# EPA's APTI Course #450/#468 Monitoring Compliance Test And Source Test Observation



# Reference Materials



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### **Notice**

This is not an official policy and standards document. The opinions and selections are those of the author and not necessarily those of the Environmental Protection Agency. Every attempt has been made to represent the present state of the art as well as subject areas still under evaluation. Any mention of products or organizations does not constitute endorsement by the United States Environmental Protection Agency (USEPA).

# **Usage of This Manual**

The Central States Air Resource Agencies Association (CenSARA) is one of several multi- jurisdictional organizations (MJOs) operating for the U.S. Environmental Protection Agency (USEPA), through the Air Pollution Training Institute (APTI), to update more of the frequently used APTI courses. The primary objectives of the MJOs are to:

- Promote the exchange of information between the States;
- Serve as a forum to discuss regional air quality issues of common concern;
- Share resources for the common benefit of the member states; and
- Provide training services to their member air pollution control agencies.

APTI provides courses on air pollution control technology, ambient air and source monitoring, and air quality management. Historically, APTI designed courses that meet the job training needs of governmental agency personnel and others in the field of air pollution. This requires a thorough examination of both the materials for instruction and the characteristics of the student audience. Based on studies conducted by APTI of those who have participated in the various training courses, courses were developed and revised to provide training that enables every student to achieve specific course objectives. A basic goal of APTI was to provide training that will enable a student to do specific jobs in his or her home environmental agency. However, recently APTI has taken a new direction and has given money to the various MJOs, of which CenSARA is one, to update needed training course for their member states.

CenSARA meets these training needs of its member states by identifying, designing, developing and delivering needed, cost-effective, responsive, and focused educational opportunities for state and local air agency staff. Agenda and course materials are obtained from a variety of sources including EPA, colleges and universities, regional training consortia, and individual instructors. Yet, due to changes in environmental regulations, the implementation of new policies, and the advancement of technologies, agendas and course materials become out-of-date. When this happens, staffs' ability to enhance skills, knowledge and abilities are constrained, limiting their ability to excel in the dynamic field of air pollution control. So by providing up-to-date, high quality educational opportunities for staff, their chances to greatly enhance their skills, knowledge and abilities is significantly improved.

Consequently, CenSARA announced a Request for Proposals (RFP) to the environmental training community to solicit technical proposals and cost bids to review current compliance test and observation programs within the USEPA and to **update** as necessary the content title, agenda topics, course length, instructor and student manuals, lectures involving presentation slides, classroom and homework exercises, and other handouts and materials for EPA's APTI Course #450/#468 entitled: "Monitoring Compliance Test and Source Test Observation." In response to CenSARA's RFP, EnviroTech Solutions, William T. "Jerry" Winberry, 1502 Laughridge Drive, Cary, North Carolina 27511, <a href="jwinberry@mindspring.com">jwinberry@mindspring.com</a>, 919-467-2785, was awarded the contract to update EPA's APTI Course #450/#468. Mr. Winberry is the author of this Student Workbook (SW) and every attempt has been made to represent the most recent advances in sampling and analytical methodology

## **Disclaimer**

This material has been developed and assembled to provide training associated with EPA's APTI Course #450/#468 entitled: "Monitoring Compliance Test and Source Test Observation." It is not intended to be used for regulatory purposes, or to be a substitute for, nor interpreted as official Agency policy. Every attempt was made to reflect the technical state of art and regulatory information as of the date of this publication. This is not an official policy and standards document. The opinions and selections are those of the author and not necessarily those of the EPA. Any mention of produces or organizations does not constitute endorsement by the EPA.

# U.S. Environmental Protection Agency Air Pollution Training Institute Course #450/#468

# Monitoring Compliance Test and Source Test Observation

# **Student Workbook (SW)**

The Central States Air Resource Agencies Association (CenSARA) is one of several multi- jurisdictional organizations (MJOs) operating for the U.S. Environmental Protection Agency (USEPA), through the Air Pollution Training Institute (APTI), to update more of the frequently used APTI courses. The primary objectives of the MJOs are to:

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agendas and course materials become out-of-date. When this happens, staffs' ability to enhance skills, knowledge and abilities are constrained, limiting their ability to excel in the dynamic field of air pollution control. So, by providing up-to-date, high quality educational opportunities for staff, their chances to greatly enhance their skills, knowledge and abilities is significantly improved. Consequently, CenSARA has taken the initiative to update EPA's APT! Course #450/#468.

The updated Course #450/#468 is targeted primarily at agency personnel who have the responsibility to monitor compliance test and source test observation of various FRMs and SW- 846 methodologies. The revised course materials provide the best available and most current information as well as relevant example exercises to improve the knowledge and expertise of agency observer personnel. The desired outcome of this effort is that agency staff be able to properly observe compliance test and perform source test observations to protect public health and the environment by developing an understanding of EPA's stack testing programs and strategy, various stack test methodologies for quantifying HAPs from industrial processes, and associated quality assurance/quality control activities and requirements.

The specific objectives of updating APTI Course #450/#468 materials include:

- Explain why sampling of source emissions for PM and HAPs is important in air pollution control agency programs;
- Define symbols and common terms used in the application of FRMs 1-5 and SW-846 source sampling;
- Recognize, interpret and apply sections of the Code of Federal Regulations, Appendix A, pertinent to source sampling for particulate pollutants;
- Understand the construction, operation and calibration of the component parts of the FRM 5 particulate matter sampling train;
- Define "Isokinetic sampling" and illustrate why it is important in sampling for PM;
- Understanding the "working" isokinetic rate equation and its derivation
- Learn how to use specific software for determining isokinetic sampling rates;
- Apply FRMs 1 through 4 in preparation for applying FRM 5 at a source to characterize PM emissions;
- Understand how the "S-type" pitot tube is constructed and standardized and how it is applied in source sampling;
- Understand the difference between systematic error and precision as applied to source test measurements;
- Properly assemble and leak check a FRM 5 sampling train;
- Describe the operation of the VOST, Semi-VOST, Acid Gas and FRM 201/201A sampling trains;
- Describe what are "condensibles" and how the FRM 202 sampling train operates to measure condensibles; and
- Calculate the "% Isokinetic" value for a source test, and interpret the effect of over or under- isokinetic values on the source test results.

One of the products of the #450/#468 update is the Student Workbook (SW). The SW provides copies of visuals presented in each technical lecture. Contained in this SW are the visuals for each of the Sessions and lessons presented in APT! Course #450/#468.

#### I. Background

Over the last several years, public awareness of air pollution and its sources has increased steadily. Specifically, since the passage of the Clean Air Act Amendments (the Act) of 1990 and the implementation of EPA's maximum achievable control technology (MACT) program, more emphasis has been placed on local, State, and Federal agencies to keep the public informed on health effects of various air pollutants and their levels of exposure. This awareness has required industry to become accountable for air pollution emissions as part of their source's compliance strategy and regulatory agencies to become knowledgeable of the methodology used to quantify reported emissions.

Traditionally, air pollution control agencies require all sources to quantitate their emissions in order to demonstrate compliance. To insure that the source test methods utilized to demonstrate compliance are performed according to EPA guidelines, regulatory agencies observe stack test to document compliance with the methodology. This has meant that sources must know how to properly sample and report emissions using EPA reference methods and that regulatory agencies must know how to properly observe these test to insure that reliable and accurate data is gathered and reported.

In addition, with the passage of the Act and Title IV, Acid Rain, those fossil-fueled-fired-steam generators (FFFSG) covered must report emissions in units of pollutant mass rate (pmr) as part of EPA's emission trading program. This required the installation and certification of velocity monitors if the continuous emission monitoring system (CEMS) data was to be used as part of EPA's market base-trading program. These new regulatory requirements have now required Agency personnel to know how to observe and verify the proper use and implementation of Federal Reference Methods 2F, 2G, and 2H in certification of the velocity CEMS as part of a source's market base-trading emission program.

Consequently, the Act has required regional, state, and local air pollution control agencies to better understand the stack test methodologies that are used to quantitate air pollution emissions from industrial sources. Agencies see a need to provide training to it's personnel on how to properly observe stack test used to meet regulatory compliance for criteria and hazardous air pollutants (HAPs).

## II. Course Objective

The objective of EPA's APTI Course #450/#468 is to provide Agency personnel the needed background information, checklist, and guidance associated with EPA methodologies involving stack test for characterizing and quantifying criteria and HAPs from industrial sources. This course will address Federal Reference Methods (FRMs)1-5 (isokinetic stack testing and stack test basics), FRMs 2F, 2G, and 2H (velocity), stack testing for volatile organic compounds (FRMs 18, 25, 25A/B), SO<sub>2</sub> (FRMs 6, 6A, and 8), NOx (FRMs 7, 7C), dioxin/furans and PCBs (FRM 23), heavy metals (FRM 29), and instrumental (FRMs 3A, 6C, and 7E).

The course will present standardized stack test methodology for sampling and analysis of air pollutants as identified in the Code of Federal Regulations (CFR), Part 60, Appendix A. In

addition, information will be presented on EPA's stack test monitoring programs associated with PM-10 (Methods 201 A/B) and condensable particulate (Method 202) monitoring from CFR 51 Subpart M. Specific source test checklists will be demonstrated during the presentation for each test methodology as part of the course. Participants will learn how to use the checklist in performing source test observations, how to observe mandated QA/QC requirements associated with each methodology, and how to use source test databases available to the air pollution scientist.

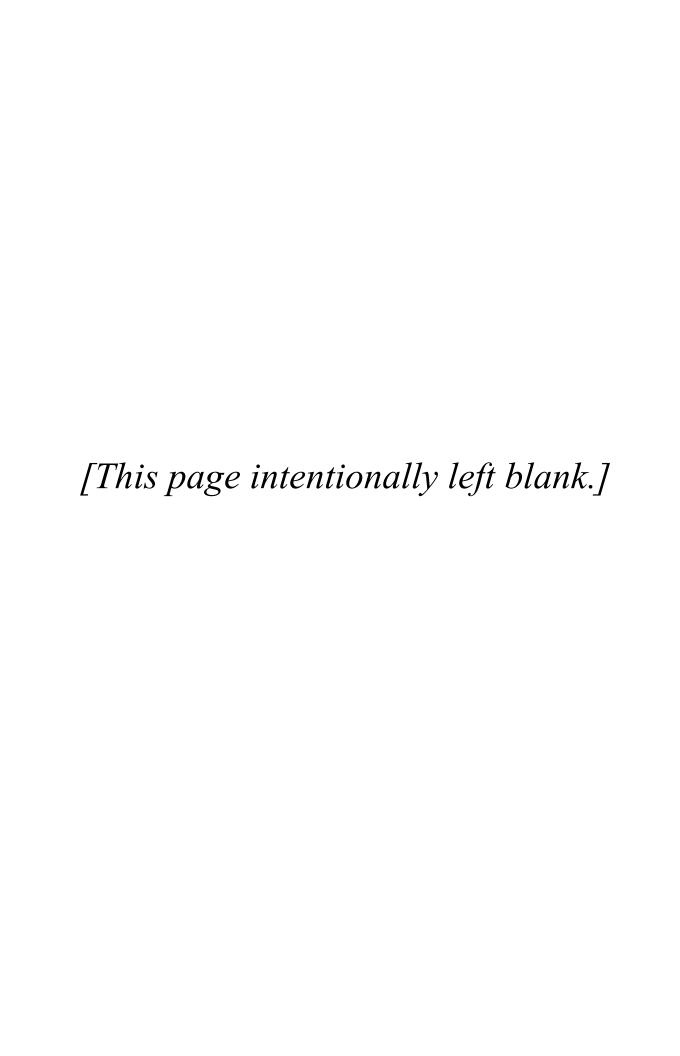
At the end of this course, the agency personnel will gain an understanding of the unique source test methods used to accurately characterize air pollutant emissions from industrial sources. The agency personnel will learn about EPA's programs that require characterization of air pollutants from industrial sources utilizing FRMs.

#### III. Course Manuals

Course presentations and videos will be supported by four manuals. They are:

- #468 Student Workbook (Hard Copy): The updated Student Workbook (SW) contains copies of selected slides from each of the lecture presentations, and Agency Inspector Checklist.
- #468 Stack Test Manual (Flash Drive): The Stack Test Manual contains full copies of selected stack test sampling and analytical methods found in the CFR, Part 60, Appendix A, and SW-846, Standard Methods.
- Apex Instruments Federal Reference Method 5 Operational Manual:
   The Federal Reference Method 5 Operation Manual is a document describing specifically the construction and operation of Federal Reference Method 5 stack testing sampling train.

   <a href="http://www.apexinst.com/cms/wp-content/uploads/2015/03/Model-500-Series-Manual-Method-5.pdf">http://www.apexinst.com/cms/wp-content/uploads/2015/03/Model-500-Series-Manual-Method-5.pdf</a>.



## Appendix A

## **Equations**

## $R_i = \arccos ine [(\cos ine Y_i)(\cos ine P_i)]$

Equation 1-2

#### General

$$\Delta H = K(\Delta p)$$

$$\overline{pmr}_s = c_s Q_s$$

$$A_s = \pi \left(\frac{D_s}{2}\right)^2$$

$$A_s = LW$$

$$F_d = \frac{20.9 - \% O_2}{\% CO_2}$$

$$\%EA = \frac{(\%O_2) + 0.5(\%CO)}{0.0264(\%N_2) - (\%O_2) + 0.5(\%CO)}$$

$$\% N_2 = 100 - \% CO_2 - \% O_2 - \% CO$$

#### Method 1

Equation 1-1

$$D_e = \frac{2LW}{L+W}$$

#### Equation 1-3

$$\overline{R} = \frac{\sum R_i}{n}$$

Equation 1-4

$$S_d = \sqrt{\frac{\sum_{i=1}^{n} (R_i - \overline{R})^2}{(n-1)}}$$

#### Method 2

Equation 2-1

$$D_e = \frac{2LW}{L+W}$$

Equation 2-2

$$C_{p(s)} = C_{p(std)} \sqrt{\frac{\Delta p_{std}}{\Delta p_{s}}}$$

Equation 2-3

$$Deviation = C_{p(s)} - \overline{C}_{p} (A or B)$$

Equation 2-4

$$\sigma(side\ A\ or\ B) = \frac{\sum_{1}^{3} \left| C_{p(s)} - \overline{C}_{p} \left( A\ or\ B \right) \right|}{3}$$

Equation 2-5

$$=M_d (1-B_{ws})+18.0 B_{ws}$$

Equation 2-6

$$=P_{bar}+P_{g}$$

Equation 2-7

$$=273+t_s$$
 for metric.

Equation 2-8

$$=460+t_s$$
 for English.

