre-test Calibration Error

- Inject zero and high level (80-90 % of span value) at the calibration valve
- Adjust the analyzer output to the appropriate levels
- Introduce the mid and low-level calibration gases
- Make no adjustments to the analyzer
- If system is linear, differences should be < 5%

17C - 50

50

### Pre-test Calibration Error

- If can't meet < 5% of the calibration gas concentration value, then system must be replaced or repaired
- No adjustments can be made to the system after the calibration error test and before the calibration drift test
  - If adjustments are required, perform the calibration drift test prior to the adjustments and repeat the calibration drift test after the adjustments

17C - 51

51

### Third Step To Perform An Analysis

- Response Time Test: Response time test is used to document response of gases by the THC/FID analytical system
  - Introduce zero gas at the calibration valve assembly
  - When the system output has stabilized, switch quickly to the high-level calibration gas

17C - 52

52

### Pre-test Requirements

- Record the time from the concentration change to the measurement system (no limit specified, just determine)
- Repeat the test three times
  - Just record results
- Response time should be < 1 minute, but can be 1-2 minutes
  - FRM 25A does not specify limit

17C - 53

53

### Fourth Step To Perform An Analysis: Sampling

- Purge the sample system for a period of time longer than the response time of the system
- Mark the start time on the data recorder after purging. Remember, all delivery pressures of the gases to the THC/FID system must be maintained at the same value used during calibration and sampling
- Begin sampling!!!

17C - 54

54

### Fifth Step To Perform An Analysis: Post-test

- Calibration Drift Determination: Immediately following completion of the test period (and hourly during the test), perform a calibration drift test
  - Reintroduce the zero and mid-level calibration gases, one at a time, to the measurement system at the calibration valve

17C - 55

55

### Post-Test Procedures

- Make no adjustments to the instrument, just record response
- If drift exceeds 3% (span value) for either gases, invalidate the test results preceding the check
  - If you fail drift test during run, then void sample to that point from the last acceptable drift test, recalibrate, and then continue!

17C - 56

56

### Organic Concentration Calculations

- Calculated as ppm<sub>v</sub> as carbon

$$C_c = K C_{meas}$$

Where:

- K = 1 for methane
- K = 2 for ethane
- K = 3 for propane
- K = 4 for butane
- K = Appropriate response factor for other organic calibration gases

17C - 57

57

### Agency Bias Check

- Agency bias check is not required by FRM 25A
- Bias check procedure:
  - Introduce bias gas standard at back of analyzer
  - Introduce bias gas standard through entire sampling system
  - If results agree within 5% of bias gas standard concentration, then PASS!

17C - 58

58

### Agency Bias Check

- Bias gas standard must be representative of the effluent as a whole with regard to BP, water solubility, and chemical reactivity
- Propane may not be used for the following facilities:
  - Bakeries, ethylene oxide sterilizers, chemical manufacturing facilities, surface coating operations and graphic arts operation

17C - 59

59

### Method 25A Notes

- The use of Method 25A usually must be justified to regulatory agencies instead of using Method 25. Key points would be:
  - Expected concentration < 50 ppm
  - VOCs known to consist of C and H
  - (CO<sub>2</sub>)(H<sub>2</sub>O) > 100 %
- Set-up instrument in environmentally controlled room to minimize instrument drift

17C - 60

60

### Method 25A Notes (Contd)

- To minimize condensation of VOCs in the analytical system, keep at least 10 °F hotter than rest of system
- Protocol 1 standard should be used for calibration, but other standards allowed if manufacturer certified accurate is 2 %
- Void test run if using expired standards....but!

17C - 61

61

### Method 25A Notes (Contd)

- The entire sampling system (probe, heated sample lines, valves and manifolds) must be maintained at stack temperature or 250 °F (May go hotter/Web Offset Presses..350 °F)
  - Actual temperature of each component may want to be recorded every 15 minutes and included in final test report

17C - 62

62

### Method 25A Notes (Contd)

- Agency may require a system bias check conducted with a certified standard that has properties (boiling point, water solubility, and reactivity) similar to the effluent as a whole. *Propane is not normally acceptable by regulatory agencies!*
  - Concentration of the system bias check standard must be similar to the concentration of the stack

17C - 63

63

### Method 25A Notes (Contd)

- The analyzer temperature and pressure must be the same during sampling as it was during calibration
- Pollutant concentration must be measured on a wet basis and reported on a dry bases
- Any run in which the average VOC concentration exceeds the span must be voided

17C - 64

64

### Method 25A Notes (Contd)

- For Destruction Efficiency (DE) Testing:
  - The same sampling method should be used; The outlet test location determines the method (i.e., concentration, % H<sub>2</sub>O etc.)
  - The results (lbs/hour) at both the inlet and outlet must be on the same bases (as propane or as VOCs)

17C - 65

65

### Method 25A Notes (Contd)

- The actual emissions should be determined if at a VOC coating source:


$$\text{Emission Rate} = \{(\text{Coating Usage}) \times (\text{Coating Usage}) \times (1 - \text{DE}) \times (\text{CE})\} + \{(\text{Coating Usage}) \times (\text{VOC Content}) \times (1 - \text{CE})\}$$

17C - 66

66

U.S. EPA APTI  
Compliance Test and Source Test  
Observation

Weakness/Strengths FRMs 18, 25, & 25A



17D - 1

1

Lecture Objectives

- Compare the Methods
- Discuss Their Advantages and Disadvantages
- Describe Current EPA Guidance on Their Use

17D - 2

2

Background

- FRM 25 - measures total VOC
- FRM 25A - measures total hydrocarbons (THC)
- FRM 18 - measures individual organic compounds

17D - 3

3

Background

- Generally, "stack testing" is performed using FRM 25A or FRM 18
- FRM 25/25A were created in order to determine the removal efficiency of a control device

17D - 4

4

Background

- Typically, once a method is promulgated (and sometimes before it is) the method will be used for a variety of purposes including functions that it was not designed to perform
- FRM 25 and FRM 25A are not applicable to mass emission rate

17D - 5

5

Background

- FRM 25
  - Samples are time integrated
  - Analysis is completed off site
- FRM 25A
  - Sampling is continuous
  - Analysis is done on site

17D - 6

6

Background

- FRM 18
  - Samples can be time integrated or semi-continuous
  - Analysis can be on site or off site

17D - 7

7

Background

- FRM 25
  - All compounds are converted to methane before measuring with an FID
- FRM 25A
  - All compounds are measured directly, as a whole, with an FID

17D - 8

8

Background

- FRM 18
  - Each compound is separated and measured individually with an FID

17D - 9

9

FRM 25 & 25A

- The FID can be applied to the determination of the mass concentration of the total molecular structure of the organic emissions under any of the following limited conditions

17D - 10

10

FRM 25 & 25A

- Where only one compound is known to exist
- When the organic compounds consist of only hydrogen and carbon

17D - 11

11

FRM 25 & 25A

- Where the relative percentages of the compounds are known or can be determined, and the FID responses to the compounds are known

17D - 12

12

FRM 25 & 25A

- Where a consistent mixture of the compounds exists before and after emission control and only the relative concentrations are to be assessed
- Where the FID can be calibrated against mass standards of the compounds emitted (solvent emissions, for example)

17D - 13

13

Advantages: FRM 25

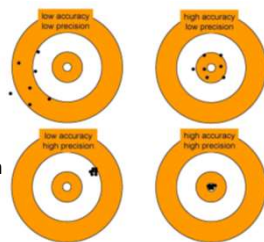
- Measures only VOC (excludes Methane)
- Responds equally to all VOC

17D - 14

14

Disadvantages: FRM 25

- Potential positive bias that may vary according to source category
- Relatively poor precision



17D - 15

15

Advantages: FRM 25A

- Very good precision
- Real time analysis
- Relatively low detection limit

17D - 16

16

Disadvantages: FRM 25A

- Does not respond equally to all VOC
- Requires a separate measurement of Methane to convert THC to VOC

17D - 17

17

Advantages: FRM 18

- Good precision
- Low detection limits
- Can exclude methane

17D - 18

18

Disadvantages: FRM 18

- Measures individual organic compounds - not total VOC
- Requires calibration standards for all measured compounds

17D - 19

19

General Guidance

USEPA Guidance Document 033  
([www3.epa.gov/ttn/emc/guidInd/gd-033.pdf](http://www3.epa.gov/ttn/emc/guidInd/gd-033.pdf))

- Use FRM 25 for unknown mixtures with concentrations greater than 50 ppm
- Use FRM 25A for unknown mixtures with concentrations less than 50 ppm

17D - 20

20

General Guidance

- Use any of the methods for known mixtures with the following conditions
  - FRM 25 should only be used for concentrations greater than 50 ppm

17D - 21

21

General Guidance

- Use any of the methods for known mixtures with the following conditions
  - FRM 25A should be calibrated with the known mixture or the results mathematically corrected for varying response factors

17D - 22

22

General Guidance

- Use any of the methods for known mixtures with the following conditions
  - FRM 18 must be calibrated for each of the compounds in the mixture

17D - 23

23

Summary

- None of the existing methods for measuring VOCs are perfect
- Because their problems can be source specific, we may have to approve alternative methods for some sources
- We must continue to improve the existing methods

17D - 24

24

### Reporting VOCs

- Many state agencies require reporting "as VOCs;" or as "carbon, methane; or propane" or "make up your own!"
- One must know how the state wants data reported for VOC emissions
- Volatile organic compounds as defined in 40 CFR 51.100

17D - 25

25

### Reporting VOCs

- The reporting format of the data must be known prior to accepting test data
  - Mass emission rates - lb/hr as carbon, methane, or propane?
  - Mass emission rates - lb/hr "as VOC"

17D - 26

26

### Case Study Molecular Weight - FRMs 25 & 25A

- Emissions testing was performed and submitted in support of a permit application
- Gas Stream consisted of ~ 100 VOCs
- Total VOCs per FRM 25A = 2.5 lb/hr as carbon

17D - 27

27

### Case Study

- One speciated compound per a compound specific test was emitted at 5 lb/hr
- Outcome
  - Facility adjusted the reported VOC emission rate using a MW that was considered 'average' for the pollutant gas stream (avg MW of the VOCs)

17D - 28

28

### Case Study

- Using the MW of carbon for mass emission rate calculation
- Consider Propylene Glycol ( $\text{CH}_3\text{CH}(\text{OH})\text{CH}_2\text{OH}$ )
- Molecular Weight is 76.10
- Assume: Concentration = 100ppm
- Qsd of 100,000 dscfm

17D - 29

29

### Case Study

- lb/hr "as carbon" (MW=12) = 18.7 lb/hr.
- lb/hr "as VOC" (MW=76.1/3) = 39.57 lb/hr.
- An error in excess of 100% due only to MW

17D - 30

30



### Case Study

- Identification of a major concern with the reporting of VOCs when using FRMs 25 & 25A
- Propose using a molecular weight adjustment
- Every organic will weigh more than just carbon

17D - 31

31

### Other Errors Involving FRM 25 & 25A

- “Response factor” error associated with FRM 25A
- The flame ionization detector (FID) used in FRM 25A does not give a 1:1 response with all organics

17D - 32

32

### FRM 18 Reporting of VOCs

- FRM 18 measures specific VOCs
- Requires knowledge of the pollutant gas stream
- Can only measure VOCs for which the GC/specific detector has been calibrated

17D - 33

33

### FRM 18 Reporting

- Difficulties
  - Sources claim that they only need to measure “total VOCs” - not speciated
  - What to do with a “soup” of VOCs?

17D - 34

34

### Summary VOC Methods

- FRM 25  
Measures Total VOC (> 50 ppm)
- FRM 25A
  - Measures Total Hydrocarbons (THC) (10-100 ppm)
- FRM 18  
Measures Individual Organic Compounds (Sub-ppm)

17D - 35

35

U.S. EPA APTI  
Compliance Test and Source  
Test Observation

*FRM 204  
PTE/TTE Enclosures,  
Capture Efficiency  
/Calculations*

18 - 1

1

USEPA Method 204

- Procedure used to determine whether a permanent or temporary enclosure meets the criteria for a total enclosure.
- An enclosure is evaluated against a set of criteria. If the criteria are met and if all the exhaust gases from the enclosure are ducted to a control device, then the volatile organic compounds (VOC) capture efficiency (CE) is assumed to be 100 percent, and CE need not be measured.

18 - 2

2

Natural Draft Opening (NDO)

- Natural Draft Opening (NDO). Any permanent opening in the enclosure that remains open during operation of the facility and is not connected to a duct in which a fan is installed.

*Equivalent diameter*

$$ED = \sqrt{\frac{4 \times A}{\pi}} \quad (\text{Circle or square/rectangle})$$

*or*

$$ED = \frac{2LW}{(L+W)} \quad (\text{square/rectangle})$$

18 - 3

3

Permanent Total Enclosure (PTE)

- Permanently installed enclosure that completely surrounds a source of emissions such that all VOC emissions are captured and contained for discharge to a control device.

18 - 4

4

Criteria for Permanent Total Enclosure

1. Any NDO shall be at least four equivalent opening diameters from each VOC emitting point unless otherwise specified by the Administrator.
2. The total area of all NDO's shall not exceed 5 percent of the surface area of the enclosure's four walls, floor, and ceiling.
3. The average facial velocity ( $F_v$ ) of air through all NDO's shall be at least 3,600 m/hr (200 fpm). The direction of air flow through all NDO's shall be into the enclosure.
4. All access doors and windows whose areas are not included in section 5.3 and are not included in the calculation in section 5.3 shall be closed during routine operation of the process
5. shall be closed during routine operation of the process
6. All VOC emissions must be captured and contained for discharge through a control device

18 - 5

5

Permanent Total Enclosure



18 - 6

6

### Temporary Total Enclosure (TTE)

- Temporarily installed enclosure that completely surrounds a source of emissions such that all VOC emissions that are not directed through the control device (*i.e.*, uncaptured) are captured by the enclosure and contained for discharge through ducts that allow for the accurate measurement of the uncaptured VOC emissions.

18 - 7

7

### Criteria for Temporary Total Enclosure

1. Any NDO shall be at least four equivalent opening diameters from each VOC emitting point unless otherwise specified by the Administrator.
2. Any exhaust point from the enclosure shall be at least four equivalent duct or hood diameters from each NDO.
3. The total area of all NDO's shall not exceed 5 percent of the surface area of the enclosure's four walls, floor, and ceiling.
4. The average facial velocity (FV) of air through all NDO's shall be at least 3,600 m/hr (200 fpm). The direction of air flow through all NDO's shall be into the enclosure.
5. All access doors and windows whose areas are not included in section 5.3 and are not included in the calculation in section 5.3 shall be closed during routine operation of the process
6. shall be closed during routine operation of the process

18 - 8

8

### Temporary Total Enclosure



18 - 9

9

### Building Enclosure (BE)

- Building Enclosure (BE). An existing building that is used as a TTE.

18 - 10

10

### Alternative Capture Efficiency

- [Guidance Document 035](#)
- Must be included in SIP
- Liquid to gas mass balance without an enclosure
- Statistical analysis is required for alternatives
  - DQO or LCL

18 - 11

11

### Data Quality Objective (DQO)

- The purpose of the DQO is to allow sources to use alternative CE test procedures while ensuring reasonable precision consistent with pertinent requirements of the Clean Air Act. The DQO requires that the width of the 2-sided 95 percent confidence interval of the mean measured value be less than or equal to 10 percent of the mean measured value (see Figure 1). This ensures that 95 percent of the time, when the DQO is met, the actual CE value will be +5 percent of the mean measured value (assuming that the test protocol is unbiased).

18 - 12

12

### Lower Confidence Limit (LCL)

- The LCL approach compares the 80 percent (2-sided) LCL for the mean measured CE value to the applicable CE regulatory requirement. The LCL approach requires that either the LCL be greater than or equal to the applicable CE regulatory requirement or that the DQO is met. A

18 - 13

13

### Lower Confidence Limit (LCL)

- The purpose of the LCL approach is to provide sources, who may be performing much better than their applicable regulatory requirement, a screening option by which they can demonstrate compliance. The approach uses less precise methods and avoids additional test runs which might otherwise be needed to meet the DQO while still being assured of correctly demonstrating compliance.

18 - 14

14

### Lower Confidence Limit (LCL) (cont.)

- It is designed to reduce "false positive" or so called "Type II errors" which may erroneously indicate compliance where more variable test methods are employed. Because it encourages CE performance greater than that required in exchange for reduced compliance demonstration burden, the sources that successfully use the LCL approach could produce emission reductions beyond allowable emissions. Thus, it could provide additional benefits to the environment as well.

18 - 15

15

### Method 204 Criteria for and Verification of a PTE or TTE

- [Method 204](#)

([https://www.epa.gov/sites/production/files/2019-06/documents/method\\_204\\_0.pdf](https://www.epa.gov/sites/production/files/2019-06/documents/method_204_0.pdf))

18 - 16

16

### Quality Control - TTE

- The success of this method lies in designing the TTE to simulate the conditions that exist without the TTE (i.e., the effect of the TTE on the normal flow patterns around the affected facility or the amount of uncaptured VOC emissions should be minimal).
- The TTE must enclose the application stations, coating reservoirs, and all areas from the application station to the oven. The oven does not have to be enclosed if it is under negative pressure. The NDO's of the temporary enclosure and an exhaust fan must be properly sized and placed.

18 - 17

17

### TTE - Baseline VOC Measurement

- Monitor the VOC concentration of the captured gas steam in the duct before the capture device without the TTE. To minimize the effect of temporal variation on the captured emissions, the baseline measurement should be made over as long a time period as practical. However, the process conditions must be the same for the measurement in section 7.5 as they are for this baseline measurement. This may require short measuring times for this quality control check before and after the construction of the TTE.

18 - 18

18

### Measure VOC inside TTE

- After the TTE is constructed, monitor the VOC concentration inside the TTE. This concentration should not continue to increase and must not exceed the safe level according to Occupational Safety and Health Administration requirements for permissible exposure limits. An increase in VOC concentration indicates poor TTE design.

18 - 19

19

### TTE VOC Measurement

- Monitor the VOC concentration of the captured gas stream in the duct before the capture device with the TTE. To limit the effect of the TTE on the process, the VOC concentration with and without the TTE must be within 10 percent. If the measurements do not agree, adjust the ventilation rate from the TTE until they agree within 10 percent.

18 - 20

20

### Enclosure Criteria Determination

1. Determine the equivalent diameters of the NDO's and determine the distances from each VOC emitting point to all NDO's. Determine the equivalent diameter of each exhaust duct or hood and its distance to all NDO's. Calculate the distances in terms of equivalent diameters. The number of equivalent diameters shall be at least four.

18 - 21

21

### Enclosure Criteria Determination

2. Measure the total surface area ( $A_T$ ) of the enclosure and the total area ( $A_N$ ) of all NDO's in the enclosure. Calculate the NDO to enclosure area ratio (NEAR) as follows:

$$NEAR = \frac{A_N}{A_T}$$

- The NEAR must be  $\leq 0.05$ .

18 - 22

22

### Enclosure Criteria Determination

3. Measure the volumetric flow rate, corrected to standard conditions, of each gas stream exiting the enclosure through an exhaust duct or hood using [EPA Method 2](#).
- The FV shall be at least 3,600 m/hr (200 fpm). Alternatively, measure the pressure differential across the enclosure. A pressure drop of 0.013 mm Hg (0.007 in. H<sub>2</sub>O) corresponds to an FV of 3,600 m/hr (200 fpm).

18 - 23

23

### Volumetric Flow Rate

- Measure the volumetric flow rate, corrected to standard conditions, of each gas stream exiting the enclosure through an exhaust duct or hood using [EPA Method 2](#).

$$FV = \frac{Q_o - QI}{A_N}$$

18 - 24

24

### Volumetric Flow Rate (cont.)

- $Q_o$  = the sum of the volumetric flow from all gas streams exiting the enclosure through an exhaust duct or hood
- $Q_i$  = the sum of the volumetric flow from all gas streams into the enclosure through a forced makeup air duct; zero, if there is no forced makeup air into the enclosure

18 - 25

25

### Enclosure Criteria Determination

4. Verify that the direction of air flow through all NDO's is inward. If FV is less than 9,000 m/hr (500 fpm), the continuous inward flow of air shall be verified using streamers, smoke tubes, or tracer gases. Monitor the direction of air flow for at least 1 hour, with checks made no more than 10 minutes apart.

18 - 26

26

### Capture Efficiency

Protocol	Enclosure Verification	Liquid Input (L)	Captured emissions (G)	Fugitive Emissions (F or $F_a$ )	Capture Efficiency Formula
PTE	RM 204	N/A	N/A	N/A	Assumed 100%
TTE Gas/Gas	RM 204	N/A	RM 204B or C	RM 204D	$G/(G+F)$
TTE Liquid/Gas	RM 204	RM 204A or F	N/A	RM 204D	$(L-F)/L$
BE Gas/Gas	RM 204	N/A	RM 204B or C	RM 204E	$G/(G-F_a)$
BE Liquid/Gas	RM 204	RM 204 A or F	N/A	RM 204E	$(L-F_a)/L$

18 - 27

27

### Method 204A – Volatile Organic Compounds Content in Liquid Input Stream

- [Method 204A](#)

([https://www.epa.gov/sites/production/files/2017-08/documents/method\\_204a.pdf](https://www.epa.gov/sites/production/files/2017-08/documents/method_204a.pdf))

18 - 28

28

### Method 204B – Volatile Organic Compounds in Captured Stream

- [Method 204B](#)

([https://www.epa.gov/sites/production/files/2017-08/documents/method\\_204b.pdf](https://www.epa.gov/sites/production/files/2017-08/documents/method_204b.pdf))

18 - 29

29

### Method 204C – Volatile Organic Compounds Emissions in Capture Stream (Dilution Technique)

- [Method 204C](#)

([https://www.epa.gov/sites/production/files/2017-08/documents/method\\_204c.pdf](https://www.epa.gov/sites/production/files/2017-08/documents/method_204c.pdf))

18 - 30

30

Method 204D – Volatile Organic  
Compounds Emissions in Uncaptured  
Stream from TTE

- [Method 204D](#)

([https://www.epa.gov/sites/production/files/2017-08/documents/method\\_204d.pdf](https://www.epa.gov/sites/production/files/2017-08/documents/method_204d.pdf))

18 - 31

31

Method 204E – Volatile Organic  
Compounds Emissions in Uncaptured  
Stream from BE

- [Method 204E](#)

([https://www.epa.gov/sites/production/files/2017-08/documents/method\\_204e.pdf](https://www.epa.gov/sites/production/files/2017-08/documents/method_204e.pdf))

18 - 32

32

Method 204F – Volatile Organic  
Compounds Content in Liquid Input  
Stream (Distillation Approach)

- [Method 204F](#)

([https://www.epa.gov/sites/production/files/2017-08/documents/method\\_204f.pdf](https://www.epa.gov/sites/production/files/2017-08/documents/method_204f.pdf))

18 - 33

33

Compliance Test and Source Test  
Observation  
Stack Testing Special Topics:



19 - 1

1

Compliance Test and Source Test  
Observation

*Stack Testing Special Topics:*

- **High Moisture**
- High Pressure Stacks
- High Temperature Stacks
- Low Flow Rate

19 - 2

2

Typical Sources With High  
Moisture Content In Stack

- Lime Hydrators
- Evaporators
- Coke Oven Quench Towers
- Ammonia Nitrate Prilling Facilities
- Steam Generators
- Processes with wet scrubbers
- Other

19 - 3

3


The Problem

- High moisture in stack gas causes pitot tube to plug, thus poor  $\Delta p$  readings (i.e., velocity measurements)
- Problems with maintaining isokinetic sampling rate (i.e.,  $\Delta H = k\Delta p$ )
- Water droplets on filter increasing pressure drop and effecting isokinetics
- Dilution of impinger solutions thus effecting collection efficiency of analytes
- Condensation in pitot tube sample lines

19 - 4

4

Water Vapor and Testing



19 - 5

5

High Moisture from a Potato Chip Fryer



19 - 6

6





7



8

### The Problem: FRM 5 Isokinetic Rate Equation

$$\Delta H = \left\{ 846.72 D_n^4 \Delta H_{@} C_p^2 (1 - B_{ws})^2 \frac{M_d T_m P_s}{M_s T_s P_m} \right\} \Delta P$$

19 - 9

9

### High Moisture Error

- With low moisture (i.e., <15 %), the error is rather small
- However, with high moisture (i.e., > 15 %), the error becomes small
- Typically, for every 1 % error in moisture determination reflects a 1 % error in isokinetics

19 - 10

10

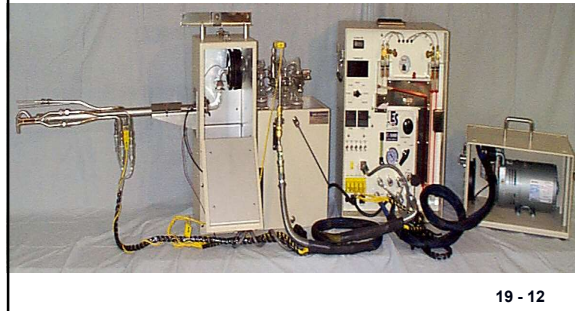
### Sampling Problems With High Moisture Stacks

- Erroneous readings due to low flow rate through orifice due to large volume of moisture drop-out in impingers
- Inaccurate control of sampling rate due to small volume of gas passing through control valves
- Non-isokinetic sampling due to fluctuations in moisture content of stack gas

19 - 11

11

### What Approaches Can Be Taken To Sample Under High Moisture Situations?



19 - 12

12



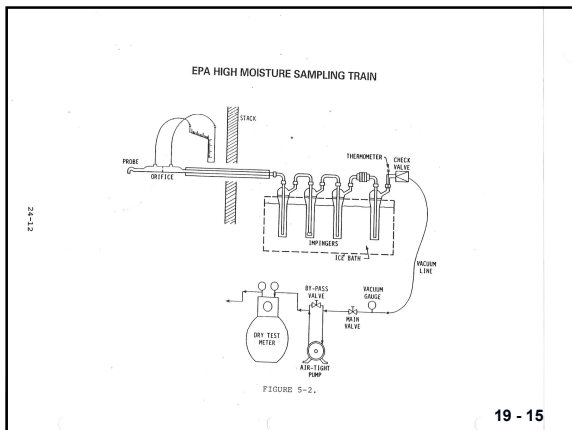
13

### General Solution #1 (Placement of Orifice Meter In Stack)

- Place orifice meter before impingers instead at end of sampling system
  - Total sample volume passes through orifice meter
  - Moisture content measurement unnecessary
  - Isokinetics not affected by moisture

19 - 14

14



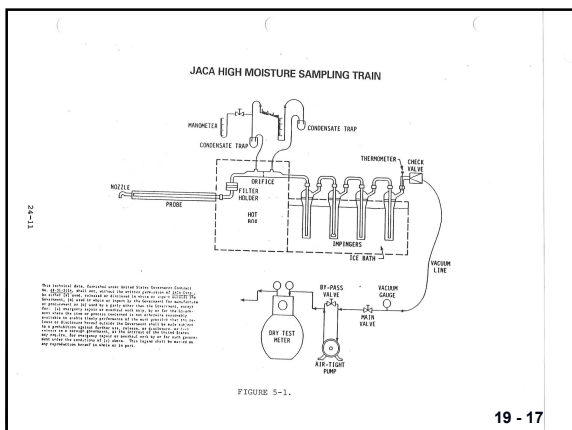
15

### General Solution #2 (Placement of Orifice Meter In Heated Filter Box)

- ◆ Orifice meter is located in heated sample box behind filter
  - Prevention of condensation at orifice
  - Protected from particulate fouling

19 - 16

16



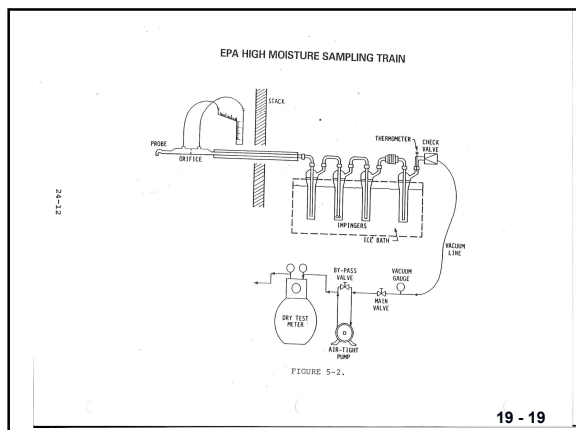
17

### General Solution #3 (In-situ Orifice with Changeable Orifice Plates)

- Orifice meter is located in the stack with changeable orifice plates (i.e., In-situ)
- Filter located before silica gel impinger
- Probe heated to prevent condensation
- Developed for use at ammonium nitrate facilities

19 - 18

18



19

### General Solution #4 (Consultant's Approach)

- ◆ Orifice meter is located in the heated filter compartment of FRM 5 sampling train
- ◆ Filter located before silica gel impinger
- ◆ Probe heated to prevent condensation and pitot tube lines cleaned by pressurized air
- ◆ Developed for use at ammonium nitrate facilities

19 - 20

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### General Solution #5

- Use FRM 5 Sampling Train Except:
  - Install cyclone and drop-out impinger in sample train to catch larger volume of water
  - Use larger 1<sup>st</sup> impinger and change periodically during test (Must leak check during each change!)
  - Install drop-out traps in pitot tube lines or blow-back lines periodically during sampling

19 - 21

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### All of The Solutions Involve Removing $B_{ws}$ From The Isokinetic Rate Equation

$$H = \left\{ 846.72 D_n^4 \Delta H @ C_p^2 \frac{M_d T_m P_s}{M_s T_s P_m} \right\} \Delta P$$

19 - 22

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### Problems Common To All Three Approaches

- Entrained water droplets
- Condensation in manometer and pitot tube lines
- Improper condensation in impingers

19 - 23

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### General Solutions

- Use of larger knock-out impinger after heated filter compartment
- Use of condenser to aid in knocking out moisture coupled with larger impinger in sampling train
- Changing impingers frequently during testing (must leak check each time)

19 - 24

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### Compliance Test and Source Test Observation

#### *Stack Testing Special Topics:*

- High Moisture
- **High Pressure Stacks**
- High Temperature Stacks
- Low Flow Rate

19 - 25

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### Stack Testing At High Pressure Sources

26

### Three Problem Areas With Stack Testing At High Pressure Stacks (> 5 “)

- Port Leakage
- Pressure Measurement Difficulties
- Sample Losses

19 - 27

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### Port Leakage

- Locations with **NEGATIVE STATIC PRESSURE**
    - Ambient air ( $O_2 = 20.9\%$ ) will be sucked into the duct
  - Locations with **POSITIVE STATIC PRESSURE**
    - Flue gas will be blown out of port into the immediate test area
- ( As the magnitude of the static pressure increases, the effects become significant.)

19 - 28

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### Minimizing Port Leakage

- Install gate valves or globe valves on ports for use during sample train insertion and removal
- Use port adapters with compression fittings around probe to seal off port during sampling

19 - 29

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### Pressure Measurement Difficulties

- During probe insertion/removal:
  - Pitot tube lines can be blown off the manometer from the force of the static pressure
  - Gauge oil in manometer can be pushed or pulled into the fluid reservoirs from the force of the static pressure
  - In extreme cases, the fluid can be pulled into pitot lines

19 - 31

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### Overcoming Pressure Measurement Difficulties

- Use compression fittings to attach pitot lines to manometer
- Install a series of shut-off valves to the pressure lines
- Measure static pressure with a magnahelic gauge

19 - 32

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### Sample Losses Can Occur

- During probe insertion/removal:
  - Filter can become unseated from the filter holder and sucked forward, along with any sample collected on the filter
  - Impinger contents can become sucked forward through the impinger train

19 - 33

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### Sample Losses Can Occur

- During sampling:
  - Probe (and all attached components of the sample train) can be inadvertently displaced by positive or negative pressure
  - Impinger train can burst from extreme positive pressure

19 - 34

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### Preventing Sample Losses

- Locations with **NEGATIVE STATIC PRESSURE**:
  - Engage the pump and allow a small amount of gas to flow through the sample train while putting the sample train into the port
- Locations with **POSITIVE STATIC PRESSURE**:
  - Engage the pump and allow a small amount of gas to flow through the sample train while taking the sample train out of the port

19 - 35

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### Preventing Sample Losses

- Use port adapters with compression fittings around probe to support sample train and keep it fixed in place
- Reduce positive pressure on impinger train
  - Insert a valve at the inlet of the impinger train to reduce gas flow
  - Use a coiled condenser at the inlet of the impingers train to rapidly cool the gas stream

19 - 36

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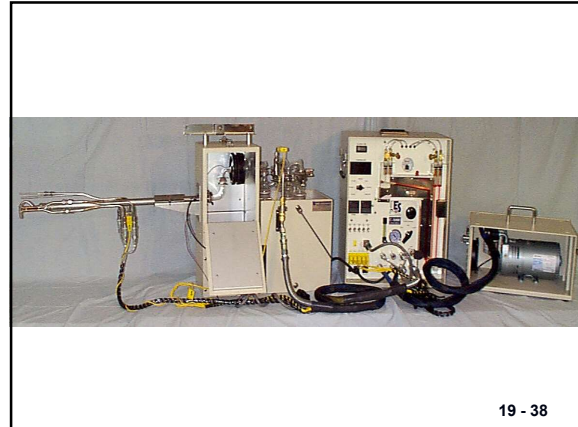
### Compliance Test and Source Test Observation

#### *Stack Testing Special Topics:*

- High Moisture
- High Pressure Stacks
- **High Temperature Stacks**
- Low Flow Rate

19 - 37

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19 - 38

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### Typical Sources With High Temperature In Stack

- Gas Turbines
- Municipal Incinerators
- Glass Furnaces
- Flares
- Kilns
- Metals Production Facilities (Primary & Secondary) Any Others?

19 - 39

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19 - 41

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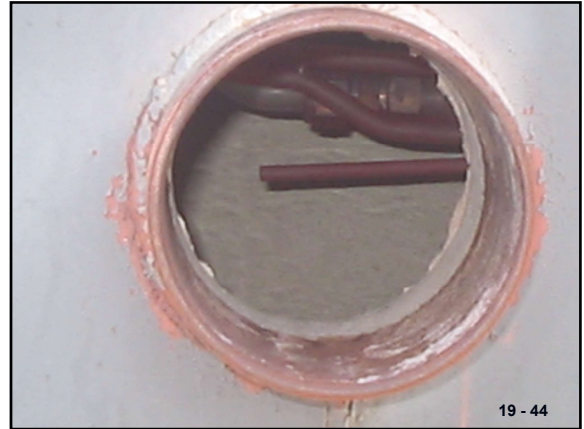


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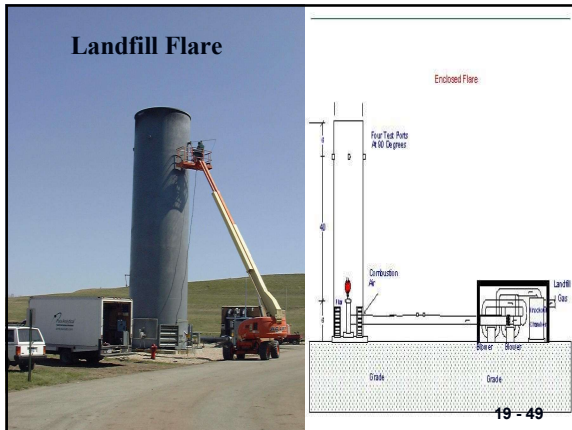
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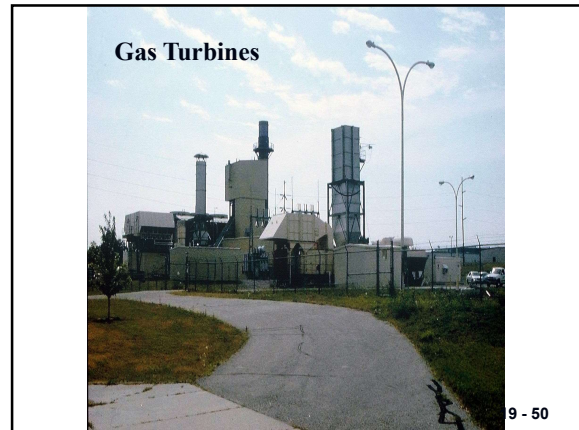
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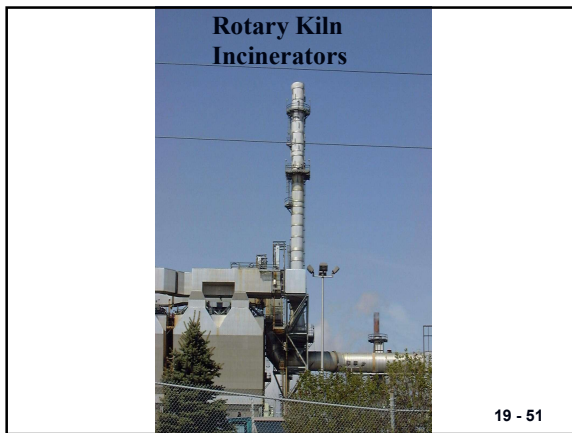
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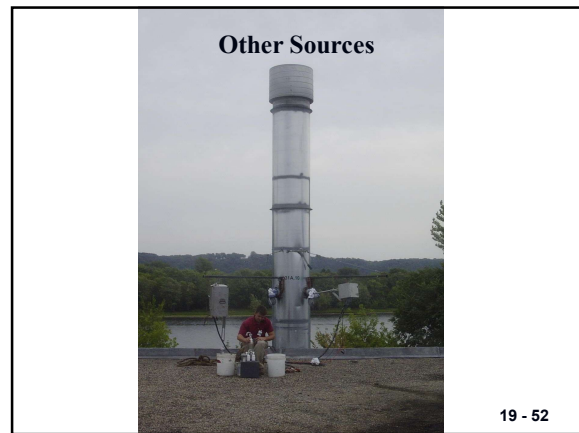
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52

**The Problem**

- High stack temperatures causes problems with obtaining proper leak check of sampling system and safety problems
- Problems with achieving airtight seal between nozzle and probe liner
- Breakage of glass probe liner due to different coefficients of thermal expansion between probe liner and stainless steel jacket

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**Stack Temperatures**

- Traditional FRM 5 good to about 700 °F
- Municipal incinerators and gas turbines usually emit effluents well in excess of 750 °F, and up to 2000 °F

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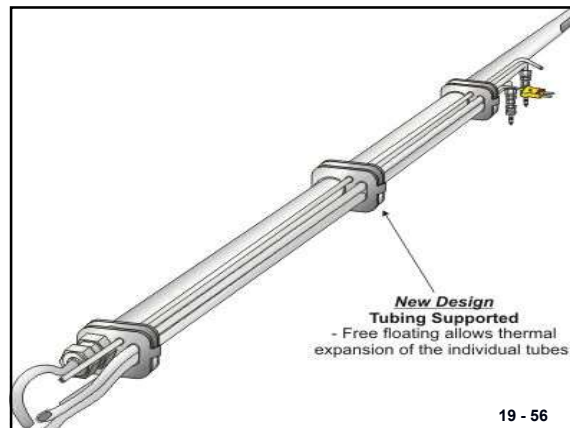


### Maximum Temperature of Various Materials

- Teflon: < 350 °F
- Glass: < 900 °F
- Stainless Steel: < 1210 °F
- Quartz: < 1650 °F
- Inconel: < 1800 °F

19 - 55

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19 - 56

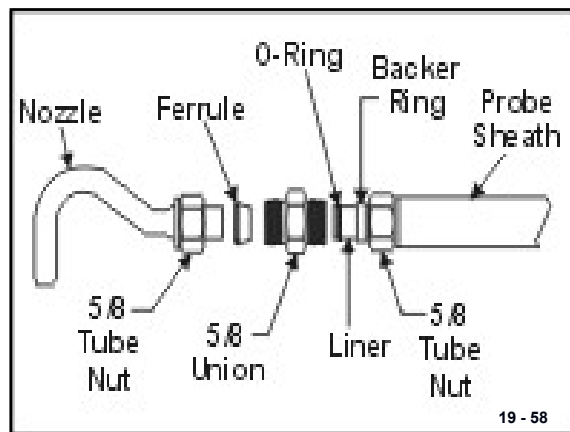
56

### Sampling Problems

- Teflon ferrules and Viton-O rings must not be used at temperatures exceeding their softening point (i.e., seal between nozzle and probe liner etc.)
- The organic material in the glue on the tape used to wrap the heating wire on the probe can burn off and bias the test
- The probe should be free of tape since there is no reason to heat the probe.