Equation 2-9

$$v_s = K_p C_p (\sqrt{\Delta p})_{avg} \sqrt{\frac{T_{s(avg)}}{P_s M_s}}$$

Equation 2-10

$$Q_{sd} = 3,600 (1 - B_{ws}) v_s A \frac{T_{std}}{T_{s(avg)}} \frac{P_s}{P_{std}}$$

Method 2F

Equation 2F-1

$$F_1 = \frac{(P_4 - P_5)}{(P_1 - P_2)}$$

Equation 2F-2

$$F_2 = C_p \sqrt{\frac{\Delta p_{std}}{(P_1 - P_2)}}$$

Equation 2F-3

% Diff = 
$$\frac{F_2^{\text{max}} - F_2^{\text{min}}}{F_2^{\text{min}}} \times 100\%$$

Equation 2F-4

$$M_s = M_d (1 - B_{ws}) + 18.0 B_{ws}$$

Equation 2F-5

$$P_s = P_{bar} + \frac{P_g}{13.6}$$

Equation 2F-6

$$T_{s(i)} = 273 + t_{s(i)}$$

Equation 2F-7

$$T_{s(i)} = 460 + t_{s(i)}$$

Equation 2F-8

$$v_{a(i)} = K_p F_{2(i)} \sqrt{\frac{(P_1 - P_2)_i T_{s(i)}}{P_s M_s}} (\cos \theta_{y(i)}) (\cos \theta_{p(i)})$$

Equation 2F-9

$$v_{a(avg)} = \frac{\sum_{i=1}^{n} v_{a(i)}}{n}$$

Equation 2F-10

$$Q_{sw} = 3,600 (v_{a(avg)}) (A) \left( \frac{T_{std}}{T_{s(avg)}} \right) \left( \frac{P_s}{P_{std}} \right)$$

Equation 2F-11

$$Q_{sw} = 3,600(1 - B_{ws})(v_{a(avg)})(A) \left(\frac{T_{std}}{T_{s(avg)}}\right) \left(\frac{P_s}{P_{std}}\right)$$

Method 3

Equation 3-1

$$M_d = 0.440 \, (\% \, CO_2) + 0.320 \, (\% \, O_2) + 0.280 \, (\% \, N_2 + \% \, CO)$$

Method 3A

Equation 3A-1

$$C_{gas} = \frac{C_{ma} - C_{oa}}{C_m - C_o} (\overline{C} - C_m) + C_{ma}$$

Method 4

Equation 4-1

$$V_{wc(std)} = \frac{(V_f - V_i)\rho_w RT_{std}}{P_{std} M_w}$$
$$= K_1 (V_f - V_i)$$

Equation 4-2

$$\begin{aligned} V_{wsg(std)} &= \frac{(W_f - W_i)RT_{std}}{P_{std}M_w} \\ &= K_2\left(W_f - W_i\right) \end{aligned}$$

Equation 4-3

$$V_{m(std)} = V_m Y \frac{(P_m)(T_{std})}{(P_{std})(T_m)}$$
$$= K_3 Y \frac{V_m P_m}{T_m}$$

Equation 4-4

$$B_{ws} = \frac{V_{wc(std)} + V_{wsg(std)}}{V_{wc(std)} + V_{wsg(std)} + V_{m(std)}}$$

Equation 4-5

$$V_{wc} = \frac{(V_f - V_i) \rho_w RT_{std}}{P_{std} M_w}$$
$$= K_1 (V_f - V_i)$$

Equation 4-6

$$V_{m(std)} = V_m \left(\frac{P_m}{P_{std}}\right) \left(\frac{T_{std}}{T_m}\right)$$
$$= K_2 \frac{V_m P_m}{T_m}$$

Equation 4-7

$$B_{ws} = \frac{V_{wc}}{V_{wc} + V_{m(std)}} + B_{wm}$$

Method 5

Equation 5-9a

$$\Delta H_{@} = 0.0319 \,\Delta H \, \frac{T_m}{P_{bar}} \, \frac{\theta^2}{Y^2 V_m^2}$$

#### Equation 5-1

$$V_{m(std)} = V_m Y \left( \frac{T_{std}}{T_m} \right) \left[ \frac{P_{bar} + \frac{\Delta H}{13.6}}{P_{std}} \right]$$
$$= K_1 V_m Y \frac{P_{bar} + \left( \frac{\Delta H}{13.6} \right)}{T_m}$$

#### Equation 5-1a

$$\left[V_m - (L_p - L_a)\right]$$

$$\left[ V_m - (L_1 - L_a) \theta_1 - \sum_{i=2}^n (L_i - L_a) \theta_i - (L_p - L_a) \theta_p \right]$$

#### Equation 5-2

$$V_{w(std)} = \frac{V_{lc} \rho_w RT_{std}}{M_w P_{std}}$$
$$= K_2 V_{lc}$$

#### Equation 5-3

$$B_{ws} = \frac{V_{w(std)}}{V_{m(std)} + V_{w(std)}}$$

#### Equation 5-4

$$C_a = \frac{m_a}{V_a \rho_a}$$

#### Equation 5-5

$$W_a = C_a V_{aw} \rho_a$$

#### Equation 5-6

$$c_s = (0.001 \ g/mg) \left( \frac{m_n}{V_{m(std)}} \right)$$

#### Equation 5-7

$$I = \frac{100T_{s} \left[ K_{3} V_{lc} + \left( \frac{V_{m} Y}{T_{m}} \right) \left( P_{bar} + \frac{\Delta H}{13.6} \right) \right]}{60 \theta V_{s} P_{s} A_{n}}$$

#### Equation 5-8

$$I = \frac{100 T_{s} V_{m(std)} P_{std}}{60 T_{std} v_{s} \theta A_{n} P_{s} (1 - B_{ws})}$$

$$= \frac{K_{4} T_{s} V_{m(std)}}{P_{s} v_{s} A_{n} \theta (1 - B_{ws})}$$

#### Equation 5-8a

$$Q = K_1 \frac{P_{bar}}{t_w + t_{std}} \frac{V_w}{\theta}$$

#### Equation 5-9

$$K' = \frac{K_1 V_m Y \left( P_{bar} + \frac{\Delta H}{13.6} \right) \sqrt{T_{amb}}}{P_{bar} T_m \theta}$$

#### Equation 5-10

$$V_m(std) = K_1 V_m \frac{P_{bar} + \frac{\Delta H}{13.6}}{T_m}$$

Equation 5-11

$$V_{cr}(std) = K' \frac{P_{bar} \theta}{T_{amb}}$$

Equation 5-12

$$Y = \frac{V_{cr(std)}}{V_{m(std)}}$$

#### Method 6

Equation 6-1

$$V_{m(std)} = V_m Y \left( \frac{T_{std}}{T_m} \right) \left( \frac{P_{bar}}{P_{std}} \right)$$
$$= K_1 Y \left( \frac{V_m P_{bar}}{T_m} \right)$$

Equation 6-2

$$C_{SO_2} = K_3 \frac{\left(V_t - V_{tb}\right) N\left(\frac{V_{soln}}{V_a}\right)}{V_{m(std)}}$$

Equation 6-3

$$RE = \frac{C_d - C_a}{C_a} (100)$$

Equation 6-4

$$V_{sb(std)} = V_{sb} \left( \frac{T_{std}}{T_{amb}} \right) \left( \frac{P_{bar}}{P_{std}} \right)$$

Equation 6-5

$$Q_{std} = \frac{V_{sb(std)}}{\theta}$$

Equation 6-6

$$V_{m(std)} = \overline{Q}_{std} \ \theta_s \ (1 - B_{wa}) \left( \frac{P_{bar} + P_{sr}}{P_{bar} + P_c} \right)$$

Equation 6-7

$$V_{m(std)} = \overline{Q}_{std} \ \theta_s \ (1 - B_{wa}) \sqrt{\frac{M_a}{M_s}} \left( \frac{P_{bar} + P_{sr}}{P_{bar} + P_c} \right)$$

#### Method 6A

Equation 6A-1

$$V_{CO2(std)} = 5.467 \, x \, 10^{-4} \, (m_{af} - m_{ai})$$

Equation 6A-2

$$V_{w(std)} = 1.336 \times 10^{-3} (m_{wf} - m_{wi})$$

Equation 6A-3

$$C_{SO_2} = 32.03 \frac{(V_t - V_{tb}) N \left(\frac{V_{soln}}{V_a}\right)}{V_{m(std)} + V_{CO_2(std)}}$$

Equation 6A-4

$$C_{CO_2} = \frac{V_{CO_2(std)}}{V_{m(std)} + V_{CO_2(std)}} x100$$

Equation 6A-5

$$C_w = \frac{V_{w(std)}}{V_{m(std)} + V_{w(std)} + V_{CO2(std)}}$$

Equation 6A-7

$$m_{SO_2} = 32.03 \left(V_t - V_{tb}\right) N \left(\frac{V_{so \ln}}{V_s}\right)$$

Equation 6A-8

$$E_{SO_2} = F_c (1.829 \times 10^9) \frac{m_{SO_2}}{(m_{af} - m_{ai})}$$

#### Equation 7-3

$$m = 2K_c A F$$

Equation 7-4

$$C = K_2 \frac{m}{V_{sc}}$$

Equation 7-5

$$RE = \frac{C_d - C_a}{C_a} (100)$$

#### Method 8

Equation 8-1

$$V_{m(std)} = V_m Y \left( \frac{T_{std}}{T_m} \right) \left( \frac{P_{bar} + \left( \frac{\Delta H}{13.6} \right)}{P_{std}} \right)$$
$$= K_1 V_m Y \left( \frac{P_{bar} + \left( \frac{\Delta H}{13.6} \right)}{T_m} \right)$$

Equation 8-2

$$C_{H_2SO_4} = K_2 \frac{N(V_t - V_{tb}) \left(\frac{V_{soln}}{V_a}\right)}{V_{m(std)}}$$

Equation 8-3

$$C_{SO_2} = K_3 \frac{N(V_t - V_{tb}) \left(\frac{V_{so \ln}}{V_a}\right)}{V_{m(std)}}$$

#### Method 6C

Equation 6C-1

$$C_{gas} = (\overline{C} - C_o) \frac{C_{ma}}{C_m - C_o}$$

#### Method 7

Equation 7-1

$$K_c = 100 \frac{A_1 + 2A_2 + 3A_3 + 4A_4}{{A_1}^2 + {A_2}^2 + {A_3}^2 + {A_4}^2}$$

Equation 7-2

$$V_{sc} = \left(\frac{T_{std}}{P_{std}}\right) \left(V_f - V_a\right) \left(\frac{P_f}{T_f} - \frac{P_i}{T_i}\right)$$

$$=K_1 \left(V_f - 25 \, ml\right) \left(\frac{P_f}{T_f} - \frac{P_i}{T_i}\right)$$

Equation 8-4

$$I = \frac{100T_{s} \left[ K_{3} V_{lc} + \left( \frac{V_{m} Y}{T_{m}} \right) \left( P_{bar} + \frac{\Delta H}{13.6} \right) \right]}{60 \theta V_{s} P_{s} A_{n}}$$

Equation 8-5

$$I = \frac{100 T_{s} V_{m(std)} P_{std}}{60 T_{std} v_{s} \theta A_{n} P_{s} (1 - B_{ws})}$$

$$= \frac{K_{4} T_{s} V_{m(std)}}{P_{s} v_{s} A_{n} \theta (1 - B_{ws})}$$

#### Method 11

Equation 11-1

$$N_s = 2.039 \frac{W}{V_s}$$

Equation 11-2

$$N_A = 0.2039 \frac{W}{V_s}$$

Equation 11-3

$$N_{\rm I} = N_T \, \frac{V_T}{V_{\rm I}}$$

Equation 11-4

$$V_{m(std)} = V_m Y \left[ \left( \frac{T_{std}}{T_m} \right) \left( \frac{P_{bar}}{P_{std}} \right) \right]$$

Equation 11-5

$$C_{H2S} = \frac{K\left[\left(V_{\mathrm{IT}} \ N_{\mathrm{I}} - V_{\mathrm{TT}} \ N_{\mathrm{T}}\right) sample - \left(V_{\mathrm{IT}} \ N_{\mathrm{I}} - V_{\mathrm{TT}} \ N_{\mathrm{T}}\right)\right]}{V_{m(std)}}$$

Method 15

Equation 15-1

$$C = \frac{(K)(P_r)}{ML}$$

Equation 15-2

$$SO_2$$
 equivalent =  $\sum (H_2S, COS, 2CS_2) d$ 

Equation 15-3

$$Average SO_2 \ equivalent = \frac{\sum_{i=1}^{N} SO_2 \ equiv_i}{N}$$

Method 15A

Equation 15A-1

$$V_{ms(std)} = \frac{V_{ms} Y(T_{std})(P_{bar})}{(T_m)(P_{std})} = \frac{K_1 Y(V_m)(P_{bar})}{T_m}$$

Equation 15A-2

$$V_{mc(std)} = \frac{k_1 Y_c (V_{mc}) (P_{bar})}{T_m}$$

Equation 15A-3

$$C_{TRS} = \frac{K_2 \left(V_t - V_{tb}\right) N \left(\frac{V_{so \ln}}{V_a}\right)}{V_{ms(std)} - V_{mc(std)}}$$

Equation 15A-4

$$C_{RG} = \frac{(C_{COS})(Q_{COS})}{Q_{COS} + Q_{N2}}$$

Equation 15A-5

$$R = \frac{C_{TRS}}{C_{RG}} x 100$$

#### Method 16

Equation 16-1

$$C = K \frac{P_r}{ML}$$

Equation 16-2

$$TRS = \sum (H_2S, MeSH, DMS, 2DMDS) d$$

Equation 16-3

$$AverageTRS = \frac{\sum_{i=1}^{N} TRS_{i}}{N(1 - B_{WO})}$$

Equation 16-4

$$C = \frac{\sum_{i=1}^{N} S_i}{N}$$

#### Method 16A

Equation 16A-1

$$V_{m(std)} = V_m Y \frac{T_{std}}{T_m} \frac{P_{bar}}{P_{std}} = K_1 Y \frac{V_m - P_{bar}}{T_m}$$

Equation 16A-2

$$C_{TRS(ppm)} = \frac{K_2 \left(V_t - V_{tb}\right) N\left(\frac{V_{soln}}{V_a}\right)}{V_{m(std)}}$$

Equation 16A-3

$$C_{RG} = \frac{(Q_{H2S})(C_{H2S})}{Q_{H2S} + Q_{CG}}$$

Equation 16A-4

$$R = \frac{C_{TRS}}{C_{RG}} x 100$$

Equation 16A-5

$$N_T = \frac{1}{ml \ Na_2 \ S_2 \ O_3 \ Consumed}$$

Equation 16A-6

$$N_{\rm I} = \frac{N_T V_T}{V_{\rm I}}$$

Equation 16A-7

$$V_{m(std)} = (\overline{Q}_{std})(\theta_s)(1 - B_{wa}) \frac{M_a}{M_b}$$

Equation 16A-8

$$C_{H2S} = \frac{K N_T (V_{TB} - V_T)}{V_{m(std)}}$$

#### Method 16B

Equation 16B-1

$$C_{TRS} = (C_{SO2})(d)$$

Equation 16B-2

$$C_{TRS} = \frac{\sum_{i=1}^{n} C_{TRS}}{N}$$

#### Method 18

Equation 18-1

$$C_s = \frac{10^6 \left(\overline{x} \, q_c\right)}{q_c + q_d}$$

Equation 18-2

$$C_s = 106 \,\overline{x} \left( \frac{q_{c1}}{q_{c1} + q_{d1}} \right) \left( \frac{q_{c2}}{q_{c2} + q_{d2}} \right)$$

#### Equation 18-3

$$C_s = \frac{G_V \times 10^6 \frac{293}{T_s} \frac{P_s}{760}}{V_m Y \frac{293}{T_m} \frac{P_m}{760} 1000}$$

$$=\frac{G_V \times 10^3 \frac{P_s}{T_s} \frac{T_m}{P_m}}{V_m Y}$$

#### Equation 18-4

$$C_s = \frac{\frac{L_V}{M} \rho (24.055 \times 10^6)}{V_m Y \frac{293}{T_m} \frac{P_m}{760} 1000} = 6.24 \times 10^4 \frac{L_V \rho T_m}{M V_m Y P_m}$$

Equation 18-5

$$C_c = \frac{C_s P_r T_i F_r}{P_i T_r (1 - B_{ws})}$$

#### Method 20

Equation 20-1

$$C_d = \frac{C_w}{1 - B_{ws}}$$

Equation 20-2

$$F_o = \frac{0.209 \, F_d}{F_c}$$

Equation 20-3

$$X_{CO2} = \frac{5.9}{F_o}$$

Equation 20-4

$$C_{adj} = C_d \; \frac{5.9}{20.0 - \% O_2}$$

Equation 23-3

$$RRF_{rs} = \frac{A_{ci} * m_{rs}}{A_{rs} m_{ci} *}$$

Equation 20-5

$$C_{adj} = C_d \frac{X_{CO2}}{\% CO_2}$$

Equation 23-4

$$R^* = \frac{A_i * m_{rs}}{A_{rs} RF_{rs} m_i *} x 100\%$$

Equation 20-6

$$E = C_d F_d \frac{20.9}{20.9 - \%O_2}$$

Equation 23-5

$$RRF_s = \frac{A_{ci} * m_s}{A_{cis} m_{ci} *}$$

Equation 20-7

$$E = C_d F_c \frac{100}{\% CO_2}$$

Equation 23-6

$$R_{s} = \frac{A_{s} m_{i} *}{A_{i} * RRF_{s} m_{s}} \times 100\%$$

Equation 20-8

$$E = C_w F_c \frac{100}{\% CO_{2w}}$$

Equation 23-7

$$MDL = \frac{2.5 A_{ai} m_i^*}{A_{ci}^* RRF_i}$$

Method 23

Equation 23-1

Equation 23-2

$$RRF_{i} = \frac{1}{n} \sum_{j=1}^{n} \frac{A_{cij} \, m *_{ci}}{A *_{cij} \, m_{ci}} -$$

Equation 23-8

$$C_{Tr} = \sum_{i=1}^{n} C_i$$

Method 25

Equation 25-1

$$C_i = \frac{m_i * A_i}{A_i * RRF_i V_{mstd}}$$

$$\Delta P = 0.01 \frac{FP_b \theta}{V_t}$$

Equation 25-2

$$V_s = 0.3857 V \left[ \frac{P_t}{T_t} - \frac{P_{ti}}{T_{ti}} \right]$$

Equation 25-3

$$C_{t} = \left[ \frac{\frac{P_{tf}}{T_{tf}}}{\frac{P_{t}}{T_{t}} - \frac{P_{ti}}{T_{ti}}} \right] \left[ \frac{1}{r} \sum_{j=1}^{r} C_{tm_{j}} \right]$$