19 - 57

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19 - 58

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### Sampling Problems

- Metal probes, at high temperatures, become catalyst (reactive surfaces) for substances in the stack gas (i.e., oxidation of metals, SO<sub>2</sub> to SO<sub>3</sub>, etc.)
- High effluent gas temperature could cause softening of the nozzle, probe and pitot tube
- Difficulty of maintaining filter box temperature at 248 °F

19 - 59

59

### Solution #1 (Construction of High Temperature Probes)

- Devise a cooling system allowing use of standard construction materials (i.e., Glass, Teflon, Stainless Steel)
  - Ambient Air
  - Water
  - Steam (Very dangerous)

19 - 60

60

### Solution #2 (Construction of High Temperature Probes)

- Construct probes of materials which can withstand high temperatures
  - Inconel
  - Special Alloys
  - Quartz

19 - 61

61

### Use of Probe Cooling Techniques ( Advantages)

- Durability of probe
- Unrestricted probe length
- Cooling of gases ensures that filter temperature can be maintained within limits
- Sensing lines (i.e., pitot tube) can be included within cooling jackets

19 - 62

62

### Use of Probe Cooling Techniques ( Disadvantages)

- Requires structural support equipment at sampling site
- Vapor pockets may form which may rupture jacket
- Condensation in probe may give problems with maintaining isokinetic sampling rate
- Cooling nozzle/pitot tube gives variable effects on stack gas flow

19 - 63

63

### Use of Quartz Probe ( Advantages)

- Stack gas effluents will not react probe material during sampling
- Absence of bulky cooling system
- No condensation in probe
- No heat expansion and distortion of probe and nozzle
- Gases not cooled below 248 °F

19 - 64

64

### Use of Quartz Probe ( Disadvantages)

- Very brittle/may crack during adding probe nozzle
- Traditionally, fixed nozzle sizes
- Probe lengths greater than 5 ft are impractical
- If using quartz probe without probe liner, then can't attach pitot tube and thermocouple wires

19 - 65

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### Miscellaneous Sampling Problems

- ◆ Sagging of probe and pitot tubes in gas effluent
- ◆ Heat radiation from process affects temperature measurements (may have to shield stack gas components)
- ◆ General safety consideration for handling hot probe and working close to stack liner

19 - 66

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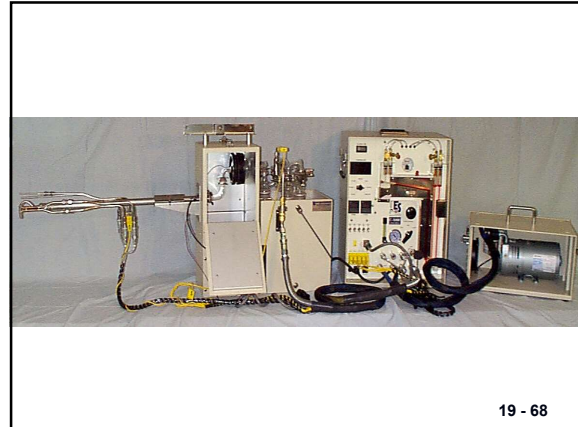
### Compliance Test and Source Test Observation

#### *Stack Testing Special Topics:*

- High Moisture
- High Pressure Stacks
- High Temperature Stacks
- **Low Flow Rate**

19 - 67

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19 - 68

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### Velocity Measurement

- Used in determination of nozzle size
- Used in obtaining K-factor for setting isokinetic rate conditions during testing
- Used in determining pollutant mass rate

19 - 69

69

### Federal Reference Method 2 Average Velocity Over Cross-Section

$$\bar{v}_s = K_p C_p (\sqrt{\Delta p})_{avg} \sqrt{\frac{T_{s(avg)}}{M_s P_s}}$$

19 - 70

70

### Average Stack Gas Dry Volumetric Flow Rate

$$Q_{std} = 3600 (1 - B_{ws(avg)}) v_{s(avg)} A \frac{T_{std}}{T_{s(avg)}} \frac{P_s}{P_{std}}$$

19 - 71

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### The Problem

- Pressure differential devices insensitive below 17 ft/second
- Unreliable pitot tube accuracy below 7 ft/second

19 - 72

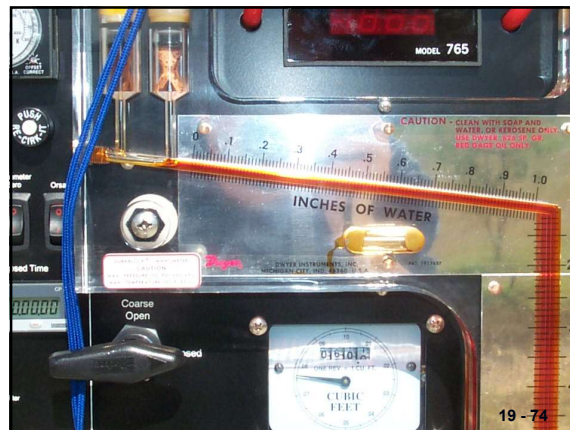
72

### The Problem

- FRM 5 typical incline manometer has incline range of 0-1 “ H<sub>2</sub>O with 0.01 “ divisions, and vertical range of 1-10 “ H<sub>2</sub>O with 0.10 “ divisions
- FRM 5 designed to monitor flows around 1.84 “ H<sub>2</sub>O, not in the 0-0.5 “ H<sub>2</sub>O range

19 - 73

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19 - 74

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### Federal Reference Method 2 Guidelines

- A differential pressure gauge other greater sensitivity shall be used:
  - The arithmetic average of all  $\Delta p$  readings at the traverse points < 0.05 “ H<sub>2</sub>O
  - For traverse of 12 or more points, more than 10 % of the individual  $\Delta p$  readings < 0.05 “ H<sub>2</sub>O
  - For traverse of < 12 points, more than one  $\Delta p$  reading < 0.05 “ H<sub>2</sub>O

19 - 75

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### Federal Reference Method 2 Guidelines

- As an alternative to criteria (1) through (3) above, the following equation may be used to determine the necessity of using a more sensitive differential pressure gauge. If T is greater than 1.05, the velocity head data are unacceptable and a more sensitive differential pressure gauge must be used.

19 - 76

76

### Determination of Sensitivity of Pressure Gauge

$$T = \frac{\sum_{i=1}^n \sqrt{\Delta p_i + K}}{\sum_{i=1}^n \sqrt{\Delta p_i}}$$

19 - 77

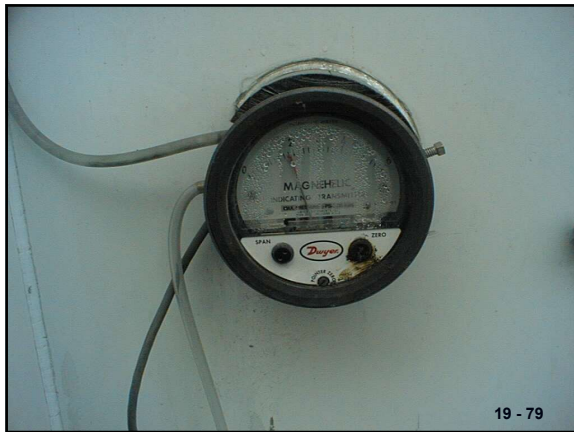
77

### Using Magnehelic Gauges Etc.

- If differential pressure gauges other than inclined manometers are used (e.g., magnehelic gauges), their calibration must be checked after each test series.
- To check the calibration of a differential pressure gauge, compare  $\Delta p$  readings of the gauge with those of a gauge-oil manometer at a minimum of three points, approximately representing the range of  $\Delta p$  values in the stack.

19 - 78

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### Alternative Approaches for Low Velocity Measurements

- The use of techniques other than Type-S pitot tubes
- Modification of the source to effect a sufficiently high velocity for using the Type-S pitot tube
- Measure velocity at a different location and use data to calculate velocity at sampling site
- Compute flow and velocity using process parameters

19 - 80

80

### Techniques For Measurement of Low Flows

- Standard pitot tube with portable inclined manometer (0-0.25 " H<sub>2</sub>O with 0.005 " H<sub>2</sub>O scale divisions) or digital manometer
- Standard pitot tube with dual scale portable inclined manometer with 0-1.0 " H<sub>2</sub>O with 0.01 " H<sub>2</sub>O scale divisions and 0-10 " H<sub>2</sub>O with 0.10 " H<sub>2</sub>O scale divisions

19 - 81

81

### Techniques For Measurement of Low Flows

- Rotating vane anemometer with digital readout (0-100 ft/sec with 1 ft/sec accuracy)
- Thermal anemometer with digital readout (0-100 ft/sec with 1 ft/sec accuracy)

19 - 82

82

### Other Low Flow Techniques

- Venturi Meters
- Orifice Meters
- Mass Flow Meters

19 - 83

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### Compliance Test and Source Test Observation

#### *Stack Testing Special Topics:*

- High Moisture
- High Pressure Stacks
- High Temperature Stacks
- Low Flow Rate

19 - 84

84

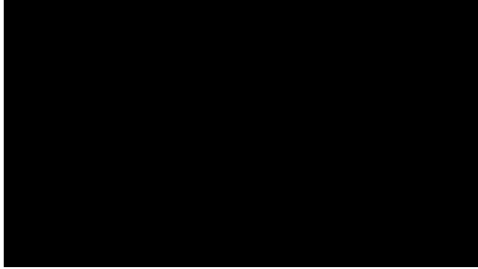
Compliance Test and Source  
Test Observation

Reciprocating Internal  
Combustion Engines (RICE)  
Sampling and Overview of  
CEMS for Engines and Gas  
Turbine Testing

20A - 1

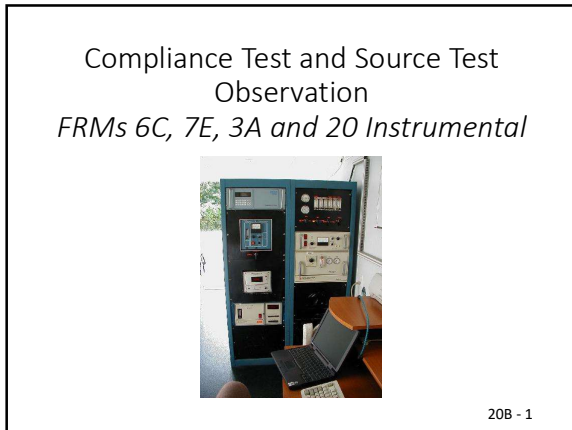
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Stationary Engines



20A - 2

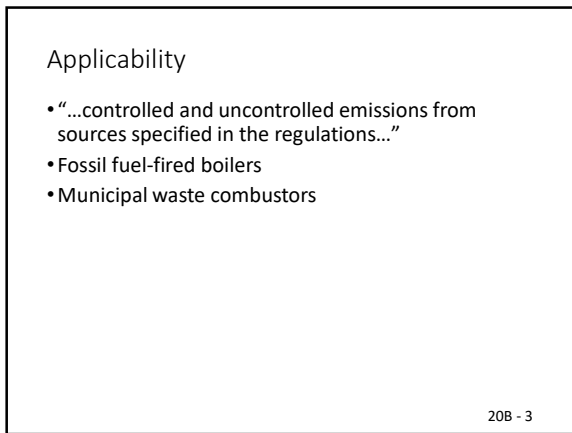
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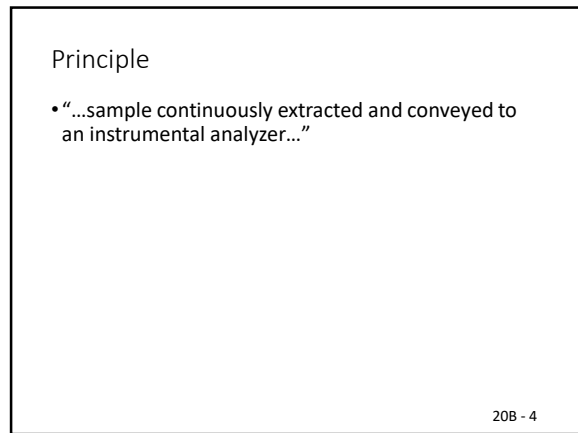
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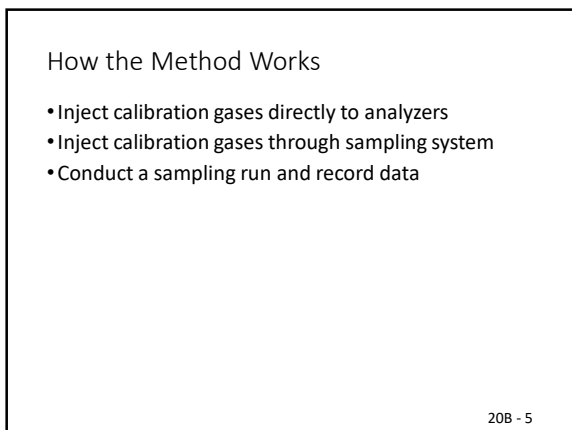
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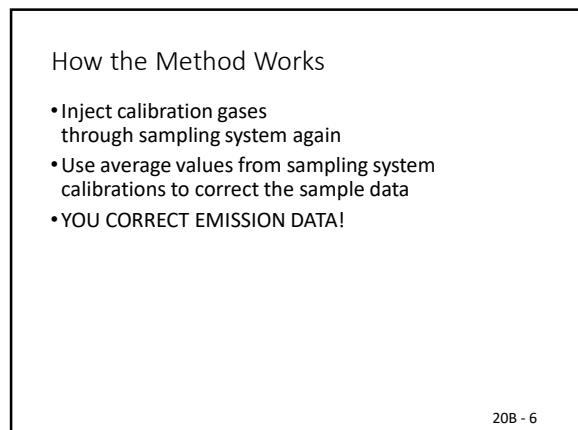
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5



6

Eight Major Points

1. Calibration Error (Both Analyzer):  
Zero, mid, high ( 2%)
2. Zero/Calibration Drift (Both Analyzer):  
Proceeding/Following Each Run:  
< 3% of span or Reject
3. Sampling System Bias Check/Recovery Check  
(Both Analyzers): Zero, Mid/High Range at Probe  
and Analyzer (5% of span)

20B - 7

7

Eight Major Points (cont.)

4. Interference Check (SO<sub>2</sub> Analyzer): Use Modified  
Method 6 (3 Runs 1 L/min) vs. Analyzer at Vent  
(7%)
5. Converter Check (NO<sub>x</sub> Analyzer): Introduce CO @  
500 ppm, SO<sub>2</sub>@200 ppm, CO<sub>2</sub>@10% and  
O<sub>2</sub>@20.9%; < 2% of span response, pass

20B - 8

8

Eight Major Points (cont.)

6. Calibration Error (Both Analyzer): Zero, mid, high ( 2%)
7. Zero/Calibration Drift (Both Analyzer):  
Proceeding/Following Each Run): < 3% of span or  
Reject
8. Sampling System Bias Check/Recovery Check(Both  
Analyzers): Zero, Mid/High Range at Probe and  
Analyzer (5% of span)

20B - 9

9

Interesting Points

- Perform Calibration Curve: High (80-100% span),  
Mid (40-60% span), Zero (<0.25% span)
- Calibration Gas Certification: Protocol 1 or Method  
6 (3 Runs/1 L/min), 5%

20B - 10

10

Interesting Points

- Span of instrument: Emission standard at 30% of  
span
- Calibration gases can be SO<sub>2</sub>/N<sub>2</sub>, SO<sub>2</sub>/Air, SO<sub>2</sub>/CO<sub>2</sub>, or  
SO<sub>2</sub>/CO<sub>2</sub>/O<sub>2</sub>
- Emission data corrected with determined bias  
number
- No EPA Method 6 audit vial required due to  
"Interference Check"

20B - 11

11

Interesting Points

- Sampling system bias test done before and after  
test, then average, and apply value to emission data  
to correct
- Zero/Calibration Drift (Both Analyzer):  
Proceeding/Following Each Run): < 3% of span; May  
not reject if pass bias check!

20B - 12

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20B - 13

13



20B - 14

14

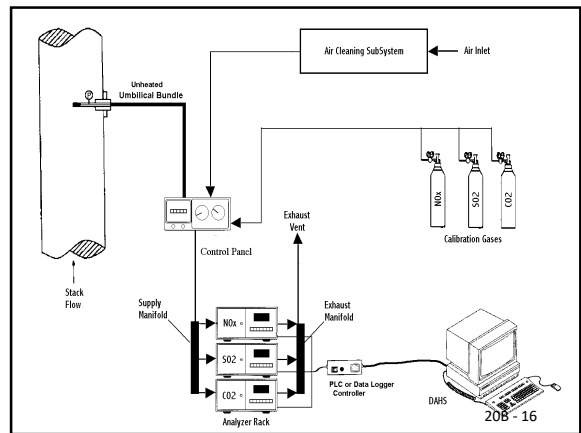
Method 6C  
Typical Analytical Methods

- Ultraviolet Absorption (UV)
- Nondispersive Infrared (NDIR)
- Fluorescence
- FTIR

• Analyzer must meet the performance requirements of this method.