Equation 25-4

$$C_c = 0.3857 \frac{V_v P_f}{V_s T_f} \left[ \frac{1}{q} \sum_{k=1}^{q} C_{cm_k} \right]$$

Equation 25-5

$$C = C_t + C_c$$

Equation 25-6

$$m_c = 0.4993 C$$

Equation 25-7

Percent recovery=1.604 
$$\frac{M}{L} \frac{V_v}{P} \frac{P_t}{T_f} \frac{C_{cm}}{N}$$

Equation 25-8

$$RSD = \frac{100}{\overline{x}} \sqrt{\frac{\sum (x_i - \overline{x})^2}{n - 1}}$$

#### Method 25A

Equation 25A-1

$$C_c = K C_{meas}$$

#### Method 26

Equation 26-1

$$\mu g \frac{Cl^{-}}{ml} = g \text{ of } NaCl \times 10^{3} \times \frac{35.453}{58.44}$$

Equation 26-2

$$\mu g \frac{Br^{-}}{ml} = g \text{ of } NaBr \times 10^{3} \times \frac{79.904}{102.90}$$

Equation 26-3

$$\mu g \frac{F^-}{ml} = g \text{ of NaF } x 10^3 \text{ } x \frac{18.998}{41.99}$$

Equation 26-4

$$m_{HX} = K V_s (S_X^- - B_X^-)$$

Equation 26-5

$$m_{X2} = V_s \left( S_X^- - B_X^- \right)$$

Equation 26-6

$$C = K \frac{m_{HX,X2}}{V_{m(std)}}$$

#### Method 26A

Equation 26A-1

$$\mu g \frac{Cl^{-}}{ml} = g \text{ of NaCl } x \cdot 10^{3} \text{ } x \frac{35.453}{58.44}$$

Equation 26A-2

$$\mu g \frac{Br^{-}}{ml} = g \text{ of } NaBr \text{ x } 10^{3} \text{ x } \frac{79.904}{102.90}$$

Equation 26A-3

$$\mu g \frac{F^{-}}{ml} = g \text{ of } NaF \text{ x } 10^{3} \text{ x } \frac{18.998}{41.99}$$

Equation 26A-4

$$m_{HX} = K V_s \left( S_{X-} - B_{X-} \right)$$

Equation 26A-5

$$m_{X2} = V_s (S_{X-} - B_{X-})$$

Equation 26A-6

$$C = K \frac{m_{HX,X2}}{V_{m(std)}}$$

#### Method 29

Equation 29-1

$$M_{fh} = C_{a1} F_d V_{soln,1}$$

Equation 29-2

$$M_{bh} = C_{a2} F_a V_a -$$

Equation 29-3

$$M_t = (M_{fh} - M_{fhb}) + (M_{bh} - M_{bhb})$$

Equation 29-4

$$Hg_{fh} = \frac{Q_{fh}}{V_{f1B}} \left( V_{so \ln, 1} \right)$$

Equation 29-5

$$Hg_{bh2} = \frac{Q_{bh2}}{V_{f2B}} \left( V_{so \ln, 2} \right)$$

Equation 29-6

$$Hg_{bh3(A,B,C)} = \frac{Q_{bh3(A,B,C)}}{V_{f3(A,B,C)}} (V_{so \ln,3(A,B,C)})$$

Equation 29-7

$$Hg_{bh} = Hg_{bh2} + Hg_{bh3A} + Hg_{bh3B} + Hg_{bh3C}$$

Equation 29-8

$$Hg_t = (Hg_{fh} - Hg_{fhb}) + (Hg_{bh} - Hg_{bhb})$$

Equation 29-9

$$C_s = \frac{K_4 M_t}{V_{m(std)}}$$

Method 0010

$$m_{Cl2} = S \times V_2$$

$$\frac{Max\ POHC_{i}\ Mass}{DV_{eff(std)}} = Max\ POHC_{i}\ conc$$

$$C = K x \frac{m}{V_{m(std)}}$$

$$\frac{LDL_{POHC} \times 10}{POHC_{i \ conc}} = V_{TBC}$$

Method 0060

$$M_{fh} = C_{a1} F_d V_{soln,1}$$

 $C_{POHC}(\mu g/ml) x sample volume(ml)$ = amount( $\mu g$ ) of POHC in sample

$$M_{bh} = C_{a2} F_a V_a$$

Method 0030

 $C_g = \frac{Wt. \ of \ Analytes \ in \ Sample, \mu g (i.e. VOST \ tubes \ \& \ condensate)}{Volume \ of \ sample \ at \ s \ tan \ dard \ conditions}$ 

$$M_t = (M_{fh} - M_{fhb}) + (M_{bh} - M_{bhb})$$

Method 0050

Equation 0050-4

Method 0061

$$m_{HCl} = S \, x \, V_s \, x \, \frac{36.46}{35.45}$$

$$m\!=\!(S\!-\!B)\ x\ V_{ls}\ x\ d$$

Equation 0050-5

$$m_{Cl2} = S \times V_2$$

Equation 0050-6

$$C = K x \frac{m}{V_{m(std)}}$$

Method 0051

$$m_{HCI} = S \times V_s \times \frac{36.46}{35.45}$$

# Appendix B

## **Abbreviations and Terminology**

%CO	Percent CO by volume, dry basis
%CO2	Percent CO2 by volume, dry basis .
%N2	Percent N2 by volume, dry basis
% <u>.</u> O2	Percent O2 by volume, dry basis
0.280	Molecular weight of N2 or CO, divided by 100
0.320	Molecular weight of O2 divided by 100
0.440	Molecular weight of CO2 divided by 100
100	Conversion to percent.
13.6	Specific gravity of mercury.
18.0	Molecular weight of water, g/g mole (lb/lb mole).
3600	Conversion Factor, sec/hr.
60	Sec/min.
Α	Cross sectional area of stack, m2 (ft2).
Α	Absorbance of sample.
Α	Analytical detection limit, µg/ml.
A1	Absorbance of the 100µg NO2 standard.
A2	Absorbance of the 200µg NO2 standard.
A3	Absorbance of the 300µg NO2 standard.
A4	Absorbance of the 400µg NO2 standard.
An	Cross-sectional area of nozzle, m2 (ft2).
В	Liquid volume of digested sample prior to aliquotting for analysis, ml.
Bws	Water vapor in the gas stream [from Method 4 (reference method) or Method 5], proportion by volume.
С	Corrected to standard conditions, mg/dsm3(lb/dscf).
С	TGNMO concentration of the effluent, ppm C equivalent.
Ca	Acetone blank residue concentration, mg/mg.

Ca Actual concentration of SO2 in audit sample, mg/dscm. Ca Actual audit sample concentration, mg/dscm. Ca1 Concentration of metal in Analytical Fraction 1A as read from the standard curve, µg/ml. Ca<sub>2</sub> Concentration of metal in Analytical Fraction 2A as read from the standard curve, (µg/ml). Cc Calculated condensible organic (condensate trap) concentration of the effluent, ppm C equivalent. Ccm Measured concentration (NMO analyzer) for the condensate trap ICV, ppm CO2. Cd Determined concentration of SO2 in audit sample, mg/dscm. Cd Determined audit sample concentration, mg/dscm. CH2S Concentration of H2S at standard conditions,mg/dscm. Ср Pitot tube coefficient, dimensionless. Type S pitot tube coefficient, dimensionless. Cp(s) Cp(std) Standard pitot tube coefficient; use 0.99 if the coefficient is unknown and the tube is designed according to the criteria of Sections 6.7.1 to 6.7.5 of this method. CS Concentration of particulate matter in stack gas, dry basis, corrected to standard conditions, g/dscm (gr/dscf). Cs Concentration of a metal in the stack gas, mg/dscm. CSO<sub>2</sub> Concentration of SO2, dry basis, corrected to standard conditions, mg/dscm (lb/dscf). Ct Calculated noncondensible organic concentration (sample tank) of the effluent, ppm C equivalent. Ctm Measured concentration (NMO analyzer) for the sample tank, ppm NMO. D Diameter of stack, in. De Equivalent diameter. F Dilution factor. Required only if sample dilution was needed to reduce the absorbance into the range of the calibration). F Sampling flow rate, cc/min. Fa Aliquot factor, volume of Sample Fraction 2 divided by volume of Sample Fraction 2A (see Section 8.3.4.)

Fd	Dilution factor (Fd = the inverse of the fractional portion of the concentrated sample in the solution actually used in the instrument to produce the reading Ca1. For example, if a 2 mL aliquot of Analytical Fraction 1A is diluted to 10 mL to place it in the calibration range, Fd = 5).		
ΔН	Average pressure differential across the orifice meter, mr H20 (in. H20).		
Hgbh	Total mass of Hg collected in the back		
Hgbh2	Total mass of Hg collected in Sample Fraction 2, μg.		
Hgbh3(A,B,C)	Total mass of Hg collected separately in Fraction 3A, 3B, or 3C, $\mu g$ .		
Hgbhb	Blank correction value for mass of Hg detected in back		
Hgfh	Total mass of Hg collected in the front		
Hgfhb	Blank correction value for mass of Hg detected in front		
Hgt	Total mass of Hg collected in the sampling train, µg.		
1	Percent of isokinetic sampling.		
K	0.127 mm H20 (metric units); 0.005 in. H20 (English units).		
K4	103 mg/µg.		
Kc	Spectrophotometer calibration factor.		
Кр	Velocity equation constant.		
L	Length.		
L	Volume of liquid injected, μl.		
L1	Individual leakage rate observed during the leak-check conducted prior to the first component change, m3/min (ft3/min)		
La	pretest leak-check or for a leak-check following a component change; equal to 0.00057 m3/min (0.020 cfm) or 4 percent of the average sampling rate, whichever is less.		
LI	Individual leakage rate observed during the leak-check conducted prior to the "ith" component change (i = 1, 2, 3n), m3/min cfm).		
Lp	Leakage rate observed during the post-test leak-check, m3/min (cfm).		
m	Mass of NOx as NO2 in gas sample, μg.		
M	Molecular weight of the liquid injected, g/g mole.		
ma	Mass of residue of acetone after evaporation,mg.		

Mbh Total mass of each metal (except Hg) collected in the back Mbhb Blank correction value for mass of metal detected in back Мс TGNMO mass concentration of the effluent, mg C/dsm3. Md Dry molecular weight, g/g mole (lb/lb mole) Md Molecular weight of stack gas, dry basis (see Section 8.6), g/g mole (lb/lb mole). Mfh Total mass of each metal (except Hg) collected in the front half of the sampling train (Sample Fraction 1), µg. Mfhb Blank correction value for mass of metal detected in front Total amount of particulate matter collected, mg. mn Ms Molec Molecular weight of stack gas, wet basis, g/g mole (lb/lb mole). Total mass of each metal (separately stated for each Mt metal) collected in the sampling train, µg. Mw Molecular weight of water, 18.0 g/g-mole (18.0 lb/lb-mole). N Total number of traverse points. total number of traverse points. n Ν Normality of barium standard titrant, meg/ml. Ν Carbon number of the liquid compound injected (N = 12 for decane, N = 6 for hexane). NA Normality of standard C6H5AsO solution, g eq/liter. NI Normality of standard I2 solution, g eq/liter. NS Normality of standard (0.1 N) Na2S2O3 solution, g eq/liter. NT Normality of standard (0.01 N) Na2S2O3 solution, assumed to be 0.1 NS, g eq/liter. р Velocity head of stack gas, mm H20 (in. H20). Р Allowable pressure change, cm Hg. Pb Barometric pressure, cm Hg. Pbar Barometric pressure at measurement site, mm Hg (in. Hg). Pf Final pressure of the intermediate collection vessel, mm Hg absolute. Pg Stack static pressure, mm Hg (in. Hg).

pi	Individual velocity head reading at traverse point "i", mm (in.) H20.		
Pi	pitch angle at traverse point i, degree.		
PI	Initial absolute pressure of flask, mm Hg (in. Hg).		
Ps	Absolute stack pressure (Pbar + Pg), mm Hg (in. Hg),		
$\Delta$ ps	Velocity head measured by the Type S pitot tube, cm (in.) $\mbox{H20}.$		
Pstd	Standard absolute pressure, 760 mm Hg (29.92 in. Hg).		
$\Delta$ pstd	Velocity head measured by the standard pitot tube, cm (in.) H20.		
Pt	Gas sample tank pressure after sampling, but before pressurizing, mm Hg absolute.		
Ptf	Final gas sample tank pressure after pressurizing, mm Hg absolute.		
Pti	Gas sample tank pressure before sampling, mm Hg absolute.		
q	Total number of analyzer injections of intermediate collection vessel during analysis (where $k=$ injection number, $1\dots q$ ).		
Qbh2	Quantity of Hg, µg, TOTAL in the ALIQUOT of Analytical Fraction 2B selected for digestion and analysis . NOTE: For example, if a 10 mL aliquot of Analytical Fraction 2B is taken and digested and analyzed (according to Section 11.1.3 and its NOTES Nos. 1 and 2), then calculate and use the total amount of Hg in the 10 mL aliquot for Qbh2.		
Qbh3(A,B,C)	Quantity of Hg, $\mu$ g, TOTAL, separately, in the ALIQUOT of Analytical Fraction 3A, 3B, or 3C selected for digestion and analysis (see NOTES in Sections 12.7.1 and 12.7.2 describing the quantity "Q" and calculate similarly).		
Qfh	Quantity of Hg, $\mu g$ , TOTAL in the ALIQUOT of Analytical Fraction 1B selected for digestion and analysis . NOTE: For example, if a 10 mL aliquot of Analytical Fraction 1B is taken and digested and analyzed (according to Section 11.1.3 and its NOTES Nos. 1 and 2), then calculate and use the total amount of Hg in the 10 mL aliquot for Qfh.		
Qsd	Dry volumetric stack gas flow rate corrected to standard conditions, dscm/hr (dscf/hr).		
R	$ \label{eq:continuous}  \mbox{[(mm Hg)(m3)]/[(K)(g-mole)] }  \mbox{\{21.85 [(in. Hg)(ft3)]/[(R)(lb-mole)]\}.} $		
r	Total number of analyzer injections of sample tank during analysis (where $j = injection number, 1 r$ ).		
Ravg	average resultant angle, degree.		
RE	Relative error for QA audit samples, percent.		

Ri resultant angle at traverse point i, degree. Sd standard deviation, degree. Т Sensitivity factor for differential pressure gauges. Tf Final absolute temperature of flask, K (R). Tf Final temperature of intermediate collection vessel, K. Ti Initial absolute temperature of flask, K (R). Tm Absolute DGM temperature Stack temperature, C (F). Ts Ts(abs) Absolute stack temperature, K (R).=273 + Ts for metric units, =460 + Ts for English units. Tstd Standard absolute temperature, 293 K (528 R). Tt Sample tank temperature at completion of sampling, K. Ttf Sample tank temperature after pressurizing, K. Tti Sample tank temperature before sampling, K. Sample tank volume, m3. Va Volume of acetone blank, ml. Volume of sample aliquot titrated, ml. Va Va Volume of absorbing solution, 25 mL. VA Volume of C6H5AsO solution used for standardization, Va Total volume of digested sample solution (Analytical Fraction 2A), mL VAI Volume of standard C6H5AsO solution used for titration analysis, mL. Vaw Volume of acetone used in wash, ml. Vf Volume of flask and valve, ml. Vf1B Volume of aliquot of Analytical Fraction 1B analyzed, ml. NOTE: For example, if a 1 mL aliquot of Analytical Fraction 1B was diluted to 50 mL with 0.15 percent HNO3 as described in Section 11.1.3 to bring it into the proper analytical range, and then 1 mL of that 50 Vf2B Volume of Analytical Fraction 2B analyzed, ml. NOTE: For example, if 1 mL of Analytical Fraction 2B was diluted to 10 mL with 0.15 percent HNO3 as described in Section 11.1.3 to bring it into the proper analytical range, and then 5 mL of that 10 mL was analyzed, Vf2B would be 0.5 ml.

Vf3(A,B,C)	Volume, separately, of Analytical Fraction 3A, 3B, or 3C analyzed, mL (see previous notes in Sections 12.7.1 and 12.7.2, describing the quantity "V" and calculate similarly).
Vi	Volume of standard I2 solution used for standardization, ml.
VIT	Volume of standard I2 solution used for titration analysis, normally 50 ml.
Vlc	Total volume of liquid collected in impingers and silica gel (see Figure 5-6), ml.
Vm	Volume of gas sample as measured by dry gas meter, dcm (dcf).
Vm	Dry gas volume as measured by the DGM, dcm (dcf).
Vm	Volume of gas sample at meter conditions, liters.
Vm(std)	Volume of gas sample measured by the dry gas meter, corrected to standard conditions, dscm(dscf).
vs	Stack gas velocity, calculated by Method 2,
vs	Average stack gas velocity, m/sec (ft/sec).
Vs	Gas volume sampled, dsm3.
Vsc	Sample volume(dry basis), ml. at standard conditions
VSI	Volume of 0.1 N Na2S2O3 solution used for standardization, ml.
Vsoln	Total volume of solution in which the SO2 sample is contained, 100 ml.
Vsoln,1	Total volume of digested sample solution (Analytical Fraction 1), ml.
Vsoln,2	Total volume of Sample Fraction 2, ml.
Vsoln,3(A,B,C)	Total volume, separately, of Analytical Fraction 3A, 3B, or 3C, ml.
Vt	Volume of barium standard titrant used for the sample (average of replicate titration), ml.
VT	Volume of standard ( 0.01 N) Na2S2O3 solution used in standardizing iodine solution (see Section 10.2.1), ml.
Vt	Sample train volume, cc.
Vtb	Volume of barium standard titrant used for the blank, ml.
VTT	Volume of standard ( 0.01 N) Na2S2O3 solution used for titration analysis, ml.
Vv	Intermediate collection vessel volume, m3.

Vw(std)	Volume of gas,corrected to standard conditions, scm (scf).		
W	width.		
W	Weight of K2Cr2O7 used to standardize Na2s2O3 or C6H5AsO solutions, as applicable (see Sections 10.2.2 and 10.2.3), g.		
Wa	Weight of residue in acetone wash, mg.		
xi	Individual measurements.		
Υ	Dry gas meter calibration factor.		
Yi	yaw angle at traverse point i, degree.		

B-8

# STACK TESTING FOR HAZARDOUS AIR POLLUTANTS (HAPs)

## FIELD OBSERVATION CHECKLIST

## PRETEST CHECKLIST

## PRETEST MEETING CHECKLIST

Date	
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	beaution!/
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Phone	
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TOTAL TOTAL BUSINES	
Phone	e-mail
	-
DUSCESSES DESCRIPTION DE	7
H1 18 18 1 20 1 110 0 7	
	Phone Phone Phone Phone

# I. FACILITY OPERATION

A. Process

a. Process Des	scription		
b. Method of p	process weight rate or fuel feed	determination	
c. Process parar	meters (list below or use operat	ion data sheet for process)	
Process Parameters to be Monitored	Design/Normal Values	Acceptable Limits	
See operations data sheet for			
d. Acceptable va e. Normal operat	lues of raw material and/or fuelting cycle and its effect on test p		
- Common Devices			
a. Control Device	e(s)		
b. Operating Para	ameters (list below or use opera	ting data sheet for process)	
10 m			

Monitored	(98.)	The Market And Property of the Control of the Contr
IN OUR REAL PARTIES AND AND ADDRESS AND AD	E. Brimo ist i	1.30
		in the second state of
		Sales City Sales
		all provided to the con-
		an all para lines
		um st) ye isi
C. Incinerator Informa	erator: Liquid Injection	Fixed HearthFluidized Bed
Rotary Combi	astor	i de l'échale. L'échale de
b. Maximum Ra	ted Heat Input	Btu/hr
c. Maximum Ra	ted Air Flow	acfm
d. Dimensions o	f Combustion Chamber(s)	ACT 2 OHISE OF
e. Does Incinera f. Maximum St g. Air Pollution Venturi Scrub Cyclone	Control Devices: Quench Tober Carbon Bed Hydrosonic Jet	ter Ratelb/min or gal/min  TowerPre-cooler  Packed Tower  Ionizing
h. Fluid Bed M	edia	rpm
i Liquid Inject	tion Type (	of Atomizationrpm
k Feed Materia	al: Solid Liquid	GasOther
1 Maximum F	eed Rate: Btu/hr Gal/	/hrLb/hrton/hr
Food Dolivo	Ty: Manual Conveyor	Screw Pump

Acceptable Limits

Operating Parameters to be | Design/normal Values

n. Identify Feed	Streams:		
No. 1:	No. 2:	No. 3:	No. 4:

# II. TRIAL BURN PARAMETERS

Parameter	Item	Test Run #1	Test Run #2	Test Run #3
Feed Rate			Test Run #2	Test Run #3
Heat Content of Feed				
Auxiliary Fuel Rates	Gas Oil			
Feed Composition	Water, % Ash, %	-		
POHC (s), % or ppm				
Other Organics				
Sulfur Content, % or ppm				
Nitrogen Cont., % or ppm				
Phosphorus Cont., % or ppm				
Metals, % or ppm				
Liquid	Viscosity Specific Gravity			
Sludges	Moisture, %			
Gases	Density			

## III. INCINERATOR PARAMETERS

Parameter	Item	Test Run #1	Test Run #2	Test Run #3
Temperature	Primary Combustion Chamber			- 150 d. 126 d. 150 -
	Secondary Combustion Chamber		meg   Jack victoria   Jacksvictoria	
	Heat Recovery Device Inlet		mina yananahi I	alia woo a waa
	Heat Recovery Device Outlet		Table Cape I	
	Air Pollution Control Device Inlet		38 1 37×0	SHILL IN ST
	Air Pollution Control Device Outlet			
	Stack Gases			
Draft (in. Water)	Primary Combustion Chamber			
	Secondary Combustion Chamber			
	Heat Recovery Inlet			
	Heat Recovery Outlet			
-ESP	Unit Voltage, Kv			
	Unit Current, ma			

-Baghouse	Pressure Drop, inches		
	Air Flow Rate, acfm		
-Dry Scrubber	Lime Feed Rate, gpm		
	Air Flow Rate, acfm		••
Air Flow Rates	Primary, acfm		
	Secondary, acfm		
Stack Gas Monitoring			
	Oxygen, %		
	CO <sub>2</sub> , %		
	CO, ppm		

Parameter	Item	Test Run #1	Test Run #2	Test Run #3
	NO <sub>x</sub> , ppm			
	HC, ppm		III S 100 CE	
	Opacity, %			mp) Chesomizus
	SO <sub>2</sub> , ppm			
	Other, ppm/%			depart of the second second second second
Feed Sample Taken?	Feed No.			gargie depósit
	Feed No.			
feet)	Feed No.	Line Seer	1	calings in
Auxiliary Fuel Samples Taken?		The state of the s		State of Once of
Scrubber pH				
Type of Alkaline Added?			in in the second	onutinos Estados 
Rate of Addition, lb/hr			orns a fig	Les ReportingRe
Ash Removal Rate, lb/hr				
Automatic Feed Cutoffs	Low Tempertature, F			
	High CO, ppm			
	Low Oxygen, %			- Company

# IV. TESTING METHODOLOGY TO BE DISCUSSED

Sampling Location	
Sampling Points	
Cyclonic Flow Check	
Pollutant Measurement Methods	
Mandatory Calibrations Sheets to be Provided	(If not provided immediately prior to starting test
program, testing should be delayed until observ	ver receives them or authorization to proceed by
Task Manager)	

OrificeDry Gas Mete	er (Y)	Nozzle	Pitot 7	Tuhe
Fuel, Raw Material/produce Samplin	ng			
Emission Rate Calculation				
Destruction Removal Efficiency Cal	culation			
Minimum Sample Volume Calculati	on			•,
Sample Recovery Area				
Dry Molecular Weight/dilution Deter	rmination			
Integrated Bag	Grab Sa	mple	Or	sat
Safety Requirements				
			4	
T				
Test Schedule				
		-		
Dlant T				
Plant Tour				

## V. SAMPLING METHODLOLGIES TO BE USED

Pollutant Parameter	Methodology	Remarks, Additional Quality Assurance, and/or Modifications
		1
VI. GENERAL COMME	NTS	
Signature of Agency Repre	sentative Affiliation o	f Representative Date
Signature of Plant Represne	etative	Date

## STACK TESTING FOR HAZARDOUS AIR POLLUTANTS (HAPs)

# FIELD OBSERVATION CHECKLIST

# FEDERAL REFERENCE METHODS 1, 2, 3, 4, AND 5

## SOURCE INFORMATION

Facility	Location
Source	Sampling Location
Test Team	Team Leader
Test Date Interval: /	Team Leader
Observer	Affiliation
Sketch of sample location (if c	different from pretest report).
	mensions, location of distrubances and ports, X-section
showing sampling poin	nts.)
Stack or duct condition:	
	on: Brick ConcreteStainless Steel
	Other
	ible?
Leaks?	2004 - 2004 - 2004 - 2004 - 2004 - 2004 - 2004 - 2004 - 2004 - 2004 - 2004 - 2004 - 2004 - 2004 - 2004 - 2004
Internal corrosion?	in 1 de la constitución de la co
	ticulate matter in sampling port area?
	e test?
Visible water of	droplets in stack?
Particulate mat	tter appears acidic?
Insulation Thic	ckness Stack under negative or positive pressure?
-	\$4ET1955
Nipple:	Langth
ID_	Length Capped ide wall Corrosion evident
Port dimensions:	ide waiieoirosion evident
Dound diamet	Or .
Pactangular: I	er W
Fauivalent dia	nmeter
Facility for movemen	
Monorail	Skateboard and rail
Other	traffic a second of the of A
	No. of receptors
Distance to re-	centors
Ground fault	circuit protection? Adequate?
	nt to port
FEDERAL REFERENCE	
Stack diameter properly deter	rmined? Method used

[Note: If stack is between 4"-12" then Met	thod 1a must be employed	edl
Measured of	n cita?	-
Total distance from application (ilstiffnance (A)	I I and a second	ters(A)
axis uowii to the sten chart and from	m A Distance D.	
1 Total Samping Points		diffeet of points to
and points at sampling location.		
Circular: No.of Ports Rectangular: Grid configuration	Points/port	
Rectangular: Grid configuration	1	
No. of Ports Points  Points located centroid of area?	s/port	
	-	
First and last traverse points from ducts:		
24 in. Diameter: 1.0 inch from wall?  12-24 in. Diameter: > 0.5 inch from wall?  Method 1 calculated correctly?	Yes	No
12-24 in. Diameter: > 0.5 inch from wall?	Yes	No No
Points properly marked on pitot tube?  Port length/interior stack accounted for in calculation Cyclonic flow check verified (<20 degrees) and corrections.		
Full leligin/interior stack accounted for in colours.	. 0	
Cyclonic flow check verified (<20 degrees) and cor Average null point angle	npleted?	
Average null point angle  Describe velocity profile of sampling plane		
Describe velocity profile of sampling plane		
Drawnistan		
Draw picture of stack with port location and upstrea	am/downstream disturba	nces marked and
notated		
Damarka		
Remarks		
	1	
FEDERAL DEFEDENCE ACTION		
FEDERAL REFERENCE METHOD 2		
Equipment identifications 1		
Equipment identified matches pretest calibration list	?	
Pitot tube: Type S Standard		
Pitot tube coefficientC	Calibration date	
Design to EPA specifications?		
Properly attached to sampling probe, if applicable?	0	
Pitot tube, lines, and manometer assembled correctly Differential pressure gauge has correct sensitivity?	?	
Differential pressure gauge has correct sensitivity?		
Measurement gauge: Manometer Magn	ehelic Range	e(s)
Gauge proper sensitivity for delta p range bei	ng measures?	` /

Magnehelic gauges calibrated against manometer	? Date
Differential pressure gauge leveled and zeroed? _ Visual check of pitot tube heads-good condition and mee	t EPA design specification?
Visual check of pitot tube heads good condition and most	or incomendación vizgion.A
Pitot tube pretest leak check?	
Cyclonic flow checked prior to test series?	Elfrain Like
Static pressure measured during the test series?	
Orientation of pitot tube correct during traverse?	res mid vis (V
Sampling port adequately sealed around pitot tube?	COURT AND THE STATE OF THE STAT
	2 1 2 2 1 1 1
Stable readings taken at each traverse point?	
Barometric pressure recorded and adjusted for elevation	Hell total rate and thouse.
(Note: Barometric pressure must be adjusted minus 0.1 A	A per 100 ft elevation increase or visa
versa for elevation decrease. Elevation at which barome	tric pressure is measured compared
to elevation at the test platform.)	
Airport:Location	P <sub>b</sub> at airport
Sampling location elevation	Change in ft.
delta in. Hg +/(0.10 ir	n. Hg/100 ft)
Stack temperature measured?	Esta rottog Sunctions i state
Stack gas moisture content determined?	
Orsat samples taken? If not, exp	plain why
Posttest leak check performed?	Leak rate results
Data recorded properly Calculate	tions correct?
Remarks	allegal to larve
(A.) 1000. [ 123.100V 145.157V	THE PROPERTY OF THE PARTY OF TH
TOTAL CONTROL SEED WAS REGIONARY CONTROL OF THE SERVICE OF THE SER	And State Children Co.
4500 BY 1-013 B	SICE ISBUILDER
FEDERAL REFERENCE METHOD 3	
Method used to acquire gas sample	
Single point grab Single point integrated	Multi-point integrated
Type of bag Type of probe Diaphrage	and the second s
Pump: One way squeeze bulb Diaphraga	m Other
Instrument used to determine concentration? Orsat	FyriteCEIVI
Is a filter used to remove particulate matter?	J. 59536.35345 1.1542 607 605 607 607
Sample train leak checked?	SCATE AND
Sample train purged with stack gas prior to collecting the	ne sample?
Sampling port properly sealed? Sampling rat	e constant?
What rate?	
Orsat performed in triplicate?	nalysis consistent?
All readings averaged and reported to nearest 0.1%?	Transfit 23 to still
Owest	
Reagents at the proper level?A	analyzer level?

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Re	agents fresh?	Da	te charged to orsat?	
An	alyzer leak checked	?	Analyzed within	8 hours?
Sai	mple line purged?		Complete about	tion of cocce?
An	larysis repeated until	l following analys	is criteria met?	non or gases!
	CO <sub>2</sub> -any three a	analyses differ by	The state of the s	
	A) = 0</th <th><math>0.3 \%</math> when <math>CO_2</math></th> <th>&gt;/= 4.0 %</th> <th></th>	$0.3 \%$ when $CO_2$	>/= 4.0 %	
	B) $ ($	$0.2 \%$ when $CO_2 <$	4.0 %	
	O <sub>2</sub> - any three ar	nalyses differ by		
	A) $ ($	$0.3$ % when $O_2 > 1$	= 15 0 %	
	B) = (</th <th><math>0.2 \%</math> when <math>O_2 &lt;</math></th> <th>15 %</th> <th></th>	$0.2 \%$ when $O_2 <$	15 %	
Method 3A	A for $O_2/CO_2$ :	70 111011 02	15 /0	* **
Sys	stem leak checked di	uring test day?		
Неа	ated sample lines us	ed prior to sample	e conditioner?	
Mo	isture visible in sam		conditioner?	
San	nple system flow rat	es within 10 %	f calibration gas flow ra	
A11	calibration gases me	easured balow 45	calloration gas flow r	ates?
Dat	a recording perform	ed by strip obort	span value of the anal	yzer?
Fue	1	E Dan	digital, manual or othe	r?
Cal	culate $F \cdot F = (20)$	$\Gamma_0$ Kan	ge	
	$\frac{1}{2}$	$0.9 - \%0_2 / \%0_0$	)=	
		E	F 5	
	Anthrocita/Time	Expected	Fo Range:	
		ite 1.015-1.130		1.600-1.836
		1.083-1.230		1.000-1.120
	Distillate Oil	1.260-1.413	Municipal Gargage	1.043-1.177
Remarks		1.210-1.370	Other	
ICHIIAIKS _				
		,		
THORD IX				
FEDERAL	REFERENCE MI	ETHOD 4		
3.6.4.1				
Method used	d to acquire moistur	e concentration in	odWet bul	
Impinger me	ethodPar	tial pressure meth	od Wet bul	h/dry Rulh
		her?	wet bul	ordry Build
Estimate of	moisture:			
Method cond	ducted in conjunctio	on with pollutant e	emission test?	
Preliminary	run: Conducted	Political (	Estimated	
Impinger me	ethod:		Delimited	
		d2		
Imni	ngers properly place	2-1	3rd 4th	
шіні	ager contents. Ist	2nd	3rd 4th	5th