20B - 15

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20B - 16

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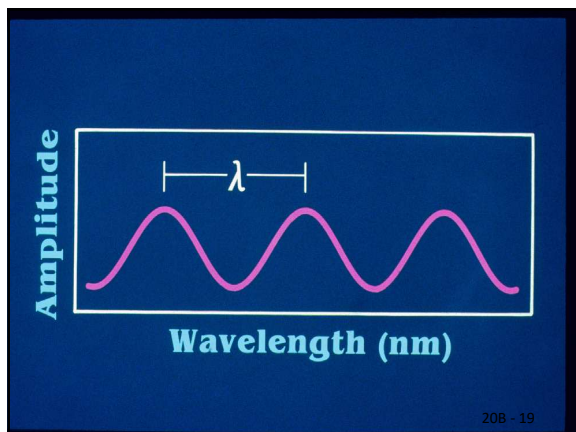
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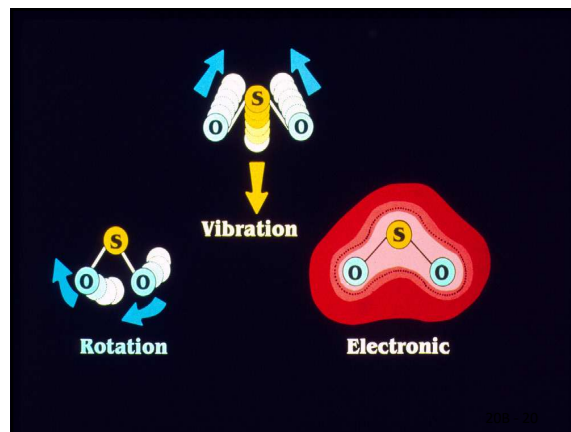


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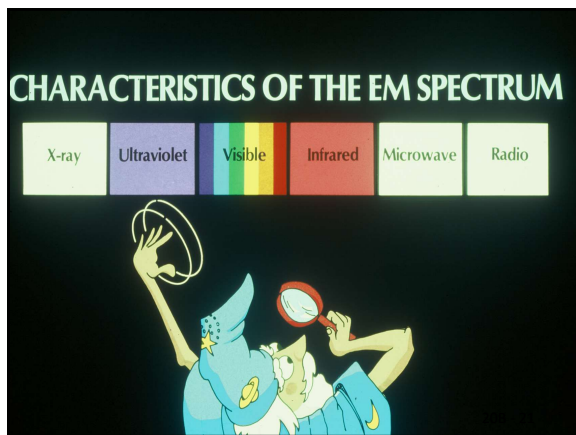
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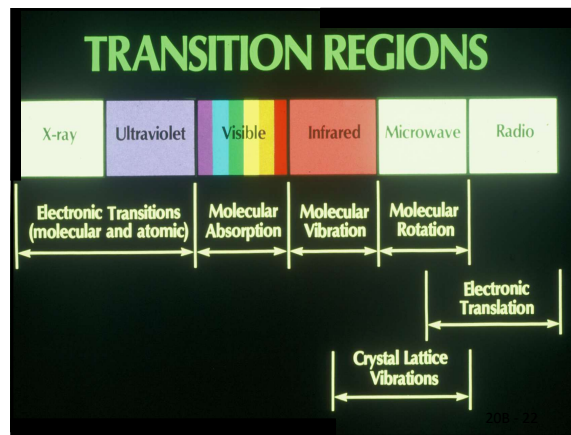
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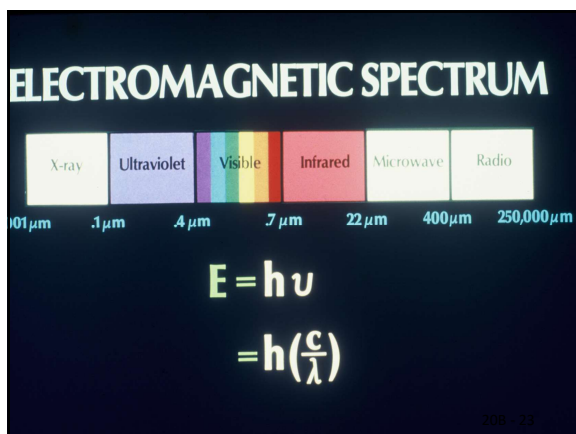
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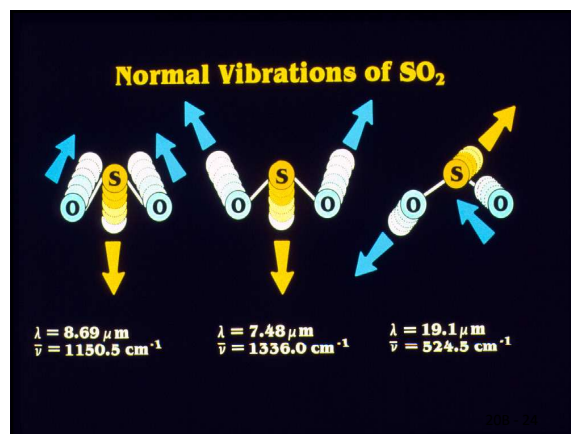
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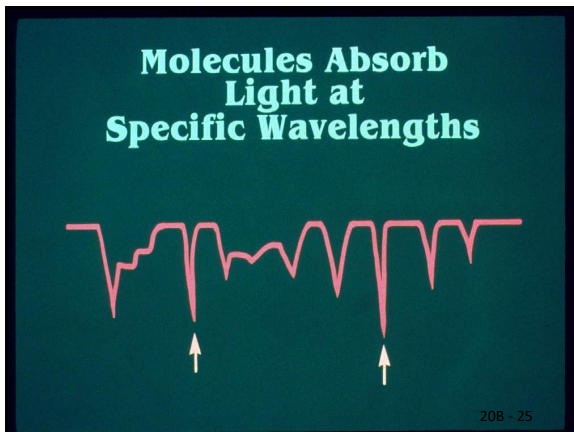
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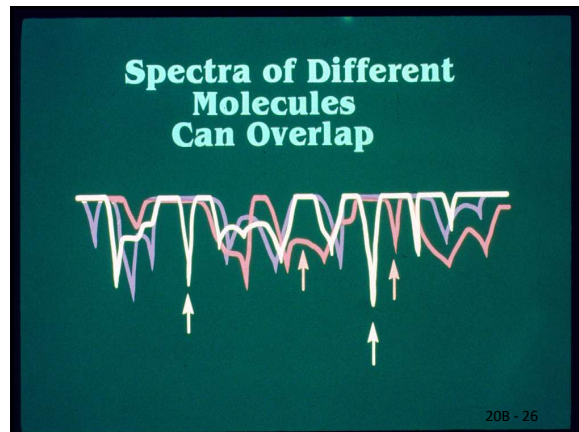
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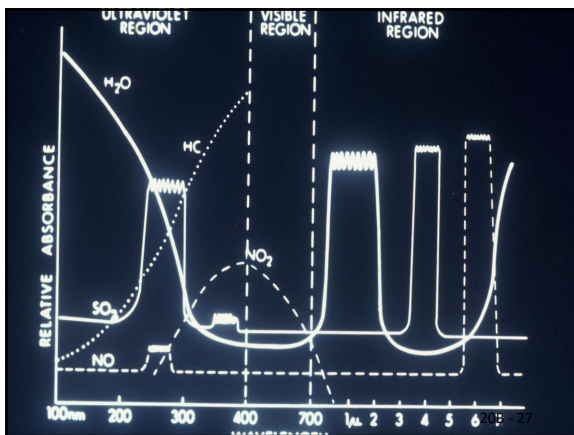
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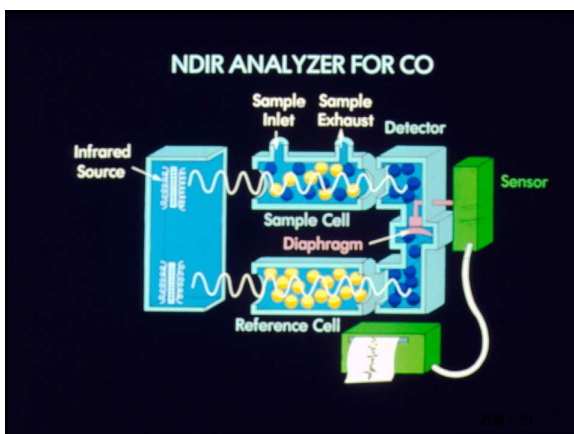
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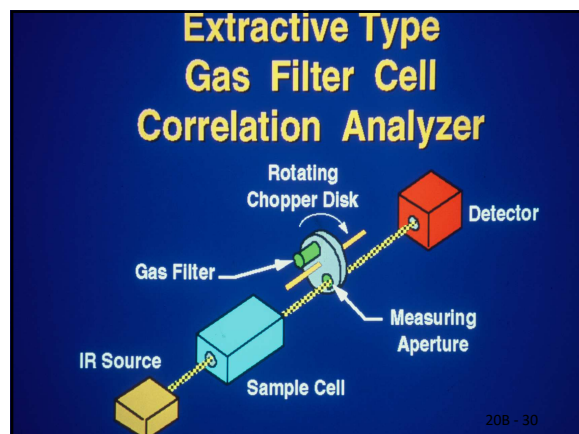
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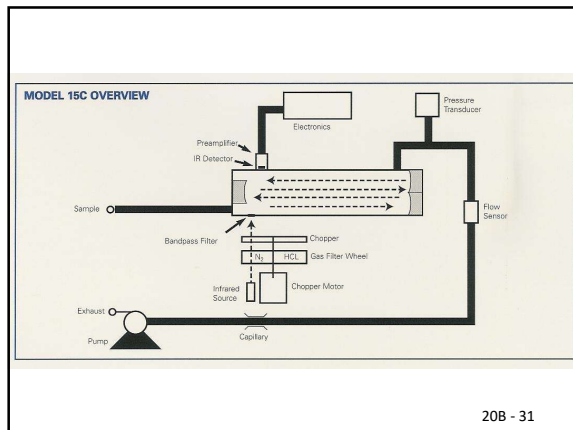
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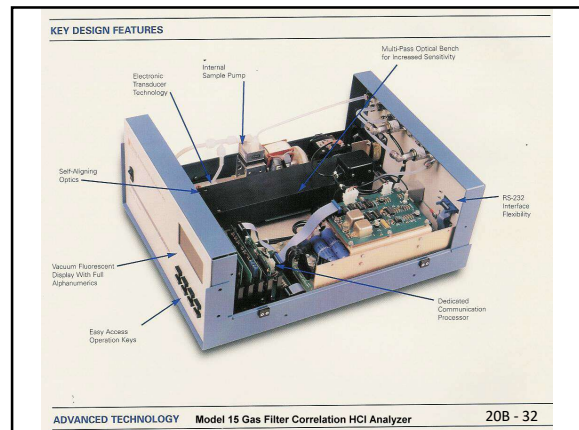
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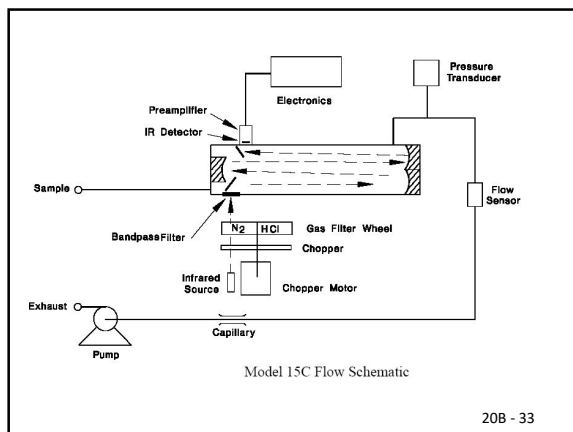
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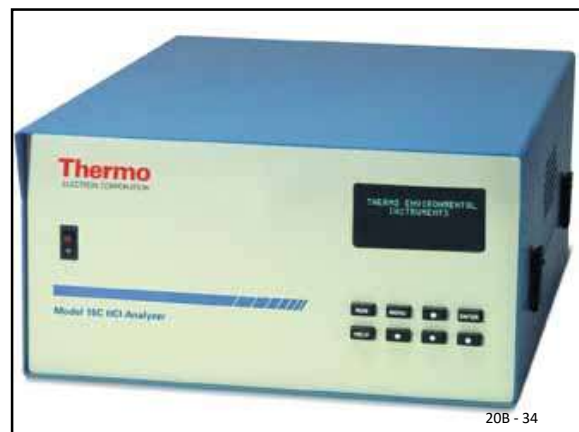
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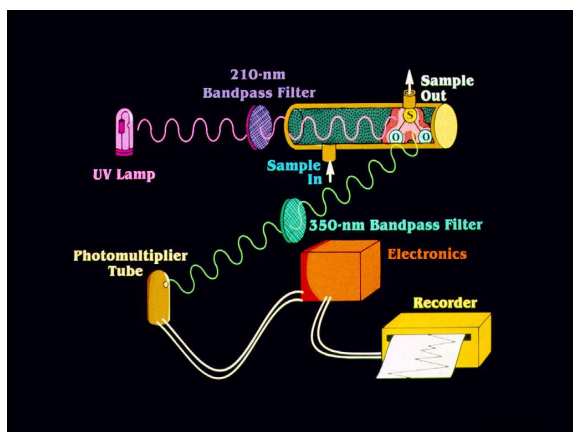
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**MODEL 43C- SO<sub>2</sub> ANALYZER**

- Microprocessor control
- SO<sub>2</sub> Specific
- Reflective U.V. filtering
- Hermetically sealed U.V. lamp
- No consumables

Thermo Environmental Resources Inc.  
Model 43C Analyzer

36

### MODEL 43C-SO<sub>2</sub> Analyzer

$$SO_2 + hu_1 \xrightarrow{I_a} SO_2^*$$

$$SO_2^* \xrightarrow{K_f} SO_2 + hu_2$$

$$I_a = I_0[1 - e^{-ax(SO_2)}]$$

$$I_f = I_0ax(SO_2) \text{ or } K(SO_2)$$

37

### Thermo Model 43C SO<sub>2</sub> Analyzer

**Pulsed Fluorescence SO<sub>2</sub> Analyzer**

**Advanced Technology**

The Model 43C integrates the proven pulsed fluorescence design of Thermo Environmental Instruments Inc. Model 43 series with an enhanced electronics package and user interface. The outcome is a sensitive, ultra stable SO<sub>2</sub> analyzer offering network operators and research scientists unlimited troubleshooting diagnostics and data communications capability.

Thermo Environmental Instruments design engineers have introduced a user interface which literally guides one through operation of the Model 43C. This is accomplished via a 4 line by 20 character Vacuum Fluorescent Display and simple layout of easy-to-use function keys. The end result is a combination of self-explanatory display messages and intuitive function entries.

User software facilities include field programmable measurement ranges and SO<sub>2</sub> concentration value storage by date and time.

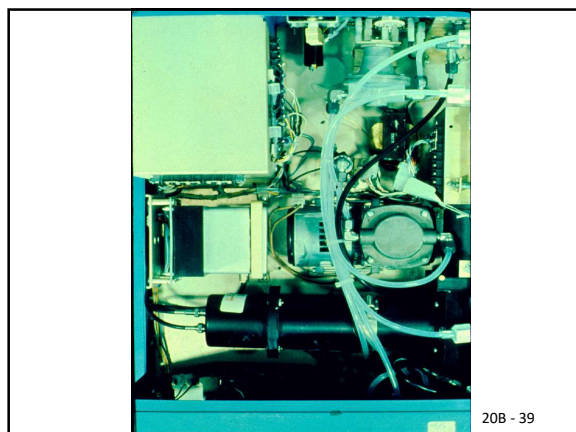
MODEL 43C SPECIFICATIONS	
Range	0-50, 100, 200, 500, 1000 ppb and 0-1, 2, 5, 10, 20, 50, 100 ppm
Zero Noise	1.0 ppb RMS (10 second averaging time)
	25 ppb RMS (60 second averaging time)
	25 ppb RMS (300 second averaging time)
Lower Detectable Limit	21.0 ppb RMS (10 second averaging time)
	1.0 ppb RMS (60 second averaging time)
	0.5 ppb RMS (300 second averaging time)

15

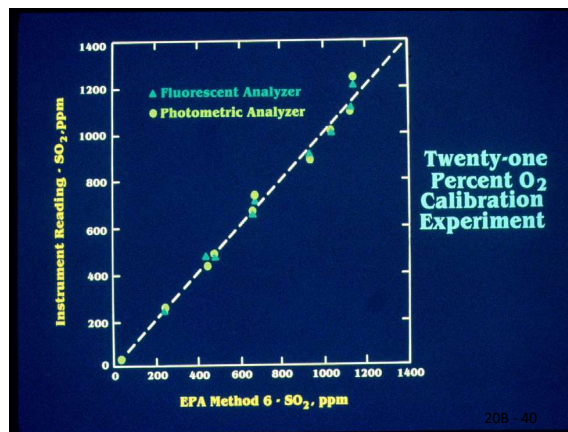
Analyze • Detect • Measure • Control™

**Thermo**  
ELECTRON OPTICS

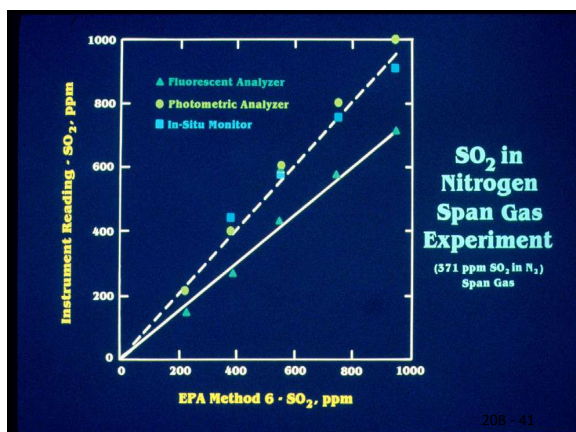
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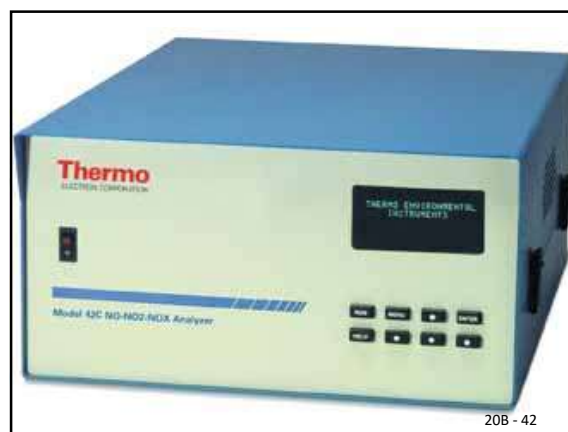
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41



42

### HOW IS NO MEASURED?

Chemiluminescence Technique

$$\text{NO} + \text{O}_3 \longrightarrow \text{NO}_2^* + \text{O}_2$$

$$\text{NO}_2^* \longrightarrow \text{NO}_2 + h\nu$$

Intensity of emitted light is proportional to NO concentration

20B - 43

43

### Chemiluminescent

Reduction of NO<sub>2</sub> to NO

$$3 \text{NO}_2 + \text{Mo} \longrightarrow 3 \text{NO} + \text{MoO}_3$$

A molybdenum catalyst, heated to ~325°C, is used to Convert NO<sub>2</sub> to NO

20B - 44

44

### Measurement Principle

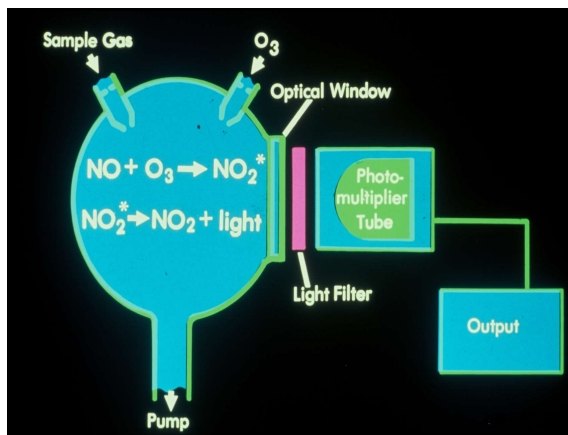
CHEMILUMINESCENCE

$$\text{NO} + \text{O}_3 \longrightarrow \text{NO}_2^* + \text{O}_2$$

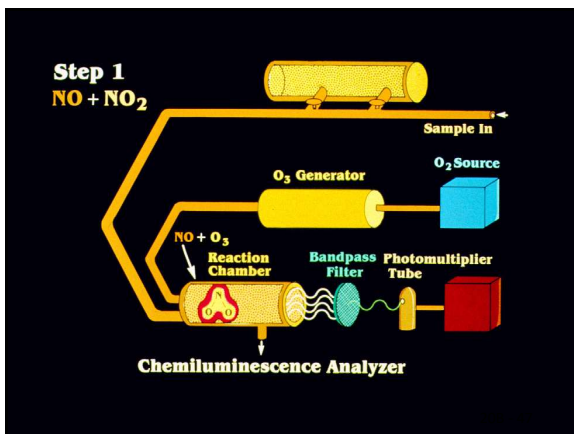
$$\text{NO}_2^* \longrightarrow \text{NO}_2 + h\nu$$

20B - 45

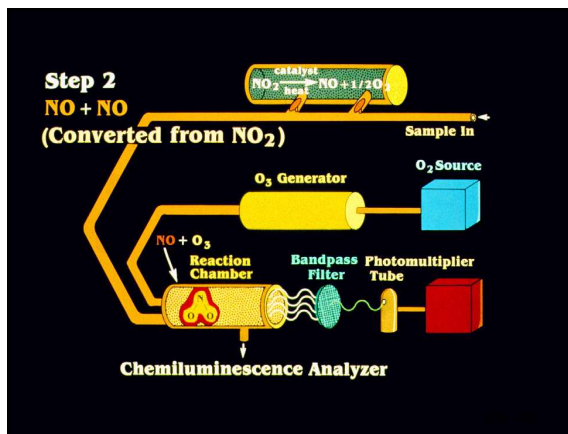
45



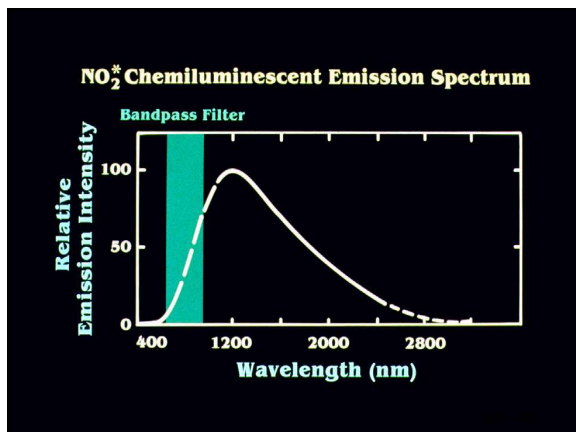
46



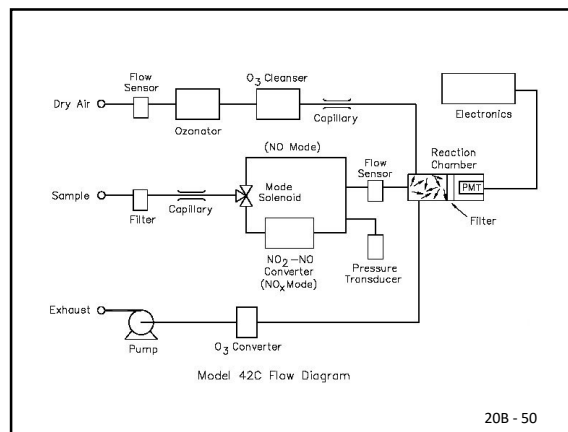
47



48



49



50



51



52

**Analytical Range**

- "...To the extent practicable, the measured emissions should be between 20 to 100 percent of the selected calibration span. ..."
- "No valid run average concentration may exceed the calibration span."