Modifications?	1000	
Carling gystom: Crushed ice?	Oth	er
Campling time nor point	Number of no	nnis
Probe heater on? Crushed ice in ice bath around imp	Temperature	Stable
Crushed ice in ice bath around imp	oingers?	
Destart looks shock conducted?		eak rate
Sampling rate constant	Isokine	tic?
All data recorded properly?		
Post leak check conducted?	Leakage	rate?
Recovery-Impinger Contents  Method: Volumetric?		
Method: Volumetric?	Gravime	etric?
Trip balance calibrated (gra Measurement of silica gel:	avimetric)?	0.1
Measurement of silica gel:	Balance?	Other
Color of silica gel?	Condition	1?
Color of silica gel?(Note: Blue-good; ]	pink-spent (unable to ab	sorb water)
All analytical data recorded	d properly?	
All readings averaged and reported to nea	rest 0.1 %?	1 -110
Moisture value consistent with historical	process values and quick	c-cneck value?
Remarks		
d. Company of the com		V-012 A SAN SAN SAN SAN SAN SAN SAN SAN SAN S
	2.00 MSE 5.00	
FEDERAL REFERENCE METHOD S	5	
- : . : 1 .: C - 1tala as must get coll	ibration list?	
Equipment identified matches pretest cal	IDIATION NSt:	regarden sg (M
Appratus:		
NOZZI E		
NOZZLE  Probe nozzle: Stainless steel	Glass	Other
Probe design: Button-hook	Flhow	Streight tube
Probe design: Button-nook Cal	culated Measu	ared three times
Nozzle size: Car	Rent opening	ilod tilloo tillioo
Nozzle condition: Nicks	bein opening	1. 092 15
TO CORE TO CORE I WHEN		
PROBE/PROBE LINER	011	ort7
Probe material: Borosilicate	Incompl	Other
Stainless steel	inconei	Other
Heating system:	1 emperat	uic
Water cooled?	Length	
PITOT TUBE		Others
Type: Type S St	tandard	Other

Properly attached to probe?				
wicels EFA guidelines for affa	10chment to probe?	3.7	ec	No
1.10411104110113				
Modifications Pitot tube coefficient				
FILTER HOLDER				
Construction: Borosilicate	Ouarta		0.1	
Construction: Borosilicate Frit construction: Glass frit? Filter support	Quartz	- C - C - C	$\_$ Other $\_$	
Filter support	Siliaana	ellon frit?		
Other Cyclone and flask used (option	nal):			·
FILTER HEATING SYSTE				
Description	171			
Description Temperature				
Temperature Gas temperature at exit of box				
Gas temperature at exit of box				
Number of impingers?			~ .	
CONDENSER  Number of impingers?  Impinger contents: 1st  4th  Cooling system?	2-1		Clean? _	
4th 5	ZIIQ	(.1	3rd	
Cooling system?		_6th		7th
Cooling system?Proper connections?				
Proper connections?  Modifications?				
Modifications?				
METER BOX ASSEMBLY				
Manufacturer	Model No			
Manufacturer	Model No.		_ Unit No.	
Delta H@ value	Date			
Condition of compliance:	Date _			
Meter box leveled?	Cime and a second			
Manometer leveled?	imer/temperature r	eadouts op	erational?	
Manometer leveled? Thermocouples calibrated?				
Thermocouples calibrated?				
Operation				
	poorded on Cally			
Filter properly numbered and re	colued on Held test	data sheet	?	
Filter checked visually for irreg	ularities?			
Filter media type?  Sampling site selected?  Stack velocity head?  Nozzle size properly selected?				
Stack velocity hand?	C: 1 1	Stack temp	perature _	
Nozzla siza proportional de la	Stack dry molec	ular weight	calculated	1?
Nozzle size properly selected? Calibration data certified availal				
Pitot tubes	Meter box Y	factor		
Probe nozzle				

authorization to proceed	me	Task Manager _	1 2 - 2 - 2
Selection of sampling points a	and time according	to methodology	!
Number of sample poi	ints	Sample time	e/point
Minimum sample volu			
Minimum run time rec	-	(30 7): 1	
Total sample time acti	ual?	77	Clear and the A.C.
Sampling train assembled pro	perly?	The state of the s	10
Filter properly centered?	Impinge	ers properly char	ged?
Number of impingers required	d?	Which Fl	KM?
Volume in each impinger: 1st	t2nd	3rd	4th
5th6th_	7th_		8th
Drying medium: Silica gel?		_Drierite	
Weight			
Pitot tube lines checked for p	lugging or leaks?	**	11.0
Stopcock grease used: Acetor	ne-insoluble?	Hea	at-stable?
Meter box leveled?	Manometers I	eveled?	
Probe heat uniform along len			
Dry gas meter field observati	on check:		
	11.0		ton for 10 minutes at
A. Operating Meter I	Box Assembly Oper	rate metering sy	stem for 10 minutes at
the state of the s	Record the volume	metered, DGM	temperature and
barometric pressu	ire.		
	o3 m	0r. p	in Ha
Final: DGM reading Initial: DGM reading Net: V <sub>m</sub> =	gft <sup>3</sup> Temp_	F P <sub>b</sub>	in Ha
Initial: DGM reading	tt Temp	T Pb	III. rig
Net: $V_m = $	ft' Avg. T <sub>n</sub>	=	+ 460 =
	$319 (T_m = 460)/P_b$		
$Y_c = 0.97 Y =$	1.03 Y =	1.27	
			T1-0
Criteria: 0.97 Y	< Y <sub>c</sub> $<$ 1.03 Y; Syste	em meets?	Exceeds?
		23 2	T . D .
B. Utilizing EPA's I	Method 5 Dry Gas I	Meter Performar	ice Test Device
a. Remove th	ne performance test	device from its	case and insert it into

- a. Remove the performance test device from its case and insert it into the gas inlet quick-connect coupling on the source sampling meter box.
- b. Turn the power to the meter box on and start the pump.
- c. Completely open the coarse flow rate control valve and close the fine flow rate control valve to give a maximum vacuum reading.
- d. Allow the orifice and source sampling meter obox to warm up for 45 minutes with flow controls adjusted as described in step c before starting quality assurance runs.

e. Make triplicate quality assurance runs. For each run, record initial and final dry gas meter volume, dry gas meter inlet and outlet temperatures, internal orifice pressure drop (Delta H), ambient temperature, and barometric pressure. Each run duration should be greater than 15 minutes. As the needle reaches the zero (12 o'clock) position, pump and stopwatch are stopped simultaneously. The dry gas volume and time are recorded.

QA Table For Evaluating DGM Orifice Value

Item	Run 1	Run 2	Run 3
DGM, final		,	
DGM, initial			
DGM, net			
DGM, T inlet (°F)			
DGM, T outlet (°F)			
DGM, T avg (°F)			
Ambient Temp. (°F)			
Pb (in. Hg)			
Orifice meter, Delta H			

f. Calculate the corrected dry gas volume for each run using the following equation:

$$Y_c = 10/V_m [ 0.0319 (T_m = 460)/P_b ]^2 =$$
 $Y_c = 0.97 Y = 1.03 Y =$ 
Criteria: 0.97 Y < Y<sub>c</sub> < 1.03 Y; System meets? \_\_\_\_\_ Exceeds? \_\_\_\_\_
Nomograph/calculator check:

a. Nomograph:

If Delta H@ = 1.80, T(meter) = 100 F, % moisture = 10 %, Ps/Pm = 1.00, calculate C.

$$C =$$
\_\_\_\_\_(0.95)

If C = 0.95,  $T_s = 200$  F,  $D_n = 0.375$ , Delta p reference = \_\_\_\_\_ (0.118)

	Delta $H = 10$ ; and lock nomograph. Set $p = 0.01$ . (0.01)
Read Delta H	
Nomograph O.K.?	Rock Harts (Marine Hole
b. Calculator:	
Calculate Delta H/	delta p using the following equation:
Delta H/Delta $p = \{846$	.72 $D_n^4$ [Delta H@] $Cp^2 (1-B_{ws})^2 (M_d T_m P_s/M_s T_s P_m)$ }
= Termer du colla	er Jach Alishmaqqalib. Judq obe birade.
	LEAT OF THE WAS A CONTROL OF THE CON
· · · = ·	agnigitada piratro de a etaluarriar yara
Parameters for cal	culator check:
	Percent Isotanoies cate dated at acid per
Item DimensionsGivenC	Calculated and a state of the s
A. Orifice meter coefficient, Delta H@ i	n. Water1.80
B. Pitot tube coefficient, Cp dimensionle	ess 0.84
C. Abs. stack pressure, $P_s = P_b + P_{st}$ in. H	g 29.96
D. Abs. meter pressure, P <sub>m</sub> +/- P <sub>b</sub> in. Hg	29.92
F Ahs meter temperature, $T_m = t_m + 460$	degrees K 560
F. Abs. stack temperature, $T_s = t_s + 460$	degrees R 760
G. Divillolocular working in war in	
H. Moisture content, B <sub>ws</sub> + % water/100	dimensionless 0.10
I. Exact nozzle diameter, D <sub>n</sub> in.0.375	abetre, cettato e relicio en 1882 Nova Popo
J. Average velocity head, Delta p in. Wa	ater 0.1
K K factor = Delta H/Delta p 13.24 (	
L. Delta H calculated for delta $p = 0.1$ in	n. Water 1.324 ()
Calculator equation set-up O.K.?	registral approval to the record of the second
None and healey later geture	
Nomograph /calculator setup:	
A. Delta H@ =	of payagetic to the section to the section of
B. $C_p = $	THE MILLIES OF THE STATE OF THE
$C. P_s = $	Proposition of
D. $P_m = $	
E. T <sub>m</sub> =	
$F. T_s = \underbrace{\text{Note that } T_s = \text{Note th$	TOTAL CONTRACTOR STATE OF THE S
$G. M_d = $	1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1
I. C Factor =	:
J. D <sub>n</sub> desired =	in. Actual in.

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MOHIOPIADH SPI HR I I K	7.0		
Coloulator act O. K	C.?		e e
Calculator set up O.K.			
Care taken to avoid scr	rapping nipple or stace	ck wall?	
Effective scal made and	Juliu Di Obe when in-	STACKY	
Trotost reak check peri	ormeu:		
Probe moved at proper	time?		٠.
Pitot tube/probe marking	ng correct for correct	t sampling points?	
Tiozzie and pitot tube t	Jaianel IO Stack Wall	at all times?	
I mer changed duling i	uii:		
Any particulate loss du	ring changing?		
Leak check before char	nging components du	iring run?	
Data birects completed,	in nik, and data prof	periv recorded?	
Percent isokinetics calc	culated at each point?	?Within	90-110 %?
Perform % isokinetic ra	ate check:		
Post-test leak check per Leakage rate  If data sheets cannot be velocity delta p, average	copied, record appro e stack delta H, appro	n. Hg oximate stack temp oximate stack gas r	erature, average sta
Gas density determinati	on: Temp, sensor tyr	ne Dra	CCUPA COULCA
Gas density determinating Temperature sensor atta	on: Temp, sensor tyr	ne Dra	CCUPA COURS
Gas density determination Temperature sensor attantovery:	on: Temp. sensor typached to probe?	oe Pre Other	CCUPA COURS
Gas density determination Temperature sensor attantovery:  Construction of probe reconstruction of pro	on: Temp. sensor typached to probe?ecovery brushes: Nyl	oe Pre Other	Ssure gauge
Gas density determination Temperature sensor attantovery:  Construction of probe rewards bottle: Clean?  Storage containers: Born	on: Temp. sensor typached to probe?ecovery brushes: Nyl	Other	Other
Gas density determination Temperature sensor attantourers:  Construction of proberowash bottle: Clean?  Storage containers: Borowash free?  Petri-dishes: Glass?	on: Temp. sensor typeched to probe?ecovery brushes: Nylosilicate glass?	oe Pre Other Other	Other
Gas density determination Temperature sensor attantovery:  Construction of probe rewards bottle: Clean?  Storage containers: Bore Leak free?  Petri-dishes: Glass?  Graduated cylinder/or be	on: Temp. sensor typeched to probe?ecovery brushes: Nylosilicate glass?Polyethylene_alance: Subdivisions	Other	Other Clean?
Gas density determination Temperature sensor attantovery:  Construction of probe rewash bottle: Clean?  Storage containers: Bore Leak free?  Petri-dishes: Glass?  Graduated cylinder/or be Balance type?	on: Temp. sensor typeched to probe?ecovery brushes: Nylosilicate glass?Polyethylene_alance: Subdivisions	Other Other Other Other  Other  Alibrated?	Other Clean? Clean? Other
Gas density determination Temperature sensor attantovery:  Construction of probe rewards bottle: Clean?  Storage containers: Bore Leak free?  Petri-dishes: Glass?  Graduated cylinder/or be Balance type?  Plastic storage container	con: Temp. sensor typeched to probe?ecovery brushes: Nylosilicate glass?Polyethylene_alance: SubdivisionsCrs: Air-tight?	Other Other Other Other  Other  Alibrated?	Other Clean? Clean? Other
Gas density determination Temperature sensor attantovery:  Construction of probe rewash bottle: Clean?  Storage containers: Bore Leak free?  Petri-dishes: Glass?  Graduated cylinder/or be Balance type?  Plastic storage container Probe allowed to cool su	con: Temp. sensor typeched to probe?ecovery brushes: Nylosilicate glass?Polyethylene_alance: SubdivisionsCrs: Air-tight?	Other Other Other Other  Other  Clean Other = 2 mL? alibrated? Clean?</td <td>Other Clean? Clean? Other</td>	Other Clean? Clean? Other
Gas density determination Temperature sensor attantovery:  Construction of probe rewards bottle: Clean?  Storage containers: Bore Leak free?  Petri-dishes: Glass?  Graduated cylinder/or be Balance type?  Plastic storage containers  Probe allowed to cool su (Note: Cap place)	ecovery brushes: Nylosilicate glass?  Polyethylene alance: Subdivisions  Crs: Air-tight?  add over nozzle tip to alance to the control of the	Other Other Other Other  Other  Clean Other  Clean Other  Clean?	Other Clean? Other
Gas density determination Temperature sensor attantovery:  Construction of probe rewash bottle: Clean?  Storage containers: Bore Leak free?  Petri-dishes: Glass?  Graduated cylinder/or be Balance type?  Plastic storage container Probe allowed to cool su	ecovery brushes: Nylosilicate glass?  Polyethylene alance: Subdivisions  Crs: Air-tight?  Ifficiently?  ed over nozzle tip to pisassembly, are all or	Other Other Other Other Other Other Clean Other Clean? Other Clean?	Other Clean? Other iclate matter?)

Clean-up area clean and protected from wi	nd?
Filter handling: Tweezers used?	Material of construction?
Surgical gloves worn?	Other
Water: Distilled?	
Stoncock grease: Acetone-insoluble?	Heat-stable Silicone?
Probe handling: Acetone rinse?	Distilled water rinse?
Particulate recovery: Probe nozzle?	Probe fitting?
Probe liner? Front hal	f of filter holder?
Blanks: Acetone D	istilled water
Acetone reagent < .001 % residue?	
Glass bottles residue <.001 %?	
Acteone blanks residue <.001 %	
Any visible particles on filter holder inside	e probe?
Color of silica gel?	Condition?
Method of silica gel transfer?	
Jars sealed tightly?	Liquid level marked on jars?
Jars locked up and chain-of-custod	ly completed?
All data forms signed and chain-of-custod	y completed?
Remarks	

## Container No. 6 (0.1 M nitric acid blank):

Equal volume placed in Container No. 6 used to rinse sample train?