53

**Performance Specifications**

- **Analyzer Calibration Error**, for non-dilution systems, means the difference between the manufacturer certified concentration of a calibration gas and the measured concentration of the same gas when it is introduced into the analyzer in direct calibration mode.
- **Analyzer calibration error**
  - Less than ± 2% of span for zero, mid, and high-range gases

54

Performance Specifications

- *System Bias* means the difference between a calibration gas measured in direct calibration mode and in system calibration mode. System bias is determined before and after each run at the low- and mid- or high-concentration levels. For dilution-type systems, pre- and post-run system calibration error is measured rather than system bias.

20B - 55

55

Performance Specifications

- *System Calibration Error* applies to dilution-type systems and means the difference between the measured concentration of low-, mid-, or high-level calibration gas and the certified concentration for each gas when introduced in system calibration mode. For dilution-type systems, a 3-point system calibration error test is conducted in lieu of the analyzer calibration error test, and 2-point system calibration error tests are conducted in lieu of system bias tests.

20B - 56

56

Performance Specifications

- **Sampling system bias**
  - Less than  $\pm 5\%$  of span for zero and mid or high-range gases
- *Drift* means the difference between the pre- and post-run system bias (or system calibration error) checks at a specific calibration gas concentration level (*i.e.* low-, mid- or high-).
- **Zero drift and calibration drift**
  - Less than  $\pm 3\%$  of span over the period of the run

20B - 57

57

Calibration Gases

- High-range = Equal to the calibration span
- Mid-range = 40-60% of span
- Zero gas =  $< 0.25\%$  of span

20B - 58

58

Calibration Gases

- Protocol 1
- Traceability protocol (G1, G2)
- Valid certificate required Uncertainty  $\leq 2.0\%$  of tag value

20B - 59

59

Measurement System Performance Test Procedures

- Measurement system preparation
  - Acquire equipment/calibration gases
  - Set-up the components
  - Warm up the analyzers
  - Adjust flow rates

20B - 60

60



Recommended Sampling System Design  
Criteria

- Remove particulate
- Remove moisture or otherwise lower the dew point of the sample
- Minimize sample loss through leaks, absorption, and reaction

20B - 61

61

Recommended Sampling System Design  
Criteria

- Allow for introduction of calibration gas through as many components as possible

20B - 62

62

Recommended  
Particulate Removal

- In-stack filter at probe tip or probe outlet
- Filter after moisture removal system to catch condensable particulate
- Final filter at analyzer inlet

20B - 63

63

Sample Handling

- Maintain the sample above the dew point temperature except in the condensers
- Use only non-reactive wetted surfaces (i.e., glass, Teflon, and stainless steel)

20B - 64

64

Moisture Removal  
Condensers

- Use ice bath, refrigerated, or thermoelectrically cooled impingers or coils
- Design condenser to minimize contact area between sample and condensate

20B - 65

65

Moisture Removal  
Condensers

- Continuously remove condensate from traps to further reduce contact with sample and limit absorption of SO<sub>2</sub> and NO<sub>2</sub>

20B - 66

66

Other Methods of Lowering Sample Dew Point

- Semi-permeable membrane dryers (Perma-Pure®)
- Dilution probes

20B - 67

67

Injecting Calibration Gases Into the Sampling system

- One of the most common problem areas
- Calibration gases should be introduced under flow conditions that are as close as possible to the sampling conditions
- Testers hate to waste calibration gas

20B - 68

68

Three Suggested Ways to Introduce Calibration Gases

- Straight Tee
- Closed Loop
- Closed Loop with Vent

20B - 69

69

Calibration Gas Introduction - Straight Tee

- No 3-way valve required
- Will not pressurize sampling system if probe filter is clean
- Uses analyzer zero readings to establish adequate calibration gas flow

20B - 70

70

Calibration Gas Introduction - Closed Loop

- Uses 3-way valve to isolate sampling system from probe
- Sample flow meter is used to match calibration gas and sample gas flows
- Pressurizing the sampling system can disguise leaks

20B - 71

71

Calibration Gas Introduction - Closed Loop with Vent

- Uses 3-way valve to isolate sampling system from probe
- Vent with rotameter ensures that calibration gas is introduced under vacuum

20B - 72

72

### Leak Check

- Not required by the method due to bias test procedure
- Should be conducted from probe tip to analyzers before and after each test

20B - 73

73

### Analyzer Calibration Error

- Less than  $\pm 2\%$  of span for zero, mid and high-range gases
- Demonstrates accuracy and linearity

20B - 74

74

### Sampling System Bias Check

- Less than  $\pm 5\%$  of span for zero and mid or high-range gases
- Check integrity of system; cannot adjust monitor calibration after calibration error (CE) test

20B - 75

75

### Emission Testing

- Unless otherwise specified in an applicable regulation or by the Administrator, when this method is used to determine compliance with an emission standard, conduct a stratification test as described in method 7E, section 8.1.2 to determine the sampling traverse points to be used. For performance testing of continuous emission monitoring systems, follow the sampling site selection and traverse point layout procedures described in the appropriate performance specification or applicable regulation (e.g., Performance Specification 2 in appendix B to this part).

20B - 76

76

### Emission Testing

- Perform a stratification test at each test site to determine the appropriate number of sample traverse points. If testing for multiple pollutants or diluents at the same site, a stratification test using only one pollutant or diluent satisfies this requirement.

20B - 77

77

### Sampling Procedures

- Conduct sampling system bias checks before and after each run
- Make no calibration adjustments prior to recording bias results after a run
- Sample run duration plus twice the sampling system response time

20B - 78

78

If System Exceeds Bias Specifications

- Run is invalid
- Fix system (maybe just re-calibrate analyzer)
- Repeat analyzer calibration error and sampling system bias checks before proceeding

20B - 79

79

If System Meets Bias Specification

- Use average of bias results before and after the run to correct the measured effluent gas concentration

20B - 80

80

Data Recording

- Strip chart or computer data acquisition system with resolution of at least 0.5% of instrument span
- Commonly done with PC-based data acquisition systems

20B - 81

81

Emission Calculations

- Data corrected for errors observed in calibration error bias checks

20B - 82

82

Interference Check

- *Interference Check* means the test to detect analyzer responses to compounds other than the compound of interest, usually a gas present in the measured gas stream, that is not adequately accounted for in the calibration procedure and may cause measurement bias.

20B - 83

83

Interference Check

- The total interference response (i.e., the sum of the interference responses of all tested gaseous components) must not be greater than 2.50 percent of the calibration span for the analyzer tested. In summing the interferences, use the larger of the absolute values obtained for the interferent tested with and without the pollutant present. The results are also acceptable if the sum of the responses does not exceed 0.5 ppmv for a calibration span of 5 to 10 ppmv, or 0.2 ppmv for a calibration span <5 ppmv.

20B - 84

84

Known SO<sub>2</sub>  
Analyzer Interferences

- Some earlier model NDIR SO<sub>2</sub> analyzers demonstrated a high bias due to residual moisture in the sample (after condenser)
- Some earlier model UV analyzers demonstrated a high bias when NO<sub>2</sub> concentrations were high relative to the SO<sub>2</sub> concentrations

20B - 85

85

Known SO<sub>2</sub>  
Analyzer Interferences

- Fluorescence analyzers suffer from quenching effects from CO<sub>2</sub> and O<sub>2</sub>

20B - 86

86

Sampling in the  
Presence of Ammonia

- Ammonia reacts with SO<sub>2</sub> in the condenser causing a low bias
- Amount of bias depends on the relative concentrations of SO<sub>2</sub> and ammonia

20B - 87

87

Sampling in the  
Presence of Ammonia

- Some success reported using dilution sampling systems
- Used modified Method 6 or modified Method 8 instead of Method 6C to ensure good results

20B - 88

88

Dilution Probes for Method 6C/7E/3A

- *Dilution-Type Systems—Special Considerations.* When a dilution-type measurement system is used, there are three important considerations that must be taken into account to ensure the quality of the emissions data. First, the critical orifice size and dilution ratio must be selected properly so that the sample dew point will be below the sample line and analyzer temperatures.

20B - 89

89

Dilution Probes for Method 6C/7E/3A

- Second, a high-quality, accurate probe controller must be used to maintain the dilution ratio during the test. The probe controller should be capable of monitoring the dilution air pressure, eductor vacuum, and sample flow rates. Third, differences between the molecular weight of calibration gas mixtures and the stack gas molecular weight must be addressed because these can affect the dilution ratio and introduce measurement bias.

20B - 90

90

Calibration Gas - Dilution Systems

- USEPA Method 205
- Not approved for acid rain (40 CFR 75) testing

20B - 91

91

Method 7E - NO<sub>x</sub>

- ? No field interference check (use Method 20 laboratory interference test)
- NO<sub>2</sub> to NO converter efficiency test (same as Method 20)

20B - 92

92

Method 7E - Ammonia (NH<sub>3</sub>) Interference Problems

- Use low temperature (molybdenum or activated carbon) NO<sub>2</sub> to NO converter to prevent conversion of NH<sub>3</sub> to NO
- Molybdenum converters lose efficiency quickly and need to be regenerated often

20B - 93

93

Method 7E - High NO<sub>2</sub>/NO Ratio in Sample

- NO<sub>2</sub> is readily absorbed by the sampling system, causing low bias
- Most NO<sub>x</sub> calibration gases contain little NO<sub>2</sub>

20B - 94

94

Method 7E - High NO<sub>2</sub>/NO Ratio in Sample

- NO<sub>2</sub> to NO converter efficiency becomes much more important
- Tester should perform NO/NO<sub>2</sub> balance adjustment

20B - 95

95

Method 3A - O<sub>2</sub> and CO<sub>2</sub>

- Any analytical technique
- Less rigorous sampling system material specification
- Option to substitute low-range check for zero gas for O<sub>2</sub> analyzers
- Laboratory interference check same as Method 20

20B - 96

96

Method 20

• **Determination of Nitrogen Oxides, Sulfur Dioxide, and Diluent Emissions From Stationary Gas Turbines**

Method 20 contains the details you must follow when using an instrumental analyzer to determine concentrations of nitrogen oxides, oxygen, carbon dioxide, and sulfur dioxide in the emissions from stationary gas turbines.

20B - 97

97

Method 20

- The use of Method 20 may be required by specific New Source Performance Standards, Clean Air Marketing rules, and State Implementation Plans and permits where measuring SO<sub>2</sub>, NO<sub>x</sub>, CO<sub>2</sub>, and/or O<sub>2</sub> concentrations in stationary gas turbines emissions are required. Other regulations may also require its use.

20B - 98

98

Method 20

- In this method, NO<sub>x</sub>, O<sub>2</sub> (or CO<sub>2</sub>), and SO<sub>x</sub> are measured using the following methods found in appendix A to this part:
- (a) Method 1—Sample and Velocity Traverses for Stationary Sources.
- (b) Method 3A—Determination of Oxygen and Carbon Dioxide Emissions From Stationary Sources (Instrumental Analyzer Procedure).
- (c) Method 6C—Determination of Sulfur Dioxide Emissions From Stationary Sources (Instrumental Analyzer Procedure).

20B - 99

99

Method 20

- (d) Method 7E—Determination of Nitrogen Oxides Emissions From Stationary Sources (Instrumental Analyzer Procedure).
- (e) Method 19—Determination of Sulfur Dioxide Removal Efficiency and Particulate Matter, Sulfur Dioxide, and Nitrogen Oxide Emission Rates.

20B - 100

100

Method 20

- You must follow the procedures of Section 8.4 of the appropriate methods listed in Section 2.0.
- A test run must have a duration of at least 21 minutes.

20B - 101

101



20B - 102

102

U.S. EPA APTI  
Compliance Test and  
Source Test Observation

RATA / CGA

21 - 1

1

Quality Assurance Activities

- Relative Accuracy Test Audit Procedures
- Cylinder Gas Audit and Linearity Check
- Opacity Calibration Error Assessment

21 - 2

2

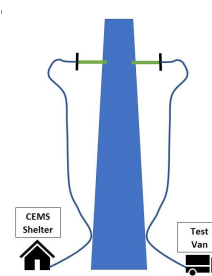
Relative Accuracy Test Audit  
(RATA)

- Requirements found in:
  - Part 60
    - New Source Performance Standards
    - Industry/Process Specific
  - Part 75
    - Acid Rain Program
    - Electric Generating Units

21 - 3

3

Relative Accuracy Test Audit  
(RATA)



Verification of CEMS  
performance by a  
third-Party testing  
company using  
USEPA Methods

21 - 4

4

Types of RATAs

- Gaseous
  - NO<sub>x</sub>
  - CO
  - SO<sub>2</sub>
  - Diluent (O<sub>2</sub> or CO<sub>2</sub>)
  - Other
- Flow Rate
- Particulate
- Mercury

21 - 5

5

RATA General Concepts

- Compare CEMS to Reference Method
- Reference Method is "Correct" data
  - Can be wet or instrumental version of the method
  - Typically, instrumental is preferred (real time data)
- Typical RATA is 12 runs, must use 9 to determine accuracy
- RATA Frequency – Varies on Rule

21 - 6

6



**RATA General Concepts (cont.)**

- RM tests should be on same basis as CEM system
  - Wet to wet, or dry to dry
- For gaseous pollutants: 21-minute runs
- For flow rate: as long as it takes to do a traverse
- Match up RM and CEM times (critical)

21 - 7

7

**Required Reference Method QC**

- Stratification test
- NOx converter efficiency
- Protocol calibration gases
- Linearity checks of analyzers
- Bias/drift checks
- Leak checks

21 - 8

8

**Part 60 RATA**

“Out of Control”

- NOx/SO<sub>2</sub>: > 20% RM mean, or >10% standard (whichever is less restrictive)
- O<sub>2</sub>/CO<sub>2</sub>: >20% RM mean, or 1% O<sub>2</sub>/CO<sub>2</sub>
- CO: >10% RM mean, or >5% standard
- “Out of Control” lasts until pass next RATA

21 - 9

9

**Part 75 RATA**

“Out of Control”

RATA	Semiannual	Annual
SO <sub>2</sub> or NO <sub>x</sub>	7.5% < RM ≤ 10% or ±15 ppm	RM ≤ 7.5% or ±12 ppm
SO <sub>2</sub> /diluent	7.5% < RM ≤ 10% or ±0.030 lb/mmBtu	RM ≤ 7.5% or ±0.025 lb/mmBtu
NO <sub>x</sub> /diluent	7.5% < RM ≤ 10% or ±0.020 lb/mmBtu	RM ≤ 7.5% or ±0.015 lb/mmBtu
CO <sub>2</sub> /O <sub>2</sub>	7.5% < RM ≤ 10% or ±1.0% CO <sub>2</sub> /O <sub>2</sub>	RM ≤ 7.5% or ±0.7% CO <sub>2</sub> /O <sub>2</sub>
Moisture	7.5% < RM ≤ 10% or ±1.5% H <sub>2</sub> O	RM ≤ 7.5% or ±0.10% H <sub>2</sub> O
Flow	7.5% < RM ≤ 10% or ±2.0% fps	RM ≤ 7.5% or ±1.5 fps

21 - 10

10

**Part 60 Requirements**

- Unit load
  - 50% of capacity, or
  - Normal” load
- Repeat every four calendar quarters
  - i.e.: annually

21 - 11

11

**Part 75 Requirements**

- Unit load
  - Test at “normal” load
  - Defined at Part 75, Appendix A, 6.5.2.1
- Frequency
  - Every 2 operating quarters (semi-annual), except:
  - Can go to annual if RA ≤ 7.5%
  - Fall back into semi-annual if RA > 7.5%

21 - 12

12

Cylinder Gas Audit (CGA)

- Challenge the CEMS three times at each audit point using a protocol gas, and use the average of the three responses in determining accuracy
- Each CEMS must be audited at least once each calendar quarter. Successive quarterly audits shall occur no closer than 2 months.

21 - 13

13

CGA (cont.)

CGA - may be conducted in three of four calendar quarters, but in no more than three quarters in succession

1. Challenge the CEMS (both pollutant and diluent portions of the CEMS, if applicable) with an audit gas of known concentration at two points

21 - 14

14

CGA (cont.)

2. Operate each monitor in its normal sampling mode, i.e., pass the audit gas through all filters, scrubbers, conditioners, and other monitor components used during normal sampling, and as much of the sampling probe as is practical.

21 - 15

15

CGA (cont.)

3. Use Certified Reference Materials (CRM's) audit gases that have been certified by comparison to National Institute of Standards and Technology (NIST) or EPA Traceability Protocol Materials (ETPM's) following the most recent edition of EPA's Traceability Protocol No. 1. As an alternative to CRM's or ETPM gases, Method 205 (See Citation 3) may be used.

21 - 16

16

CGA (cont.)

- The difference between the actual concentration of the audit gas and the concentration indicated by the monitor is used to assess the accuracy of the CEMS

21 - 17

17

Cylinder Gas Audit (CGA)  
Part 60

CGA Calibration Gas Requirements

Audit Point	Pollutant Analyzers % of Span	CO <sub>2</sub> % by volume (actual conc.)	O <sub>2</sub> % by volume (actual conc.)
1	20 to 30	5 to 8	4 to 6
2	50 to 60	10 to 14	8 to 12

21 - 18

18

### CGA vs Linearity

- Part 60 CGA
  - 2 gases: low (20-30% of span) and mid (50-60% of span)
  - Criteria < 15% or ≤5 ppm difference
  - Performed in 3 quarters per year with RATA performed in 4<sup>th</sup> quarter
- Part 75 Linearity
  - 3 gases: low (20-30% of span), mid (50-60% of span), and high (80-100% of span)
  - Criteria < 5% or ≤5 ppm difference
  - Performed in every QA operating quarter

21 - 19

19

### CGA: Out-of-Control Period

- An out-of-control period occurs when the CGA at any of the two concentrations (four for dual range) exceeds the applicable specifications (>15% error or 5 ppm difference). The out-of-control period begins with the hour of the failed CGA and ends with the hour of a satisfactory CGA following the corrective action.
- During the time the CEMS is out-of-control the CEMS data may not be used in calculating emission compliance nor be counted toward meeting minimum data availability.

21 - 20

20

### Linearity Check – Part 75

- Cal gas requirements are based on % of span per the following:

Low	20 – 30% of span value
Mid	50 – 60% of span value
High	80 – 100% of span value
- Calibration gases **MUST** be EPA Protocol certified
- Out-of-control occurs if any of the three audit level runs exceeds 5% or alternately 5 ppm difference for NOx/SO2 or 0.5% difference for CO2/O2
- Exemptions, grace periods, and extensions exist for linearity

21 - 21

21

U.S. EPA APTI  
Compliance Test and  
Source Test Observation

Method 205  
Gas Dilution System

22 - 1

1

**Background**

- Originated as Conditional Test Method 007 (CTM-007)
  - Assures Regional, State, and Local Authorities the gas dilution systems in use were producing accurate calibration gas at a fixed site.
  - Allow testers the advantage of avoiding costs and burden associated with purchasing transporting multiple gas cylinders over long distances.
- Promulgated as a Reference Method on May 30, 1994, as Method 205
  - Allows dilution system for most instrumental test method that requires multi-level cylinder gases.
  - Allows use of dilution systems when conducting performance specifications according to 40 CFR Part 60, Appendix F (CGAs), with Administrator Approval.
    - Administrative Approval for this has been delegated to Regions and in many instances down to the state level.

22 - 2

2

**Equipment Criteria**

- Gas Dilution System
  - Multiple vendors, however, the market appears to be dominated by a single provider
    - Internal mass flow controllers (MFC) used to set dilution ratio
    - Dilution Ratio can be set by other equipment (e.g., critical orifice, capillary tubes, etc...)
  - Must produce a calibration gas within  $\pm 2$  percent of the predicted value
  - Must be recalibrated once per calendar year using a NIST-traceable primary flow standards with an uncertainty  $\leq 0.25$  percent.
    - Must be labeled with the calibration date and expiration date
    - **NO** set requirement to report the calibration documentation...
- High and Mid-Level Calibration Gas
  - Protocol Gas is recommended
  - Mid Level gas **SHALL** be within 10% of one of the dilution levels.

22 - 3


3

**Mass Flow Controller and Meters**


22 - 4

4

**Gas Dilution System Calibration**



- No set calibration procedure for the systems
  - Critical Orifices/Capillary Tubes are fixed
  - Mass Flow Meters and Controllers should be calibrated at multiple flow rates
- Requirement to use a primary standard with an uncertainty of 0.25 % should restrict most testers from performing this measurement in-house.
  - Primary Standards of the quality are Cost Prohibitive (20-50K initial cost)
  - A number of metrology labs/vendors capable of maintaining these calibrations.
  - Appropriate alternative to using a primary standard that has proven uncertainty below  $\leq 0.25$  % is a Laminar Flow Element (i.e., Molbloc). Not currently included in the method, but any future revisions would include transfer standards.



22 - 5

5

**Method 205 (Requirements)**

- Field Evaluation (Mandatory)
  - Must be performed at the **Test Site**, prior to testing.
  - Prepare two different dilutions within the range of each dilution device.
    - Calculate a predicted value based on the dilution set-point(s) and high-level concentration
    - Challenge the Dilution System
      - At each set-point three times, by introducing gas to the analyzer through the dilution system
        - Precision Check –  $< 2\%$  of the average response
        - Accuracy Check –  $< 2\%$  of the predicted value
      - Introduce a mid-level gas (protocol gas and within 10% of a dilution level) directly to the analyzer
        - Accuracy Check –  $< 2\%$  of the certified concentration

22 - 6

6

### Method 205 (Requirements)

- Lab Evaluation (Optional)
  - Applies to reactive compounds (i.e., non-propane THC's , TRS compounds)
  - Must be conducted on an annual basis for each reactive compound
  - Same Procedures as the Field Evaluation

22 - 7

7

### Example – NOx/O<sub>2</sub> rata

#### Field Calibration - Oxygen Analyzer

- Instrument (Span for Testing) – O<sub>2</sub> - 21.0% **NOx – 12.2 ppmv**
- High Calibration Gas – O<sub>2</sub> @ 21.0%, **NO @ 99.2 ppmv** – Protocol Gas
- Mid-Level Calibration Gas – 20.9%, **NO @ N/A** – Protocol Gas
- Predicted Dilution Levels @ 2.1% and 21.0%
- Average Dilution Response of 2.2% and 20.6%
- Mid-Level Calibration Response – 20.9%

Acceptable

22 - 8

8

### Example A – NOx/O<sub>2</sub> RATA

#### Field Calibration - Oxygen Analyzer

- Instrument (Span for Testing) – O<sub>2</sub> - 21.0% **NOx – 12.2 ppmv**
- High Calibration Gas – O<sub>2</sub> @ 21.0%, **NO @ 99.2 ppmv** – Protocol Gas
- Mid-Level Calibration Gas – 20.9%, **NO @ N/A** – Protocol Gas
- Predicted Dilution Levels @ 2.1% and 21.0%
- Average Dilution Response of 2.2% and 20.6%
- Mid-Level Calibration Response – 20.9%

Good - Incorporated the dilution range for all analyzers  
Bad – Mid level Verification check performed at the "0" dilution point.  
Hmmm.... Was there a leak in the calibration system?

22 - 9

9

### Example B – THC, CO, AND O<sub>2</sub> Compliance Test

#### Field Calibration – Carbon Monoxide Analyzer

- Instrument (Span for Testing)  
CO – 100 ppmv, THC – 10 ppmv ,O<sub>2</sub> - 15.0%
- High Calibration Gas – Certified ± 5 %  
CO @ 10,000 ppmv, Propane @ 500 ppmv, O<sub>2</sub> @ 20.9
- Mid-Level Calibration Gas – Protocol Gas  
CO @990 ppmv, THC @ N/A, O<sub>2</sub> @ N/A, –
- Predicted Dilution Levels @ 1,000 ppmv and 5,000 ppmv
- Average Dilution Response of 1000 ppmv and 5000 ppmv
- Mid-Level Calibration Response – 1000 ppmv

Acceptable?

22 - 10

10

### Example B – THC, CO, AND O<sub>2</sub> Compliance Test

#### Field Calibration – Carbon Monoxide Analyzer

- Instrument (Span for Testing) – CO - 100 ppmv, **THC 10 ppmv ,O<sub>2</sub> - 15.0%**
- High Calibration Gas – CO @ 10,000 ppmv, **Propane @ 500 ppmv, O<sub>2</sub> @ 20.9**  
– Certified ± 5 %
- Mid-Level Calibration Gas – CO @990 ppmv, **THC @ N/A, O<sub>2</sub> @ N/A,** – Protocol Gas
- Predicted Dilution Levels @ 1,000 ppmv and 5,000 ppmv
- Average Dilution Response of 1000 ppmv and 5000 ppmv
- Mid-Level Calibration Response – 1000 ppmv


Good – Met The Method Criteria  
Bad – Did Not Bracket the Dilution Range (10:1 vs 200:1)  
Should of – Used a more appropriate high-level calibration gas  
Could of – Additional mid-level verification for high dilution ratio  
Hmmm.... That data looks really good

22 - 11

11

### Cylinder Gas Audits (CGAs)

- Can I use a Dilution System for Cylinder Gas Audit ?
  - Section 1.1 permits the use for CGA under Part 60
  - Broadly Applicable Alternative 25 (ALT-025) permitted the use under Part 63 as well. (September 3, 1999)
- You still must conduct the field evaluation at each site.
  - Multiple Gases Requirement (High and Mid) still required
  - Field evaluation takes a significant amount time.
- Diminishing Returns
  - Field Evaluation test should take twice as long as a normal CGA
  - Protocol Gas for Criteria Pollutants are widely available and relatively inexpensive with a long shelf life
    - 10 Year Certificate
    - Gas Cost – less than \$250/ Demurrage (2 cents/day) = 10 year cost \$323
- Compelling Applications
  - When cylinder gases are very expensive
    - Reactive Compounds
    - Low-Level Standards
  - When cylinder gases are not widely available
  - For some reason, if the tester cannot predict the exact concentration needed



22 - 12

12

### Method 205 Concerns

- Indeterminate Method Criteria
  - Calibration of the Dilution System
  - No record keeping
  - Maximum/Minimum Dilution Ratio Undefined, manufacture suggestion
- Technology
  - Open to any device that meets criteria
  - Multiple (Blended) Gas Calibration is undefined
  - Data Reporting/Recording/Logging

22 - 13

13

### Acid Rain Program (Part 75) Applications

- Method 205 is only permitted with Administrator Approval
- Part 75 is a “Cap and Trade” System
  - Tighter Protocol Gas Requirements (PGVP)
  - Quarterly Audits have a tighter criteria than CGAs
  - Quality Protocol Gases are widely available.

22 - 14

14

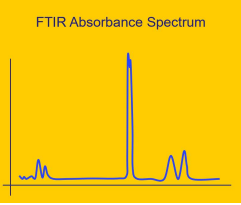
### Future Revisions to Method 205

- No immediate plans for major revisions to Method 205
  - Minor revision to incorporate the use of NIST transfer standards to calibrate the dilution devices.
- Future Revisions
  - Report/Record Requirements
  - Limit CGAs of criteria pollutants
  - Requirement to bracket dilution ranges
  - Defined System Calibration Requirements
  - PS 12 or 18 Applicability
  - Formatting Change – EMMC Format

22 - 15

15

### U.S. EPA APTI Compliance Test and Source Test Observation *FRM 320 and 321 FTIR*



23 - 1

1

### Introduction to FTIR Operation

- Absorption peaks in an infrared absorption spectrum arise from molecular vibrations
- Absorbed energy causes molecular motions which create a net change in the dipole moment

23 - 2

2

### Introduction to FTIR Operation

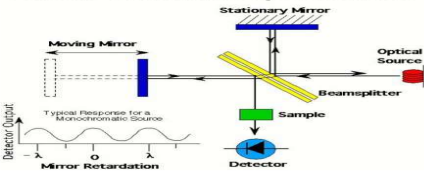
- Fourier-transform infrared spectroscopy is a vibrational spectroscopic technique, meaning it takes advantage of asymmetric molecular stretching, vibration, and rotation of chemical bonds as they are exposed to designated wavelengths of light.
- Fourier transform is to transform the signal from the time domain to its representation in the frequency domain

23 - 3

3

### FTIR Theory and Instrumentation

**Typical Fourier Transform Spectrometer**



- Light enters the spectrometer and is split by the beam splitter. The figure above shows what is referred to as the Michelson interferometer

23 - 4

4

### FTIR Theory and Instrumentation

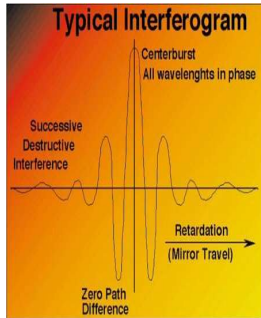
- Light originates from a He-Ne laser
- Half of the light is reflected 90 degrees, while the other half passes through the beam splitter and hits the moving mirror
- The split beams are recombined, after having traveled different distances, they exhibit an interference pattern with each other
- As they pass through the sample, the detector collects the interfering signals and returns a plot of response v. mirror displacement known as an interferogram

23 - 5

5

### FTIR Theory and Instrumentation

- The heart of the system is the interferometer in which the light from the source is divided into two beams.
- Beams pass through the sample cell and then recombine resulting in a signal.
- All information required to identify and quantify the gases in the sample is present in the interferogram.
- Interferogram signal is converted to a frequency spectrum by a mathematical technique called Fourier Transformation.



23 - 6

6

### FRM 320

- Measurement of Vapor Phase Organic and Inorganic Emissions by Extractive Fourier Transform Infrared (FTIR) Spectroscopy
  - 1.0 Introduction
  - 2.0 Summary of Method
  - 3.0 Definitions
  - 4.0 Interferences
  - 5.0 Safety
  - 6.0 Equipment and Supplies

23 - 7

7

### FRM 320 (cont'd)

- Measurement of Vapor Phase Organic and Inorganic Emissions by Extractive Fourier Transform Infrared (FTIR) Spectroscopy
  - 7.0 Reagents and Standards
  - 8.0 Sampling and Analytical Procedure
  - 9.0 Quality Control
  - 10.0 Calibration and Standardization
  - 11.0 Data Analysis and Calculations
  - 12.0 Method Performance

23 - 8

8

### FRM 320 (cont'd)

- Measurement of Vapor Phase Organic and Inorganic Emissions by Extractive Fourier Transform Infrared (FTIR) Spectroscopy
  - 13.0 Method Validation Procedure
  - 14.0 Pollution Prevention
  - 15.0 Waste Management
  - 16.0 References
  - Addendum to Test Method 320
    - Protocol for the Use of Extractive FTIR for the Analyses of Gaseous Emissions from Stationary Sources

23 - 9

9

### FRM 320 (cont'd)

- Measurement of Vapor Phase Organic and Inorganic Emissions by Extractive Fourier Transform Infrared (FTIR) Spectroscopy
  - Addendum A to Test Method 320
    - Protocol for the Use of Extractive FTIR for the Analyses of Gaseous Emissions from Stationary Sources
  - Addendum B to Test Method 320
    - Identifying Spectral Interferents
  - Addendum C to Test Method 320
    - Estimating Noise Levels

23 - 10

10

### FRM 320 (cont'd)

- Measurement of Vapor Phase Organic and Inorganic Emissions by Extractive Fourier Transform Infrared (FTIR) Spectroscopy
  - Addendum D to Test Method 320
    - Estimating Minimum Concentration Measurement Uncertainties
  - Addendum E to Test Method 320
    - Determining Fractional Reproducibility Uncertainties
  - Addendum F to Test Method 320
    - Determining Fractional Calibration Uncertainties
  - Addendum G to Test Method 320
    - Measuring Noise Levels

23 - 11

11

### FRM 320 (cont'd)

- Measurement of Vapor Phase Organic and Inorganic Emissions by Extractive Fourier Transform Infrared (FTIR) Spectroscopy
  - Addendum H to Test Method 320
    - Determining Sample Absorption Pathlength and Fractional Analytical Uncertainty
  - Addendum I to Test Method 320
    - Determining Fractional Model Uncertainties

23 - 12

12



### FRM 320 Sampling Types

- Screening
- Emission Test
- Validation

23 - 13

13

### FRM 320 (cont'd)

- Measurement of Vapor Phase Organic and Inorganic Emissions by Extractive Fourier Transform Infrared (FTIR) Spectroscopy
  - System involves typical CEM probe and pump to extract the sample to the FTIR analytical bench
  - An IR spectra of the sample is digitized from the FTIR gas cell
  - "Reference spectra" prepared in the laboratory of the standard samples of interest compared to the digitized FTIR spectra of the sample
  - Self-validation method in utilizing a QA analyte spike of the extracted sample at the probe

23 - 14

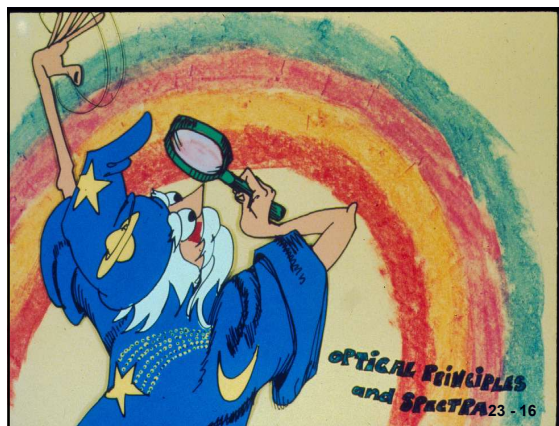
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### FRM 320

- "...This method applies to the analysis of vapor phase organic or inorganic compounds which absorb energy in the mid-infrared spectral region, about 400 to 4000  $\text{cm}^{-1}$  (2.5 to 2.5  $\mu\text{m}$ ). This method is used to determine compound-specific concentrations in a multi-component vapor phase sample, which is contained in a closed-path cell. Spectra of samples are collected using double beam infrared absorption spectroscopy. A computer program is used to analyze spectra and report compound concentrations."

23 - 15

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### Infrared Spectroscopy

- Infrared light (IR) waves at discrete frequencies to molecular bond motions
- Vibrational and pure rotational motions
- When the frequencies match, energy is absorbed by that bond and resulting excitation increases molecular bond energy state (non-ionizing)

23 - 17

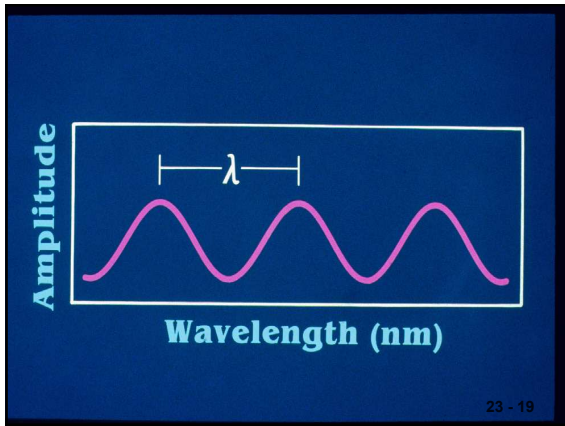
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### Infrared Spectroscopy

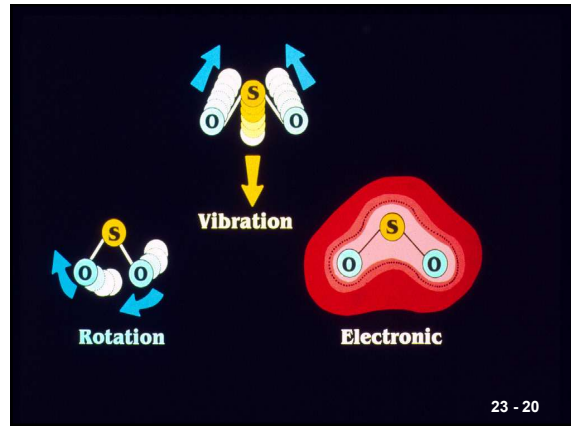
- The energy absorbed by the bond at discrete frequencies is proportional to the number of molecules
- FTIR spectrum is a plot of decreased energy at discrete frequencies corresponding to the absorption bands of the compounds in the sample. High resolution 0.5  $\text{cm}^{-1}$