(Note: Need only if total chromium is being measured and on	nly
one blank per field test.)	
Fluid level properly marked?	
All jars adequately labeled?	
Jars sealed tightly?Liquid level marked on jars?	
Jars locked up and chain-of-custody completed?	
Tetlon tape used to secure seal of jars?	
All data forms signed and chain-of-custody completed?	
Gas sample volume corrected to standard temperature and pressure?	
Remarks:	
Distribution 10 1 - 1-10 1	

f. Calculate the corrected dry gas volume for each run using the following equation:
$Y_c = 10/V_m [0.0319 (T_m = 460)/P_b]^2 =$
$Y_c = $ $0.97 Y = $
0.97  Y =
1.03  Y =
Criteria: 0.97 Y < Y <sub>c</sub> < 1.03 Y; System meets? Exceeds? Nomograph/calculator check:
a. Nomograph:
If Delta H@ = 1.80, $T(meter) = 100 F$ , % moisture = 10 %, $Ps/Pm = 1.00$ , calculate C.
C = (0.95)
If $C = 0.95$ , $T_s = 200 \text{ F}$ , $D_n = 0.375$ , Delta p reference =(0.118)
Align: Delta p = 1.0 with Delta H = 10; and lock nomograph. Set p = 0.01.  Read Delta H(0.01)  Nomograph O.K.?
b. Calculator:
Calculate Delta H/delta p using the following equation:
Delta H/Delta p = $\{846.72 \ D_n^4 [Delta H@] \ Cp^2 \ (1-B_{ws})^2 (M_d T_m P_s/M_s T_s P_m) \}$
=
=
Parameters for calculator check:
Item Dimensions Given Calculated
A. Orifice meter coefficient, Delta H@ in. Water 1.80
C. Abs. stack pressure, $P_s = P_b + P_{st}$ in. Hg 29.96
D. Abs. meter pressure, $P_m + /- P_b$ in. Hg 29.92
E. Abs. meter temperature, $T_m = t_m + 460$ degrees R 560
F. Abs. stack temperature, $T_s = t_s + 460$ degrees R 760
G. Dry molecular weight, M <sub>wd</sub> lb/lb-mole 30 H. Moisture content, B <sub>ws</sub> + % water/100 dimensionless 0.10
I. Exact nozzle diameter, D <sub>n</sub> in 0.375

Criteria: 0.97 Y < Y <sub>c</sub> < 1.03 Y; System meets?	Exceeds	
D. Hilliaina FDA2 36 d. 1.55		

# B. Utilizing EPA's Method 5 Dry Gas Meter Performance Test Device

- a. Remove the performance test device from its case and insert it into the gas inlet quick-connect coupling on the source sampling meter box.
- b. Turn the power to the meter box on and start the pump.
- c. Completely open the coarse flow rate control valve and close the fine flow rate control valve to give a maximum vacuum reading.
- d. Allow the orifice and source sampling meter box to warm up for 45 minutes with flow controls adjusted as described in step c before starting quality assurance runs.
- e. Make triplicate quality assurance runs. For each run, record initial and final dry gas meter volume, dry gas meter inlet and outlet temperatures, internal orifice pressure drop (Delta H), ambient temperature, and barometric pressure. Each run duration should be greater than 15 minutes. As the neddle reaches the zero (12 o'clock) position, the pump and stopwatch are stopped simultaneously. The dry gas meter volume and time are recorded.

QA Table For Evaluating DGM Orifice Value

Item	Run 1	Run 2	Run 3
DGM, final	ASTRUCTOR OF CHISTOPHEN	artustr o oldast and	
DGM, initial		1900	CHITTE OF W.
DGM, net	CHROMICH EVILLE	NORTH AND ALERCA	1
DGM, T inlet (°F)		3.3.3.333 Vac	
DGM, T outlet (°F)	Erican In the San Anna	Casa Hange and Casa	BITTER SECTION S
DGM, T avg (°F)		- Lucius Stage - Fra	bushin seCore
Ambient Temp.:(°F)			State Special
Pb (in. Hg)			1110000
Orifice meter, Delta H	r		

### STACK TESTING FOR HAZARDOUS AIR POLLUTANTS (HAPs)

#### FIELD OBSERVATION CHECKLIST

#### **SW-846, METHOD 0061**

# DETERMINATION OF HEXAVALENT CHROMIUM EMISSIONS FROM STATIONARY SOURCES

SOURCE INFORM	ATION	••
Facility	Lo	ocation
Source	Sar	mpling
Location		
Test Team	Team Le	ader
Test Date Interval:	/ /to	eader
Observer	Affiliati	ion
PRETEST MEETIN	G CHECKLIST	
Please reference Pret	est Checklist.	
FEDERAL REFER	ENCE METHODS 1 TH	ROUGH 5
Please reference Fede	eral Reference Methods 1 t	hrough 5 Checklist
SW-846, METHOD	0061	
DETERMINATION FROM STATIONA		HROMIUM EMISSIONS
	111 - 11	1'-49
Equipment identified	matches pretest calibration	on list?pinger reagent is continuously recirculated t
Train Design: Recirc	ulating train where the imp	Pump/Sprayer design?
the nozzie. Aspirator	design:	i unip/opiayer design:
Apparatus:		
NOZZLE		
Probe nozzle	: Glass/Teflon (Required)_	Other
Probe design	: Button-hook	Other Other
Nozzle size:	Calculated	dMeasured three times
Nozzle cond	tion: Nicks/Chips	
PROBE/PR	OBE LINER	
Probe mater	al: Glass/Teflon (Required	1)

300 mL of 0.1 M nitric acid used in sample recovery placed in
Container 8A?
Fluid level properly marked?
(Note: Need only one blank per field test.)
Container No. 8B (Reagent water blank):
100 mL of reagent water blank placed in Container 8B?
Fluid level properly marked?
(Note: Need only one blank per field test).
Container No. 9 (Nitric acid impinger reagent blank):
200 mL of nitric acid impinger reagent placed in Container 9?
Fluid level properly marked?
(Note: Need only one blank per field test).
Container No. 10 (Permanganate reagent blank):
100 mL of permanganate impinger reagent placed in Container 10?
Fluid level properly marked?
(Note: Need only one blank per field test).
Container No. 11 (8M HCl blank):
200 mL of reagent water placed in Container No. 11?
25 mL of 8 M HCl placed in Container No. 11?
Fluid level properly marked?
(Note: Need only one blank per field test).
Container No. 12 (Filter blank):
Unused filter from same lot of field filter placed in Container No. 12?
Petri dish sealed?
All jars adequately labeled?
Jars sealed tightly?
Liquid level marked on jars?
Jars locked up and chain-of-custody completed?
Teflon tape used to secure seal of jars?
All data forms signed and chain-of-custody completed?
Gas sample volume corrected to standard temperature and pressure?
Remarks

Container No. 2 (Probe rins	e/acetone):
Acetone rinse?	Distilled water rings?
Probe nozzle?	Probe fitting?
Probe liner?	Probe fitting?  Front half of filter holder?
I fuld levels properly	/ marked?
Container No. 3 (Probe rins	e/ 100 mL nitric acid)
Exactly 100 mL of n	itric acid used?
Probe nozzle?	Probe fittings?  Front half of filter holder?
Probe liner?	Front half of filter holder?
rulu levels properly	marked?
Ally visible particles	or permanganate solution (brown color) on filter
noticel of inside prob	e?
Container No. 4 (Impingers	1 through 3):
Liquids measured vo	lumetrically to within 0.5 mJ 2
Liquids in one or sev	eral containers?
Impingers, back half	of filter housing connecting glasswore rings.
williexactly 100 mL	of 0.1 M nitric acid?
ridid levels properly	marked?
Container No. 5A (Normally	empty impinger 4):
Liquid measured volu	imetrically to within 0.5 ml 2
impinger rinsed with	exactly 100 mL of 0.1 M nitric acid?
riuld levels properly	marked'/
Container No. 3B (Impingers	5 and 6 containing permanganate solutions).
Permanganate solutio	n color?
Spelli (Complete blea	ching of purple color)?
Liquid measured volu	metrically to with 0.5 mL?
unpingers rinsed with	treshly prepared 100 ml permanagenete and 2
mibnigers tillsed with	100 mL reagent water?
raid levels properly i	narked?
(Note: Bottles sho	uld not be filled completely to allow venting.)
Contained No. 3C (Rinsing of	impingers 5 and 6 with 8 M HCD.
200 mL reagent water	added to Container No. 5C?
Exactly 50 mL of 8 M	HCl used to rinse impingers 5 and 6?
Fluid level properly m	arked?
Color of Col	containing silica gel):
Color of recovered sili	ca gel?
Method of silica gel tra	ansferred?
Container was all 1.1	nearest 0.5 g'?
container property lab	cred/seared?
Container No. 7 (Acetone blar	1K):
100 mL placed in Cont	
Fluid level properly ma	arked?
(Note: If partici	ulate matter is not being determined, then an
action lank is r	not necessary.)
Container No. 8A (0.1 M nitrio	Cacid blank):

Care taken to avoid scrapping nipple or stack wall?	_
Effective seal made around probe when in-stack?	
Pretest leak check performed?	_
	_
Probe moved at proper time?Pitot tube/probe marking correct for correct sampling points?	_
Nozzle and pitot tube parallel to stack wall at all times?	_
Filter changed during run?	_
Any particulate loss during changing?	_
Filter changed during run?  Any particulate loss during changing?  Leak check before changing components during run?	
Data sheets completed, in ink, and data properly recorded?	
Percent isokinetics calculated at each point?Within 90-110 %?	_
Perform % isokinetic rate check:	
Delta H/Delta p = $\{846.72 D_n^4 [Delta H@] Cp^2 (1-B_{ws})^2 (M_d T_m P_s/M_s T_s P_m)\} =$	
K-factor changed during run?	
New K-factor	_
Velocity pressures and orifice pressure readings recorded accurately?	
Post-test leak check performed?(Mandatory)	_
Leakage rate@ in. Hg	
If data sheets cannot be copied, record approximate stack temperature, average stack	
velocity delta p, average stack delta H, approximate stack gas moisture, approximate	
dry stack gas molecular weight, nozzle diameter, pitot tube coefficient. Gas density	
determination: Temp. sensor type Pressure gauge	_
Temperature sensor attached to probe?Other	
Recovery:	
Construction of probe recovery brushes: NylonCleanOther	-
Wash bottle: Clean/glass?	
Storage containers: Borosilicate glass?OtherClean?	
Leak free?Teflon-lined caps?Petri-dishes: Glass?PolyethyleneOtherClean?	_
Petri-dishes: Glass? Polyethylene Other Clean?	
Graduated cylinder/or balance: Subdivisions = 2 mL?Other</td <td></td>	
Balance type?Calibrated?Plastic storage containers: Air-tight?Clean?	
Probe allowed to cool sufficiently?	—,
(Note: Cap placed over nozzle tip to prevent loss of particulate matter?(	
During sampling train disassembly, are all openings capped?	
Clean-up area: Description	
Clean-up area clean and protected from wind?	_
Sample recovery:	
Container No. 1 (Filter):	
Filter handling: Polypropylene tweezers used?	
Surgical gloves worn?Other	
Any particulate matter spilled?	

# Calculate Delta H/delta p using the following equation:

Delta H/Delta $p = {$	(846.72 D <sub>n</sub> <sup>4</sup> [Delta H@] C	$p^2 (1-B_{ws})^2 (M_d T_m P_s/M_s T_s P_m)$
=		,
		( Of the agilities .
=		Anglocal -
Parameters for	calculator check:	Asheral Arthur
A. Orifice meter coefficient, Delta H	(a) in Water 1 90	
D. Filol libe coefficient (in dimension	mlecc 0 81	
		1 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7
, - III . , I B III. I	115 27.72	
E. Abs. meter temperature, $T_m = t_m + t_m$	460 degrees R 560	
1. Aus. stack temperature, $I_s = t_s + 4$	60 degrees R 760	्रिक्तिय राज्यस्य व्यवसार
G. Dry molecular weight, M <sub>wd</sub> lb/lb-m	10le 30	
H. Moisture content, B <sub>ws</sub> + % water/10 I. Exact nozzle diameter, D <sub>s</sub> in 0.375	ou dimensionless 0.10 _	
I. Exact nozzle diameter, D <sub>n</sub> in. 0.375 J. Average velocity head, Delta p in. K. K factor = Delta H/Delta p 13.24(	Water 0.1	and the second s
L. Delta H calculated for delta $p = 0.1$	l in. Water 1.324(	
		· 3/4 2
Calculator equation set-up O.K	C.?	
	Barrell Porte	in cafeotek (* )
Nomograph /calculator setup:		
A. Delta H@ =		
B. C <sub>p</sub> =		
C. P <sub>s</sub> =	- nosy	mick s
D. P <sub>m</sub> =		
L. Im	Later of a Control	- FR - 17
$\Gamma \cdot \Gamma_{S} = \underline{\hspace{1cm}}$		
G. $M_d =$		- 5
11. 70 141		
I. C Factor =	And the page in the	1 7127
J. Di desired —	in Actual	in in
S. 2 01ta p		
L. Delta H calculated =	1 616-1	Gradien St.
Nomograph set up O.K.?  Calculator set up O.K.?  K-factor figured properly?	C N c Lidgere	त अद्भु कु रहेर्य

OA Table For Evaluating DGM Orifice Value

Item	Run 1	Run 2	Run 3
DGM, final		7	
DGM, initial	-	-	
DGM, net			
DGM, T inlet (°F)			
DGM, T outlet (°F)			
DGM, T avg (°F)			
Ambient Temp. (°F)			
Pb (in. Hg)			
Orifice meter, Delta H			

f. Calculate the corrected dry gas volume for each run using the following equation: .

$$Y_c = 10/V_m [0.0319 (T_m = 460)/P_b]^2 =$$
 $Y_c = 0.97 Y = 1.03 Y =$ 
Criteria: 0.97 Y < Y<sub>c</sub> < 1.03 Y; System meets? \_\_\_\_\_ Exceeds? \_\_\_\_\_

Nomograph/calculator check:

a. Nomograph:

If Delta H@ = 1.80, T(meter) = 100 F, % moisture = 10 %, 
$$Ps/Pm = 1.00$$
, calculate C.

$$C =$$
\_\_\_\_\_(0.95)

If 
$$C = 0.95$$
,  $T_s = 200$  F,  $D_n = 0.375$ , Delta p reference = \_\_\_\_\_(0.118)

Align Delta 
$$p = 1.0$$
 with Delta  $H = 10$ ; and lock nomograph. Set  $p = 0.01$ . Read Delta  $H$ \_\_\_\_\_\_(0.01) Nomograph O.K.?

b. Calculator:

### A. Operating Meter Box Assembly

Operate metering system for 10 minutes at the H@ value. Record the volume metered, DGM temperature and barometric pressure.

Final: DGM reading Initial: DGM reading Net: V <sub>m</sub> =	$ \underline{ft^3 \text{ Temp}}_{ft^3 \text{ Temp}} $ $ \underline{ft^3 \text{ Avg. } T_m = 0} $	(119C)	°F P <sub>b</sub> °F P <sub>b</sub> °F + 46	0 =	in. Hg _ in. Hg
$Y_c = 10/V_m [0.0319 (T_m = 460)]$ $Y_c = 0.97 Y = 1.03 Y =$	$/P_b]^2 = \phantom{AAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAA$	() (d. 8) (1. 1. 2) (1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1	1910 2010 42 1920 (T 1930 (T)	uz eA	
Criteria: 0.97 Y < Y <sub>c</sub> < 1.03 Y; B. Utilizing EPA's Method 5 D	System meets? Try Gas Meter F	Perform	Exceed	ls?	ce

- a. Remove the performance test device from its case and insert it into the gas inlet quick-connect coupling on the source sampling meter box..
- b. Turn the power to the meter box on and start the pump.
- c. Completely open the coarse flow rate control valve and close the fine flow rate control valve to give a maximum vacuum reading.
- d. Allow the orifice and source sampling meter box to warm up for 45 minutes with flow controls adjusted as described in step c before starting quality assurance runs.
- e. Make triplicate quality assurance runs. For each run, record initial and final dry gas meter volume, dry gas meter inlet and outlet temperatures, internal orifice pressure drop (Delta H), ambient temperature, and barometric pressure. Each run duration should be greater than 15 minutes. As the needle reaches the zero (12 o'clock) position, the pump and stopwatch are stopped simultaneously. The dry gas meter volume and time are recorded.

(Note: If particulate emissions are not to be determined, the filter need not	be
desiccated or weighted.)	
Filter checked visually for irregularities?	
Filter media type? Stack temperature	
Sampling site selected? Stack temperature Stack velocity head? Stack dry molecular weight calculated?	
Stack velocity head? Stack dry molecular weight calculated:	
Nozzle size properly selected?  Motor box V factor	
Calibration data certified available: Pitot tubes Meter box Y factor	
Meter box delta H@Magnehelic gauge	
Thermocouples Probe nozzle Probe nozzle	
(Note: If calibration sheets are not available, contact Task Manager for	
authorization to proceed. Authorization to proceed:	
YesNo DateTimeTask Manager	,
Date Task Manager	
Selection of sampling points and time according to methodology?	
Number of sample pointsSample time/point	
Minimum sample volume required?	
Minimum run time required?	
Total sample time actual?	
Sampling train assembled properly?  Filter properly centered?  Number of impingers required?  Impingers properly charged?	
Filter properly centered?impingers properly charged?	
Number of impingers required?	
Sample train preparation (Volume added to each impinger):	
1st (normally empty)	
2nd/3rd (100 mL of HNO <sub>3</sub> /H <sub>2</sub> O <sub>2</sub> )	
4th (normally empty)	
5th/6th (100 mL of permanganate solution)	
(Note: Reagent prepared fresh daily?	
7th (200-300 g of preweighted silica gel)	
Weight (Initial)	
Pitot tube lines checked for plugging or leaks?  Stopcock grease used: Acetone-insoluble?  Heat-stable?	
Stopcock grease used: Acetone-insoluble?	
Meter box leveled? Manometers leveled?	
Probe heat uniform along length of probe?	
Dry gas meter field observation check:	

	Town			
	Type: Type S	Standard	LO G MOR C	Other
	Properly attached to probe	2?		
	Meets EPA guidelines for	attachment to probe	? Yes_	No
	Modifications			Ségia
	Pitot tube coefficient			
	FILTER HOLDER			SOURCE EVECES
	Construction: Borosilicate	On	artz	Othor
	Frit construction: Glass fri	it?	Teflon frit?	Other
	Without organic binder?  Cyclone and flask used (or	Silico	Clean?	709 1 109
	Cyclone and flask used (or	ptional):	Cicaii:	Tax stat attention
	FII TED HEATING OVE			3.2500.5.2
	FILTER HEATING SYS Description Temperature	SIEM		
	Temperature at exit of			d
	Gas temperature at exit of	box		
	8.8	O JOHEN E SUCE	THE TOWNS	NETTERN TAX CREETE
	COMDENSER			
	Number of impingers?	Land Patricks	Alexandra City	Clean?
	Teflon impingers used?			P Cycle 1
	Teflon impingers used? Impinger contents: 1st 4th Cooling system?	2nd	3rc	desprising and and
	4th	5th	6th	7th
	o o o ming by blotti.			
	Proper connections (leak fr Modifications?			
	All glassware properly clea	ned as specified in m	ethodology (Ho	at ton victor the 1
	soapy water, 3X with tap w	rater. 3X reagent water	er soaked in 10	% nitric acid for 4
	hours, 3X reagent water, rin	nsed with acetone the	en air dry then	opening across decid
	paraffin until use?)	, the	on an dry, then (	spennig covered with
			anno roa ma	mid 7 il transfered
	METER BOX ASSEMBL			
	Manufacturer	Model No	Uni	it No.
	Delta H@ value	Date		
	Dry gas meter "Y" value			
	Condition of sampling equi	pment?	e Or selft wie	Formula Annet
	TATOLO DOX IEVEIEU/			
	Timer/temperature readouts	operational?		
	Manometer leveled?		Visit of the	
	Manometer leveled?  Thermocouples calibrated?		- 144 144 A 144 A	
		130	er Bazar andada era	
Opera				
	Filter properly numbered an	d recorded on field to	est data sheet?	

#### STACK TESTING FOR HAZARDOUS AIR POLLUTANTS (HAPs)

# FIELD OBSERVATION CHECKLIST SW-846, METHOD 0060

### DETERMINATION OF METALS IN STACK EMISSIONS

#### **SOURCE INFORMATION**

Facility	Location _			
Source_	_Sampling _			Location
Test Team	I eam Lead	er		
Test Date Interval: / /	to	/	/	
Observer_	Affiliation			
PRETEST MEETING CHECKLIS				
Please reference Pretest Checklist				
FEDERAL REFERENCE METHO	DDS 1 THRO	UGH 5		
Please reference Federal Reference M	lethods 1 thro	ough 5 C	hecklist.	
SW-846, METHOD 0060				
DETERMINATION OF METALS	IN STACK	EMISS)	IONS	
Equipment identified matches pretest Particulate matter measured concurre Metals under evaluation: SbAs HgNiP_SeAg Mercury emissions being measured (impingers 4, 5, and 6 are not necessar	ntly with met BaBe TlZn If mercury en	cals?Cd Other nissions	_CrCo_ _Other_ are not bein	CuPbMn OtherOther ng measured, then
Apparatus:				
~				
NOZZLE				
Probe nozzle: Glass (Require	d)			Other
Probe design: Button-hook			O1	ther
Nozzle size:	Calculated_		Meası	ired three times
Nozzle condition: Nicks/Chip	os			
PROBE/PROBE LINER				
Probe material: Borosilicate_			Quartz	
Heating system:		Tem	perature _	
Water cooled?		_Length		

SW-846, METHOD 0030/0031 TEST OBSERVATION SHEET (CON'T)

Sand tomb Book Brook Land	Run 1	Run 2	Run 3 Run 4	Run 5 Run 6
9. DATA SHEETS			8.45	Cramit I
<ul><li>a. Observer Signed Data Sheets?</li><li>b. Data Sheets Submitted to Observer?</li></ul>	aeghin Tg. 7		A roll such	D nin ab
10. AUDIT CYLINDER RUN	75 D 570	(.aps. )	Soulaged Training	niv c ton i
<ul><li>a. Audit Cylinder Acquired From EPA?</li><li>b. Compound Group and Range Within Guidelines?</li><li>c. Source Test Team To Conduct four (4)</li><li>Runs According to Audit Procedures</li></ul>	i sgory.		Cirgo Shale legan ba es lo Liaca es lo Liaca	l uni s
Supplied with Kit. Can Be Conducted Either Prior To or After Scheduled Test Runs.		-3° 7° 2° ()	the daski c gedor Pholesia Chandis beed	7 -
d. Audit Runs: - Date - Time Interval - Sampler ID - Cylinder No Range	Cancolline Care	ater: Fi		Media
<ul><li>Expiration Date</li><li>Cylinder Pressure (Before)</li><li>(After)</li><li>Run</li></ul>	- setgare	O stoom	arthiu Let-Culsed a Just Shippud ca	Line & Sand
<ol> <li>Leak Check Before Run?</li> <li>Leak Check After Run?</li> <li>Volume Collected</li> <li>Cartridge Sealed?</li> <li>Cartridge Labeled Properly?</li> <li>Cartridge Stored &lt; 4 °C?</li> <li>Cartridge ID Number</li> </ol>	0 qx8	is 7.8		87

SW-846, METHOD 0030/0031 TEST OBSERVATION SHEET (CON'T)

	Run 1	Run 2	Run 3	Run 4	Run 5 Run 6
7. BLANKS					
<ul> <li>a. Field Blank: For Every 6 Cartridge Sets,</li> <li>Obtain One Set, Place Near Sampling Train</li> <li>For 5 Minutes, Replace Caps, Store &lt; 4° C.</li> <li>- Field Blank Set Taken?</li> <li>- Labeled Properly?</li> <li>- Stored Properly &lt; 4 °C?</li> </ul>					
<ul> <li>b. Trip Blank: For Every 6 Cartridge Sets,</li> <li>Obtain One Set, Do Not Uncap, Store &lt; 4 °C.</li> <li>- Trip Blank Set Taken?</li> <li>- Labeled Properly?</li> <li>- Stored Properly &lt; 4 °C?</li> </ul>					
<ul> <li>c. Field Blank D.I. Water: Fill One Vial</li> <li>With Field D.I. Water to Overflow, Cap, Store</li> <li>- Field Blank D.I. Water Take?</li> <li>- Labeled Properly?</li> <li>- Stored Properly?</li> </ul>					
8. SHIPPING					
<ul> <li>a. Chain-of-Custody Sheets Completed?</li> <li>b. Samples Shipped at &lt; 4 °C?</li> <li>c. Shipping Mode (UPS, Fed. Exp., Other)?</li> </ul>					

SW-846, METHOD 0030/0031 TEST OBSERVATION SHEET (CON'T)

	Run 1	Run 2	Run 3	Run 4 Ru	ın 5	Run 6
5. TRAIN OPERATION				133217.1	0 1	2441
<ul> <li>a. Probe in Stack At Sampling Point?</li> <li>b. Sample Port Sealed?</li> <li>c. Stack Gas Purged Through Probe via Isolation Valve Prior To Starting Run?</li> <li>d. Valve Opened for Condenser?</li> <li>e. Inlet to 1st Sorbent &lt; 20 °C?</li> </ul>	zon.			7 A G 74 LSo		
f. Test Time: - Run Start - Run End - Net Sampling Time - Sampling Rate - Minimum Sampling Time Met? h. Dry Gas Meter - Final (L) - Initial (L) - Net (L) - Minimum Volume of Liters Met?	SO tha					
5. SAMPLE RECOVERY		07515	in a lact	Citica Gen		
a. Cartridges Removed With Gloved Hands and End Caps Replaced? b. Cartridges Properly Labeled? c. Cartridges Stored at < 4 °C? d. Condensate Recovered in Vial and Topped Off With DI Water? c. Condensate Vial Properly Labeled? d. All Samples Logged Into Master Field Log Book? d. Chain-of-Custody Completed and Signed?						

# SW-846, METHOD 0030/0031 TEST OBSERVATION SHEET

1. GENERAL			1 8			
a. Date b. Run No. C. Code No.			,			
2. CARTRIDGE INFORMATION	Run 1	Run 2	Run 3	Run 4	Run 5	Run 6
<ul> <li>a. Cartridge ID</li> <li>- Cartridge No. 1</li> <li>- Cartridge No. 2</li> <li>- Cartridge No. 3</li> <li>Certificate of Cleaniness? (Yes/No)</li> </ul>						Ţ
3. TRAIN SET-UP				1		
<ul> <li>a. Cartridges Placed Properly and Correctly Oriented? (Yes/No)</li> <li>b. Condensers Operating Properly?</li> <li>c. Condenser Trap in Place?</li> <li>d. Silica Gel in Place?</li> <li>e. Probe at Operating Temperature?</li> </ul>						
4. TRAIN LEAK CHECK						
Initial  a. Checked @ - 10 " Hg?  b. Leak Rate ( <0.1 " Hg for 1 min.)?  c. Vented through Charcoal Tube?  Intermittent  a. Checked at Highest Vacuum?  b. Leak Rate ( < 0.1 " Hg for 1 min.)?  c. Vented through Charcoal Tube?.						

Recovery:			
Storage containers: Bore	osilicate		
glass?	Other	Clean?	
Leak free?	Teflon liners		
Clean-up area: Description			
Clean-up area clean and	protected from wind?		
Recovery personnel cov	er hands with cotten gloves	for corbont tubes	
Sorbent cartridges cappe	ed at both ends?	ior sorbein tubes	recovery? _
Sorbents properly market	ed for particular run?	The section of the section	10042
Sorbents stored at < 4 °C	until analyzed?	to be the second second second	27 C 378 C L
Knockout trap capped?	until analyzed!	Marrian Aurila	3 2 5 977
	1 1 1 2	TESAV D公益等的表示。 US	a conference
All data forms signed an	d chain-of-custody complete	ed?	maron 1300
	Pt 32 1.022/16 19	20	

-	abtracted from Station Pb ( 0.1 " Hg X ft per
100 ft)	
Describe condition of sampling equipment:	
Operation	
	G. 1.
Sampling site selected?	Stack temperatureStack dry molecular weight calculated?
Stack velocity head?	_Stack dry molecular weight calculated?
Nozzle size properly selected (if applicable)?	sMeter box Y factor
Calibration data certified available: Pitot tube	S Meter box Y factor
Rotameters Magnen	elic guage
Thermocouples Probe nozzle	contact Task Manager for authorization to
(Note: If calibration sneets are not available, C	Mo
proceed. Authorization to proceed: Yes	No Task Manager
DateIme_	according to methodology?
Selection of sampling points and time	Sample time/point
Number of sample points	Sample time/point
	per cartridge set:
Total sample time actual?	f wall?
Sampling point at average stack gas v	elocity?
Average stack gas temperature?	,
Sampling train assembled properly?	sampling train, keep all openings where
(Note: During preparation of s	red with Teflon film or aluminum foil.)
Sorbent traps properly orientated in sa	123
Draing madium: Silica gel?	Drierite
	or leaks?
Meter have leveled?	nometers leveled?
Proha heat uniform along length of n	robe?
	ly?
	or stack wall?
	en in-stack?
Dretest leak about performed (Dequir	red)?Leak rate <0.1 "Hg?
Look shook performed through probe	9
Ditat tube/probe marking correct for	?correct sampling point?
	times?
Data shoots completed in ink and de	ata properly recorded?
	nta property recorded:
Probe maintained at 120 +/- 14 C:	

Isolation valve?	Quantity?	Stainless steel?
ORGANIC SAMPLIN		
Three sections: condense	er	sorbent trap
condensate knocl	kout trap	sorbent trap
Condenser maintains sta	ck gas not exceeding	g 20 °C
Condenser: water cooled	? cools	, 20 C
		gas temperature not
Design of sorbent tran: S	Single unit?	Dual units?
Thermocouple well in he	ed of sorbent tran?	Dual units?
Sorbent in traps?1	a of sorbeilt trap?	to a second second
Sorbent certified clean (<	10 ng per target and	3
Date of sorbent certificat	ia-9	1500.).
Sorbent stored < 4 °C bet	fore use?	Within 4 weeks?
Chain-of-custody with so	orhent tran?	oil?
Sorbent trap received wra	anned in aluminum for	2.110
Coolant? (Ice water?)	sphed in aidillinum 10	011?
Knockout tran directly be	low sorbant tran ?	Pobe corulé. Samiese sicul
Type of knockout trap?	now sorbent trap?	Apple noted a Maria Maria Section
Vacuum grease of any kir	nd DDOLUDITED!	ales segniser etatos edore electros sel egal edore elaleris 82) h cequ <sup>e</sup>
detain grease of any kin	IG LYOUIBITED!	That say (18) bearing?
METER BOX ASSEME		
Manufacturer	MadalN	class gonda o /r a/X
Dry gas meter measuresin	IVIOUEI NO	Unit No
Dry gas meter "Y" value	nicis:re	Unit NoesNo
Dry gas meter measure vo	Jume within 1 0/2	Yes No
Rotameters calibrated?	runic willing 1 %0? _	National Property of the Control of
Calibration date?	and Proper	YesN
Condition of sampling equ	uinment?	normalingende i in vidori militaria sensa affinitagnia!
Meter box leveled?	arpinent:	金月(1) 13年 [5] 15日(15) 13月(15)
Timer/temperature readou	ts operational?	
Manometer leveled?	ts operational?	2.020 75 1 force 1750 From 100
Thermocouples calibrated	(Pand within 2 000)	
Barometer: Mercury, Ane	roid Other	?
Vacuum gauge: A fler cilia		
Sause. Illier Sille	a german/	Danca (0 20 66 TT 10
Leak free pump?	ter vacuum gauge? _	Kange (0-30 * Hg)?
Temperature readoutes Di-	1 10	www.sam
Parameter Anancia	ital?Analog	g?Dial Thermometer?
Barometer. I Hidrord:	Mercu	iry?
Calibrated against_	T	
AirportLocation		esser en estastas de estas en estas en estas en en estas en en estas en
Lievation		feet above and lavel
Sampling location	elevation	feet above sea level

-Calibration range of GC/MS, ng (0-3,000 ng)

2. Calculation: Quantity of POHC to be collected:

Quantity collected (ng), =  $[A \times (1-B) \times C \times D \times E]/(F \times G \times H)$ 

Where:

A = POHC feed rate, lb/hr

B = DRE (as decimal)

C = 453.59 g/lb

D = Sample volume, L

 $E = 1 \times 10^9 \text{ ng/g}$ 

F = 60 min/hr

G = Stack gas flow rate, dscfm

 $H = 28.316 L/ft^3$ 

3. Perform calculation for:

% DRE of 99.9; 99.99; 99.999 and 99.9999

Sample volumes: 5, 10, 15, and 20 liters

4. Consturct matrix for % DREs and sample volumes:

		Total ng collected		
% DRE	5 L	10 L	15 L	20 L
99.9	- 110	ODST THRU		
99.99	Jan Deff 12 d	gneid asbodish	administration of	9
99.999			0.680.1	130.4 - 9-1/6
99.9999				

## 5. Selection of sample volume:

At the required DRE, select the total volume to be sampled so that the maximum ng collected will be within the mid-range of the calibration curve. Sample volume must not exceed 20 liters.

Sample volume:			
1	741 DEC 1 1/48 21 1 1 1	Lpr	Υ

### 6. Sampling rate:

The sampling rate is dependent on the total sampling time and total volume to be collected and must be between 0.25 and 1.0 Lpm. At no time shall sample rate exceed 1.0 Lpm.