23 - 18

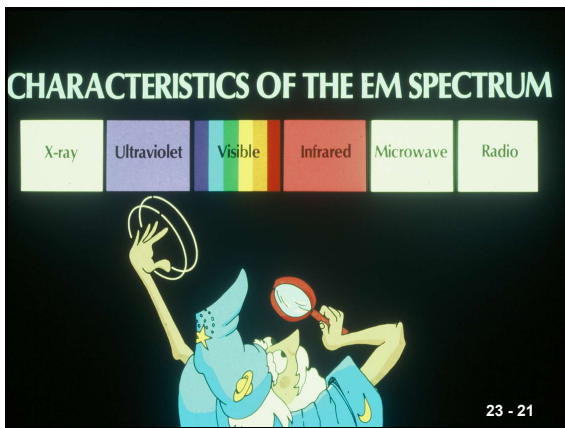
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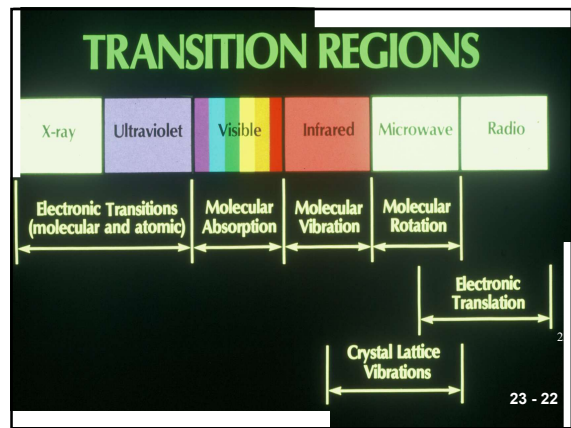
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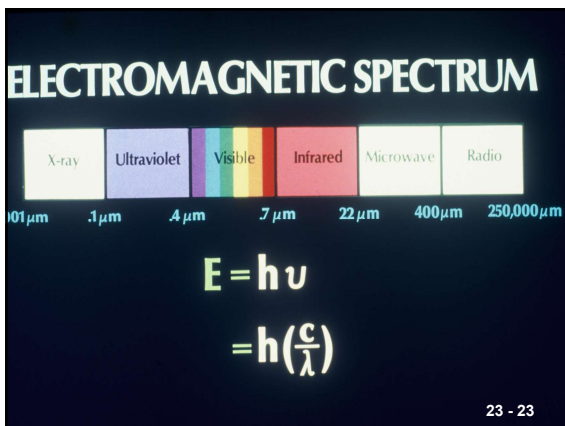
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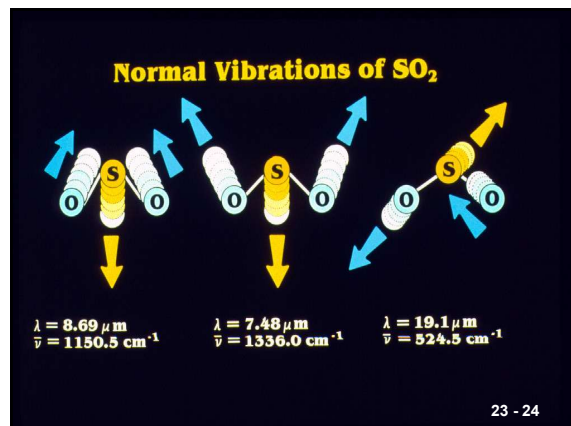
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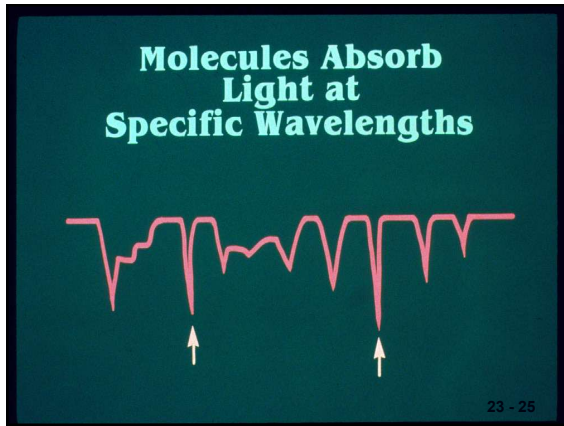
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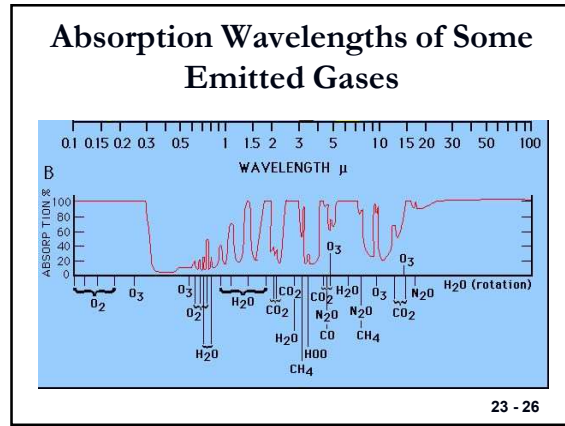
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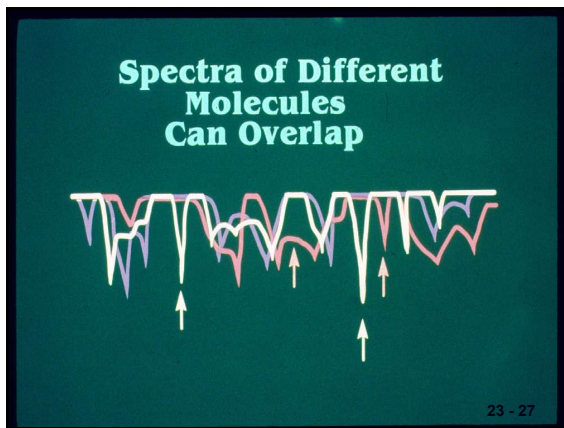
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**Beer-Lambert Law**

$$I = I_0 e^{-\alpha c l}$$

**I** = intensity of radiation through the sample  
**I<sub>0</sub>** = intensity of radiation with  $c = 0$  or  $\alpha = 0$   
 **$\alpha$**  = absorption coefficient  
**c** = gas concentration  
**l** = pathlength of radiation through the gas

23 - 29

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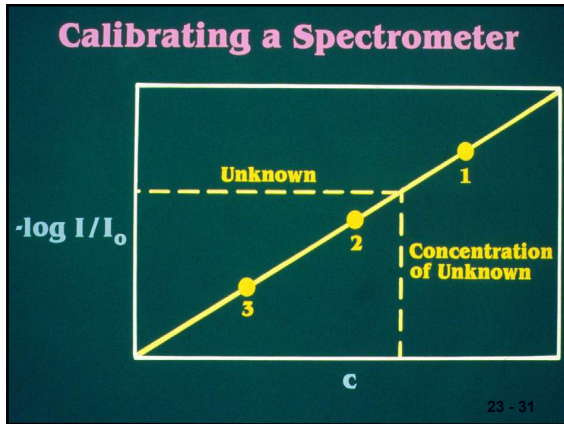
**From Beer-Lambert Law:**

$$A = \log I/I_0 = \alpha c l$$

**Direct Relationship**

23 - 30

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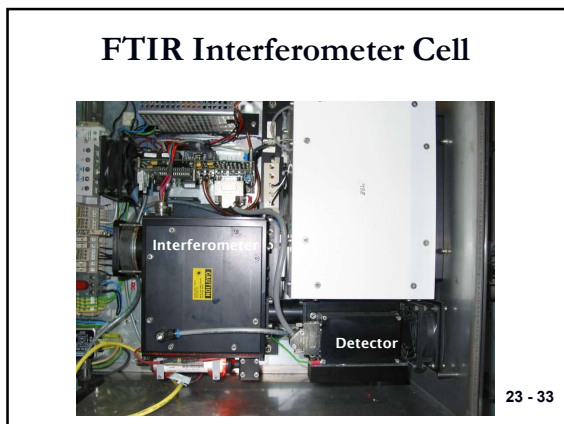
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**Infrared Band Centers Of Some Common Gases**

Gas	Band Center ( $\mu\text{m}$ )	Wave Number ( $\text{cm}^{-1}$ )
NO	5.0-5.5	1800-2000
NO <sub>2</sub>	5.5-20	500-1800
SO <sub>2</sub>	8-14	700-1250
H <sub>2</sub> O	3.1, 5-5.5, 7.1-10	1000-1400 1800-3200
CO <sub>2</sub>	2.7, 5.2, 8-12	850-3700
NH <sub>3</sub>	10.5	950

23 - 32

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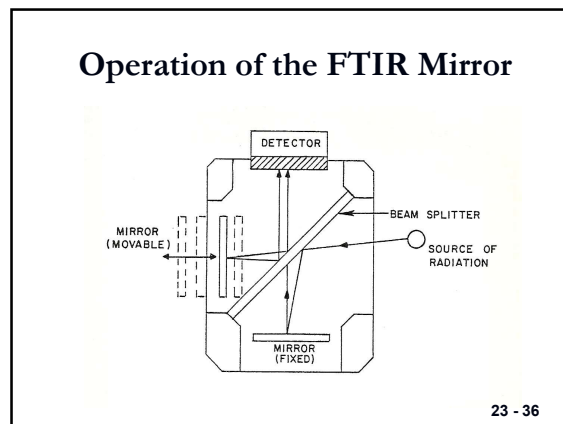
33

- Operation of the FTIR Spectrometer**
- IR energy enters the spectrometer
  - A beam splitter reflects back 50 percent and transmits 50 percent of the incoming infrared radiation
  - The two beams are then reflected back to the beam splitter by a moving mirror and a stationary mirror
  - Depending on the position of the moving mirror, these two beams recombine with a specific path difference between them
- 23 - 34

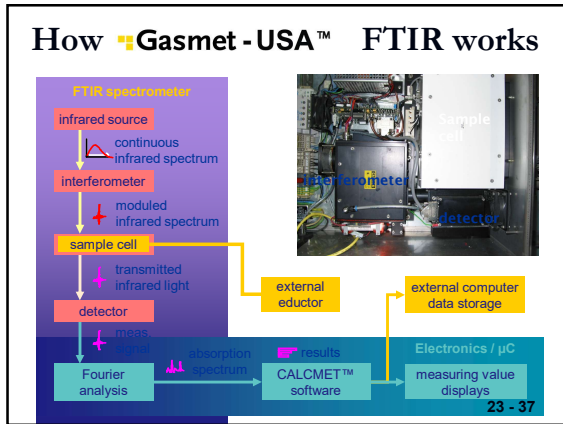
34

- Operation of the FTIR Spectrometer**
- This produces the interferogram
  - The interferogram is generated by the interferometer modulating the infrared beam as the moving mirror is translated
  - The modulated frequencies depend on the wavelength of the incident radiation and the velocity of the moving mirror
  - The interferogram is produced after absorption by the sample and is detected by the detector
- 23 - 35

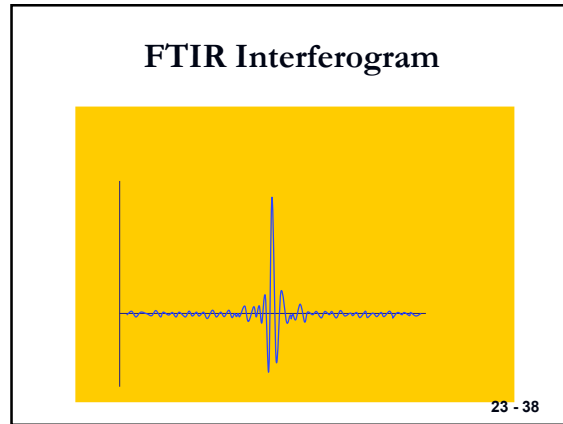
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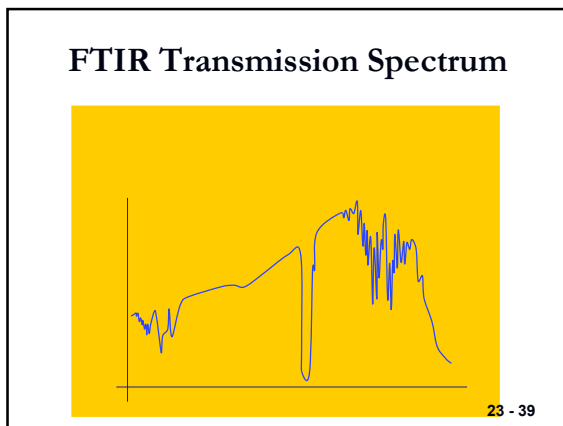
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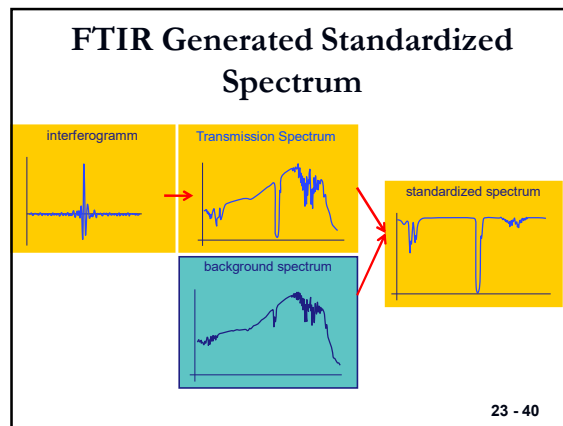
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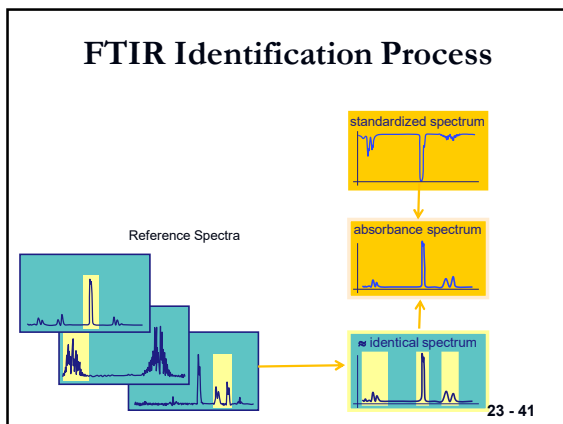
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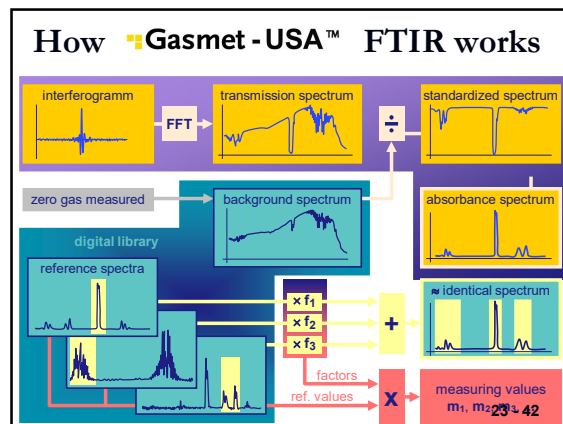
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43

### Components of FRM 320

- Sample probe: Glass, stainless steel or other appropriate material of sufficient length and physical integrity to sustain heating.
- Particulate filter: A glass wool plug inserted at the probe tip and a filter to remove particulate matter.
- Heat trace sample line: Heated sufficiently to prevent condensation.

23 - 44

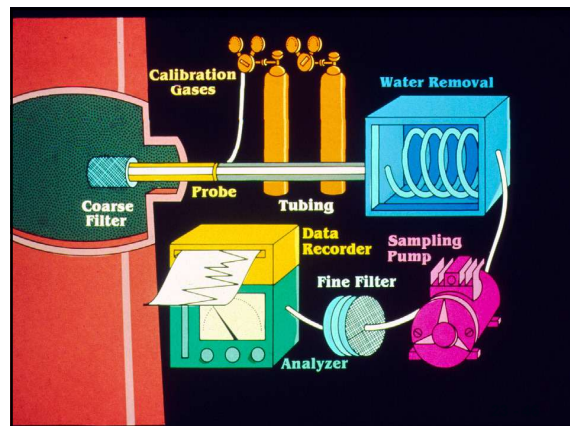
44

### Components of FRM 320

- Gas Distribution Manifold: A heated manifold allowing the operator to control flows of gas standards and samples directly to the FTIR system or through sample conditioning system. May use heated flow meters, heated valves etc.
- Calibration/Analyte Spike Assembly: A three-way valve assembly to introduce analyte or surrogate spikes into the sampling system at the outlet of the probe upstream of the out-of-stack filter and the FTIR analytical system.
- FTIR Analytical Bench

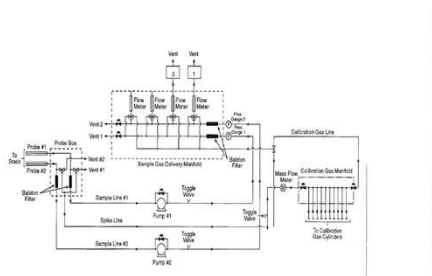
23 - 45

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46

### FRM 320 Extractive FTIR Sampling System



23 - 47

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### Sampling and Analysis Procedures

- Set-up Sampling System
- Pre-test Preparation and Evaluation
  - Select required detection limit ( $DL_i$ ) and maximum permissible Analytical Uncertainty ( $AU_i$ ) for each analyte. Estimate maximum expected concentration of each analyte.
  - List potential interferences
  - Determine Fractional Reproducibility Uncertainty ( $FRU_i$ )

23 - 48

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### Sampling and Analysis Procedures

- Pre-test Preparation and Evaluation (Cont'd)
  - Calculate Minimum Analyte Uncertainty (MAU)
  - Prepare computer program and input reference spectra for all analytes
- Leak-Check Sampling System
  - From probe to pump
  - FTIR cell
- Determine Linearity of Detector

23 - 49

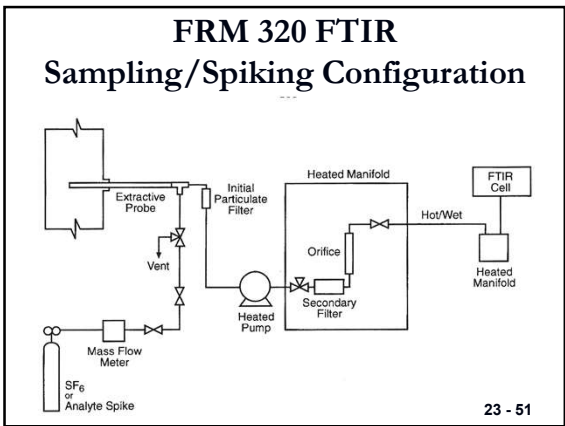
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### Sampling and Analysis Procedures

- Perform Background Spectrum with dry nitrogen in FTIR cell
  - Also have in data base spectra of major interferences
- Pre-test Calibrations
  - Fill FTIR cell with Calibration Transfer Standard (CTS). CTS should be certified  $\pm 2\%$  by manufacturer. Record spectra
  - QA Spike to probe to FTIR analytical bench using certified standard (70-130 % recovery)
- Begin Sampling

23 - 50

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### Sampling and Analysis Procedures

- Post-test QA
  - Verify instrument parameters
  - Perform post-test CTS spectra ( $\pm 5\%$ )

23 - 52

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### FRM 320 QA Activities

- Analytical Spike (Section 9)-Three spiked samples, analyte concentration in the spike sample compared to expected spike concentration to verify that the sampling/analytical system is working properly
- QA Spike Procedure (Section 8.6.2)- QA Spike to probe to verify that sampling/analytical system is working.
- Response Time Determination (Section 9.2.2)-
- Validation Procedure (Section 13)-

23 - 53

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### FRM 320 QA Activities

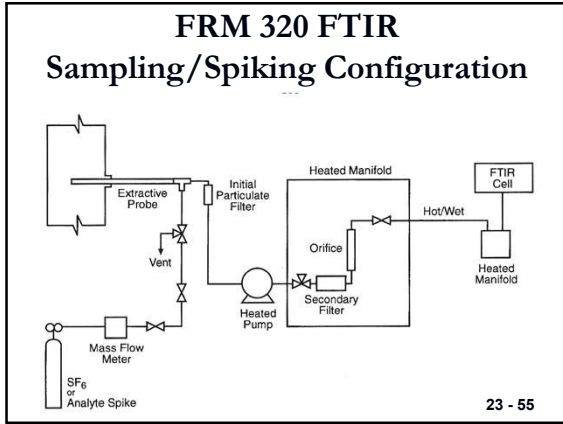
- Method Validation Procedure (Section 13)- Similar to QA Spike procedure in that one acquires two un-spiked samples, then introduces QA Spike gas into continuous flow of sample gas. Collect spectra of two sample gases.
  - Use FRM 301 to calculate bias as:
 
$$B = S_m - CS$$

Where:

- B = Bias at spike level
- $S_m$  = Mean concentration of the analyte spiked samples
- CS = Expected concentration of the spiked samples

23 - 54

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55

### FRM 320 QA Activities

- Method Validation Procedure (Section 13)-
  - Use Method 301 to evaluate statistical significance of the bias.
  - If bias is significant ( $0.7 \leq CF \leq 1.3$ ), then develop a correction factor (CF) is calculated and emission results are multiplied by the CF for final analyte concentration.
  - If  $CF \geq \pm 30$  percent, then the test method is considered to be “not valid.”