## STACK TESTING FOR HAZARDOUS AIR POLLUTANTS

#### FIELD OBSERVATION CHECKLIST

# SW-846, METHOD~0030~AND~METHOD~0031

# SAMPLING AND ANALYSIS FOR VOLATILE ORGANIC COMPOUNDS

#### **SOURCE INFORMATION**

Facility	_Location
Cource	Sampling Location
Test Team	
Test Date Interval: / /	to/
Observer	Affiliation
PRETEST MEETING CHECKLIST	T
Please reference Pretest Checklist	
FEDERAL REFERENCE METHO	DDS 1 THROUGH 5
Please reference Federal Reference M	ethods 1 through 5 Checklist.
SW-846, METHOD 0030	
VOLATILE ORGANIC SAMPLIN	NG TRAIN (VOST)
Fauinment identified matches pretest	calibration list?
Principle organic hazardous constitue	calibration list?
3 4.	5. 6.
7 8.	5. 6. 9. 10. POLIC food rate:
For each waste feed stream stream co	infaining POHOS, calculate POHO feed fate.
1 POHC concentration in wa	aste feed:
2. Waste feed rate	lb/hr
	11.7
gal/hr Xlb/g	ral (density) = 1b/hr
3. POHC feed rate in each wa	aste feed stream:
decimal wt (% PC	OHC) X waste feed rate (lb/hr) = lb POHC/hr
Verification of Method 0030 (VOST)	) sample volume to be collected:
1 Basis:-% Destruction Rem	noval Efficiency (DRE) expected, %
-Quantity of Po	OHC to be collected, ng.
\( \tau_{11111} \)	

Container #4 (Condensate trap): Labeled/volume measured?	_
Container #5 (Train component rinse): From filter to 1st impinger:	
Labeled/volume measured?	_
Container #6 (Silica gel): Color noted/capped/weighted. Containers #2-5 stored	
under "blue ice" (<4 C) and during shipment? Container #1 shipped	
unrefrigerated?	
All data forms signed and chain-of-custody completed?	_
Remarks	_

approximate dry stack gas molecular weight  Gas density determination: Temp, sensor type				ma==1 1:
Gas density determination: Temp. sensor type_ Temperature sensor attached to probe?	transfer de la co	Pressure gar	IGE	, nozzle dia
Temperature sensor attached to probe?_	references	Other	.50	<del></del>
	ton malina a i		/ 10.1	
Recovery:				
Post-test leak check performed (Mandatory)? _ Construction of probe recovery brushes: Nation	conduction d	ohe care		
				_
GlassPolyethyleneOthe	er	Clean?		
Delegant 0	- 2 mL?_	Other		
Balance type? Calibrated?  Plastic storage containers (To store silica gel): A		4.1.4	£ 51	_
reastic storage containers (To store silica gel). A	Air-tight?	Cle	an?	_
riode anowed to cool sufficiently?				_
(Note: Cap placed over nozzle tip to pre	vent loss of pa	rticlate matt	er?)	_
During Sampling Hall (IISASSEMPLY are all onen	1200 10			
Clean-up area clean and protected from wind?  Filter handling: Tweezers used?	= hatel	unling Hall		_
Clean-up area clean and protected from wind?				_
				-
Water: Distilled?  Stopcock grease: Acetone-insoluble?  Probe handling: Acetone rinse?	a biotice of a	-datein		-
Stopcock grease: Acetone-insoluble?	Heat-stable Si	licone?		-
Probe handling: Acetone rinse? I	Distilled water	rinse?		-
Particulate recovery: Probe nozzle?  Probe liner?  Front half of	Probe fitting?	arm mid of		-
Probe liner? Front half of Blanks: Methanol Methylene chlo Any visible particles on filter holder inside probe	filter holder?	A SIN		
Blanks: MethanolMethylene chlo	oride	- Alteria V		
Any visible particles on filter holder inside probe Color of silica gel?	?	er in person		
Solution Solutions :				
All jars adequately labeled?		muse prosit		
Jalo Scaled lightly!		- tre		
Methylene chloride/methyl alcohol used in recovery	ery?			
Distilled-in-glass grade?  Resin bed capped at both ends?	1 V			
Knockout trap capped?				
Knockout trap capped?	easured/weigh	ited?		
Shipping Containers:	T 200710 2001	-fgun		
Container #1 (Petri dish): Filter inside?		<u> </u>		
Container #2 (Probe assembly rinse): Rinse with a	methanol/metl	nylene chlori	de?	
Container #3 (Sorbent trap): Labeled/ends sealed?		James Officer		

	/ater 0.1	
K. K factor = Delta H/Delta $p13.24$ ( _		
_	in. Water1.324 (	
Calculator equation set-up O.K	?	
Nomograph /calculator setup:		
A. Delta H@ =		
B. C <sub>p</sub> =		
C. P <sub>s</sub> =		
I. C Factor =		
J. D <sub>n</sub> desired =	in. Actual	in.
K.Avg. Delta p =		
L. Delta H calculated =		
Name and heat up OV 2		
K-facotr figured properly?	nipple or stack wall?	
	obe when in-stack?	
-		
Probe moved at proper time?	ect for correct sampling points?	
	to stack wall at all times?	
	to stack want at times:	
	langing?	
Leak check before changing c		
Data silvers completed, in ma,	and data properly recorded?at each point?Within 90-110 %? _	
Perform % isokinetic rate che		
remonn 70 isokinetie rate ene	CK.	
Delta H/Delta p = $\{846.72 D_n\}$	$^{4}[Delta H@] Cp^{2} (1-B_{ws})^{2} (M_{d}T_{m}P_{s}/M_{s}T_{s}P_{m})\} =$	= 7
K-factor changed during run?	New K-factor pressure readings recorded accurately?	
Velocity pressures and orifice	pressure readings recorded accurately?	
Post-test leak check performe	:d?(I	Mandatory)
Leakage rate	ed? (I	
If data sheets cannot be copie	d, record approximate stack temperature, avera	ige
	, average stack delta H	
approxim	nate stack gas moisture	,

$Y_c = 0.97 \text{ Y} = $ $1.03 \text{ Y} = $	e de la compansión de l
Criteria: $0.97 \text{ Y} < \text{Y}_{c} < 1.0$	3 Y; System meets?Exceeds?
Nomograph/calculator check:	nti rativo. Undo a visitaturo STR III o
a. Nomograph:	
If Delta H@ = $1.80$ Ps/Pm = $1.00$ , calcu	T(meter) = 100 F, % moisture = 10 %, alate C.
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	(0.95)
If $C = 0.95$ , $T_s = 20$	0 F, $D_n = 0.375$ , Delta preference = (0.118)
Align Delta p = 1.0 = 0.01.  Read Delta H_  Nomograph O.K.?_	with Delta H = 10; and lock nomograph. Set p(0.01)
b. Calculator:	Salito i Octobra estado e específica de la composição de la composição de la composição de la composição de la
Calculate Delta H/de	elta p using the following equation:
Delta H/Delta p = $\{846.72 D_n^4[$	Delta H@] $Cp^2 (1-B_{ws})^2 (M_d T_m P_s/M_s T_s P_m)$
Parameters for calcu	lator check:
D. Abs. meter pressure, $P_m + /- P_b$ in. Hg 29.9 E. Abs. meter temperature, $T_m = t_m + 460$ deg. F. Abs. stack temperature, $T_s = t_s + 460$ deg. G. Dry molecular weight M. Jb/lb mole 3.0	Water 1.80

- a. Remove the performance test device from its case and insert it into the gas inlet quick-connect coupling on the source sampling meter box.
- b. Turn the power to the meter box on and start the pump.
- c. Completely open the coarse flow rate control valve and close the fine flow rate control valve to give a maximum vacuum reading.
- d. Allow the orifice and source sampling meter box to warm up for 45 minutes with flow controls adjusted as described in step c before starting quality assurance runs.
- e. Make triplicate quality assurance runs. For each run, record initial and final dry gas meter volume, dry gas meter inlet and outlet temperatures, internal orifice pressure drop (Delta H), ambient temperature, and barometric pressure. Each run duration should be greater than 15 minutes. As the needle reaches the zero (12 o'clock) position, the pump and stopwatch are stopped simultaneously. The dry gas meter volume and time are recorded.

OA Table For Evaluating DGM Orifice Value

Item	Run 1	Run 2	Run 3
DGM, final			
DGM, initial			
DGM, net			
DGM, T inlet (°F)			
DGM, T outlet (°F)			
DGM, T avg (°F)			
Ambient Temp. (°F)			
Pb (in. Hg)			
Orifice meter, Delta			

f. Calculate the corrected dry gas volume for each run using following equation:

$$Y_c = 10/V_m [0.0319 (T_m = 460)/P_b]^2 =$$
\_\_\_\_\_\_\_

authorization to present A	are not available, co	ontact Task Manager for	or
authorization to proceed. At	ithorization to prod	ceed: Yes	_No
111110	Lask	Manager	
Selection of sampling points	and time according	of to methodology?	
Number of sample p	oints	Sample time/poi	nt
Transmitted Sample VO	nume remitten is a	scm or 105 () 2000	
Transmitted I tull tillic I	CUIIII CII /		
Total sample time ac	tual?	and the state	
	tareise points:	AMAGALLA S	-
(Note: During prepar	ration of sampling	train, keep all openings	
Filter properly centered?	Imni	ngers proporty change	wnere
Number of impingers require	ed? Whi	ch EDM2	
Filter properly centered?  Number of impingers require Volume in each impinger: 1s 5th  6th	et 2nd	CII FRIVI!	
5th 6th	7+1	3rd	4th
Distilled organic-free water (Drying medium: Silica gel?	Type II) used?		
Drying medium: Silica gel?_ Weight (200-300 gray)	0)	_Drierite	
Weight (200-300 gran	ms?)	6-16 mesh?	
filot libe lines checked for p	olugging or leaks?	with a with one of	
Pitot tube lines checked for p Stopcock grease used: Aceto (Note: Do not use sto	ne-insoluble?	Heat-stabl	e?
(Note: Do not use sto	pcock grease upstr	eam of sorbent bed!)	
vieter box leveled?	Manometers	leveled?	
and meat annionn along len	igui of brobe?		
in grass infer used, install noz	Zle using Viton-A	O-ring when stools tone	
are< 260°CW	Voven glass-fiber g	asket >260°C	peratures
		200 0	
Ory gas meter field observation	on check:		
A. Operating Meter E	30x Assembly		
1 3 1 1 1 1 1	7 ON 1 ROSCIIIOIY		
perate metering system for	10 minutes at the D	14-110-1	and more than
volume metered DGM tempo	roture and 1	elta Ha value. Recor	d the
rolume metered, DGM tempe	rature and barome	tric pressure.	
Final: DGM reading	tt Temp	°F P <sub>b</sub>	in. Hg
Initial: DGM reading	ft' Temp	$^{\circ}F P_{b}$ $^{\circ}F P_{b}$ $^{\circ}F + 460 = $	in. Ho
Net: $V_m = $	$_{\rm ft}$ Avg. $T_{\rm m} =$	°F + 460 =	
$Y_c = 10/V_m [0.0319 (T_m = 2)]$	$(460)/P_b 1^2 =$		
	1217/21/2017	DU 201 S.D. D. B. STE WICHE	
$Y_c = 0.97 Y =$			
1.03 Y =	7 S. July 11 S. July 12 S. July 1		
	<u> </u>	1 Marine Control Street	
Critoria: 0.07 V	V. C		
Criteria: $0.97 \text{ Y} < \text{Y}_c < 1.03$	Y; System meets?	Exceeds?	
B. Utilizing EPA's Me	ethod 5 Dry Gas M	eter Performance Test	Davica
	MULLOS TO THE	I CITOTITIANCE LEST	DEVICE

D-26

contam

IMPINGER TRAIN Number of impingers?		Cle	ean?	
Impinger contents: 1st (Wa	ter?)	2n	d (Water?)	
3rd (Empty/ or caustic solu				
5th6th		7th	81	:h
Volume/weight of contents	of impingers	s: 1st (10	0 mL?)	2nd (100 mL?)
3rd (Empty?)				
5th 6th		7th	81	th · ·
Impinger types: Greenburg	-Smith?		Standard?	
Impinger tip design: Taper	ed tip?		Standard tip	?
Cooling system?				
Proper connections?				
Modifications?				
METER BOX ASSEMB	LY			
Manufacturer	Mode	l No		nit No.
Delta H@ value		Date		
Dry gas meter "Y" value_		Date		
Dry gas meter measure vol	ume within l	%?		
Condition of sampling equ				
Meter box leveled?				
Timer/temperature readou				
Manometer leveled?				
Thermocounles calibrated	(Read within	1.3 C?)?		
Barometer: Mercury	Aner	oid	Othe	er
Barometer capable of mea	suring atmos	pheric pr	essure within	2.5 mm Hg?
ration		C 11		0
Filter properly numbered				
	N. 6. 41 1			2
Filter has organic binder (	Filter has organic binder (Method requires no organic binder)?  Filter manufacturer  Filter manuf. Number			
Filter manufacturer		Filte	manui. Num	iber
Filter weighted to constan				
Filter checked visually for	irregularities	s?		5.0/9
Filter collection efficiency	meets EPA	s specific	cation of 99.9	0 %0.
Stopcock grease used is so	olvent-insolu	ble, heat-	stable silicon	e grease?
Sampling site selected? Stack velocity head?		1 1	Stack te	mperature
Stack velocity head?	Stac	k dry mo	lecular weigh	t calculated?
Nozzle size properly selec	eted?			
(Note: During sam	ipling run, no	zzle can	not be change	ed!)
Calibration data certified	available: Pit	ot tubes_	Mete	er box Y factor
Meter box delta H@	M	lagneheli	c guage	
Thermocouples	Drohan	07710		

Nozzle condition: Nicks	Bent opening		
LYODE/LYOBE LINEK			
Probe material: Borosilicate Inconel	Quartz	Stainless ste	a1
Inconel Heating system: Water cooled?	Other		
Heating system:	Temperature (120	C+/- 14 °C)	
Water cooled?	Length	0 .7-14 C)_	
Water cooled? Probe liner: Borosilicate/quartz Temperature sensor attached to	(up to 480 °C)	Ouartz(40	0.000.00
Temperature sensor placed in ar	n interference-free arrar	oement with n	roha?
	Service Management of the American	igomone with pr	·.
PITOT TUBE			ortho -
Type: Type S St Properly attached to probe?	andard	0.1	
Properly attached to probe?  Meets EPA guidelines for attach Modifications			(Frair-Bir
Meets EPA guidelines for attach	ment to probe?	Yes	No
Modifications Pitot tube coefficient			erio (co
			The T
FILTER HOLDER			
Construction: Borosilicate  Frit construction: Glass frit?	Quartz	Other	
The state of the s	letion to	1°1 ↑ ' J	
11	Silicone gasket		an existed a
Other	Clean?		Las PAGLACE
Cyclone and flask used(optional)	): 7227.722	J. 1 16 12 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	S- ye -
FILTER HEATING SYSTEM	. dand va		
Description			
1 chiperature (120+/- 14		2000 - 2000 - 0	v +20
Gas temperature at exit of Box _		233 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	2 1 1 1 2 1
ORGANIC SAMPLING MOD	ULE		
Three sections: Condenser	Sorbent	tran	
Condensate knockout trap	ooroom	пар	
Condenser maintains stack gas no	ot exceeding 20 °C (68	<sup>0</sup> F)2	
Sorbent trap jacketed to maintain	internal gas temperatu	re not exceeding	2000
(001):			
Design of sorbent trap: Single un Thermocouple well in bed of sorb	it?	al unita?	
Thermocouple well in bed of sort	pent Tran?	al uillis?	1177
Sorbent in trap? (XAD-2?)	тар	20	
Sorbent certified clean (< 10 ng p	per target analyta(1)(1)	20 grams?	Margani i
Data at combant - 1'C .: a	targer analyte!)!	1.1.4.4.5	
Chain-of-custody with sorbent tra	Wit	thin 4 weeks?	
Sorbent tran received wranged in	.p.		
Sorbent trap received wrapped in Coolant? (Ice water?)	aluminum foil?	No.	
Coolant. (100 Water:)			
Knockout trap directly below sort		100	
Type of knockout trap?			

# SOURCE SAMPLING FOR HAZARDOUS AIR POLLUTANTS (HAPs)

### FIELD OBSERVATION CHECKLIST

**SW-846, METHOD 0010** 

# SAMPLING AND ANALYSIS FOR SEMI-VOLATILE ORGANIC COMPOUNDS

#### SOURCE INFORMATION

	1
S 1 THROUGH 5	
hods 1 through 5 Che	cklist.
POUNDS	
alibration list?	
Glass	Other
Elbow	Streight tube
alculated	Measured three times
	to