23 - 56

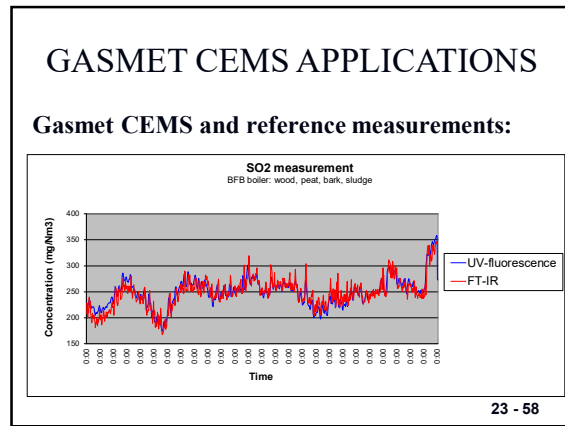
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### FRM 320 Interferences

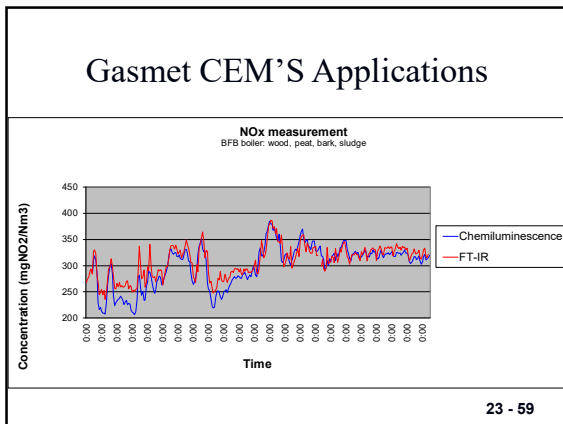
- Analytical Interferences (Background and Sampling)
  - Background interference occurs when unexpected change in background spectra from dirt on lenses, changes in detector sensitivity, changes in infrared source etc. This requires a new background to be generated.
  - Spectral interferences from mostly water and CO<sub>2</sub> which causes interferences with measurement analyte wavelength.

23 - 57

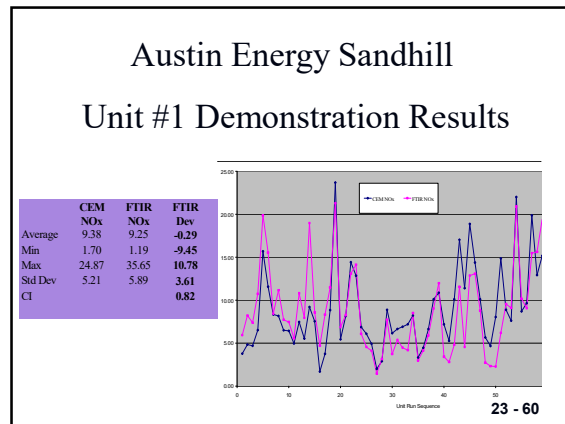
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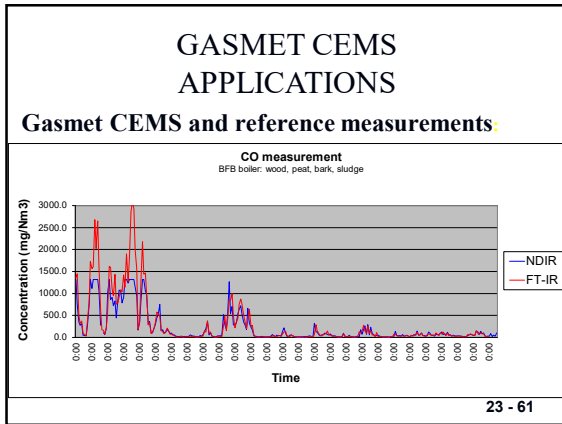


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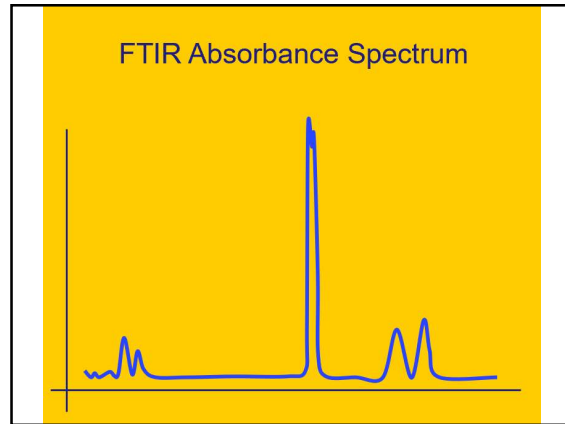


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## Fourier Transform Infrared (FTIR) Reference Spectra

EPA United States Environmental Protection Agency

Technology Transfer Network  
Emission Measurement Center Spectral Database

You are here: EPA Home > TTN Main > Emission Measurement Center > Spectral Database > Fourier Transform Infrared FTIR Reference Spectra

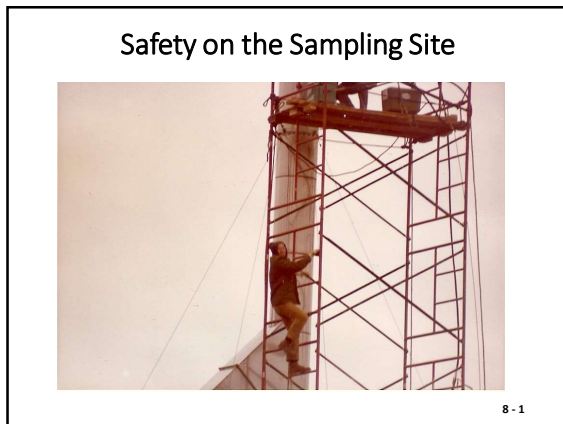
**Fourier Transform Infrared (FTIR) Reference Spectra**

The Clean Air Act Amendments (CAAA) was published in November 1990. Title II of the Clean Air Act includes a list of 189 hazardous air pollutants (HAPs) for which test methods must be established. An extractive stack sampling method, using FTIR, has been developed for measuring HAPs. As one of the initial tasks in the project development, reference spectra were developed for as many of the HAPs as possible. Attached is a table which contains the quantitative reference spectral library as of June 1993. The table includes several columns of information for each file. The pathlength is the pathlength of the sample cell used to record that particular spectrum. The TEMP column is the temperature at which the compound was measured. Spectra were recorded for each compound at four or at least two different concentrations when possible. Duplicate spectra were recorded for every concentration for quality assurance purposes. The ASC column is the accepted standard concentration which was assigned by the chemical standard. The ASC values should be used for data analysis. Duplicate samples were obtained for each concentration. These spectra were developed following the Protocol for Speciated FTIR for Analysis of Gas Emissions - Refer to the FTIR TECHNOLOGY DEVELOPMENT Report for additional information regarding these spectra.

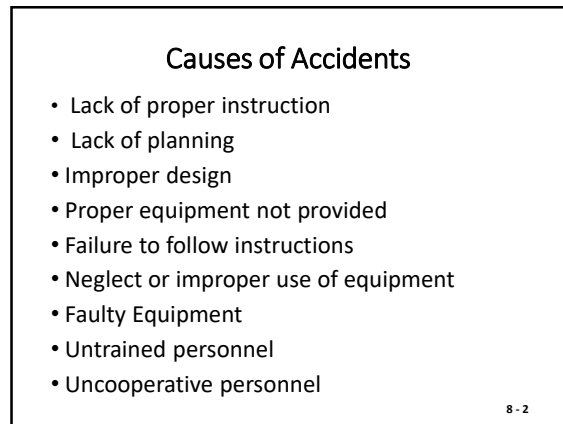
CAAS reg. no.	Compound Name	Symbol	Pathlength (m)	Temp (°C)	Concentration (ppm)	Resolution (ÅSC)	Resolution (µm <sup>-1</sup> )
57-14-7	1,1-Dimethyl hydrazine	C2H8N2	2.25	100	494.1	0.25	
57-14-7	1,1-Dimethyl hydrazine	C2H8N2	2.25	100	95.8	0.25	
57-14-7	1,1-Dimethyl hydrazine	C2H8N2	2.25	100	500	0.25	
57-14-7	1,1-Dimethyl hydrazine	C2H8N2	2.25	100	99.9	0.25	
79-00-5	1,1,2-Trichloroethane	C2H3Cl3	2.25	100	100.1	0.25	
79-00-5	1,1,2-Trichloroethane	C2H3Cl3	2.25	100	100.1	0.25	

23 - 63

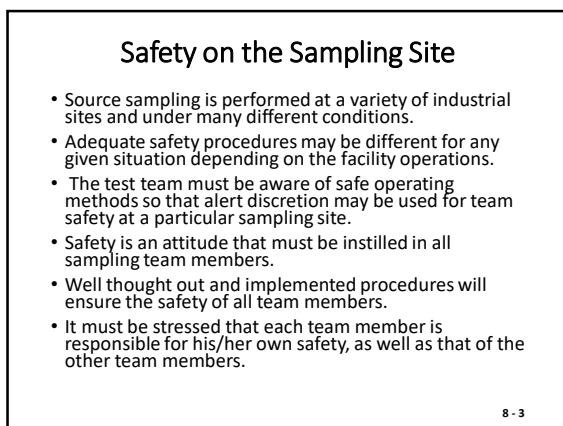
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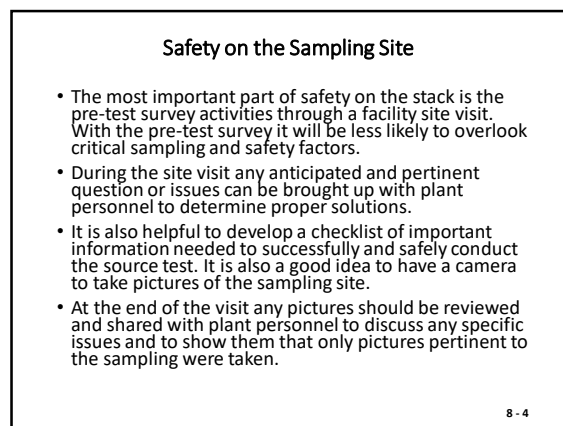
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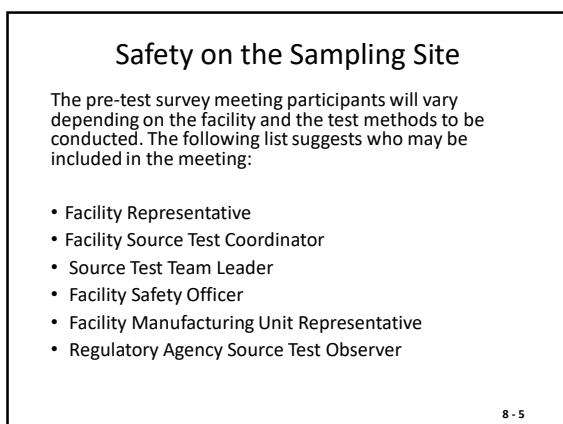
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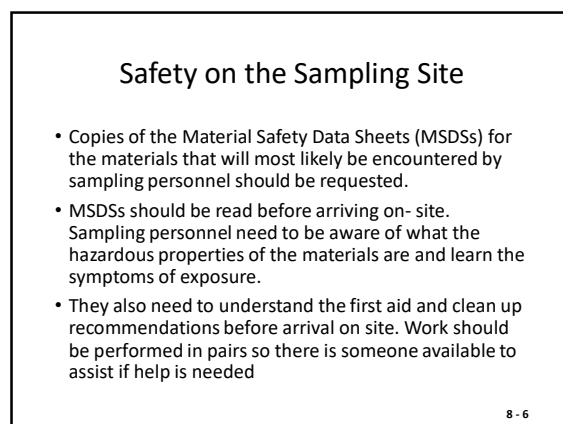
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### Safety on the Sampling Site

- The Source Evaluation Society (SES) Safety Guidelines Handbook Second Edition is an excellent reference document specifically for source testing personnel.
- The manual is a compilation of submissions from different members of the SES Safety Committee and is intended to be a living document.
- It also contains information on first aid, hazardous chemicals, site safety checklists and a CD version of the NIOSH Pocket Guide to Chemical Hazards.
- However, it is stated in the guidebook that; **any OSHA requirements supersedes the information contained in the Handbook** (<http://www.sesnews.org/>).

8 - 7

7

### SES Safety Guidelines Handbok

<http://www.sesnews.org/index.php?q=node/21>

8 - 8

8

### Safety on the Sampling Site

- Chapter 22 in the SES Safety Guidelines Handbook lists the items to include when conducting a Facility walk-through. They are:
- Request to have the Facility Safety Officer and the source test coordinator participate in the walk-through.
- Inspect the source locations to be sampled and the access to and from the testing sites. Ask questions about anything that may be a safety issue for the sampling crew. Also consider the safety risk that the sampling may have on other personnel at or near the test site.
- Make a list of modifications and repairs that need to be done prior to sampling. Review the list with the appropriate facility representatives before leaving the meeting. Establish accountabilities for each action item on the list. Plan to follow up on the action items before returning to conduct the source sampling.

8 - 9

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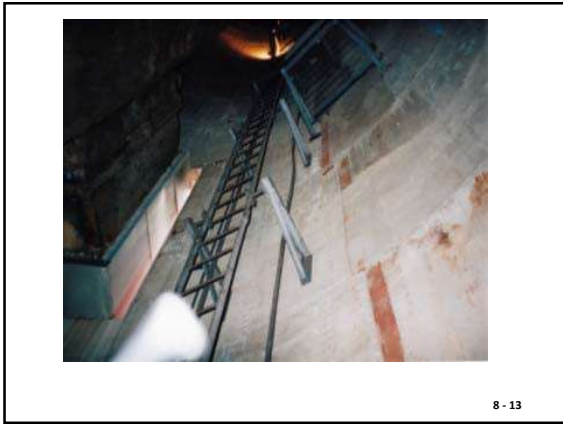
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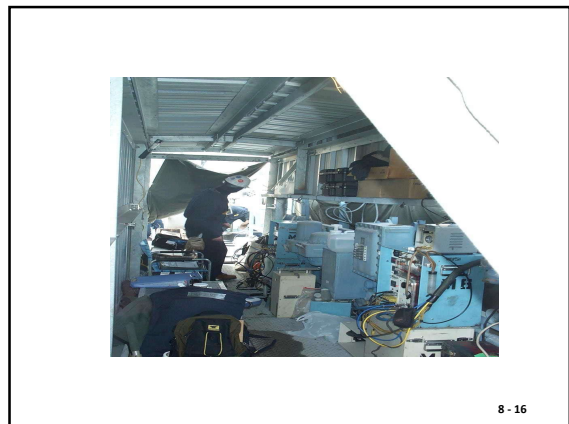
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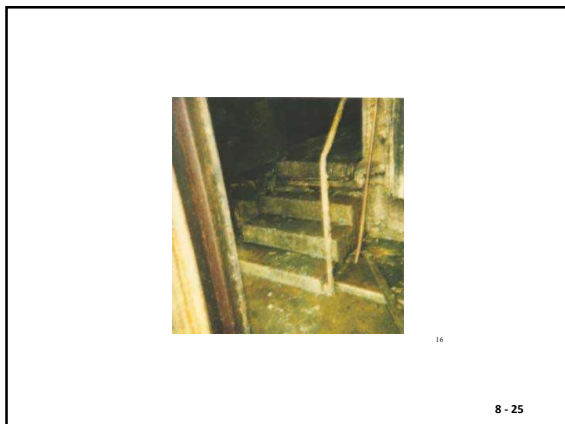
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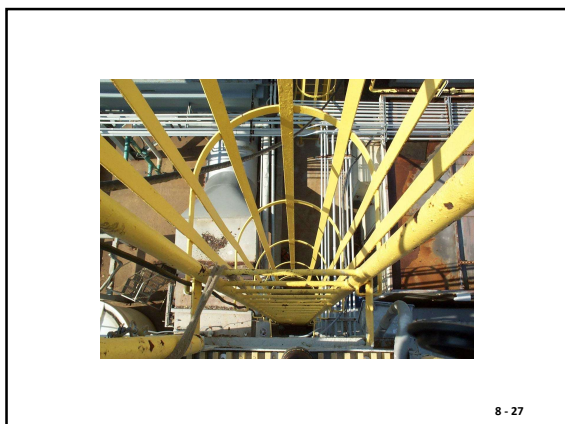
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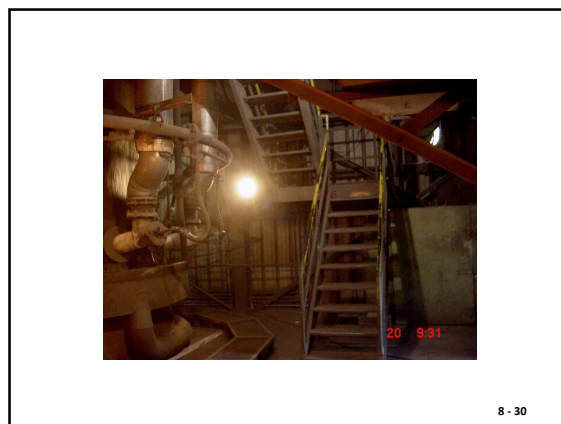
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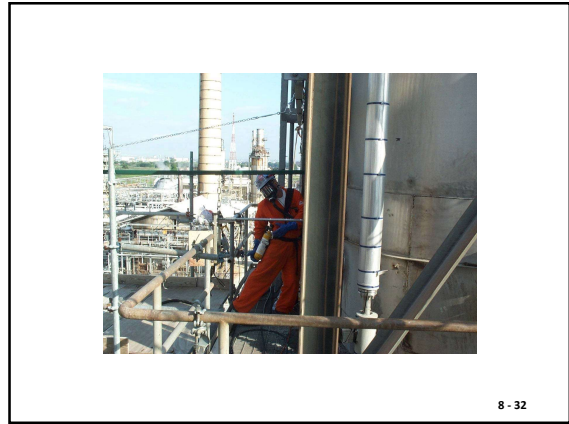


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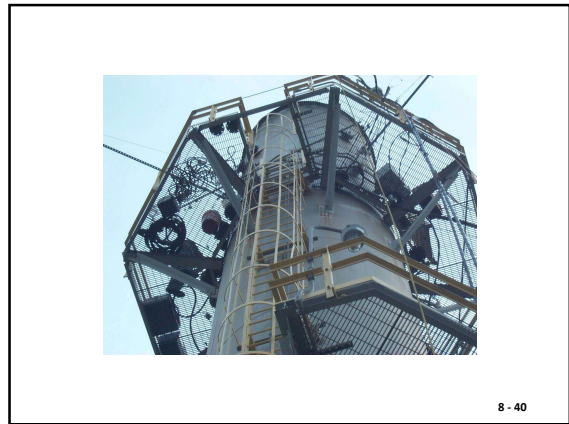
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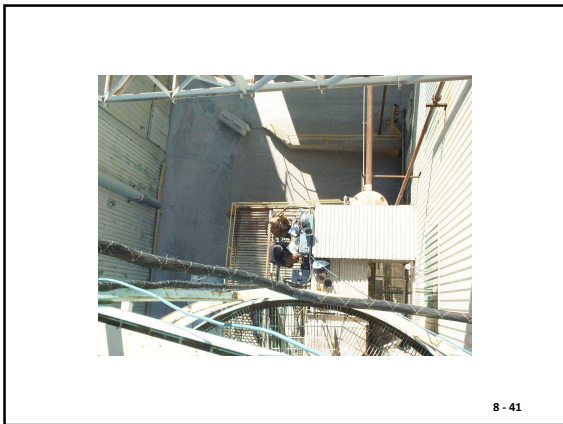
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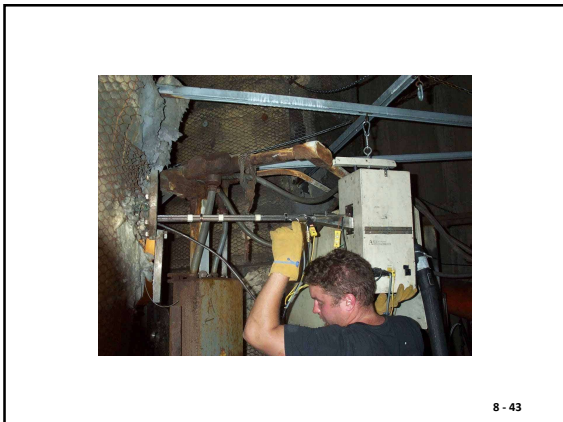


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